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COMPUTATIONS OF SOOT AND NO_x EMISSIONS FROM GAS TURBINE COMBUSTORS

FINAL REPORT

by

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P.O. Box 5217
Phoenix, Arizona 85010



Prepared for

National Aeronautics and Space Administration
NASA-Lewis Research Center
Cleveland, Ohio 44135

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FOREWORD

This document is the final report for work performed by the Garrett Turbine Engine Company under Contract NAS3-22542. This program, under the sponsorship of the National Aeronautics and Space Administration (NASA) Lewis Research Center accomplished the technical effort involved in the computations of emissions using a 3-D combustor computer program.

The assistance and guidance rendered by Dr. C. J. Marek, who was the NASA Project Manager for the program, is acknowledged.

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CHAPTER I

INTRODUCTION

A. Background

Significant advances have been made in combustor analytical modeling over the past five years. The use of advanced numerics and kinetics has given the combustion engineer the ability to predict internal combustor flow field characteristics. These advanced tools, while still in their incipient stages, offer the potential of reducing the design and development time required for gas turbine combustors. At the same time, the analytical models increase the understanding of the phenomena affecting combustor performance and provide the basis for designing better combustors. The optimization of the design process will require a judicious blend of the emerging analytical tools (correlated and updated with test data) with the established empirical techniques.

Starting in 1970, Garrett has demonstrated a company commitment to develop combustor analytical design tools and utilize them in the everyday design and development process. In addition to extensive company-sponsored efforts, a significant contribution to this highly successful effort has been the USARTL Combustor Design Criteria Validation Program (Contract DAAJ02-75-C-0044).¹ Among the models developed under the above-mentioned USARTL program was the 3-D Combustor Performance Model, which is the basis for the present program. The present program entailed extending the capability of the model to predict pollutant emissions of nitrogen oxides and smoke.

B. Objectives

The objective of the program was to utilize and extend an existing three-dimensional(3-D) combustor performance computer program:¹

- o To predict pollutant emissions of smoke and NO_x ;
- o To include the influence of soot, CO_2 , and H_2O on radiation heat transfer; and
- o To extend the two-step hydrocarbon oxidation mechanism to a more detailed four-step scheme.

The program consisted of four tasks:

- o Task I - Formulation of the Method
- o Task II - Computer Coding
- o Task III - Computation of Test Cases
- o Task IV - Reporting and Documentation.

In Task I, a method was formulated to predict the emissions of soot and NO_x and to extend the radiation and hydrocarbon oxidation models.

In Task II, the method was incorporated into the 3-D combustor program in order to compute the emissions of NO_x and soot and the radiant transfer to the combustor walls.

In Task III, the resulting program was exercised for idle, cruise, and takeoff conditions of a JT8D combustor.

In Task IV, reports were submitted to NASA during and at the end of the program.

C. Summary

This report is the Final Report of the computations of emissions program, and presents the work carried out by Garrett under the program. Chapter II of the report includes a brief description of the original 3-D combustor performance computer program, provided for completeness. Chapters III and IV describe the soot emissions model and the influence of soot on radiation heat transfer. The NO_x emissions model and the hydrocarbon oxidation mechanism are described in Chapters V and VI, respectively. Chapter VII includes a description of the results of the computations. Chapter VIII contains concluding remarks. Chapters IX and X, respectively, contain a list of nomenclature and list of references, as cited in this report. Finally, Appendices A, B, C, and D contain, respectively, a description of the 3-D program, the program input, a list of FORTRAN variables and a listing of the new 3-D combustor performance program.

CHAPTER II

DESCRIPTION OF THE 3-D COMBUSTOR PERFORMANCE PROGRAM

The 3-D Combustor Performance Model Computer Program that forms the basis of the present work, is briefly described. For complete details, refer to Report No. USARTL-TR-55C.¹

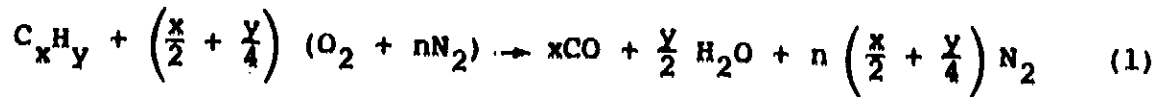
The 3-D program is general and is capable of predicting recirculating turbulent flow in gas-turbine combustion chambers. Reacting or nonreacting, swirling or nonswirling, diffusion and/or premixed flames, and gaseous and/or liquid fuel combustion can be handled by the program. The program computes the following variables in the region of interest:

- o Axial, radial, and swirl velocity components;
- o Pressure;
- o Enthalpy (temperature); in conjunction with the equation of state, the temperature determines the density variations in the flow field;
- o Turbulent kinetic energy and its dissipation rate;
- o Mass fractions of total fuel (mixture fraction), unburned fuel, oxygen, carbon monoxide, CO_2 and H_2O .
- o Three radiation flux vectors;
- o Spray trajectory, droplet size distribution, and evaporation rates.

The program employs the following physical models to solve the variables mentioned above:

- o Turbulence - Two-equation ($k-\epsilon$) turbulence model to obtain turbulent kinetic energy and its dissipation rate.

- o Chemistry - Two-step chemical reaction scheme:



- o Chemical Reaction Rate - Fuel and CO consumption rates are assumed to be governed by either the time-averaged Arrhenius model or the turbulent eddy break-up model.

- o Radiation - A six-flux model of radiation.

The transport equations for all dependent variables ϕ are written in the following general form:

$$\text{div} (\rho \vec{u} \phi - \frac{\mu_t}{\sigma_\phi} \text{grad } \phi) = S_\phi \quad (3)$$

where ρ denotes the mixture density, \vec{u} the velocity vector, μ_t the effective or turbulent viscosity, σ_ϕ the effective Prandtl/Schmidt number, S_ϕ the sources of ϕ ; i.e., S_ϕ includes the creation/destruction of ϕ plus other quantities that do not fall under the convective and diffusive terms. Table E-1 in Appendix E includes a list of the dependent variables ϕ and their source terms.

An iterative, general finite-difference solution procedure suitable for 3-D elliptic flows in complex geometries is used to solve the above system of coupled, nonlinear partial-differential equations. The solution procedure involves discretizing the differential equations by integration over elementary finite-difference control volumes surrounding grid nodes that are nonuniformly spaced over the flow field.

CHAPTER III

SOOT EMISSIONS

In this chapter, soot formation and oxidation in combustion chambers are discussed. A general background on soot emissions is provided first. Details of the soot formation and oxidation mechanisms reported in the literature are discussed next. Quasi-global expressions for soot formation and oxidation are described. A description of the influence of turbulence on soot formation and oxidation is included. The approach adopted in the present work is described next. This approach considers the influence of turbulent fluctuations on soot formation and oxidation rates.

A. Background

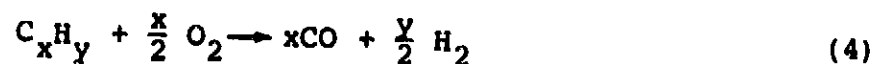
The particulate emission of primary concern in the combustion of hydrocarbon fuels is soot, which is evident in the form of exhaust smoke. The emission of smoke from gas turbine engines is responsible for the following problems:

- o Higher liner temperatures due to increased radiative heat transfer
- o Impingement of carbon on metal surfaces, resulting in erosion and reduced equipment lifetimes
- o Distortion of fuel spray distribution due to carbon deposits, leading to hot spots
- o Visible pollution and associated health hazards
- o Tactical problems in military applications.

Recently, attention is being directed toward the combustion of alternate fuels derived from coal liquids and shale oil. Since the use of these fuels results in significant increases in smoke production, a better understanding of the physical and chemical processes governing soot production is needed.

The processes governing the formation and subsequent oxidation of soot are of a particularly complex nature; and, as such, quantitative models of soot production have yet to be developed. Soot is not an equilibrium product of combustion; and, therefore, its formation is influenced as much by the physical processes of atomization, evaporation, and fuel/air mixing as by reaction kinetics. Soot is generally produced anywhere within the combustor where fuel/air mixing is inadequate, resulting in oxygen-deficient, high-temperature zones.

For the pressures and temperatures normally prevalent in gas turbine combustors, equilibrium calculations indicate that solid carbon appears when there is insufficient oxygen to oxidize the hydrocarbon to CO and H₂ according to the relation:



That is, the carbon-oxygen mass ratio for incipient soot formation is 12:16; or, alternatively, the atomic C-O ratio is unity. However, since soot formation is essentially a nonequilibrium phenomenon, experimentally, soot is observed at C-O ratios (a) much less than unity at low temperatures (<2000°K); and (b) greater than unity at higher temperatures.²

Smoke levels are primarily dependent on the following:

- o Air/fuel mixing
- o Temperature

- o Equivalence ratio
- o Residence time of air/fuel mixture
- o Pressure
- o Fuel composition.

These factors influence both the formation and subsequent oxidation of soot and are dependent on engine operating conditions, details of the combustor internal flow field, fuel droplet characteristics, etc.

B. Mechanism of Soot Formation

Detailed discussions of the many mechanisms proposed to explain the chemical and physical processes governing soot formation are available in reviews by Haynes and Wagner,³ Street and Thomas,⁴ Palmer and Culliss,⁵ Gaydon and Wolfhard,⁶ Homann,⁷ and Bittner and Howard.⁸ Based on the information available, the process of soot formation can be considered to occur in three distinct stages:

- o Soot-particle nucleation
- o Agglomeration and surface growth
- o Coagulation.

The first stage of soot-particle nucleation is the most difficult to describe, and there is considerable controversy regarding this. The two most viable hypotheses advanced to date are based on ionic and radical polymerizations.

The theory of ionic polymerizations contends that positive ions serve as the nuclei for carbon formation in flames.^{9,10} Based on this theory, Howard¹¹ showed that the chain structure of carbon particles and the uniform size of the spherical chain units can be explained. Experiments by Howard and coworkers¹² have demonstrated this theory to be feasible.

The theory of radical polymerizations considers that fuel pyrolysis gives rise to elementary unsaturated hydrocarbon molecules (e.g., acetylene), which polymerize via radical chain mechanisms.¹³ Thus, soot formation is mainly due to gas-phase reactions and is not directly due to liquid pyrolysis. This mechanism has also been proposed by Porter¹⁴ as the "Acetylene Mechanism of Soot Formation." Mass spectrometric measurements of species such as C_2H_2 , C_4H_2 , C_6H_2 , C_8H_2 , etc. obtained in flames¹³ and shock-tube investigations¹⁵ tend to support the radical polymerization theory. However, since a continuation of such a chain-reaction sequence cannot lead directly to carbon particles,¹³ chain-branching and ring-closure, followed by agglomeration and dehydrogenation,^{5,16} must take place at some point prior to soot formation.

In the second stage of soot formation (agglomeration and surface growth), spherical units of carbon particles (about 250Å in size) are formed by agglomeration and surface growth of the nuclei formed in the first stage.

Finally, in the third stage, the coagulation of the spherical carbon particles leads to the characteristic chain-like structure of soot. Dehydrogenation continues through both the second and third stages.

Jensen¹⁷ proposed a model that treats the various steps of soot formation in some detail. The model agreed qualitatively with experimental observations in a methane flame. However, due to the complexities associated with the detailed reaction mechanism, and uncertainties in the rate constants, the Jensen model is not suitable for gas-turbine combustor analysis.

Since quantitative description of the soot formation mechanism applicable to general conditions are not available, quasi-global models as described later in this chapter are required for the computation of soot emissions.

C. Mechanism of Soot Oxidation

Analytical and empirical literature on soot oxidation is extensive. However, because of the complexities involved, considerable controversy exists concerning the mechanism of soot oxidation, and many basic questions have yet to be answered. Consideration of soot oxidation processes is important, since soot concentration in the exhaust gases is determined by both the relative rates of soot formation and oxidation in the flame zone and the surface oxidation rate in hot post-flame gases. In this Chapter, a limited review of the soot oxidation models and a rationale for selecting the model used in the present work is presented.

Many studies have been reported on the derivation of mass-transfer (oxidation) rates for single-carbon particles in a hot-oxidizing ambient environment. Recently, studies on the theory of burning carbon particles were made by Avedesian and Davidson,¹⁹ Ubhayakar and Williams,²⁰ and Libby and Blake.²¹ These studies involved simplifying assumptions with regard to the fluid-mechanical and chemical aspects of the problem. Amundson and coworkers^{22,23,24} presented a model for the diffusion and chemical reaction in the boundary layer surrounding a burning spherical carbon particle in a quiescent gas. The model accounted for radiation and for the homogeneous combustion of CO in the gas phase and the heterogeneous surface reactions of carbon with oxygen and CO₂. The model predicted the distribution of the product concentrations around the particle.

High-temperature soot oxidation rates were measured by Lee, et al.,²⁵ in the tail of propane diffusion flames. The soot oxidation rate (R_{ox}) per unit particle surface area was determined as a function of temperature and partial pressure of oxygen, as follows:

$$R_{ox} = 1.09 \times 10^5 P_{O_2} T^{-1/2} \exp(-19725/T) \text{ kg/m}^2\text{s} \quad (5)$$

The measurements were conducted in the temperature range of 1310° to 1670°K. Tesner and Tsibulevsky²⁶ also measured flame-soot oxidation rates over the temperature range of 1400° to 2000°K and found good agreement with the above expression. Feugier²⁷ measured soot concentrations in fuel-rich ethane-oxygen flames and deduced a kinetic expression for the oxidation of soot particles similar to the one by Lee, et al.²⁵

Based on the measurements of the surface oxidation rates of pyrolytic graphite and the similarity of small soot particles to pyrolytic graphite at the microscopic level, Radcliffe and Appleton²⁸ proposed that the soot oxidation rate should exhibit a local maximum (for a fixed O_2 partial pressure and increasing temperature) at temperatures from 2000° to 2500°K for O_2 partial pressure in the range of 0.05 to 1.0 atmosphere. Additionally, the soot oxidation rate should exhibit a first-order dependence on the O_2 partial pressure for $P_{O_2} \leq 0.01$ atmosphere and, at higher pressures, should asymptotically approach a zero-order dependence. The semi-empirical formula for soot oxidation rate proposed by Nagle and Strickland-Constable²⁹ (discussed later in this chapter) confirms this behavior. The model of Lee, et al., can be derived from that of Nagle and Strickland-Constable for fuel-lean conditions. Therefore, the more general model of Nagle and Strickland-Constable has been adopted in the present work.

D. Quasi-global Models of Soot Formation and Oxidation

Since the elementary steps in the formation and oxidation of soot are not totally understood, the present program uses quasi-global models that characterize soot production occurring via a few overall steps. Such models have been successful in predicting soot production.³² In this section, some of the quasi-global models reported in the literature are described.

The quasi-global models do not predict the size of soot particles. With the current state-of-the-art, it is not possible to predict the size of formation of the soot particles in any practical flow situation. Therefore, it is assumed that particles are produced at a known size. It may also be assumed that particles are produced in accordance with a specified size distribution (e.g., Gaussian).

Tesner, et al.,³³ proposed a soot production model which grouped the complex processes of pyrolysis, nuclei formation, and soot formation into three rate-limited subglobal steps that include (a) a pyrolysis rate first order in hydrocarbon concentration, (b) a chain branching and chain termination rate for soot nuclei formation rate, and (c) a soot formation rate.

Pyrolysis:

$$n_o = a_o C_{fu} \exp(-E/RT) \text{ (part./m}^3\text{.s)} \quad (6)$$

Nuclei Formation:

$$R_{n,f} = n_o + (f-g)n - g_o Nn \text{ (part./m}^3\text{.s)} \quad (7)$$

Soot Formation:

$$R_{S,f} = m_p (a - bN)n \text{ (kg/m}^3\text{.s)} \quad (8)$$

where a_0 , E , f , g , g_0 , a , and b are constants for a given fuel; n_0 is the rate of spontaneous formation of nuclei; n is the nucleus concentration; N is concentration of soot particles; m_p is the mass of a soot particle; and $R_{n,f}$ and $R_{s,f}$ are the nuclei and soot formation rates, respectively.

Khan and Greeves³⁴ proposed a single-step global expression as a function of the partial pressure of unburned hydrocarbons (P_{HC}), the unburned equivalence ratio (ϕ_u), and the temperature (T):

$$R_{s,f} = 0.468 P_{HC} \phi_u^3 \exp(-40,000/RT) \text{ gm/cm}^3\text{s} \quad (9)$$

This model is overly sensitive to the equivalence ratio and, therefore, is not considered in the present work. In addition, in both the above models, soot oxidation rates are not considered.

Edelman, et al.,³² consider both soot formation (R_f) and soot oxidation (R_{ox}) and express the net soot formation rate as:

$$\frac{dC_s}{dt} = R_f - A_t R_{ox} \quad (10)$$

where A_t equals total surface area available for oxidation. This model is more general and, therefore, it has been adopted in the present work with appropriate modifications to account for turbulence effects as described next in Section E. The formation step is expressed by a modified Arrhenius type of relation:

$$R_f = AT^\alpha C_{HC}^a C_{O_2}^b \exp(-E/RT) \text{ gm/cm}^3\text{s} \quad (11)$$

where C_{O_2} , C_{HC} equal the concentration of unburned oxygen and hydrocarbon (gm/cm^3) and where A , α , a , b , E are model constants.

For the oxidation step, Edelman, et al.,³² adopt the semi-empirical formula of Nagle and Strickland-Constable²⁹ for pyrolytic graphite oxidation; this formula is nonlinear and non-Arrhenius in P_{O_2} and T :

$$A_t R_{OX} = 12 \left[\left(\frac{K_A P_{O_2}}{1 + K_2 P_{O_2}} \right) \psi + K_B P_{O_2} (1 - \psi) \right] A_t \text{ gm/s} \quad (12)$$

where:

$$\psi = [1 + K_T / (K_B P_{O_2})]^{-1} \quad (13)$$

$$K_A = 20 \exp(-30,000/RT) \text{ gm/cm}^2 \cdot \text{s atm} \quad (14)$$

$$K_B = 4.46 \times 10^{-3} \exp(-15,200/RT) \text{ gm/cm}^2 \cdot \text{s. atm.} \quad (15)$$

$$K_T = 1.51 \times 10^5 \exp(-97,000/RT) \text{ gm/cm}^2 \cdot \text{s} \quad (16)$$

$$K_2 = 21.3 \exp(4100/RT) \text{ atm}^{-1} \quad (17)$$

Shock-tube measurement¹⁸ of soot oxidation rates qualitatively confirms the features of the above formula. With these expressions for soot formation and oxidation and assuming a single-soot particle size of 250\AA , Edelman, et al.³² obtained close agreement of the predicted soot concentration (mg/l) with the experimental data in a jet-stirred reactor. Thus, these expressions assume perfect mixing. In a gas-turbine combustor, however, regions of unmixed species will exist, and turbulence will also influence the soot production rates. As such, modifications to these expressions are required before they can be used for a general 3-D turbulent flow.

E. Influence of Turbulence on Soot Formation and Oxidation

Magnussen, et al.,^{35,36} have proposed a model that accounts for the influence of turbulent fluctuations on soot production rates.

In turbulent flows, chemical reaction occurs when reactants at a sufficiently high temperature are mixed at the molecular level. The molecular mixing process is analogous to the dissipation (ϵ) of turbulent kinetic energy k and is associated with the smallest scales of turbulence. Dissipation is concentrated in highly strained regions of the fluid occupied by fine structures with characteristic dimensions of the same magnitude as the Kolmogorov microscale. The reactants are molecularly mixed in these fine structures, where reaction occurs. Magnussen, et al., proposed the following expressions for the mass fraction contained in the fine structures:

$$\gamma^* = 9.7 \cdot (R_t)^{-3/4} \quad (18)$$

where R_t is the turbulence Reynolds number, and the rate of transfer of mass per unit mass between the fine structures and the surrounding fluid is:

$$\dot{m} = 23.6 \cdot (R_t)^{-1/4} \frac{\epsilon}{k} \quad (19)$$

The rate of reaction is proportional to $\dot{m}X$ where X is the fraction of small-structure eddies that are sufficiently heated to react. It is assumed that X is proportional to the ratio of local reacted fuel concentration and total fuel concentration. Thus, the rate of reaction is:

$$R_{fu} = 23.6 (R_t)^{-1/4} \frac{\epsilon}{k} X C_{min} \quad (\text{kg/m}^3 \text{ s}) \quad (20)$$

where

$$X = \frac{C_{pr}/(1 + i)}{C_{pr}/(1 + i) + C_{fu}} \quad (21)$$

C_{\min} is the smaller of C_{fu} and (C_{O_2}/i) and i is the stoichiometric oxygen requirement. The temperature T^* of the reacting fine structures is T above the local time-mean temperature T :

$$T^* = T + \Delta T = T + \frac{\Delta H_R C_{\min}}{\rho C_p} \quad (22)$$

where

ΔH_R = the heat of reaction

C_p = the specific heat

and the surrounding temperature T^0 is

$$T^0 = T - \Delta T \frac{\gamma^* \chi}{1 - \gamma^* \chi} \quad (23)$$

Using Equations (6) and (8), the mean rates of nuclei and soot formation are then expressed as:

$$\begin{aligned} R_{n,f} = & n_{O,T^*} \gamma^* \chi \quad \rho/\rho^* + n_{O,T^0} (1 - \gamma^* \chi) \quad \rho/\rho^0 \\ & + (f - g)_n - g_O \quad n^* N^* \gamma^* \chi \quad \rho/\rho^* \\ & - g_O \quad n^0 \quad N^0 (1 - \gamma^* \chi) \quad \rho/\rho^0 \end{aligned} \quad (24)$$

and

$$\begin{aligned} R_{s,f} = & m_p (a - b N^*) \quad n^* \gamma^* \chi \quad \rho/\rho^* + m_p (a - b N^0) n^0 \\ & (1 - \gamma^* \chi) \quad \rho/\rho^0 \end{aligned}$$

Finally, the mean rates of nuclei and soot oxidation are expressed as:

$$R_{n,c} = R_{fu} \quad n/C_{fu} \quad (\text{part}/\text{m}^3 \text{ s}) \quad (26)$$

$$R_{s,c} = R_{fu} \quad C_s/C_{fu} \quad (\text{kg}/\text{m}^3 \text{ s}) \quad (27)$$

Magnussen, et al., used this model to compute the soot concentrations in a turbulent C_2H_2 diffusion flame. By adjusting the particle diameter [entered as m_p , the particle mass in Equation (8), and the constant a_0 in Equation (6), good agreement with experimental measurements was obtained.

F. Present Approach

The model adopted for computing soot emissions in the present program is described in the following paragraphs.

The computation of soot emissions involves the solution of two additional transport equations for the concentrations of (a) nuclei and (b) soot. These two equations are of the same general form as Equation (3) solved by the 3-D Combustor Program. To complete the equation specifications, the source terms and the Schmidt numbers for these two variables are as follows:

The source term in the nuclei concentration equation is expressed as

$$R_{n,f} - R_{n,c} \quad (28)$$

where $R_{n,f}$ is given by the smaller of the two values from Equations (7) and (24); $R_{n,c}$ is given by Equation (26). Thus, these expressions amount to the use of the turbulent reaction rates, subject to the limitation that they cannot be greater than the rates under well-stirred reactor conditions.

The source term in the soot concentration equation is similarly expressed as

$$R_{s,f} - R_{s,c} \quad (29)$$

where $R_{s,f}$ is given by the smaller of the two values from Equations (11) and (25); $R_{s,c}$ is given by the smaller of the two values from Equations (12) and (27).

The turbulent Schmidt numbers σ_s and σ_n for soot and nuclei concentrations are assumed the same as for gaseous fuel (i.e., 0.9).

In the computations carried out in the present work, a distribution of two particle sizes was considered: a small size of 0.025 microns as resulting from nucleation and a large size of one micron as resulting from fuel droplet pyrolysis and char formation. The relative rates of formation of these two sizes of particles was assumed to be 90-10 percent. The consideration of two particle sizes leads to the solution of a transport equation of the same general form as Equation (1) for the concentration of the particles in each size. The extension to other sizes is straightforward but involves extra computational effort, since an additional equation must be solved for each additional size considered. In view of the several assumptions inherent in the analysis of soot production, the consideration of other size groups is not necessary at this stage.

The calculation of soot formation is bypassed if the temperature is less than a value below which the formation rates are negligible. It is also bypassed if the local carbon-to-oxygen ratio is less than the incipient soot formation limit. Both of these limits of temperature and carbon-to-oxygen ratio are inputs to the calculation procedure and can be varied at will.

A lack of data exists for computing particle coagulation. Attempts to model particle growth in flames^{38,39} have had little success. No definite conclusions could be reached with these models. A lack of understanding of the phenomena and the absence of data reduces coagulation computations to mere speculation. Therefore, this phenomenon is not addressed in the present work.

CHAPTER IV

RADIATION HEAT TRANSFER

A. Background

The contributors to radiation in combustors fueled by hydrocarbons are soot, CO_2 , H_2O (vapor), inorganic particles, CO, unburned fuel (C_xH_y), NO_x , and SO_2 . Only the influence of soot, CO_2 , and H_2O (vapor) are considered in the present work. Although CO and unburned C_xH_y contribute to emission and attenuation of radiation within flames, these contributions are localized and of secondary importance when total heat-transfer rates are considered. The contributions of NO_x and SO_2 can be neglected because of their low concentrations.

The determination of the influence of soot on radiant heat transfer reduces to two factors: (a) soot distribution in the flame and (b) the radiative properties of gas-soot mixtures. The first was discussed in the preceding chapter. Radiative properties of gas-soot mixtures are discussed in this chapter.

The radiation properties of the principal radiating species including soot, CO_2 , and H_2O , are significantly nongrey. Consequently, the calculation of the radiation properties is a time-consuming task. However, spectral calculations are unnecessary since approximate calculations (by means of curve fits) are more convenient and provide good accuracy.⁴⁰

An approximate curve-fit procedure for the calculation of radiation properties is employed in the present work.

B. Radiation Properties of Soot, CO₂, and H₂O Mixtures

The absorptivity (α) of the gas-soot mixture includes the soot absorptivity, the absorptivity due to the absorption bands of CO₂ and H₂O, and corrections for the overlapping of bands.

Utilizing the spectral data,⁴¹ the gas absorptivity is calculated by taking a summation over the absorption bands of CO₂ and H₂O. In the approximate calculation method adopted here, a simpler approach is used. The gas absorptivity α_g is written as⁴²

$$\alpha_g = \epsilon_g (T/T_s)^{(0.6-0.2\zeta)} \quad (30)$$

$$\text{where } \zeta = P_w / (P_w + P_c) \quad (31)$$

$$\epsilon_g = \text{gas emissivity at a temperature } T \text{ and path length } LT_s/T$$

$$T, T_s = \text{gas and blackbody source temperatures, respectively}$$

$$P_c, P_w = \text{partial pressures of CO}_2 \text{ and H}_2\text{O}$$

ϵ_g is given by

$$\epsilon_g = \epsilon_c + \epsilon_w - \Delta\epsilon_{cw} \quad (32)$$

$$\text{where } \epsilon_c, \epsilon_w = \text{emissivities of CO}_2 \text{ and H}_2\text{O}$$

$$\Delta\epsilon_{cw} = \text{overlap correction factor}$$

ϵ_g can be computed using a temperature adjusted version of Leckner's⁴³ approximate overlap correction $\Delta\epsilon_{cw}$, and approximating

ϵ_c and ϵ_w by curve fits of P_c , P_w , PL , and T to spectral calculations. In the range of interest in gas-turbine combustors, such calculations agree to within 5 percent of the spectral calculations and the experimental results.

The temperature adjusted version of Leckner's⁴³ overlap correction $\Delta\epsilon_{cw}$, which accounts for the 2.7 and 15 μ m overlapped regions for mixtures of CO_2 and H_2O , is⁴⁰

$$\Delta\epsilon_{cw} = \frac{\xi}{(10.7 + 101\xi)} - \frac{\xi}{111.7}$$

$$\{\log_{10}[101.3(P_c + P_w)L]\}^{2.76} F(T)$$

$$\text{for } (P_c + P_w)L \geq 0.1 \text{ atm-m}$$

$$= 0 \text{ for } (P_c + P_w)L < 0.1 \text{ atm-m}$$

where ξ is defined by Equation (31) and $F(T)$ is given by:

$$F(T) = -1.0204 \times 10^{-6}T^2 + 2.2449$$

$$10^{-3}T - 0.23469 \quad (T \text{ in degrees K})$$

The coefficients involved in the curve fits of ϵ_c and ϵ_w to P_c , P_w , PL and T are given in Reference 40 and are not reproduced here.

The absorptivity (α) of the gas-soot mixture is given by

$$\alpha = \alpha_s + \alpha_g - \alpha_s \alpha_g \quad (33)$$

With α_g obtained above, it remains to determine α_s , the soot absorptivity. This is obtained by the method of Felske and Tien.⁴⁴ This method assumes that the complex refractive index of soot is independent of wavelength and that the soot particle diameter is small compared to the wavelength of radiation, so that scattering is negligible. The spectrally integrated absorptivity α_s can then be written in a closed-form expression to determine α_s .

By using the radiative property calculations of the type described above, Sarofim⁴⁵ indicated that radiation calculations can be made with fair confidence, and that the major source of uncertainty in such calculations is soot concentration, rather than gas-radiation properties.

C. Present Approach

The six-flux radiation model incorporated into the 3-D Combustor Performance Computer Program was used in computing radiation heat transfer in the present work.

This model is based on the Schuster-Hamaker approximation.⁴⁶ It should be noted that, as pointed out by Siddall,⁴⁷ other flux model approximations such as Milne-Eddington and Schuster-Schwarzschild can be represented by the same form of flux equations with constants being different.

The differential equations describing the variations of the fluxes along six directions can be reduced to the following three second-order ordinary differential equations:

$$\frac{d}{dx} \left(\frac{1}{a+S} \frac{dR^X}{dx} \right) = a (R^X - E) + \frac{S}{3} (2R^X - R^r - R^z) \quad (34)$$

$$\frac{1}{r} \frac{d}{dr} \left(\frac{r}{a+S+\frac{1}{r}} \frac{dR^r}{dr} \right) = a (R^r - E) + \frac{S}{3} (2R^r - R^X - R^z) \quad (35)$$

$$\frac{1}{r} \frac{d}{d\theta} \left(\frac{1}{a+S} \frac{dR^z}{d\theta} \right) = a (R^z - E) + \frac{S}{3} (2R^z - R^X - R^r) \quad (36)$$

Where the composite-fluxes R^X , R^r and R^z are defined as

$$R^X = \frac{1}{2} (I_{X+} + I_{X-}) \quad (37)$$

$$R^r = \frac{1}{2} (I_{r+} + I_{r-}) \quad (38)$$

$$R^z = \frac{1}{2} (I_{\theta+} + I_{\theta-}) \quad (39)$$

where I_{x+} , I_{r+} , and $I_{\theta+}$ are the fluxes along the positive directions of axial, radial, and circumferential directions, respectively; I_{x-} , I_{r-} , and $I_{\theta-}$ are the corresponding fluxes along the negative directions.

a = Absorption coefficient, defined as radiation absorbed per unit length

S = Scattering coefficient, defined as radiation scattered per unit length

E = Black body emissive power $= \sigma T^4$

σ = The Stefan-Boltzman constant

The absorption coefficient a is related to the absorptivity α of the gas-soot mixture and the path length L by:

$$a = -\frac{1}{L} \ln (1-\alpha)$$

In the original version of the 3-D combustor program,¹ the radiation properties were assigned constant values. For the present work, the absorption coefficient was computed locally as a function of gas and soot concentrations by the approximate procedure described above.

The scattering due to soot particles, which are generally of diameters below one micron, is negligible. In the present work, a uniform value of 0.01m^{-1} was assumed for the scattering coefficient.

CHAPTER V

NITROGEN-OXIDE EMISSIONS

A. Background

Nitrogen oxides (NO_x) are formed during any combustion process involving air within the normal range of adiabatic flame temperatures and comprise nitric oxide (NO), nitrogen dioxide (NO_2), and small amounts of nitrous oxide (N_2O). For turbopropulsion engines, the NO_x emissions consist mostly of NO , particularly at high power conditions, where maximum NO_x concentrations are encountered. However, the contribution of NO to total NO_x emissions decreases at low power points. The NO_x is conventionally expressed in mass units of NO_2 , to which the NO would eventually react in the atmosphere.

The major influences contributing to the formation of NO_x are (a) high flame temperature, (b) the availability of oxygen as provided by excess air, and (c) sufficient residence time for the reactions to take place. Formation of NO is preceded by the generation of N and O atoms. Nitrogen (N) atoms are formed by the dissociation of nitrogen (N_2) in the air at high temperatures, and can also be a product of hydrocarbon reactions if the fuel contains nitrogen. Oxygen (O) atoms are formed primarily from oxygen (O_2) dissociation. Thus, NO forms both in the reaction zone and in the post-reaction, high-temperature gases. A super-equilibrium of O , N , and OH concentrations (i.e., concentrations exceeding equilibrium levels) in the reaction zone leads to NO formation in this zone (often termed as 'prompt NO '). Nitric oxide formation is controlled by rate-limited reactions, and its calculation is dependent on a knowledge of other radical concentrations.

The conservation equations for the radical and NO_x concentrations form a set of coupled 'stiff' nonlinear differential equations and their solution requires special integration procedures. One such procedure, which has been developed by Pratt and Wormeck,⁴⁸ is described next. This procedure has been incorporated into the 3-D combustor program and has been used to compute the NO_x emissions in the present work.

B. The Chemical Kinetics Program

The conservation equations for the species involved in NO_x production form a set of 'stiff' equations. Pratt and Wormeck⁴⁸ have developed a numerically efficient computer program (CREK) for the solution of such a set of equations. The CREK procedure is briefly described in the following paragraphs.

The species and energy conservation equations for a node, P, are expressed in the following standard finite-difference form:

$$A_P \phi_P = A_E \phi_E + A_W \phi_W + A_N \phi_N + A_S \phi_S + A_H \phi_H + A_L \phi_L + S_\phi \quad (40)$$

where A is the finite-difference coefficient containing the convective and diffusive fluxes; ϕ is the dependent variable (species concentration, enthalpy); S_ϕ is the source of ϕ ; subscripts E, W, N, S, H, and L refer to the six neighboring nodes of P.

The CREK program is used to solve the above finite-difference equation. The solution is simultaneous for all the species concentrations and temperature at a given node P; and proceeds node-by-node until all of the nodes in the flow field are covered. The solution procedure involves the derivation of a set of Newton-Raphson correction equations for the species concentrations and temperature. These equations are solved iteratively by pivoted Gaussian elimination.

The program requires as input the following information:

- (1) Previous solution or estimate of ϕ_P and temperature at node P;
- (2) Pressure at node P;
- (3) Finite-difference coefficients $A_P, A_E, A_W, A_N, A_S, A_H,$ and A_L , as calculated in the 3-D combustor program;
- (4) $\phi_P^* = (A_E\phi_E + A_W\phi_W + A_N\phi_N + A_S\phi_S + A_H\phi_H + A_L\phi_L)/A_P$
- (5) Enthalpy source coefficients Q, where, enthalpy source = $-(Q_0 + Q_1T + Q_2T^2 + Q_3T^3 + Q_4T^4)$.

The outputs from the program are

- (1) Mole numbers of all chemical species;
- (2) Temperature at node P;
- (3) Density at node P.

Further details of the CREK procedure are contained in Reference 48.

C. Present Approach

The number of species considered in the present program is 14: $C_xH_y, C_{x-2}H_{y-2}, CO, CO_2, H, H_2, O, O_2, OH, H_2O, N, N_2, NO, NO_2$. Here, $C_{x-2}H_{y-2}$ denotes the intermediate hydrocarbon as explained in Chapter VI. Each of these species concentrations is governed by a transport equation of the same general form as Equation (3). To complete the equation specifications, the source terms and the

Schmidt numbers for these variables have to be determined. The turbulent Schmidt numbers, σ_ϕ , for all the species are assumed to be 0.9. The computation of the source terms, S_ϕ , is based on the reaction mechanism given in Table I. The calculation involved for each reaction is illustrated below with reference to the reaction $A+B \rightleftharpoons C+D$.

The laminar Arrhenius rate

$$R_L = \rho^2 M_A M_B A T^b \exp (-E/RT) \quad (41)$$

where M_A and M_B are the mass fractions of A and B.

The turbulent eddy-break-up rate for species A is

$$R_T = C_R \rho M_{MIN} \epsilon / k \quad (42)$$

where C_R is a constant, ρ is the density, and where M_{MIN} is the smaller of M_A and M_B/i , i being the mass of B required per unit mass of A in this reaction. The rate of production/consumption of A is

$$R = \text{smaller of } R_L \text{ and } R_T$$

The backward rate is treated similarly. All of the reactions listed in Table I and the global reactions discussed in Chapter VI are treated in this way, and the sources due to chemical reaction in the conservation equations for the species are obtained by summing the rates due to all of these reactions. The resulting species equations are solved by the computer program CREK described above. This determines the concentrations of all of the species. Modifications have been made to the CREK program in the present work in order to treat the global reactions and the eddy-break-up rates for the reaction steps.

TABLE I. NO_x REACTION MECHANISM.

$$K_f = 10^x T^b \exp (-E/RT)$$

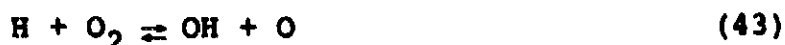
Reaction					X	b	E/R (°K)	
1.	H	H	M	= H2	M	12.300	-1.000	0.0
2.	O	O	M	= O2	M	11.000	-1.000	0.0
3.	H	OH	M	= H2O	M	13.850	-1.000	0.0
4.	H	O2		= OH O		11.350	0.0	8400.000
5.	O	H2		= OH H		10.240	0.0	4730.000
6.	H	H2O		= OH H2		10.920	0.0	10050.000
7.	O	H2O		= OH OH		10.760	0.0	9000.000
8.	N2	O		= NO N		9.000	0.0	25000.000
9.	N	O2		= NO O		5.000	1.000	2000.000
10.	N	OH		= NO H		9.000	0.0	0.0
11.	N2	O2		= N NO2		11.431	-1.000	60600.000
12.	NO	NO		= N NO2		7.000	0.0	0.0
13.	NO	O2		= NO2 O		9.000	0.0	22900.000
14.	H	NO2		= NO OH		10.477	0.0	0.0

NOTE: Values are in SI units.

Reverse rate constant obtained from forward rate constant equilibrium constant.

The consideration of a detailed mechanism as shown in Table I is computationally time consuming when considering a three-dimensional problem. The chemical kinetics solution involves a point-by-point procedure, proceeding from one grid node at a time to the next until all nodes are covered. At any stage, the species concentrations at the nodes that are yet to be solved also influence the concentrations at the node currently being solved. Therefore, the concentrations at the nodes not yet solved, have to be estimated or are known from the previous iteration. Due to this explicit (as opposed to implicit) nature of the coupling between values at neighboring nodes, the solution has to be repeated several times in order to achieve convergence with attendant large computer times.

In order to reduce computer times, the partial equilibrium assumption has been used in some work reported in the literature. This involves the assumption that the following four bimolecular reactions are equilibrated:



This assumption reduces the number of kinetic equations to be solved. The equilibration of these reactions in several premixed combustion systems is supported by the studies of References 49-51. Their equilibration in a CH_4 -Air diffusion flame was demonstrated by Mitchell, et al.²⁵ They showed that these reactions are in equilibrium over a range of equivalence ratios from little less than unity up to approximately 2.5 for a flame at atmospheric pressure with the reactants initially at about 300°K. The equilibration of these reactions at different conditions, more closely resembling those in gas-turbine combustors, has not been demonstrated. Thus,

the partial equilibrium assumption may not be valid in all regions of a gas-turbine combustor; hence, it has not been used in the present work. The present approach, although more time-consuming, is general and does not involve any simplifications regarding the chemistry.

There have been reports of fast integrators for stiff kinetic equations in recent literature, e.g., Reference 57. The use of these instead of CREK (which was used in the present work because of its availability in a well-tested form while other schemes were still in their development and testing phases) will reduce computer times and will make fine grid 3-D computations possible without undue computational costs. The framework for the kinetics calculations has been provided here and the substitution of CREK for another procedure should be a straightforward task. The use of fast integrators will also enable the treatment of a more detailed reaction mechanism for NO_x . Thus, steps involving species such as HCN (on fuel-rich side) can be included if reliable kinetic data is available.

CHAPTER VI

THE FOUR-STEP HYDROCARBON OXIDATION MECHANISM

A. Background

A successful modeling of combustion systems depends on an adequate description of the reaction mechanism. For hydrocarbon oxidation, a large number of species participating simultaneously in numerous elementary kinetic steps is required to specify the reaction mechanism. This results in "stiff" differential equations requiring special time-consuming integration methods. For a complex 3-D problem, the computing costs would be prohibitive. Besides the large number of species equations to be solved, the elementary steps and their rate constants are not well known except for the simplest of hydrocarbons e.g., CH_4 . To get around this problem, the gas turbine combustion modeling effort has frequently been simplified by using a global approach that reduces chemistry to the specification of an overall global oxidation scheme, which can predict quantities of interest: fuel consumption and heat release rates.

The oxidation of hydrocarbon fuel can be described by the following basic steps:

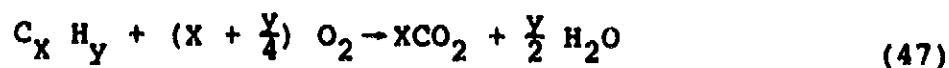
- (a) Transformation of the hydrocarbon fuel into intermediate hydrocarbons and hydrogen with little release of energy;
- (b) Oxidation of intermediates to CO and H_2 ;
- (c) Oxidation of CO to CO_2 ;
- (d) Oxidation of H_2 to H_2O .

Steps (b) through (d) are exothermic and are responsible for the release of energy and associated temperature rise. A global reaction scheme, which is designed to correctly model the oxidation process, must include a description of these steps.

B. Hydrocarbon Reaction Mechanisms

One Step Scheme

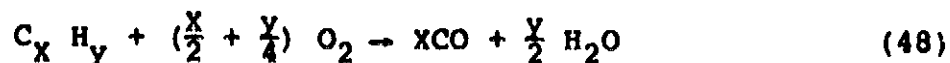
The simplest global mechanism is the one-step scheme:



The advantage of this mechanism is its simplicity; it involves the solution of the conservation equations for unburned fuel and the mixture fraction. The heat release and the concentrations of the other species are then obtained from linear functions of the amount of fuel consumed. This mechanism, however, fails to predict the important characteristics of hydrocarbon oxidation, i.e., the formation of intermediates and CO, which influence the process considerably. As a result, this mechanism is inadequate for obtaining quantitative predictions.

Two-Step Scheme

A slightly more complex scheme is the two-step mechanism:

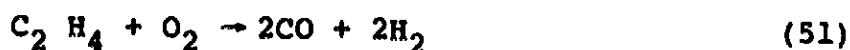
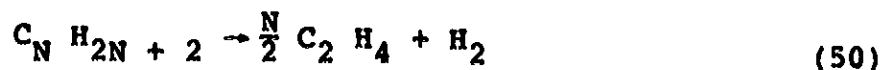


This involves the solution of one additional equation: that for the concentration of CO. Here again, the formation of intermediates is ignored and so this mechanism cannot predict the time delay

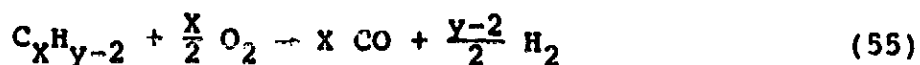
between the initial disappearance of fuel into intermediates and a significant rise in temperature.

Four-Step Scheme

The simplest mechanism which accounts for the essential features of the hydrocarbon oxidation is the following four-step scheme proposed by Hautman, et al.⁵³



This scheme is valid only for aliphatic hydrocarbons of the type $C_N H_{2N} + 2$. To accommodate a general hydrocarbon $C_X H_Y$, the first two steps have been modified in the present work:



This scheme involves the solution of two additional equations: for the concentrations of $C_X H_{Y-2}$ and H_2 .

The rate expressions for the four-step scheme developed primarily from propane oxidation results⁵³ are

$$\frac{d[C_X H_Y]}{dt} = -10^x \exp(-E/RT) [C_X H_Y]^a [O_2]^b [C_X H_{Y-2}]^c \text{ mole/cc-s} \quad (56)$$

$$\frac{d[C_xH_{y-2}]}{dt} = -10^x \exp(-E/RT) [C_xH_{y-2}]^a [O_2]^b [C_xH_y]^c \text{ mole/cc-s} \quad (57)$$

$$\frac{d[CO]}{dt} = \left\{ -10^x \exp(-E/RT) [CO]^a [O_2]^b [H_2O]^c \right\} \times S \text{ mole/cc-s} \quad (58)$$

$$\frac{d[H_2]}{dt} = -10^x \exp(-E/RT) [H_2]^a [O_2]^b [C_xH_{y-2}]^c \text{ mole/cc-s} \quad (59)$$

where [CO], etc. are the species concentrations in gm-moles/cc. The parameters⁵³ for (56) are $x = 17.32 \pm 0.88$, $E = 49,600 \pm 2400$, $a = 0.50 \pm 0.02$, $b = 1.07 \pm 0.05$, and $c = 0.40 \pm 0.03$;

for (57), $x = 14.70 \pm 2.00$, $E = 50,000 \pm 5000$, $a = 0.90 \pm 0.08$, $b = 1.18 \pm 0.10$, and $c = -0.37 \pm 0.04$;

for (59), $x = 13.52 \pm 2.2$, $E = 41,000 \pm 6400$, $a = 0.85 \pm 0.16$, $b = 1.42 \pm 0.11$, and $c = -0.56 \pm 0.20$;

and for (58), $x = 14.6 \pm 0.25$, $E = 40,000 \pm 1200$, $a = 1.0$, $b = 0.25$, and $c = 0.50$;

$S = 7.93 \exp(-2.48\phi)$, where ϕ is the initial equivalence ratio and S cannot take values greater than 1.

The rate expressions were found to predict within reasonable accuracy flow reactor and shock tube results on propane oxidation, which encompass an equivalence ratio range 0.12 to 2.0, a temperature range 960 to 1540K, and a pressure range 1 to 9 atm. With modification to the parameters, experimental flow reactor results on the oxidation of butane, 2- and 3-methylpentane, and n-octane are also predicted.⁵³

The tolerance bands on the various parameters reflect the sensitivity of the predictions to these parameters and the modifications necessary to the values of these parameters in order to

obtain predictions in agreement with experimental measurements for different conditions. In the present work, it was found that the tolerance band on most of the parameters is rather wide and that for any given flow, changing a parameter from its lower to its upper limit can alter the predictions significantly. For the results reported in Chapter VII, the median values of all the parameters were used. Further comparison with more experimental measurements is necessary in order to narrow the tolerance bands and obtain more certain values.

C. Present Approach

The four-step mechanism described above has been incorporated into the 3-D Combustor Performance Program. This involved the solution of two additional differential equations of the same general form as Equation (3), for the concentrations of C_XH_{Y-2} and H_2 . The source terms in these equations were obtained from the mechanism given by Equation (50-55). The rate expressions given by Equations (56-59) were modified by the eddy-break-up rate to account for the influence of turbulence. The procedure used was the same as that for the fuel equation¹. The effective Schmidt numbers for these two species were assumed to be the same as for other species, i.e., 0.9.

Other modifications to the 3-D program to incorporate the four-step scheme were:

- o The source terms for C_XH_Y and CO were modified to be in accordance with the four-step scheme: C_XH_Y consumed in Step (1); CO produced in Step (2) and consumed in Step (3).
- o Mixture molecular weight, density, enthalpy (and hence temperature) calculation sequences were modified to include the two new species: C_XH_{Y-2} and H_2 .

- o Computations of O_2 , CO_2 , H_2O concentrations from element conservation were modified to include the two new species: C_XH_{Y-2} and H_2 .

The four-step scheme was proved to be far superior to the two-step scheme in computations of a plug flow reactor (see Chapter VII, Results).

CHAPTER VII

RESULTS AND DISCUSSION

In this section, the results of the computations performed in the present program are described. The results of the validation of the four-step hydrocarbon oxidation scheme are presented followed by computations of the emissions from a JT8D combustor.

A. Four-Step Hydrocarbon Oxidation Scheme Results

Measurements in a plug flow reactor were conducted by Hautman, et al.,⁵³ for lean, stoichiometric, and rich propane flames. These measurements were used to test the validity of the four-step scheme. Computations were performed for these three cases with both the two-step and four-step schemes. Sixty axial grid points were used in these computations. Reduction of the axial spacing by a factor of two, showed negligible changes, thus demonstrating the grid-independency of the results.

Comparison of the results with the measurements are shown in Figures 1, 2, and 3 for the lean, stoichiometric and rich cases, respectively. From these figures, it is clear that the four-step scheme is far superior to the two-step scheme in predicting the salient features of hydrocarbon combustion.

Figure 1 (a, b, and c) shows the two-step and four-step hydrocarbon oxidation scheme predictions and the corresponding measurements for the lean C_3H_8 flame. The four-step predictions of CO_2 , C_3H_8 , and temperature agree very closely with the measurements. The four-step CO and H_2 predictions are slightly higher than the measurements, but the discrepancy is not large. Since in the predictions all the intermediates are lumped into C_2H_4 , the total measured intermediates are shown in Figure 1c for a more meaningful comparison; here, again, the agreement is good. On the other hand,

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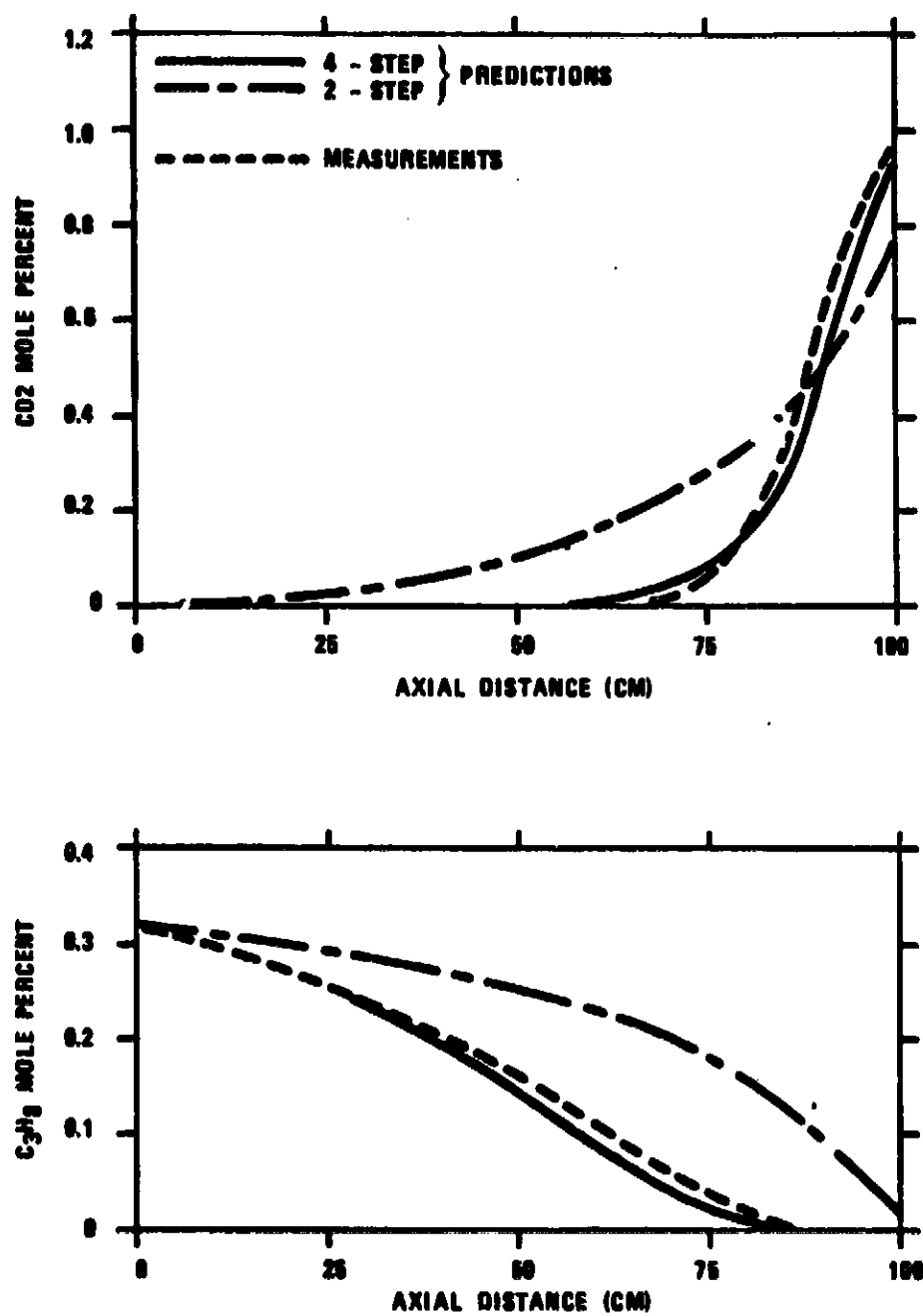


Figure 1a. Lean C₃H₈ Flame ($\phi = 0.12$).

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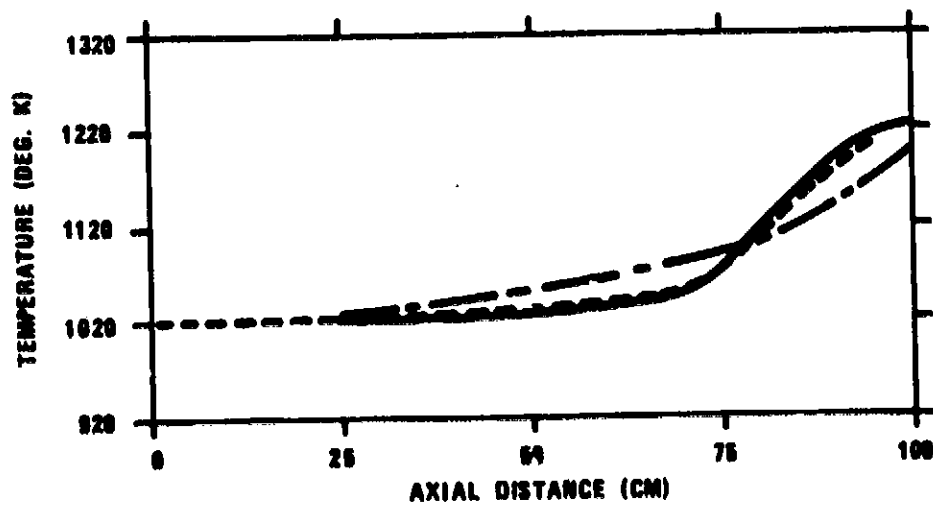
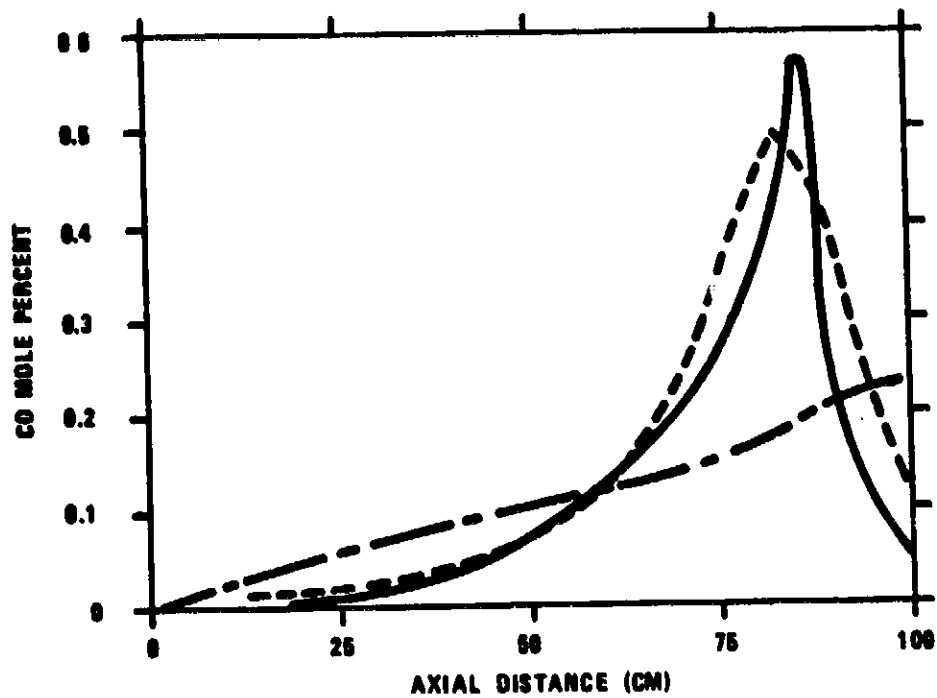


Figure 1b. Lean C_3H_8 Flame ($\phi = 0.12$).

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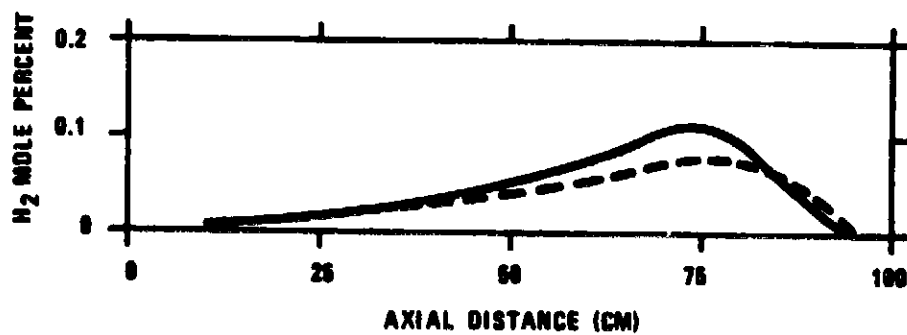
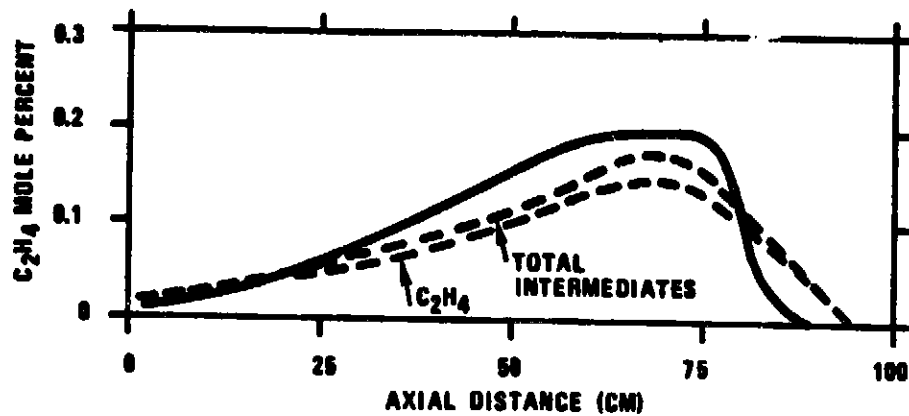


Figure 1c. Lean C_3H_8 Flame ($\phi = 0.12$).

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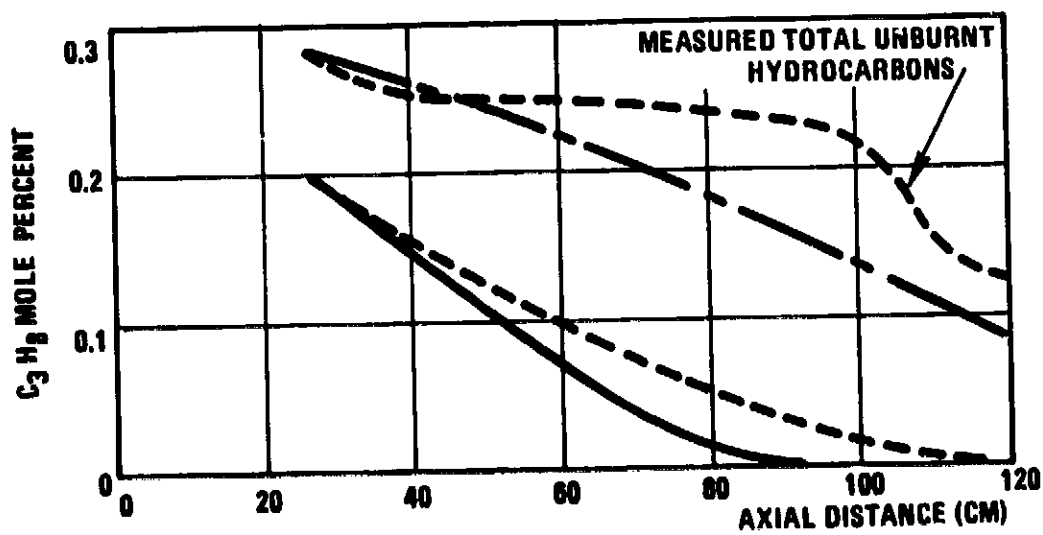
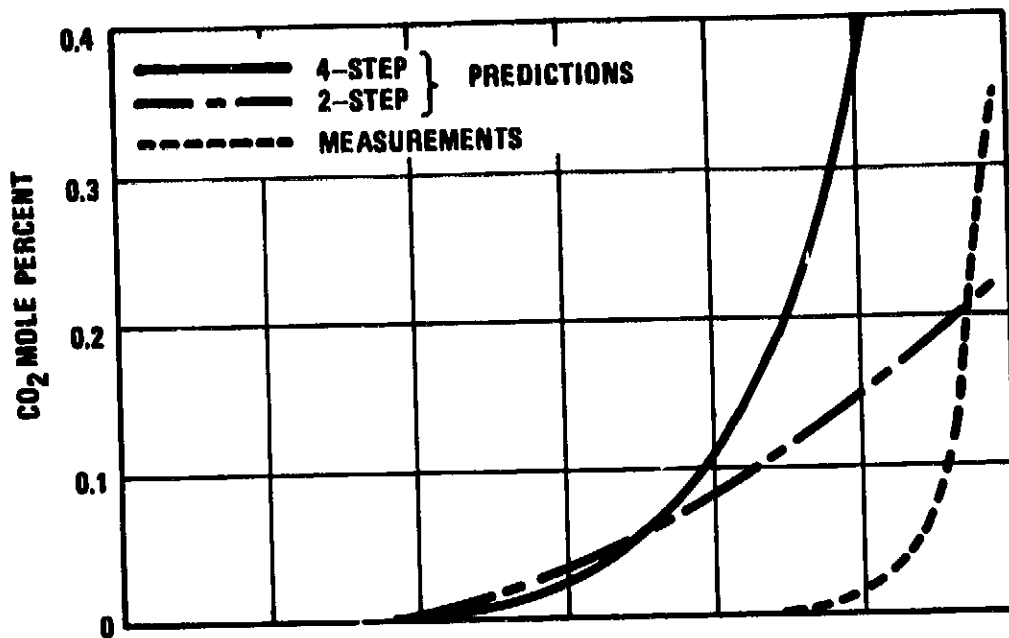


Figure 2a. Stoichiometric C₃H₈ Flame ($\phi=0.98$).

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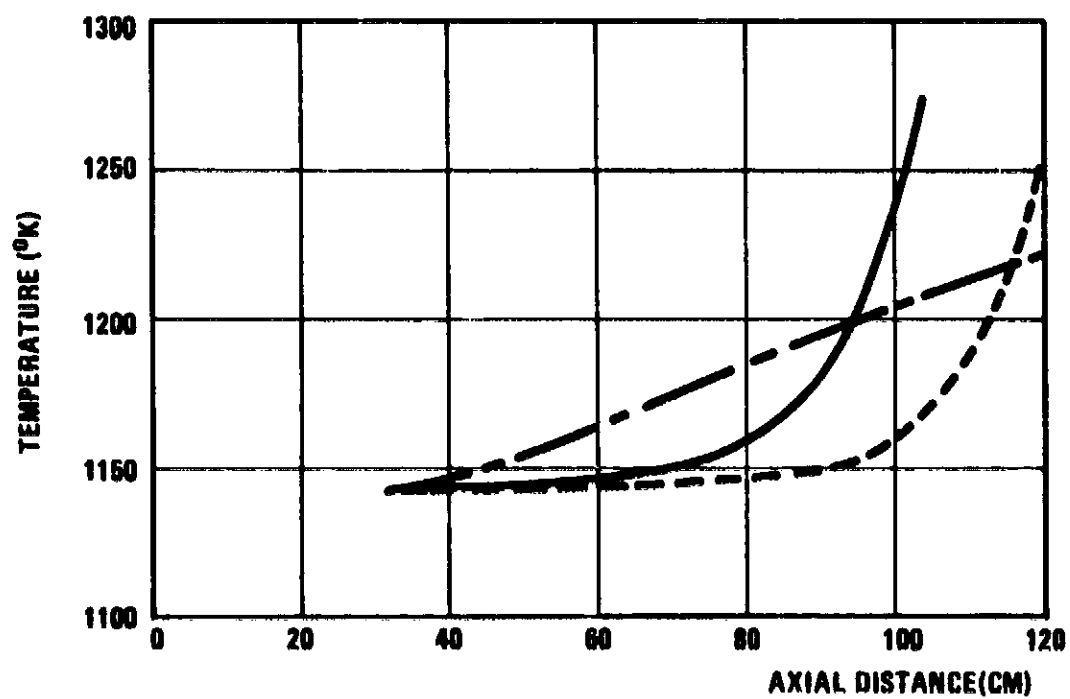
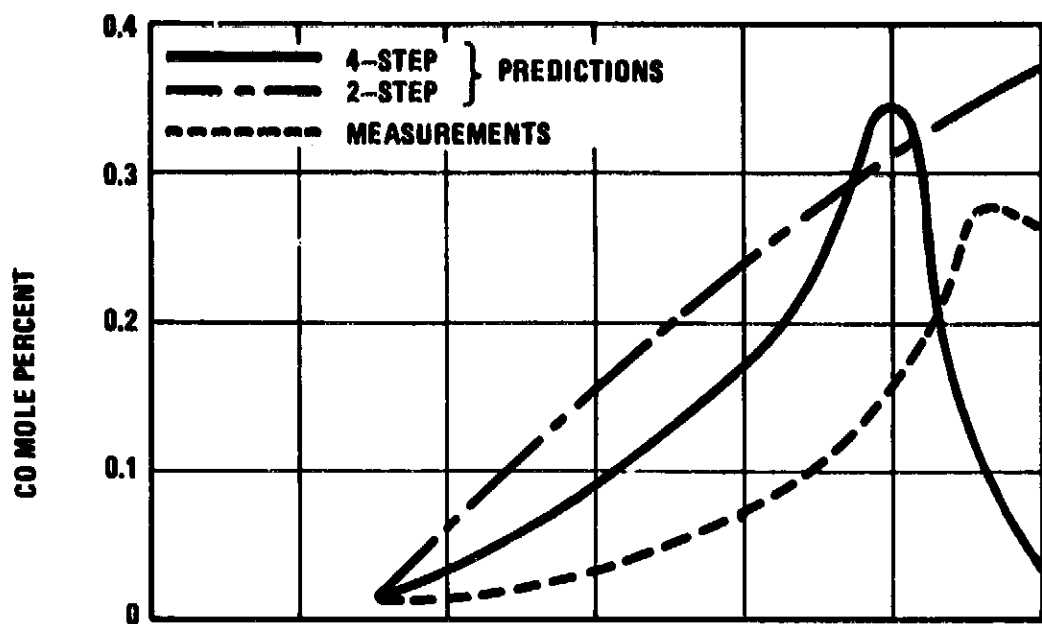


Figure 2b. Stoichiometric C_3H_8 Flame ($\phi=0.98$).

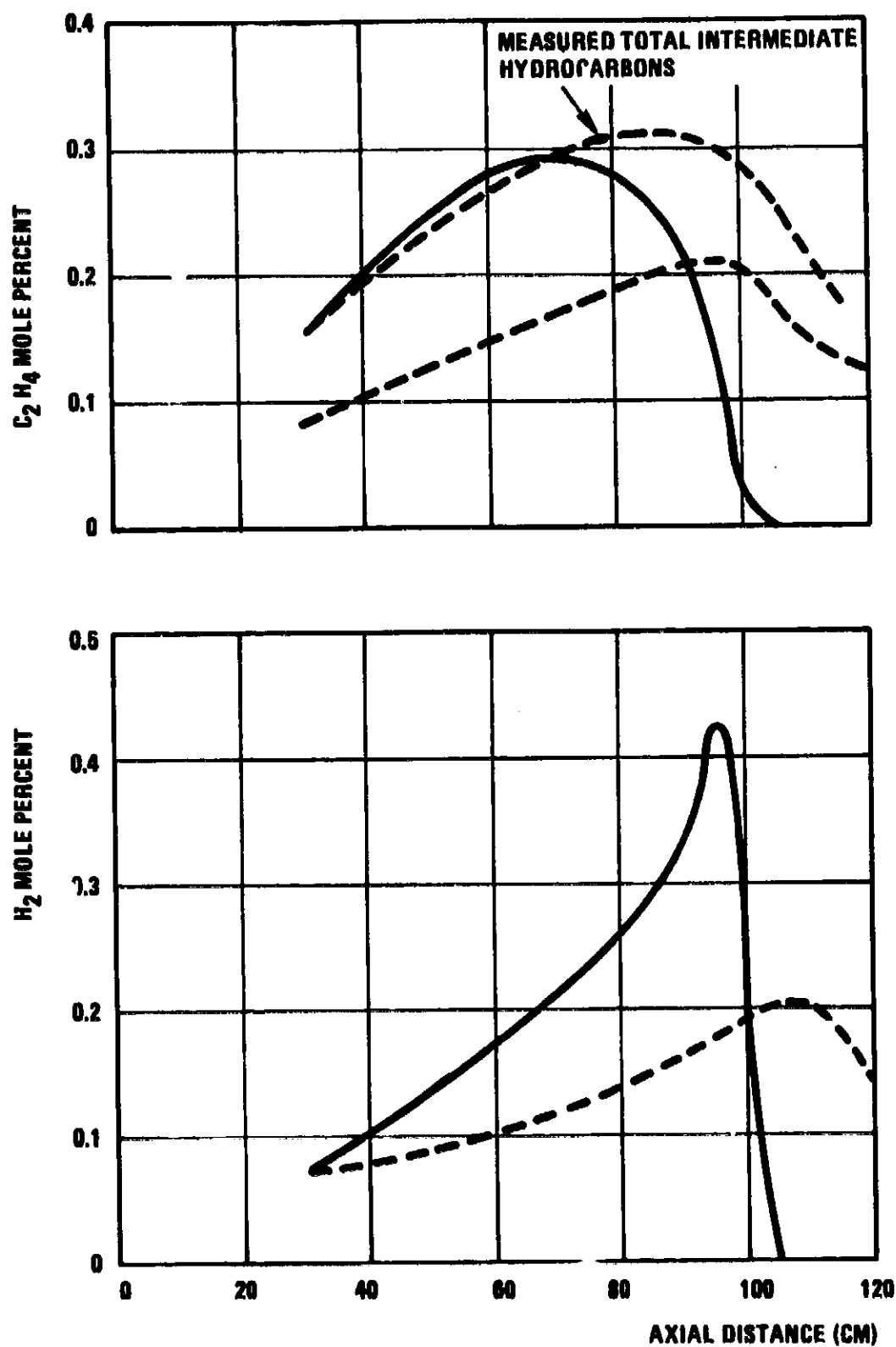


Figure 2c. Stoichiometric C₃H₈ Flame ($\phi=0.98$).

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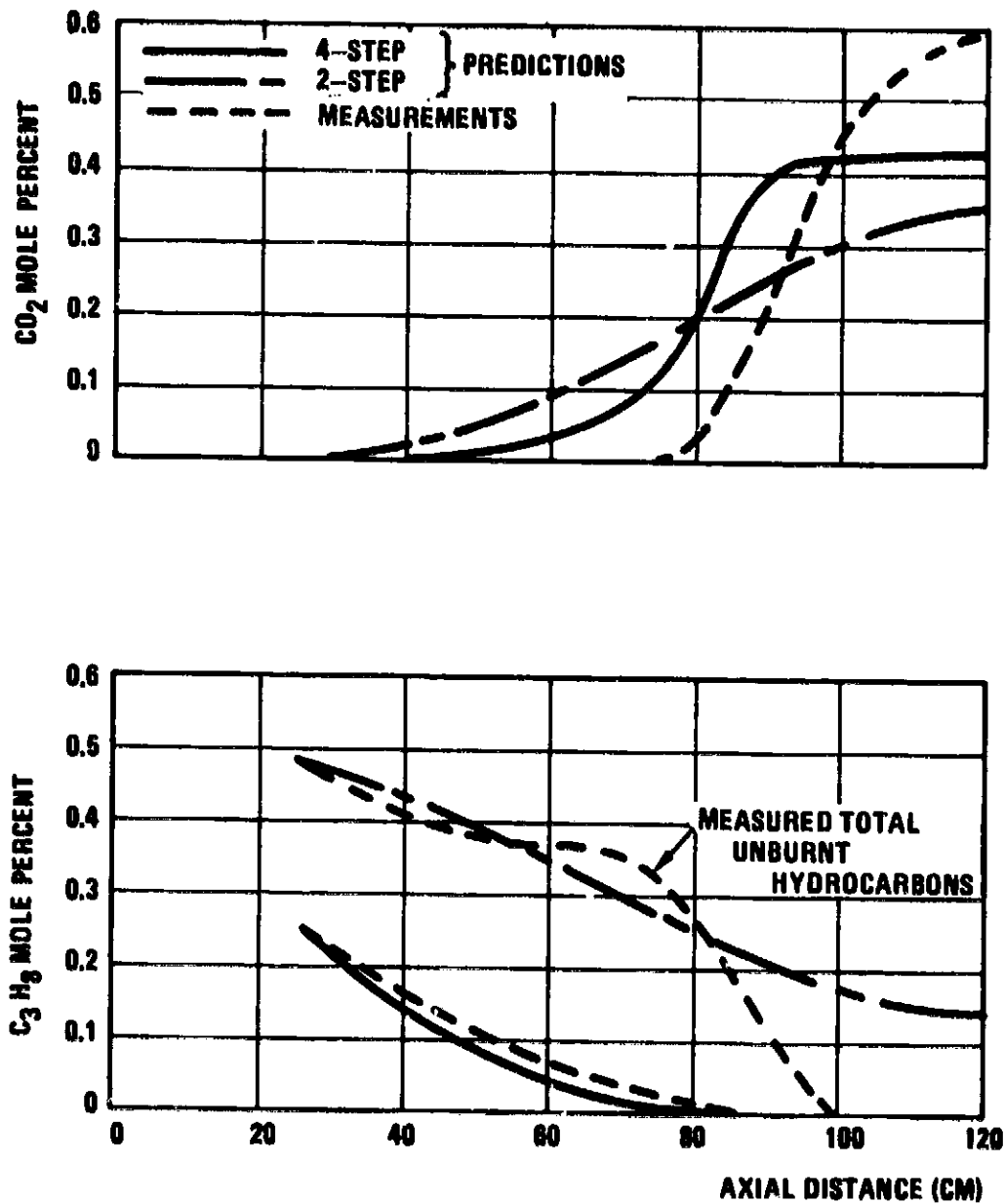


Figure 3a. Rich C₃H₈ Flame ($\phi=1.59$).

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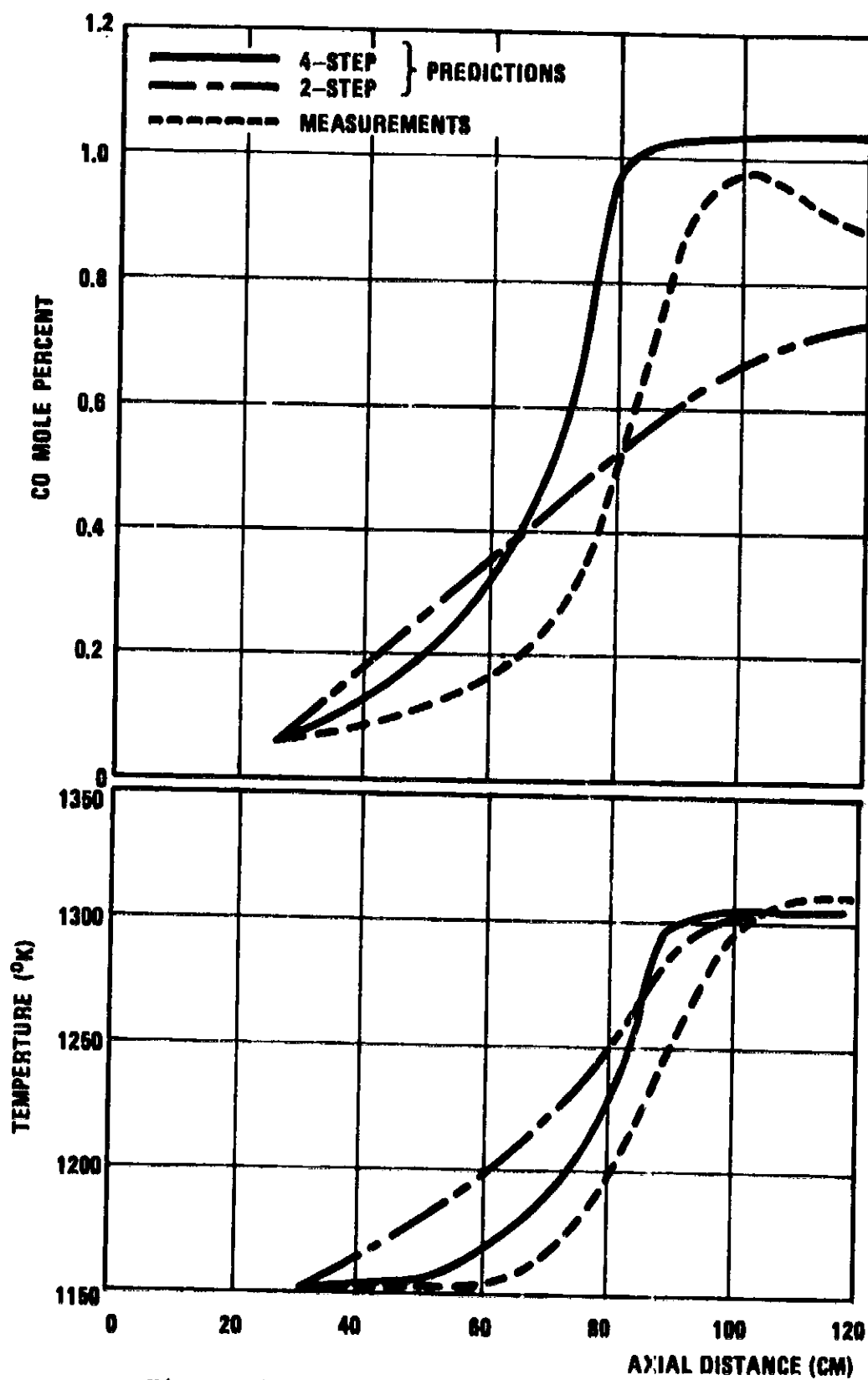


Figure 3b. Rich C_3H_8 Flame ($\phi=1.59$).

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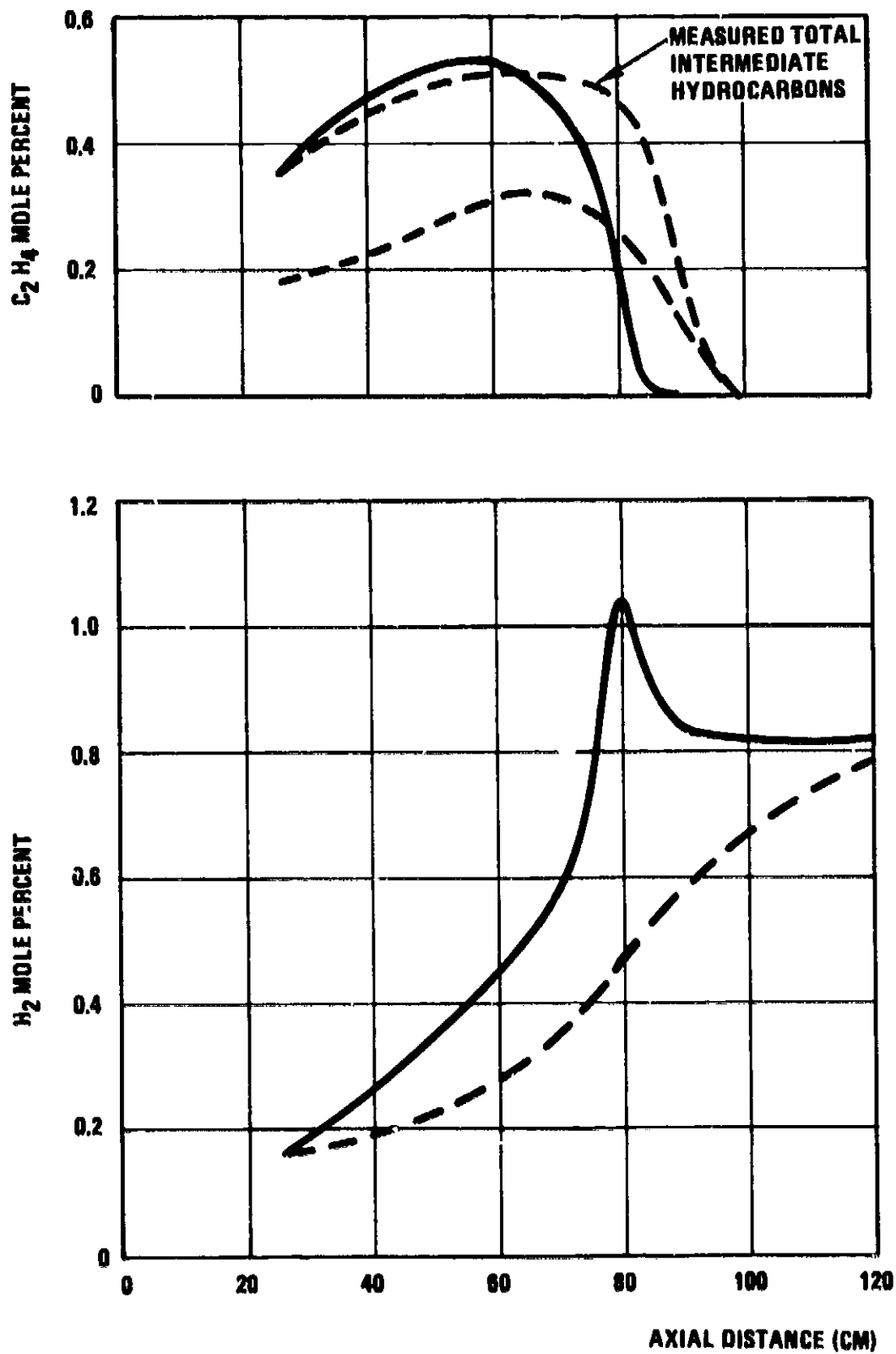


Figure 3c. Rich C_3H_8 Flame ($\phi=1.59$).

the two-step predictions show considerable discrepancy for all the species and for the temperature.

Figure 2 (a, b, and c) shows the measurements and predictions for the stoichiometric case. Here the four-step predictions are not as good as for the lean case; however, compared to the two-step predictions, the four-step results are in much closer agreement with the measurements. A major discrepancy is the predicted (four-step) H_2 concentration, which is considerably higher than the measured values.

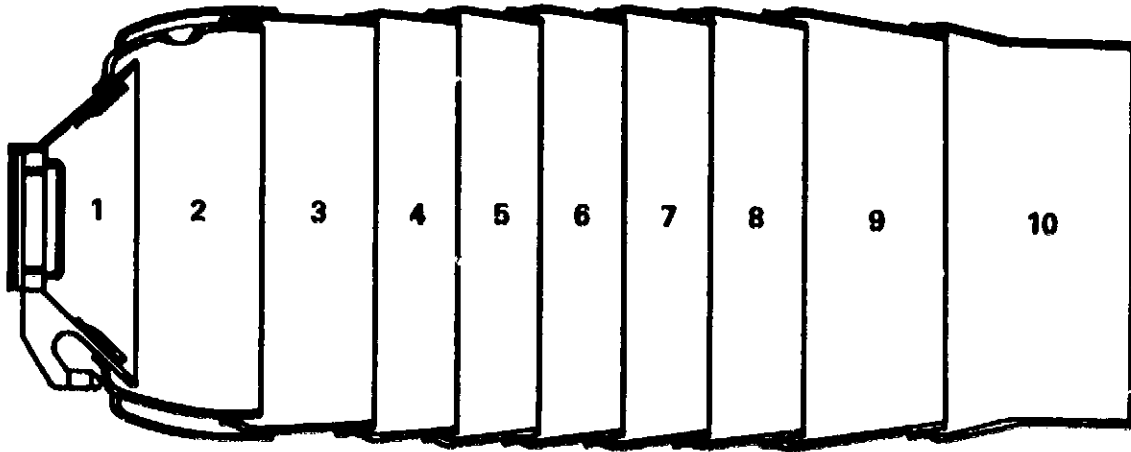
Figure 3 (a, b, and c) shows the measurements and predictions for the fuel-rich case. Here, again, the four-step predictions, although not in very close agreement with the measurements, are far superior to the two-step predictions. The four-step fuel concentration and temperature profiles are in good agreement with the measurements; CO , CO_2 , and C_2H_4 are in fair agreement. Again, the H_2 concentration is overpredicted as in the stoichiometric case.

As shown by these results, a problem not resolved with the four-step scheme is the discrepancy between predicted and measured H_2 and H_2O concentrations, especially at stoichiometric and fuel rich conditions. The H_2 oxidation rate is predicted to occur more slowly, and results in an excess of H_2 and under-prediction of H_2O , as compared to the measurements. A similar observation was also made by Hautman, et al.⁵³

B. JT8D Combustor Computations

The 3-D Combustor Performance Program was set up and run for a JT8D-17 combustor as shown in Figure 4. This combustor uses a single pressure atomizing injector on the centerline of the can. Air is admitted around the injector through a 45-degree swirler. The operating points for the computations represent idle, cruise, and take-off and are given below:

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FUEL INJECTOR AND PRIMARY SWIRLER EQUIVALENT
METERING AREA 7.61 PERCENT

Equivalent Metering Area

Louver Cooling Air		Combustion Air	
Panel	%	Panel	%
1	1.53	2	7.93
2	5.62	3	1.92
3	7.56	5	8.00
4	5.69	8	15.85
5	4.24	9	18.09
6	3.41		
7	3.42		
8	3.43		
9	2.78		
10	1.81		

Figure 4. JT8D-17 Combustor.

Condition	Airflow lbs/sec	Pressure psia	Temperature °F	Fuel/Air Ratio
Idle	4.06	39.6	260	0.0074
Cruise	7.87	103.0	657	0.0138
Take-Off	16.45	256.0	825	0.0182

The steps adopted in the solution procedure for the JT8D combustor are outlined below:

- (1) The 3-D combustor program was used to solve for the variables: velocity, pressure, turbulence energy and dissipation, enthalpy (temperature), mixture fraction, mass fractions of unburned fuel, C_xH_y , CO, and H_2 . At this stage, the soot and radiation equations were not solved, and the solution was carried on until a convergence level of approximately 5 percent in cumulative mass residual was reached.
- (2) The soot and radiation equations were solved next. The radiation fluxes appear as sources in the enthalpy equation; and this, in turn, influences the other dependent variables. The solution of the variables in Step (1) was repeated coupled with the soot and radiation equations. The process was continued until a convergence level of approximately 1 percent was reached.
- (3) The NO_x equations were solved next. The solution of the variables in Steps (1) and (2) was repeated, coupled with the NO_x equations. The process was continued until the convergence level desired for the final solution (~0.5 percent) was reached.

The reason for adopting the above stepwise procedure was to cut down on required computer time. Since the soot is generally present only in small concentrations, it will influence the main flow field only slightly and so delaying the solution of the soot and radiation (which is mainly from soot) equations resulted in a considerable saving of computer time. Similarly, the NO_x species have an even smaller influence on the other variables and so their solution was further delayed. Due to the point-by-point nature of the NO_x solution, this solution had to be repeated a number of times to achieve convergence, as explained in Chapter V.

A flow chart of the overall solution procedure is given in Figure 5. The various steps are executed automatically by the program from start to completion.

Computations were performed with both the two-step and four-step hydrocarbon oxidation schemes and with a grid of $10 \times 10 \times 5$ (axial \times radial \times tangential) points. Due to the coarseness of the grid, it was not possible to simulate exactly all of the geometrical details of the combustor. However, the main features were simulated as closely as possible. Due to the large computer times required for the NO_x calculations, as explained in Chapter V, increasing the number of grid points significantly over that used was found to be computationally prohibitive.

The central processor time on a CYBER 730 computer with the two-step hydrocarbon scheme was 0.044 seconds per iteration per internal node (boundary nodes that are not calculated are excluded here) when the NO_x chemical kinetics solution was not activated. For the NO_x solution, the central processor time was an additional 0.2-0.3 second per iteration per internal node. Typically 100-150 iterations were required before the NO_x solution was turned on, after which an additional 50-100 iterations were required to achieve convergence. Thus for the chosen grid ($10 \times 10 \times 5$), a complete run required 3000-5000 seconds depending on the conditions

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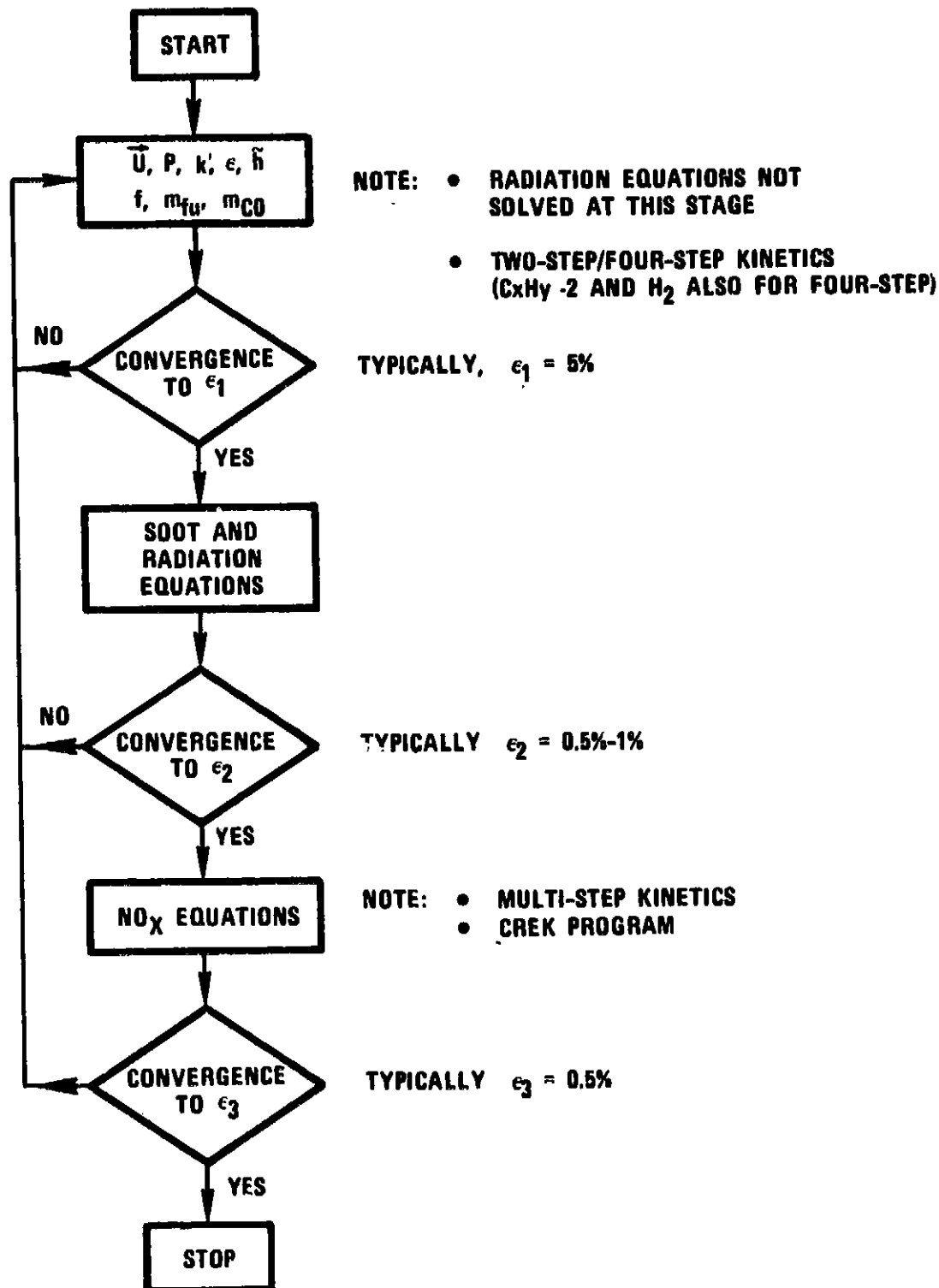


Figure 5. Flowchart of Overall Solution Procedure.

for the run (which influences the number of iterations to convergence), with the bulk of the time spent on NO_x calculations. Since the four-step scheme involved the solution of additional equations for the intermediate hydrocarbon and H_2 , the computation times were about 10-15 percent higher than those with the two-step scheme. The central memory required for the $10 \times 10 \times 5$ grid was 173,500 octal words.

The predicted emissions index for the idle, cruise, and take-off conditions with the two-step and four-step schemes is shown in Tables IIa and IIb. For the idle case, the predicted smoke concentration is very small and much lower than that experimentally observed. The formation of soot, as modeled, is governed by the local temperature and fuel/air ratio and also turbulent fluctuations. Since the temperature and fuel/air ratio are low for the idle case, the model does not predict significant soot formation. Obviously, other factors that have not been modeled and that are not precisely known, govern soot formation under such conditions.

For the cruise and takeoff cases, the emissions indices for soot and NO_x show the correct trends and are reasonably close to the measurements that are available. The differences between the two-step and four-step schemes are not significant in the prediction of the emissions index, which represents an integrated value at the combustor exit. The differences in the two schemes are significant in the primary zone of the combustor.

The predicted radiation flux to the combustor wall for the conditions of idle, cruise, and takeoff is shown in Table IIIa for the two-step scheme and in Table IIb for the four-step scheme. The values are reported at the primary, secondary, and tertiary zones which are at 6, 21, and 33cm downstream of the fuel nozzle; these correspond to the locations at which measurements were conducted by Claus⁵⁶ for different operating conditions. The predicted radiation fluxes show the correct trends; i.e., the flux is

TABLE IIa. PREDICTED EMISSIONS INDEX WITH TWO-STEP HYDROCARBON OXIDATION SCHEME.

Condition	Emission Index Gm of Emissions/Kg of Fuel	
	Smoke	NO _x
Idle	0.26 E-3 (0.6) ⁵⁵	≈0
Cruise	1.6	15
Takeoff	1.5 (2.8) ⁵⁵	28 (24.4) ⁵⁴

NOTE: Values in parentheses are experimental measurements from indicated reference.

TABLE IIb. PREDICTED EMISSIONS INDEX WITH FOUR-STEP HYDROCARBON OXIDATION SCHEME.

Condition	Emission Index Gm of Emissions/Kg of Fuel	
	Smoke	NO _x
Idle	0.056 (0.6) ⁵⁵	≈0
Cruise	1.3	13
Takeoff	1.2 (2.8) ⁵⁵	27 (24.4) ⁵⁴

NOTE: Values in parentheses are experimental measurements from indicated reference.

**TABLE IIIa. PREDICTED WALL RADIATION FLUX WITH
TWO-STEP HYDROCARBON OXIDATION
SCHEME.**

Condition	Primary Zone (W/M ²)	Secondary Zone (W/M ²)	Tertiary Zone (W/M ²)
Idle	2.9E4	3.46E4	1.03E4
Cruise	5.55E5	8.98E5	2.23E5
Takeoff	7.89E5	1.33E6	4.26E5

**TABLE IIIb. PREDICTED WALL RADIATION FLUX WITH
FOUR-STEP HYDROCARBON OXIDATION
SCHEME.**

Condition	Primary Zone (W/M ²)	Secondary Zone (W/M ²)	Tertiary Zone (W/M ²)
Idle	1.06E4	1.35E4	3.19E3
Cruise	3.78E5	9.01E5	2.13E5
Takeoff	6.40E5	1.34E6	3.72E5

maximum in the secondary zone and minimum in the tertiary zone. This trend was experimentally observed by Claus.⁵⁶ The level of the flux also corresponds to that measured by Claus for slightly different conditions. Due to the differences in the conditions for which measurements and predictions were made, a direct comparison of the two is not shown.

For the idle case, since the soot concentrations were predicted to be very low, the predicted radiation fluxes are also towards the low side. The predicted radiation flux with the four-step scheme is lower than that with the two-step scheme for the idle case, but the soot predictions show the opposite trend, i.e., slightly higher with the four-step scheme. This occurs because, in the predictions for the idle case, the radiation from the soot is low and is due to its small concentration. The gas radiation is important and is predicted to be higher with the two-step scheme because of a faster temperature rise.

The computations performed for the three operating conditions of the JT8D combustor show that the present model is capable of producing reasonable predictions of the emissions of smoke and NO_x and of the wall radiation flux.

CHAPTER VIII

CONCLUSIONS

In the present work, a method was formulated for the following:

- o computation of soot and NO_x emissions from a combustor
- o inclusion of the effects of soot on radiant heat transfer, and
- o extension of the two-step hydrocarbon oxidation scheme to a four-step one.

The method was coded into the Garrett 3-D Combustor Performance Program. A description of the program, list of Fortran variables, and program listing have been included in the report to aid the reader in understanding the emissions model.

The computations that were performed show that the method is capable of producing reasonable results. The lack of accurate experimental data has precluded more detailed validation of the model. As reliable experimental data becomes available, further computations will reveal the capabilities and limitations of the model and the modifications necessary to overcome the limitations.

CHAPTER IX

NOMENCLATURE

All symbols were defined in the report at the point when first referenced. The following is a list of symbols used often in the report.

- a = Absorption coefficient
- C_i = Time-mean concentration of species i
- C_p = Specific heat
- D = Particle diameter
- E = Activation energy
- k = Kinetic energy of turbulence
- K_b = Backward reaction rate constant
- K_C = Equilibrium constant
- K_f = Forward reaction rate constant
- m_i = Mass fraction of species i
- n = Nuclei concentration
- n_0 = Rate of spontaneous nuclei formation
- N = Concentration of soot particles
- P = Pressure
- R = Reaction rate
- S = Scattering coefficient
- S_ϕ = Source term of dependent variable ϕ
- t = Time
- T = Temperature

\vec{u} = Velocity vector
 ϵ = Emissivity; dissipation rate of turbulence
 ϕ = General dependent variable
 ν = Kinematic viscosity
 μ_t = Effective viscosity
 σ = Stefan-Boltzmann constant
 σ_ϕ = Prandtl/Schmidt number of dependent variable ϕ
 ρ = Density
 λ = Wavelength

Subscripts

fu = Fuel
 i = Species i
 n = Nuclei
 O_2 = Oxygen
 pr = Products
 S = Soot
 ϕ = Dependent variable

Superscripts

\star = Fine structure
 \circ = Surrounding fluid

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APPENDIX A
DESCRIPTION OF THE 3-D
COMBUSTOR PERFORMANCE PROGRAM

APPENDIX A

DESCRIPTION OF THE 3-D COMBUSTOR PERFORMANCE PROGRAM

The 3-D performance model is a three-dimensional recirculating-flow program that is capable of analyzing a variety of combustor configurations, including can, can-annular, and annular. The program solves for the three velocity components, U, V, and W, species concentrations, C_{XH_Y} , $C_{XH_{Y-2}}$, C(S), CO, CO₂, H, H₂, O, O₂, OH, H₂O, N, N₂, NO, NO₂, turbulence quantities from the k- ϵ turbulence model, and three radiation fluxes. In addition, the use of primitive variables makes modifications to the boundary conditions easy, allowing the user to analyze complex inlet geometries. Also provided is a subroutine for calculating the trajectories and evaporation rates of a fuel-nozzle spray. The functions of the various subroutines are briefly described below.

Program MAIN (a computer listing has been provided in Appendix D) is divided into two basic sections. Up to card MA.167, the routine is concerned with reading the input data and converting it to the program's internal units which are Systeme International (S.I.). The input sequence is covered in Appendix B so only the units will be discussed. Cards MA.7 to MA.11 are used to define seven arrays which convert lengths associated with dimensions and lengths associated with velocity, energy, mass, temperature, pressure, and angles respectively. By proper specification in the data statements, the user may employ those input units that are most convenient. The output units are always S.I. From card MA.168 on, MAIN's function is to call the other various routines in their proper sequence.

Subroutine INIT performs some preliminary calculations (AL.10 to AL.155), prints the input data (AL.156 to AL.258), and defines

the initial conditions and some of the boundary conditions on the various arrays (AL.259 on). In section AL.48 through AL.78, two arrays, JKIN and IKIN, are defined. They merely contain flags which indicate the locations of mass injection points. Cards AL.261 to AL.272 contain logic for the restart option. If Tape 0 from a previous run is saved and then made available for use during a subsequent run, the program will read the initial and boundary conditions from it.

Subroutine ALLMOD contains several entry points which perform miscellaneous calculations pertaining, usually, to the boundary nodes where modifications to the standard equation are in order. The cyclic nature of the boundary conditions in the θ or K direction is evident in FMOD as well as limits to the species mass fractions. VELMOD allows the inlet swirl velocity to be increased gradually over a number of iterations and assures that overall continuity is maintained at the exit plane. DENMOD makes alterations to the density at the boundaries to maintain the correct mass-flow rate. GAMOD specifies the wall viscosity values as calculated by the wall functions. SOMAS is used to initialize an array DIVG which is used later in the program. The largest entry point SOMOD contains logic for modifying the equation coefficients and source terms when cooling slots, walls, and droplet evaporation are present. Each variable has its own section and accounts for transfer with the walls and mass addition from the evaporating fuel. SOMODZ deals only with the Z -direction radiation equation and is in a section alone as the data storage is slightly different for this variable.

Subroutine OUTPUT is used for printout purposes. The emissions index of SOOT and NO_x is calculated and printed here. Subsequently, subroutine FPRINT is called for the printout of all dependent variables.

Subroutine AUX performs the auxiliary calculations for temperature, density, viscosity, and source terms. Entry DENS uses AU.11 to AU.56 to calculate temperature. Cards AU.52 to AU.56 limit the values calculated in order to account for dissociation and early iteration fluctuations. With known temperature, density is then determined from AU.57 to AU.108. VISCO obtains effective viscosity from turbulent kinetic energy and dissipation and calculates Y^+ for use by the wall function routine. GAMMA obtains the effective diffusion coefficients. SOURCE contains all calculations for source terms with the exception of the aforementioned modifications in SOMOD. Again, each variable has its own section, with coding that is quite straightforward and requires no explanation.

Subroutine AUXRAD performs the same function as AUX except that it pertains only to the radiation equations.

Subroutine SPRAY is used to determine the evaporation rate of the fuel-nozzle spray. A large section, from SP.106 to SP.269, deals with locating the droplet, determining free-stream conditions, and handling the situation where the droplet approaches a boundary. Next, various fuel and free-stream properties are evaluated (to SP.292). The drag forces and time step are then determined and used to obtain new velocities and location. If the droplet is below the boiling temperature, no evaporation occurs (SP.340 to SP.347); but, when the boiling temperature is reached, evaporation rates are calculated, and the appropriate entries to the evaporation array (EVAP) are made. Information concerning momentum changes due to evaporation are also stored in their respective arrays and later (SP.382 to SP.425) on a scratch file for use when the three momentum equations are solved.

The coefficients for each variable are generated and the solution routine called in subroutine STRIDE. First, equations for U,

V, and W are handled (ST.117 to ST.632), then the pressure perturbation (P') is obtained (ST.633 to ST.714) and used to correct the velocities (ST.716 to ST.753) so that mass errors are reduced. Then, the remaining variables are solved with the radiation equations having their own special section (ST.915 to ST.937). The chemical kinetics calculations are contained from NOX.230 to NOX.342. Here the inputs to program CREK are prepared and the outputs from CREK are stored in the respective arrays.

STRAD is a subroutine used in the radiation model which performs the same function as STRIDE performed for the other variables.

Subroutines ABSORB, ASYMP, CHEBY, DLECK, EGAS, PENTA, SOOT and SCRTCH (from Ref. 40) are used to compute the absorbtivity of gas-soot mixtures.

SOLVE provides a solution to the equations generated in STRIDE. A full three-dimensional solution would be time consuming and would require enormous computer storage. Therefore, an approximate solution is obtained by "sweeping" through the field several times alternately solving along one direction, while holding the values in the other two fixed. The variable ICTDMA (NV) at S0.36 is used to specify the number of such sweeps. As the program converges, and the variables assume their final values, the solution becomes more accurate. Due to the cyclic nature of the boundary conditions in the θ -direction, a cyclic tri-diagonal matrix algorithm (CTDMA) is used for this direction; the coding sequence is contained in SOLVE2.

Subroutine FPRINT is used for the printout of field values of dependent variables.

The last part of the program contains the chemical kinetics subroutines: CREK, CALC, SPECE, CREKO AND HCPS.

Subroutine CREK is the main routine called from the 3-D program. It controls the solution strategy: equilibrium or kinetic and problems associated with lack of convergence.

Subroutine CALC construct the Newton-Raphson correction matrix for both equilibrium and kinetic states and solves for the corrections by a standard Gaussian elimination procedure. In the present work, modifications have been made to this subroutine in order to incorporate the four-step hydrocarbon oxidation scheme and to compute the reaction rates from the eddy-break-up model.

Subroutine SPECE contains the Newton-Raphson iteration procedure for both equilibrium and kinetic states.

Subroutine CREKO is the initializing subroutine and is used for the input of element, thermodynamic and reaction mechanism data.

Subroutine HCPS is used for computing the enthalpy, constant pressure specific heat and the entropy of the species.

Further details of the chemical kinetics subroutines are contained in Ref. 48.

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APPENDIX B
PROGRAM INPUT
DESCRIPTION

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APPENDIX B

PROGRAM INPUT DESCRIPTION

Card Set	Variable	Format	Description
1	TITLE	20A4	Each card is a heading for a particular three-dimensional array that is printed out. These never change (33 cards).
2	TITLE2	10A4	Case title card.
3	LP1	8(I2,8X)	Number of grid nodes in axial (x) direction.
	MP1		Number of grid nodes in radial (y) direction.
	NP1		Number of grid nodes in tangential (z) direction.
	IPLAX		01 For plane geometry; 02 For axisymmetric geometry.
	MODEL		01 For laminar viscosity; 02 For k- ϵ viscosity model.
	MODER		01 For kinetic controlled combustion; 02 for kinetic and turbulence controlled combustion.
	IPAR		01 For absolute pressure; 02 For relative pressure.
	ITRAD		01 No radiation; 02 With radiation; radiation properties specified; 03 With radiation; radiation properties calculated.
4	IU	8(I2,8X)	01 Input units are international system (i.e., meters, kilograms, degrees kelvin, newtons, joules, radians, seconds or combinations thereof); 02 User selected input units.
	MODEN		01 Density is fixed at the value of "Den" on Card Set 19; 02 Density calculated from perfect gas law.
	INTAPE		00 Initial conditions not printed; 08 Initial conditions printed.

Card Set	Variable	Format	Description
	IDW		00 Inner boundary is axis of symmetry; 01 Inner boundary is wall.
	IRES		00 This is a new case; 01 This is a restart of previous case.
5	ISOLVE	8(I2,8X)	An 01 in proper field indicates that this particular variable will be solved for; an 00 indicates that it will not be. Order of variables: u, v, w, p', k, ϵ , ϕ , mfu, mCH, mCO, mH ₂ , h, n, sl, s2, 14*0 (14 species solved by CREK), Rx, Ry, Rz.
6	ICTDMA	8(I2,8X)	Indicates the number of "sweeps" made in the solve routine for each variable. Order of variables as in Card Set 5.
7	IPRINT	8(I2,8X)	An 01 indicates that this variable will be printed, an 00 indicates that it will not be. Order of variables as in Card Set 1.
8	RELAX	8E10.4	Relaxation parameters for each variable. Order of variables as in Card Set 5. In addition, pressure, density, effective viscosity at end of the set.
9	PR	8E10.4	Laminar Prandtl numbers for each variable. Order of variables as in Card Set 5.
10	PREF	8E10.4	Turbulent Prandtl numbers for each variable. Order of variables as in Card Set 5.
11	X	8E10.4	X-coordinates (LP1 values).
12	RI Y	8E10.4	Radius of inner boundary. Y-coordinates as measured from inner boundary (MP1-1) values. Since Y(1) is <u>always</u> 00, RI is read in its place.
13	Z	8E10.4	Z-coordinates (NP1 values).
14	IWEI	8(I2,8X)	I-node at which upstream inclined wall ends.
	JWIO	See Fig. B-1	J-node at which upstream outer inclined wall starts.

Card Set	Variable	Format	Description
	IWEO		I-node at which downstream inclined wall starts.
	JWOO		J-node at which downstream outer inclined wall ends.
15	IWLI	8(I2,8X)	Starting I-nodes of the calculation domain when inclined wall is present. (Skip if IWEI = 2).
16	JWLO	8(I2,8X)	Ending J-nodes of the calculation domain at upstream outer inclined wall. (Skip if IWEI = 2).
17	IWLO	8(I2,8X)	Ending I-nodes of the calculation domain when inclined wall is present. (Skip if IWEO = L).
18	JWLO	8(I2,8X)	Ending J-nodes of the calculation domain at downstream outer inclined wall. (Skip if IWEO = L).
19	PRESS	8E10.4	System pressure.
	DEN		The value of density if option MODEN = 01 is selected.
	ABSOR		Absorption coefficient in radiation model (if ITRAD = 2).
	SCATR		Scattering coefficient in radiation model (if ITRAD = 2).
	AKFAC		Internally defined turbulent kinetic energies are AKFAC time the appropriate velocity squared.
	ALFAC		Internally defined turbulent length scales are ALFAC time the appropriate distance.
20	CXX	8E10.4	Carbon atoms in fuel molecule.
	HYY		Hydrogen atoms in fuel molecule.
	HFU		Heat of formation of fuel.
	FUMCO		Initial value assigned to MCO.
21	PREXP1	8E10.4	Preexponent of 1st reaction.
	ARCON1		Activation energy divided by gas constant of 1st reaction (E/R).
	CR1		Constant in turbulence controlled reaction rate of 1st reaction.

Card Set	Variable	Format	Description
	PREXP2		Pre-exponent of 2nd reaction.
	ARCON2		Activation energy divided by gas constant of 2nd reaction (E/R).
	CR2		Constant in turbulence controlled reaction rate for 2nd reaction.
22	PREXP3	8E10.4	Pre-exponent of 3rd reaction.
	ARCON3		Activation energy divided by gas constant of 3rd reaction (E/R).
	CR3		Constant in turbulence controlled reaction rate for 3rd reaction.
	PREXP4		Pre-exponent of 4th reaction.
	ARCON4		Activation energy divided by gas constant of 4th reaction (E/R).
	CR4		Constant in turbulence controlled reaction rate for 4th reaction.
23	AA1	8E10.4	Exponent on species concentration in the reaction rate for 1st reaction.
	BB1		
	CC1		
	AA2		Exponent on species concentration in the reaction rate for 2nd reaction.
	BB2		
	CC2		
24	AA3	8E10.4	Exponent on species concentration in the reaction rate for 3rd reaction.
	BB3		
	CC3		
	AA4		Exponent on species concentration in the reaction rate for 4th reaction.
	BB4		
	CC4		
25	C1	8E10.4	Turbulence model constant.
	C2		Turbulence model constant.
	CD		Turbulence model constant.
	AMU		The value of the viscosity if option MODEL = 01 is specified. Also the laminar viscosity used in the "wall functions".
	ERROR		Program will terminate if total error in mass becomes less than this value.
	TCYLW		Temperature of cylindrical portion of combustor and of dome.
	TLIP		Temperature of cooling slot lip.
26	LASTEP	2(I3,7X),	Maximum number of iterations.
	IJUMP	6(I2,8X)	Number of iterations between array printout.

Card Set	Variable	Format	Description
	JSW1		J-node at start of dome inlet.
	JSW2		J-node at end of dome inlet.
	NUINJ		Number of axial injection points (cooling slots).
	NVINJ		Number of radial injection points.
27	USW	8E10.4	Axial velocity of dome inlet.
	VSW		Radial velocity of dome inlet.
	SWNO		Ratio of tangential to axial velocity at dome inlet.
	AFSW		Flow rate of fuel and air through dome inlet.
	FSW		Flow rate of fuel through dome inlet.
	TSW		Temperature at dome inlet.
28	NFNZ	2(I2,8X), 6E10.4	00 No liquid fuel nozzle; 01 Liquid fuel nozzle present.
	ISPRAY		Droplet evaporation routine is called every ISPRAY iterations.
	TFUEL		Initial temperature of liquid fuel.
29	XO	8E10.4	X-location of origin of fuel nozzle spray.
	YO		Y-location of origin of fuel nozzle spray.
	ZO		Z-location of origin of fuel nozzle spray
	ALFA		Nozzle cone angle.
	BETA		Nozzle back angle.
	DELTA		Nozzle down angle.
	THETA1		Initial spray cone segment angle.
	THETA2		Final spray cone segment angle.
	RNSL		Number of spray cone rays.
	WFF		Fuel flow rate.
	SMD		Sauter mean diameter.
	VFUEL		Initial fuel droplet velocity.
	RFUEL		Radius of fuel nozzle. (Skip Set 29 if NFNZ=0)
30	IUINJ	8(I2,8X)	Skip Sets 30-35, if NUINJ=0. I node location of cooling slots
31	JUINJ	8(I2,8X)	J node location of cooling slots.
32	UINJ	8E10.4	Cooling slot axial velocity.
33	WUINJ	8E10.4	Cooling slot tangential velocity.

Card Set	Variable	Format	Description
34	AUINJ	8E10.4	Cooling slot mass flow rate.
35	TUINJ	8E10.4	Cooling slot temperature.
			Skip Sets 36-43, if NVINJ=0.
36	IVINJ	8(I2,8X)	I node location of radial injection.
37	JVINJ	8(I2,8X)	J node location of radial injection
38	KVINJ	8(I2,8X)	K node location of radial injection.
39	VINJ	8E10.4	Radial injection velocity.
40	EVINJ	8E10.4	Radial injection turbulent kinetic energy.
41	DVINJ	8E10.4	Radial injection turbulence length scale.
42	AVINJ	8E10.4	Radial injection mass flow rate.
43	TVINJ	8E10.4	Radial injection temperature.
44	NSOOT	8(I2,8X)	=0, SOOT calculations not performed; =1, SOOT calculations performed.
	ISOOT		soot calculation started after ERROR falls to SSOOT or after ISOOT number of iterations.
	MPART		Number of soot particle sizes.
			Sip Sets 45-48 if NSOOT=0.
45	SSOOT	8E10.4	See ISOOT.
	AO		Constant a_0 in soot nuclei formation rate, equation (6).
	ARCONN		Activation energy divided by gas constant in soot nucleus formation rate, equation (6).
	AAA		Constant a in soot formation rate, equation (8).
	BBB		Constant b in soot formation rate, equation (8).

Card Set	Variable	Format	Description
	FMG		Constant (f-g) in soot nucleus formation rate, equation (7).
	GO		Constant g_0 in soot nucleus formation rate, equation (7).
	RHOP		Particle density.
46	PREXPS	8E10.4	Pre-exponent in soot oxidation rate, equation (11).
	ARCONS		Activation energy divided by gas constant in soot oxidation rate, equation (11).
	ALPHA		Temperature exponent in soot oxidation rate, equation (11).
	AAS		Exponent on fuel concentration in soot oxidation rate, equation (11).
	BBS		Exponent on oxygen concentration in soot oxidation rate, equation (11).
	DHR		Heat of fuel combustion reaction.
	CINCP		Incipient carbon/oxygen ratio for soot formation.
	TINCP		soot calculation bypassed if temperature \leq TINCP.
47	DPART	8E10.4	soot particle diameters (in microns).
48	FRACP	8E10.4	Relative rates of formation of soot particle sizes.
49	IRAD SRAD	I2,8X, E10.4	Radiation calculation started after ERROR falls to SRAD or after IRAD number of iterations. (Skip if ITRAD=1).
50	NNOX	3(I2,8X),	=0 NO _x calculations not performed; =1 NO _x calculations performed.
	INOX	2E10.4	NO _x calculations started after ERROR falls to SNOX or after INOX number of iterations.
	ITNOX		Number of iterations of NO _x solution at final iteration of flow solution.
	SNOX		See INOX.
	TNOX		NO _x calculation bypassed if temperature \leq TNOX.

After these 50 card sets, the input to the chemical kinetics program CREK must be provided. This is described below in Tables B-1, B-2 and B-3.

TABLE B-1. ELEMENTS INPUT CARDS.

Order	Contents	Format	Card Columns
First	ELEMENTS	3A4	1 to 8
Any	One card for each distinct element present in the chemical system. Each card contains: 1) Atomic symbol of element-- must agree with that used in THERMØ data. 2) Atomic weight of the element 3) Values of oxidation state of the element (positive, negative or zero).	A2 F10.6 F10.6	1 to 2 10 to 19 20 to 29
Last	Blank Card	--	--

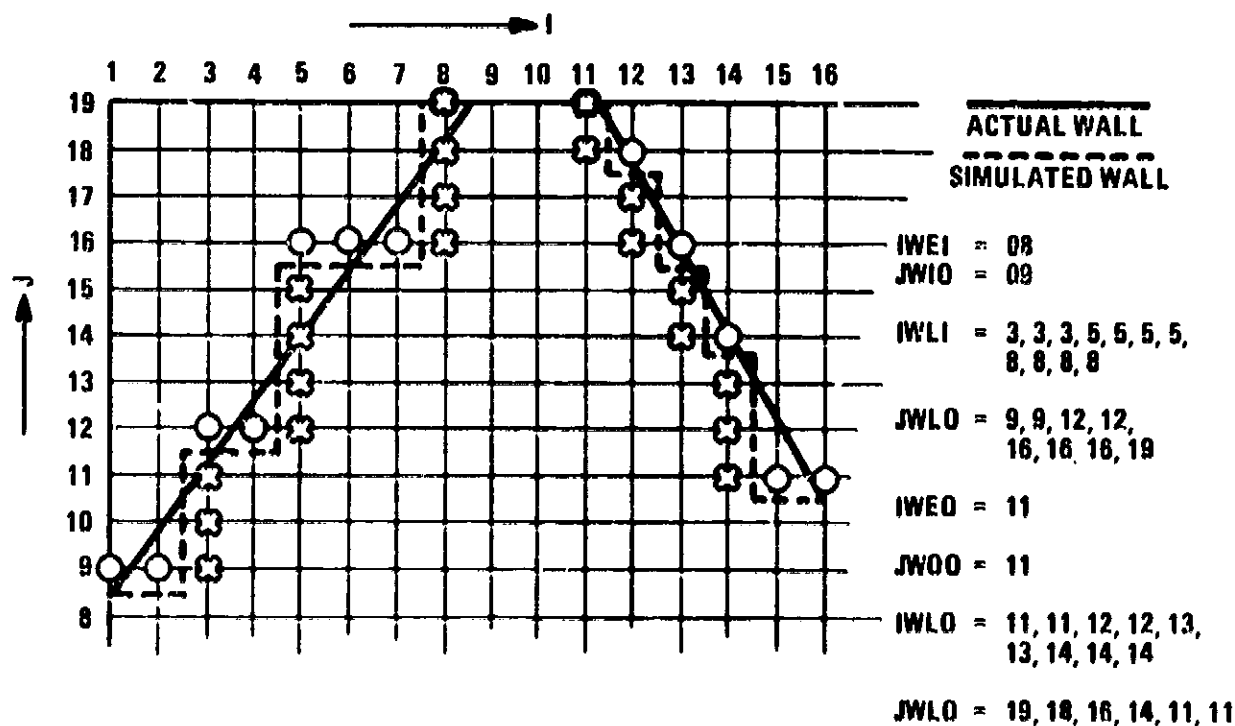


Figure B-1. Definitions of Inclined Wall Indices.

TABLE B-2. THERMØ INPUT CARDS.

Order	Contents	Format	Card Columns
First	THERMØ	3A4	1 to 6
Any	Sets of four cards <u>in sequence</u> for each species in the chemical system. The card formats for each set are, in order:		
First in set	1) Molecular symbol or name of species	3A4	1 to 12
	2) Date	2A3	19 to 24
	3) Atomic Symbols and formula	4(A2,F3.0)	25 to 44
	4) Phase (gas only, letter G)	A1	45
	5) Temperature range, deg K	2F10.3	46 to 65
	6) Integer 1	I15	80
Second in set	1) Coefficients (z_i , $i=1,5$) for upper temperature range. See Note A.	5E15.8	1 to 75
	2) Integer 2	I5	80
Third in set	1) Coefficients z_6 and z_7 for upper temperature range, and z_3 for lower. See Note A.	5E15.8	1 to 75
	2) Integer 3	I5	80
Fourth in set	1) Coefficients (z_i , $i=4,7$) for low temperature interval. See Note A.	4E15.8	1 to 60
	2) Integer 4	I20	80
Last	Blank Card	--	--

Note A: The coefficients (z_i , $i=1,7$) are those which appear in the polynomial expression for the constant pressure specific heat.

TABLE B-3. MECHANISM INPUT CARDS.

Order	Contents	Format	Card Columns
First	MECHANISM	3A4	1 to 9
Any	One card for each distinct forward (or optionally, reverse) reaction step in the mechanism specified. Each card contains:		
	1) Molecular symbols of up to three reactant species. See Note A.	3(2A4)	1 to 24
	2) Molecular symbols of up to three product species. See Note A.	3(2A4)	25 to 48
	3) Exponent B_j . See Notes B and E.	F8.3	49 to 56
	4) Exponent N_j . See Note B	F8.3	57 to 64
	5) Activation temperature T_j , deg K. See Notes B and E.	F8.3	65 to 72
	6) Options:		
	a) for forward reactions, date or comments, etc.	2A4	73 to 80
	b) for reverse reactions, REVERSE. See Note C.	2A4	73 to 79
	c) for global oxidative pyrolysis of hydrocarbon fuels, GLOBAL. See Note D.	2A4	73 to 78
	d) for rate data in cgs units, CGS. See Note E.	--	--
		--	--
Last	Blank Card		

NOTES:

- A. Symbols must be identical to those used in THERMO data cards.
 B. As used in modified Arrhenius expression

$$k_j = 10^{B_j} T_j^{N_j} \exp(-T_j/T), \text{ with units}$$

$\text{m}^3 \text{ kg-mole}^{-1} \text{ s}^{-1}$ for bimolecular reactions, and
 $\text{m}^6 \text{ kg-mole}^{-2} \text{ s}^{-1}$ for termolecular reactions.

- C. If REVERSE is specified, Columns 1 to 48 are ignored. Card with reverse rate data must therefore follow immediately the card with data for the associated forward reaction, and must be in same units.

TABLE B-3. MECHANISM INPUT CARDS (Contd.).

- D. All GLOBAL cards must precede other cards in MECHANISM data deck.
- E. If CGS is punched in Columns 73-75, B_j must correspond to $\text{cm}^3 \text{gmol}^{-1} \text{s}^{-1}$ or $\text{cm}^6 \text{gmol}^{-2} \text{s}^{-1}$, and T_j must be the activation energy, kcal/gmol.

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APPENDIX C

LIST OF FORTRAN VARIABLES

In this appendix a description of the Fortran variables is provided. Table C-1 contains the variables in the 3-D Combustor Program and Table C-2 contains the variables in the chemical kinetics program CREK.

TABLE C-1
LIST OF FORTRAN VARIABLES IN 3-D COMBUSTOR PROGRAM

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
A	STRAD	COEFFICIENT IN TONA SOLUTION.
AAA	AUX,MAIN	CONSTANT IN SOOT FORMATION (SEE INPUT).
AAS	AUX,MAIN	EXPONENT ON FUEL CONCENTRATION IN SOOT OXIDATION RATE (SEE INPUT).
AA1	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
AA2	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
AA3	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
AA4	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
ABSOR	MAIN INIT AUXRAD	ABSORPTION COEFFICIENT (IF ITRAD=2).
ABSP	INIT AUX AUXRAD	ARRAY TO STORE ABSORPTION COEFFICIENT.
ALDEF	AUX,DATA	COEFFICIENTS TO LIMIT TEMPERATURE TO ACCOUNT FOR DISSOCIATION.
ACOND	SPRAY	COEFFICIENT IN THERMAL CONDUCTIVITY CALCULATION.
AEXP1	INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME (=AA1).
AEXP2	INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME (=AA2).
AEXP3	INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME (=AA3).
AEXP4	INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME (=AA4).
AFSW	MAIN INIT	AIR+FUEL FLOW THROUGH DOME INLET.

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TABLE C-1 (CONTD.)

FORTTRAN	SUBROUTINE	DEFINITION
VARIABLE	WHERE	
	DEFINED OR	
	USED OFTEN	

AK	DATA ALLMOD	VON KARMAN CONSTANT.
AKA,AKB	AUX	RATE CONSTANTS IN SOOT OXIDATION EXPRESSION.
AKFAC	MAIN INIT ALLMOD	INTERNALLY DEFINED TURBULENT KINETIC ENERGIES ARE AKFAC TIMES THE APPROPRIATE VELOCITY SQUARED.
AKK,AKT	AUX	RATE CONSTANTS IN SOOT OXIDATION EXPRESSION.
AKZ	AUX	RATE CONSTANT IN SOOT OXIDATION EXPRESSION.
AL	INIT	TURBULENCE LENGTH SCALE.
ALFA	MAIN SPRAY	NOZZLE CONE ANGLE.
ALFAC	MAIN INIT ALLMOD	INTERNALLY DEFINED TURBULENT LENGTH SCALES ARE ALFAC TIMES THE APPROPRIATE DISTANCE.
ALIN	INIT	INLET TURBULENCE LENGTH SCALE.
ALNGHT	INIT	LENGTH OF COMBUSTOR.
ALPHA	AUX,MAIN	TEMPERATURE EXPONENT IN SOOT OXIDATION RATE (SEE INPUT).
ALPHAS	AUXRAD	ABSORPTION COEFFICIENT.
ALX,ALXM	STRIDE	CONVECTION FLUX IN X DIRECTION.
ALXP,ALX1	STRIDE	CONVECTION FLUX IN X DIRECTION.
ALY,ALYM	STRIDE	CONVECTION FLUX IN Y DIRECTION.
ALYP,ALY1	STRIDE	CONVECTION FLUX IN Y DIRECTION.
ALZ,ALZM	STRIDE	CONVECTION FLUX IN Z DIRECTION.
ALZP,ALZ1	STRIDE	CONVECTION FLUX IN Z DIRECTION.
AMASS	INIT	TOTAL AIR FLOW RATE.
AMT	SPRAY	FUEL EVAPORATION RATE FOR ONE TIME STEP.
AMU	MAIN AUX ALLMOD	LAMINAR VISCOSITY (SEE INPUT).

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TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
AND	AUX	SOOT NUCLEUS FORMATION RATE AT MEAN TEMPERATURE.
ANDD	AUX	SOOT NUCLEUS FORMATION RATE IN FLUID SURROUNDING FINE STRUCTURES.
ANDSTR	AUX	SOOT NUCLEUS FORMATION RATE IN FINE STRUCTURES.
ANUC	ALL	SOOT NUCLEUS CONCENTRATION.
AO	AUX,MAIN	CONSTANT IN SOOT NUCLEUS FORMATION RATE (SEE INPUT).
AP	SOLVE	COEFFICIENT IN TDMA SOLUTION.
APP	SOLVE	COEFFICIENT IN CYCLIC TDMA SOLUTION.
ARCONN	AUX,MAIN	ACTIVATION ENERGY DIVIDED BY GAS CONSTANT IN SOOT NUCLEUS FORMATION RATE (SEE INPUT).
ARCONS	AUX,MAIN	ACTIVATION ENERGY DIVIDED BY GAS CONSTANT IN SOOT OXIDATION RATE (SEE INPUT).
ARCON1	AUX,MAIN INIT	ACTIVATION ENERGY IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARCON2	AUX,MAIN INIT	ACTIVATION ENERGY IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARCON3	AUX,MAIN INIT	ACTIVATION ENERGY IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARCON4	AUX,MAIN INIT	ACTIVATION ENERGY IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARFA	ALLMOD STRIDE	AREA OF CONTROL VOLUME SURFACE.
AREAT	AUX	SOOT PARTICLE SURFACE AREA.
ARG	AUX	TEMPORARY USAGE.
ARG	SPRAY	SQUARE OF DROPLET DIAMETER.
ARRHEN	AUX	ARRHENIUS REACTION RATE.
AS	SPRAY	DROPLET SURFACE AREA.
ASH	ALLMOD	ABSOLUTE OF CONTINUITY ERROR.
ASUR	CRFK	SEE TABLE C-2.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ASW	INIT	FLOW RATE OF AIR THROUGH DOME INLET.
ASWRLR	INIT	DOME INLET AREA.
AT	SPRAY	QUANTITY USED IN THERMAL CONDUCTIVITY CALCULATION.
AUINJ	MAIN ALLMOD	MASS FLOW RATE THROUGH FILM COOLING SLOT.
AVINJ	MAIN ALLMOD	MASS FLOW RATE THROUGH DILUTION HOLES.
AXM	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X- DIRECTION.
AXMK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X- DIRECTION, USED IN CYCLIC TDMA.
AXP	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X+ DIRECTION.
AXPK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X+ DIRECTION, USED IN CYCLIC TDMA.
AYM	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y- DIRECTION.
AYMK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y- DIRECTION, USED IN CYCLIC TDMA.
AYP	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y+ DIRECTION.
AYPK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y+ DIRECTION, USED IN CYCLIC TDMA.
AZM	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z- DIRECTION.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
AZMK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z- DIRECTION, USED IN CYCLIC TDMA.
AZP	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z+ DIRECTION.
AZPK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z+ DIRECTION, USED IN CYCLIC TDMA.
A1-A6	AUX	TEMPORARY USAGE.
A4	INIT	TEMPORARY USAGE OF FLOW AREA.
B	STRAD	COEFFICIENT IN TDMA SOLUTION.
BBB	AUX,MAIN	CONSTANT IN SOOT FORMATION (SEE INPUT).
BRS	AUX,MAIN INIT	EXPONENT ON O ₂ CONCENTRATION IN SOOT OXIDATION RATE (SEE INPUT).
BB1	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
BB2	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
BB3	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
BB4	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
RCOND	SPRAY	COEFFICIENT IN THERMAL CONDUCTIVITY CALCULATION.
BEE	SPRAY	DRIVING FORCE FOR MASS TRANSFER.
BETA	MAIN SPRAY	NOZZLE BACK ANGLE.
BEXP1	INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME (=BB1).
BEXP2	INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME (=BB2).
BEXP3	INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME (=BB3).

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TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
BEXP4	INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME (=BR4).
BK	SOLVE	TEMPORARY USAGE.
BP	SOLVE	COEFFICIENT IN TDMA SOLUTION.
BPP	SOLVE	COEFFICIENT IN CYCLIC TDMA SOLUTION.
BT	SPRAY	QUANTITY USED IN THERMAL CONDUCTIVITY CALCULATION.
CANG	MAIN	CONSTANT TO CONVERT UNITS ON ANGLES.
CARB	AUX	MASS FRACTION OF ELEMENTAL CARBON.
CC1	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
CC2	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
CC3	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
CC4	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
CD	AUX ALLMOD	CONSTANT IN TURBULENCE MODEL.
CDS,CD1	SPRAY	DROPLET DRAG COEFFICIENT.
CERU1	INIT	EDDY-BREAK-UP CONSTANT FOR FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
CERU2	INIT	EDDY-BREAK-UP CONSTANT FOR SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
CERU3	INIT	EDDY-BREAK-UP CONSTANT FOR THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
CERU4	INIT	EDDY-BREAK-UP CONSTANT FOR FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
CENER	MAIN	CONSTANTS TO CONVERT UNITS ON ENERGY.
CEXP1	AUX,INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME (=CC1).

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
CEXP2	AUX,INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME (=CC2).
CEXP3	AUX,INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME (=CC3).
CEXP4	AUX,INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME (=CC4).
CFR	ALLMOD AUX INIT	SKIN FRICTION COEFFICIENT.
CINCP	AUX,MAIN	INCIPENT CARBON/OXYGEN RATIO FOR SOOT FORMATION.
CK	SOLVE	TEMPORARY USAGE.
CLEND	MAIN	CONSTANTS TO CONVERT UNITS ON LENGTHS.
CLENV	MAIN	CONSTANTS TO CONVERT UNITS ON VELOCITIES.
CMASS	MAIN	CONSTANTS TO CONVERT UNITS ON MASS.
CND	OUTPUT	NOX EMISSIONS INDEX.
COND1	SPRAY	THERMAL CONDUCTIVITY OF FUEL VAPORS.
CONS	SPRAY	TEMPORARY USAGE.
CONS2	AUX	TEMPORARY USAGE.
CON2	SPRAY	FRACTION OF FUEL EVAPORATED.
COSA	SPRAY	COSINE OF HALF THE NOZZLE CONE ANGLE.
COSR	SPRAY	COSINE OF NOZZLE BACK ANGLE.
COSD	SPRAY	COSINE OF NOZZLE DOWN ANGLE.
COST	SPRAY	COSINE OF CURRENT SPRAY CONE SEGMENT ANGLE.
CP	AUX ALLMOD	CONSTANT PRESSURE SPECIFIC HEAT.
CPI	INIT AUX	CONSTANT PRESSURE SPECIFIC HEAT.
CPLF	SPRAY	SPECIFIC HEAT OF LIQUID DROPLET.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
CPR	AUX	CONSTANT PRESSURE SPECIFIC HEAT.
CRESS	MAIN	CONSTANTS TO CONVERT UNITS ON PRESSURE.
CPSUM	ALLMOD AUX	CONSTANT PRESSURE SPECIFIC HEAT OF GAS MIXTURE.
CP1	SPRAY	SPECIFIC HEAT.
CR1	AUX,MAIN	EDDY-BREAK-UP CONSTANT IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME (=CERU1).
CR2	AUX,MAIN	EDDY-BREAK-UP CONSTANT IN SECOND STEP OF OF HYDROCARBON OXIDATION SCHEME (=CERU2).
CR3	AUX,MAIN	EDDY-BREAK-UP CONSTANT IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME (=CERU3).
CR4	AUX,MAIN	EDDY-BREAK-UP CONSTANT IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME (=CERU4).
CSMO	OUTPUT	SMOKE EMISSIONS INDEX.
CTEMP	MAIN	CONSTANT TO CONVERT UNITS ON TEMPERATURE.
CX	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE/DIFFUSIVE FLUX IN X DIRECTION.
CXU,CXUP	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE FLUX IN X DIRECTION.
CXX	INIT AUX MAIN	NUMBER OF CARBON ATOMS IN THE FUEL.
CY	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE/DIFFUSIVE FLUX IN Y DIRECTION.
CYP		NOT USED.
CYU,CYUP	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE FLUX IN Y DIRECTION.
CZ	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE/DIFFUSIVE FLUX IN Z DIRECTION.
CZP		NOT USED.
CZU,CZUP	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE FLUX IN Z DIRECTION.
CA	AUX,MAIN	CONSTANT IN TURBULENCE MODEL.

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TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
C2	AUX,MAIN	CONSTANT IN TURBULENCE MODEL.
DANG	SPRAY	DELTA(ANGLE).
DELTA	SPRAY MAIN	FUEL NOZZLE DOWN ANGLE.
DELTAT	AUX	TEMPERATURE RISE.
DEN	AUX,MAIN	DENSITY (SEE INPUT).
DENOM	SOLVE	TEMPORARY USAGE.
DENST	AUX	DENSITY.
DENSTY	STRIDE	DENSITY.
DEVAP	SPRAY	FRACTION OF FUEL EVAPORATED IN ONE TIME STEP.
DFAC	MAIN STRIDE	QUANTITY USED TO GRADUALLY INTRODUCE 2 DIRECTION DIFFUSION.
DFTW	TSOLVE	DIFFERENTIAL OF HEAT TRANSFER W.R.T. TEMPERATURE.
DHR	AUX,MAIN	HEAT OF FUEL COMBUSTION REACTION.
DIA	SPRAY	INSTANTANEOUS DROPLET DIAMETER.
DIA0	SPRAY	INITIAL DROPLET DIAMETER.
DIST	ALLMOD AUX STRIDE	INTERNOAL DISTANCE.
DIVG	STRIDE ALLMOD	MASS IMBALANCE AT A CONTROL VOLUME.
DK	SOLVE	TEMPORARY USAGE.
DLIM	SPRAY	CONSTANT TO LIMIT TIME STEP.
DM	SPRAY	DROPLET MASS.
DMDOT	OUTPUT	MASS FLOW RATE.
DP	SOLVE	COEFFICIENT IN CYCLIC TONA SOLUTION.
DPART	AUX,MAIN	SOOT PARTICLE DIAMETERS.

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TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
DQCH	TSOLVE	HEAT TRANSFER COEFFICIENT.
DQRH	TSOLVE	DIFFERENTIAL OF RADIATION HEAT TRANSFER W.R.T. TEMPERATURE.
DRHODP	STPIDE	PARTIAL DERIVATIVE OF DENSITY W.R.T. PRESSURE.
DSNCO	AUX	TEMPORARY USAGE IN CO SOURCE TERM.
DSOFU	AUX	TEMPORARY USAGE IN FUEL SOURCE TERM.
DSOH	AUX	TEMPORARY USAGE IN ENTHALPY SOURCE TERM.
DSOOT	OUTPUT	TEMPORARY USAGE.
DSOSP	AUX	TEMPORARY USAGE IN C ₂ H ₂ -2 AND H ₂ SOURCE TERMS.
DSND	SPRAY	RATIO OF DROPLET DIAMETER TO SMD.
DT	STRIDE	TIME INCREMENT.
DTF	SPRAY	TEMPERATURE RISE OF DROPLET.
DTHTA	SPRAY	DIFFERENCE BETWEEN INITIAL AND FINAL SPRAY CONE SEGMENT ANGLES.
DTI	SPRAY	LIMIT ON TIME STEP TO AVOID NUMERICAL INSTABILITY.
DTI1-7	SPRAY	LIMITS ON TIME STEP TO AVOID NUMERICAL INSTABILITY.
DU	STRIDE SOLVE AUX	PRESSURE-VELOCITY COEFFICIENT FOR U-VELOCITY.
DUOXM	AUX	PARTIAL DERIVATIVE OF U W.R.T. X AT I LOCATION.
DUOXF	AUX	PARTIAL DERIVATIVE OF U W.R.T. X AT I+1 LOCATION.
DUOYM	AUX	PARTIAL DERIVATIVE OF U W.R.T. Y AT I LOCATION.
DUOYP	AUX	PARTIAL DERIVATIVE OF U W.R.T. Y AT I+1 LOCATION.
DUOZM	AUX	PARTIAL DERIVATIVE OF U W.R.T. Z AT I LOCATION.
DUOZF	AUX	PARTIAL DERIVATIVE OF U W.R.T. Z AT I+1 LOCATION.
DUIOXJ	AUX	PARTIAL DERIVATIVE OF UI W.R.T. XJ.
DV	STRIDE SOLVE AUX	PRESSURE-VELOCITY COEFFICIENT FOR V-VELOCITY.

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TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
DVDXM	AUX	PARTIAL DERIVATIVE OF V W.R.T. X AT J LOCATION.
DVDXP	AUX	PARTIAL DERIVATIVE OF V W.R.T. X AT J+1 LOCATION.
DVDY	AUX	VELOCITY GRADIENT NEAR A WALL.
DVDYM	AUX	PARTIAL DERIVATIVE OF V W.R.T. Y AT J LOCATION.
DVDYP	AUX	PARTIAL DERIVATIVE OF V W.R.T. Y AT J+1 LOCATION.
DVDZM	AUX	PARTIAL DERIVATIVE OF V W.R.T. Z AT J LOCATION.
DVDZP	AUX	PARTIAL DERIVATIVE OF V W.R.T. Z AT J+1 LOCATION.
DVINJ	INIT PAIN	RADIAL INJECTION TURBULENCE LENGTH SCALE.
DW	STRIDE SOLVE AUX ALLMOD	PRESSURE-VELOCITY COEFFICIENT FOR W-VELOCITY.
DWDXM	AUX	PARTIAL DERIVATIVE OF W W.R.T. X AT K LOCATION.
DWDXP	AUX	PARTIAL DERIVATIVE OF W W.R.T. X AT K+1 LOCATION.
DWDYM	AUX	PARTIAL DERIVATIVE OF W W.R.T. Y AT K LOCATION.
DWDYP	AUX	PARTIAL DERIVATIVE OF W W.R.T. Y AT K+1 LOCATION.
DWDZM	AUX	PARTIAL DERIVATIVE OF W W.R.T. Z AT K LOCATION.
DWDZP	AUX	PARTIAL DERIVATIVE OF W W.R.T. Z AT K+1 LOCATION.
DX	AUX	INTERNODAL DISTANCE IN X DIRECTION.
DX	SPRAY	DISTANCE TRAVELED BY DROPLET IN X DIRECTION.
DY	INIT AUX	INTERNODAL DISTANCE IN Y DIRECTION.
DY	SPRAY	DISTANCE TRAVELED BY DROPLET IN Y DIRECTION.
DZ	AUX INIT	INTERNODAL DISTANCE IN Z DIRECTION.
DZ	SPRAY	DISTANCE TRAVELED BY DROPLET IN Z DIRECTION.
E	ALLMOD DATA	CONSTANT E IN LOG-LAW OF THE WALL.

TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
EDK	STRIDE AUX	DISSIPATION DIVIDED BY TURBULENCE ENERGY.
EDK1J	STRIDE	DISSIPATION DIVIDED BY TURBULENCE ENERGY AT NODE I,J,K.
EDK2	AUX	DISSIPATION DIVIDED BY TURBULENCE ENERGY SQUARED.
EE	SPRAY	CONSTANT IN DROPLET BOILING POINT CALCULATION.
EMDOT	AUX	RATE OF MASS TRANSFER BETWEEN FINE STRUCTURES AND SURROUNDING FLUID.
EMDOTR	AUX	TEMPORARY USAGE.
EMI	INIT AUX TSOLVE ALLMOD	$\pm EMISW / (2.0 - EMISW)$.
EMISIN	INIT	INLET EMISSIVITY.
EMISR	INIT ALLMOD	GAS EMISSIVITY.
EMISW	ALLMOD INIT	WALL EMISSIVITY.
EMIN	AUX	TEMPORARY USAGE.
EMP	AUX	MASS OF SOOT PARTICLE.
EMPR	AUX	MASS FRACTION OF PRODUCTS.
EMV	STRIDE	TOTAL CONVECTIVE AND DIFFUSIVE MASS INFLOW INTO A FINITE-DIFFERENCE CELL, SEE TABLE C-2.
ENM	AUX	MEAN SOOT PARTICLE CONCENTRATION.
ENND	AUX	SOOT PARTICLE CONCENTRATION IN FLUID SURROUNDING FINE STRUCTURES.
ENNRH1	AUX	ENM DIVIDED BY GAS DENSITY.
ENNSTP	AUX	SOOT PARTICLE CONCENTRATION IN FINE STRUCTURES.
END	AUX	SOOT NUCLEUS CONCENTRATION IN FLUID SURROUNDING FINE STRUCTURES.

TABLE C-1 (CONTD.)

FORTRAN	SUBROUTINE	DEFINITION
VARIABLE	WHERE	
	DEFINED OR	
	USED OFTEN	

ENRHO	AUX	MEAN SOOT NUCLEUS CONCENTRATION DIVIDED BY GAS DENSITY.
ENSTP	AUX	SOOT NUCLEUS CONCENTRATION IN FINE STRUCTURES.
ENSTR1	AUX	TEMPORARY USAGE.
ENSTR2	AUX	TEMPORARY USAGE.
EP	SOLVE	COEFFICIENT IN CYCLIC TOMA SOLUTION.
ER	CRK	EQUIVALENCE RATIO, SEE TABLE C-2.
ERROR	MAIN	PROGRAM WILL TERMINATE IF TOTAL ERROR IN MASS BECOMES LESS THAN THIS VALUE.
ER1	INIT	ACTIVATION ENERGY FOR THE FIRST STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON1).
ER2	INIT	ACTIVATION ENERGY FOR THE SECOND STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON2).
ER3	INIT	ACTIVATION ENERGY FOR THE THIRD STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON3).
ER4	INIT	ACTIVATION ENERGY FOR THE FOURTH STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON4).
ET	SPRAY	VARIABLE IN DROPLET BOILING POINT CALCULATION.
EVAP	SPRAY ALLMOD STRIDE	EVAPORATION RATE OF LIQUID FUEL.
EVAPI-W	SPRAY	INTERPHASE MOMENTUM TRANSFER IN X, Y, Z DIRECTIONS.
EVINJ	INIT MAIN	RADIAL INJECTION TURBULENCE ENERGY.
EVSU	SPRAY ALLMOD	ARRAY USED TO STORE INTERPHASE MOMENTUM TRANSFER.
F	ALL	ARRAY USED TO STORE DEPENDENT VARIABLES.
FAC	SPRAY	TEMPORARY USAGE.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
FACP	AUXRAD	TEMPORARY USAGE.
FAV	AUX	AVERAGE RADIATION FLUX.
FCH	ALL	INTERMEDIATE HYDROCARBON CONCENTRATION.
FOFU		NOT USED.
FEND	SOLVE	QUANTITY USED IN CYCLIC TDMA.
FEVAP	SPRAY	FRACTION OF FUEL EVAPORATED.
FEXIT	INIT	UNBURNT FUEL MASS FRACTION.
FH2	ALL	HYDROGEN MASS FRACTION.
FK	INIT	INLET TURBULENCE KINETIC ENERGY.
FKFU		NOT USED.
FLO	INIT	FLOW RATE AT EACH AXIAL STATION.
FLOW	OUTPUT	MASS FLOW RATE.
FLOWIN	INIT ALLMOD	INLET MASS FLOW RATE.
FLOWOT	ALLMOD	FLOW RATE AT EXIT PLANE.
FLPCO2	INIT AUX AUXRAD	CO2 MASS FRACTION.
FLPE	AUX AUXRAD	EMISSIVE POWER.
FLPH2O	INIT AUX AUXRAD	H2O MASS FRACTION.
FLPN2	INIT AUX AUXRAD	N2 MASS FRACTION.
FLPOX	INIT AUX AUXRAD SPRAY	O2 MASS FRACTION.

TABLE C-1 (CONTD.)

FORTRAN	SUBROUTINE	DEFINITION
VARIABLE	WHERE	
	DEFINED OR	
	USED OFTEN	

FLPTE	AUX AUXRAD	TEMPERATURE.
FLZP	SOLVE	F VALUE AT NODE Lzp.
FNA		NOT USED.
FNG	AUX,MAIN	CONSTANT IN SOOT NUCLEUS FORMATION RATE (SEE INPUT).
FMGF	AUX	TEMPORARY USAGE.
FQ	CREK	SEE TABLE C-2.
FRACP	AUX,MAIN	RELATIVE RATES OF FORMATION OF SOOT PARTICLE SIZES.
FRACT	SPRAY	CUMULATIVE MASS FRACTION OF DROPLETS IN DIFFERENT SIZE GROUPS.
FS	ALL	ARRAY USED TO STORE SPECIES MASS FRACTIONS.
FSLP	STRIDE	TEMPORARY STORAGE FOR FS(LP).
FST	INIT	STOICHIOMETRIC VALUE OF MIXTURE FRACTION.
FSTOIC	INIT AUX	STOICHIOMETRIC VALUE OF MIXTURE FRACTION.
FSW	INIT MAIN	FLOW RATE OF FUEL THROUGH DOME INLET.
FTW	TSOLVE	RADIATIVE+CONVECTIVE HEAT TRANSFER.
FUARAT	INIT	FUEL/AIR RATIO.
FUB	INIT AUX AUXRAD	MASS FRACTION OF BURNT FUEL.
FUEL	INIT	FUEL FLOW RATE AT EACH AXIAL STATION.
FUELF	INIT	MASS FRACTION OF UNBURNT FUEL.
FUELI	INIT	MIXTURE FRACTION.
FUELS	INIT	LIQUID FUEL FLOW RATE AT EACH AXIAL STATION.
FUMCO	INIT MAIN	INITIAL ESTIMATE OF CO MASS FRACTION.

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TABLE C-1 (CONTD.)

***** FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION *****
FUMSW	INIT	FUEL/AIR RATIO AT DOME INLET.
FUOX	INIT	MIXTURE FRACTION AT EACH AXIAL STATION.
FUOXSW	INIT	MIXTURE FRACTION AT DOME INLET.
FUT	STRIDE	MIXTURE FRACTION.
FUTOT	INIT	TOTAL FUEL FLOW RATE.
FX	SPRAY	DRAW FORCE ON DROPLET IN X DIRECTION.
FXM	ALL	INTERPOLATION FACTOR FOR X- DIRECTION NODAL DISTANCES.
FXP	ALL	INTERPOLATION FACTOR FOR X+ DIRECTION NODAL DISTANCES.
FY	SPRAY	DRAW FORCE ON DROPLET IN Y DIRECTION.
FYM	ALL	INTERPOLATION FACTOR FOR Y- DIRECTION NODAL DISTANCES.
FYP	ALL	INTERPOLATION FACTOR FOR Y+ DIRECTION NODAL DISTANCES.
FZ	SPRAY	DRAW FORCE ON DROPLET IN Z DIRECTION.
FZM	ALL	INTERPOLATION FACTOR FOR Z- DIRECTION NODAL DISTANCES.
FZP	ALL	INTERPOLATION FACTOR FOR Z+ DIRECTION NODAL DISTANCES.
GAM	ALL	DIFFUSION COEFFICIENT.
GAMAS	AUX	MASS FRACTION OF FLUID IN FINE STRUCTURES.
GAMDDL	ALLMOD	TEMPORARY USAGE.
GAML P	AUX STRIDE	DIFFUSION COEFFICIENT AT NODE LP.
GAMLXM	AUX	DIFFUSION COEFFICIENT AT NODE LXM.
GAMLYM	AUX	DIFFUSION COEFFICIENT AT NODE LYM.
GAML7M	AUX	DIFFUSION COEFFICIENT AT NODE L7M.
GAMM	AUX	AVERAGE DIFFUSION COEFFICIENT.
GAMP	AUX	AVERAGE DIFFUSION COEFFICIENT.
GAMPT2	AUX	AVERAGE DIFFUSION COEFFICIENT.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
GASCON	AUX,MAIN	UNIVERSAL GAS CONSTANT DIVIDED BY MOLECULAR WEIGHT OF AIR.
GFNR	AUX	GENERATION RATE OF TURBULENCE ENERGY.
GO	AUX,MAIN	CONSTANT IN SNOT NUCLEUS FORMATION RATE (SEE INPUT).
GPSI	AUX	-GAMAS*PSI.
GPSIP	AUX	GPSI DIVIDED BY DENSITY OF FINE STRUCTURES.
H	ALL	ENTHALPY.
HCO	INIT	HEAT OF COMBUSTION OF CO.
HCRAT	INIT	TEMPORARY USAGE.
HCRFI	ALLMOD	TEMPORARY USAGE.
HEIGHT	INIT	CHANNEL HEIGHT OF COMBUSTOR.
HEVAP	SPRAY	HEAT OF VAPORIZATION OF LIQUID FUEL.
HFU	MAIN INIT	HEAT OF FORMATION OF FUEL.
HFUEL	SPRAY	HEAT OF COMBUSTION OF FUEL.
HPI	ALLMOD AUX INIT	TEMPORARY USAGE FOR ENTHALPY.
HSURC	STRIDE	MIXTURE ENTHALPY.
HSUM	AUX ALLMOD INIT STRIDE	ENTHALPY OF GAS MIXTURE.
HT	SPRAY	HEAT TRANSFER COEFFICIENT FOR DROPLET HEATUP.
HTC	ALLMOD AUX	HEAT TRANSFER COEFFICIENT.
HTCEXT		EXTERNAL HEAT TRANSFER COEFFICIENT (NOT USED).
HTCI	TSOLVE	HEAT TRANSFER COEFFICIENT.
HYY	INIT MAIN AUX	NUMBER OF HYDROGEN ATOMS IN FUEL.

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TABLE C-1 (CONTD.)

F0RTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
H1,H2	INIT	ENTHALPY(TEMPORARY USAGE).
IB	SPRAY	INDEX TO DENOTE LOCATION OF I BOUNDARY.
ICONVG	STRIDE	=0,CHEMICAL KINETICS SOLUTION NOT CONVERGED, =1,CHEMICAL KINETICS SOLUTION CONVERGED.
ICTDMA	SOLVE PAIN	NUMBER OF SWEEPS FOR EACH VARIABLE IN SOLVE (SEE INPUT).
IDCH	DATA,INIT AUX	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
IDCO	DATA,INIT AUX	INDEX FOR CO MASS FRACTION.
IDCO2	DATA,INIT AUX	INDEX FOR CO2 MASS FRACTION.
IDFU	DATA,INIT AUX SPRAY STRIDE ALLMOD	INDEX FOR FUEL MASS FRACTION.
IDH1	DATA	INDEX FOR H ATOM MASS FRACTION.
IDH2	DATA,INIT AUX	INDEX FOR H2 MASS FRACTION.
IDH2O	DATA,INIT AUX	INDEX FOR H2O MASS FRACTION.
IDK	AUX	=01 FOR RATE CONTROLLED COMBUSTION, =02 FOR MIXING CONTROLLED COMBUSTION.
IDNO	DATA	INDEX FOR NO MASS FRACTION.
IDNO2	DATA	INDEX FOR NO2 MASS FRACTION.
IDN1	DATA	INDEX FOR N ATOM MASS FRACTION.
IDN2	DATA,INIT ALLMOD AUX STRIDE	INDEX FOR N2 MASS FRACTION.
IDO	DATA	INDEX FOR O ATOM MASS FRACTION.

TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ID01	DATA	INDEX FOR O1 MASS FRACTION.
ID02	DATA, INIT ALLMOD UX STRIDE	INDEX FOR O2 MASS FRACTION.
IDW	MAIN ALLMOD STRIDE AUX	TYPE OF BOUNDARY AT J=1(SEE INPUT).
IE	ALL	ENDING VALUE OF I(LOCAL VALUE OF IMLO).
IEHD	FPRINT	ENDING VALUE OF I FOR PRINTOUT.
IG	SPRAY	DO-LOOP INDEX FOR DROPLET SIZE GROUPS.
IGAM1-2	DATA ALLMOD	INDEX TO DENOTE TYPE OF BOUNDARY CONDITION FOR A DEPENDENT VARIABLE.
IGPNT	SPRAY	INDEX FOR DIAGNOSTIC PRINTOUT.
IHCPS	WAPS	INDEX FOR CALCULATING THERMODYNAMIC PROPERTIES.
IJUMP	OUTPUT PATH	NUMBER OF ITERATIONS BETWEEN PRINTOUT.
IKIN	INIT ALLMOD AUX STRIDE	INDEX FOR BOUNDARY CONDITIONS.
IL	STRIDE	TEMPORARY USAGE.
IL	SPRAY	DO-LOOP INDEX FOR DROPLET RAYS.
ILC	CREK	SEE TABLE C-2.
ILH	CREK	SEE TABLE C-2.
ILOC	SPRAY	I INDEX FOR DROPLET LOCATION.
IMAT	CREK	SEE TABLE C-2.
IMAX	MAIN ALLMOD	I LOCATION OF MAXIMUM CONTINUITY ERROR.
INCOMP		INDEX TO DENOTE COMPRESSIBILITY(NOT USED).

TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
IND	STRIDE	INDEX USED IN RADIATION CALCULATIONS.
INDX	ALLMOD	-1 IF U VELOCITY IS NEGATIVE AT EXIT, OTHERWISE =0.
INOX	SPRAY	INDEX FOR TYPE OF BOUNDARY.
IND	SOLVE	DO-LOOP INDEX.
INDMAX	SOLVE	NUMBER OF TOMA SWEEPS.
INOX	MAIN STRIDE	INDEX TO DECIDE ON NOX CALCULATIONS(SEE SNOX).
INTAPE	MAIN	INDEX FOR INITIAL FIELD PRINTOUT(SEE INPUT).
INV	INIT STRIDE	TEMPORARY USAGE.
IOLD	SPRAY	PREVIOUS I LOCATION OF DROPLET.
IONE	FPRINT	FIRST VALUE OF I FOR PRINTOUT.
IP	STRIDE	TEMPORARY USAGE.
IPAR	MAIN STRIDE	INDEX FOR ABSOLUTE OR RELATIVE PRESSURE(SEE INPUT).
IPLAX	MAIN STRIDE	INDEX FOR PLANE OR AXISYMMETRIC FLOW(SEE INPUT).
IPRINT	FPRINT MAIN	INDEX FOR PRINTOUT OF DEPENDENT VARIABLES (SEE INPUT).
IRAD	MAIN	INDEX FOR RADIATION SOLUTION(SEE SRAD).
IREF	MAIN	I LOCATION OF REFERENCE PRESSURE LOCATION.
IPES	MAIN INIT STRIDE AUX	INDEX FOR RESTARTING SOLUTION(SEE INPUT).
IS	ALL	STARTING VALUE OF I(LOCAL VALUE OF INLI).
ISOLVE	STRIDE MAIN AUX	INDEX FOR SOLUTION OF DEPENDENT VARIABLES (SEE INPUT).

TABLE C-1 (CONTD.)

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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ISOOT	MAIN	INDEX FOR SOOT SOLUTION(SEE SSOOT).
ISP	MAIN	TEMPORARY USAGE.
ISPRAY	MAIN	NUMBER OF ITERATIONS BETWEEN SPRAY SOLUTIONS.
ISTART	FPRINT	STARTING VALUE OF I FOR PRINTOUT.
ISTEP	MAIN STRIDE AUX OUTPUT	NUMBER OF CURRENT ITERATION.
ISTOP	FPRINT	ENDING DEPENDENT VARIABLE INDEX FOR PRINTOUT.
ISTR	STRIDE	FIRST I LOCATION.
ISTRT	FPRINT	STARTING DEPENDENT VARIABLE INDEX FOR PRINTOUT.
ISTR1	SOLVE STRAD	=IS-1.
ISTUN		INDEX FOR STEADY/UNSTEADY FLOW(NOT USED).
ISUM	SOLVE	=ISTR+L.
ISUM	STRAD	=IS+IE.
ISUM1	SOLVE	=IS+IE.
ISWP	SOLVE STRIDE	INDEX USED FOR Y-TDMA SWEEP DIRECTION.
ITER	CREK	NUMBER OF CURRENT ITERATION OF CREK SOLUTION.
ITNOX	STRIDE MAIN	NUMBER OF ITERATIONS OF NOX SOLUTION AT FINAL ITERATION OF FLOW SOLUTION.
ITR	STRIDE	NUMBER OF CHEMICAL KINETICS ITERATIONS.
ITR	TSOLVE	=1 IF RADIATION IGNORED, =2 IF RADIATION CONSIDERED.
ITRAD	TSOLVE MAIN AUX	INDEX FOR RADIATION SOLUTION(SEE INPUT).
ITWALL	AUX	INDEX FOR WALL TEMPERATURE SOLUTION(SEE INPUT).
ITYPE	SPRAY	=1 FOR HEATING DROPLET, =2 FOR BOILING DROPLET.

TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
IU	MAIN	INDEX FOR TYPE OF UNITS (SEE INPUT).
IU	SPRAY	$-IUTNJ-1$.
IUINJ	ALLMOD MAIN INIT	I NODE LOCATION OF COOLING SLOTS.
IVINJ	INIT MAIN ALLMOD	I NODE LOCATION OF RADIAL INJECTION HOLES.
IWEI	MAIN	I NODE AT WHICH UPSTREAM INCLINED WALL ENDS.
IWED	MAIN	I NODE AT WHICH DOWNSTREAM INCLINED WALL STARTS.
IWLI	ALL	STARTING I NODES OF CALCULATION DOMAIN WHEN INCLINED WALL IS PRESENT.
IWLO	ALL	ENDING I NODES OF CALCULATION DOMAIN WHEN INCLINED WALL IS PRESENT.
IXY	SOLVE STRIDE	INDEX FOR DIRECTION OF TQMA SWEEPS.
JB	SPRAY	INDEX TO DENTITE LOCATION OF J BOUNDARY.
JE	ALL	LOCAL VALUE OF JWLO-1.
JJ	INIT	TEMPORARY USAGE.
JJ	SOLVE STRIDE	DO-LOOP INDEX.
JJJ	STRIDE	NUMBER OF REACTION STEPS (JJ OF CRIN, SEE TABLE C-21).
JKIN	INIT ALLMOD AUX STRIDE	INDEX FOR TYPE OF BOUNDARY.
IL	STRIDE	TEMPORARY USAGE.
JLJC	SPRAY	J LOCATION OF DROPLET.
JM	ALL	$-(J-1) \div IMAX$.
JMAX	MAIN ALLMOD	J LOCATION OF MAXIMUM CONTINUITY ERROR.

TABLE C-1 (CONTD.)

CONTINUED
FROM TABLE C-1

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
JNDX	MAIN	TEMPORARY USAGE.
JOLD	SPRAY	PREVIOUS J LOCATION OF DROPLET.
JONE	FPRINT	FIRST J VALUE FOR PRINTOUT.
JP	STRIDE	TEMPORARY USAGE.
JPLANE	AUXRAD STRAD ALLMOD	VALUE OF J (INDEX FOR Y LOCATION) WHEN SOLVING Z DIRECTION RADIATION FLUX.
JREF	MAIN	J LOCATION OF REFERENCE PRESSURE NODE.
JS	ALL	LOCAL VALUE OF JNLT+1.
JSTR	STRAD SOLVE STRIDE	STARTING J VALUE.
JSTR1	SOLVE STRAD	=JS-1.
JSUM	SOLVE	=JSTR+N.
JSUM	STRAD	=JS+JE.
JSUM	FPRINT	=JONE+MP1.
JSUM1	SOLVE	=JS+JE.
JSWP	SOLVE STRIDE	INDEX USED FOR X-TONA SWEEP DIRECTION.
JSW1	INIT,MAIN ALLMOD	J NODE AT START OF DOME INLET.
JSW2	INIT,MAIN ALLMOD	J NODE AT END OF DOME INLET.
JTRAD	MAIN	TEMPORARY USAGE.
JU	SPRAY	=JUNIJ.
JUINJ	INIT,MAIN ALLMOD	J NODE LOCATIONS OF COOLING SLOTS.
JVINJ	INIT,MAIN ALLMOD	J NODE LOCATIONS OF RADIAL INJECTION HOLES.

TABLE C-1 (CONTO.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
JWII	INIT,MAIN	J NODE AT WHICH UPSTREAM INNER INCLINED WALL STARTS.
JWIO	INIT,MAIN	J NODE AT WHICH UPSTREAM OUTER INCLINED WALL STARTS.
JWLI	ALL	STARTING J NODES OF THE CALCULATION DOMAIN AT INNER INCLINED WALL.
JWLO	ALL	ENDING J NODES OF THE CALCULATION DOMAIN AT OUTER INCLINED WALL.
JWOI	INIT,MAIN ALLMOD AUX STRIDE	J NODE AT WHICH DOWNSTREAM INNER INCLINED WALL ENDS.
JWOO	INIT,MAIN ALLMOD AUX STRIDE	J NODE AT WHICH DOWNSTREAM OUTER INCLINED WALL ENDS.
J1,J2	INIT	TEMPORARY VALUES FOR JWLI AND JWLO.
KEND	SOLVE	VALUE OF K AT LAST Z LOCATION.
KENOM1	SOLVE	=KEND-1.
KENOM2	SOLVE	=KEND-2.
KJC	SPRAY	TEMPORARY USAGE.
KJK	ALLMOD OUTPUT	TEMPORARY USAGE.
KJM	ALL	=KM(K)+JM(J).
KK	STRAD	TEMPORARY USAGE.
KLOC	SPRAY	K LOCATION OF DROPLET.
KM	ALL	=(K-1)*NJ*MK.
KMAX	MAIN ALLMOD	K LOCATION OF MAXIMUM CONTINUITY ERROR.
KNIN	SOLVE	=KSTR+1.
KOLD	SPRAY	PREVIOUS K LOCATION OF DROPLET.

TABLE C-1 (CONTO.)

GENERAL PURPOSE
OF POOL QUALITY

FORTTRAN	SUBROUTINE	DEFINITION
VARIABLE	WHERE DEFINED OR USED OFTEN	

KONF	FPRINT	FIRST K VALUE FOR PRINTOUT.
KONTRN	AUX	CONTROL INDEX =1 ON FIRST ITERATION, OTHERWISE 2.
KONTPO	STRAD	CONTROL INDEX =1,2,3 WHEN NV=LVRX,LVRY,LVRZ.
KOUNT	TSOLVE	NUMBER OF ITERATIONS ON WALL TEMPERATURE.
KREF	MAIN	K LOCATION OF REFERENCE PRESSURE NODE.
KSTR	STRIDE STRAD AUX SOLVE	FIRST K LOCATION.
KSUM	SOLVE	=KEND+KSTR-2.
KSUM	STRAD	=2+N.
KVINJ	INIT ALLNOG MAIN	K NODE LOCATION OF RADIAL INJECTION HOLE.
L	ALL	=LP1-1.
LADIAN	CREK	SEE TABLE C-2.
LASTEP	MAIN STRIDE	MAXIMUM NUMBER OF ITERATIONS.
LCONVG	CREK	SEE TABLE C-2.
LCV	STRIDE	NUMBER OF CONTROL VOLUMES IN X DIRECTION(=L-1).
LDERUG	CREK	SEE TABLE C-2.
LENER	CREK	=.FALSE., ENERGY EQUATION COMPLETELY DECOUPLED FROM SPECIES EQUATIONS AND SPECIES CONCENTRATIONS OBTAINED AT SPECIFIED TEMPERATURE, =.TRUE., COMPLETE ENERGY EQUATION IS USED.
LEQUIL	CREK	SEE TABLE C-2.
LIJ	ALL	=I+JN(I).
LIJNV	SOLVE	INDEX FOR VALUE AT K=1 PLANE IN F ARRAY.
LIJ2	STRIDE	=LIJ+KNI(2).

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION

LIK	AUXRAD STRAD	$=I+KN(K)$.
LNOP,LMPJ	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LNRG	CREK	SEE TABLE C-2.
LOMP,LPM	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LOPP	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LP	ALL	$=I+JN(J)+KN(K)$.
LPR	STRIDE	INDEX TO REFER TO Z- LOCATION.
LPC	ALL	TEMPORARY USAGE.
LPCE	SOLVE	TEMPORARY USAGE.
LPCM	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO INTERMEDIATE HYDROCARBON MASS FRACTION.
LPCH1	STRIDE	INDEX USED TO REFER TO INTERMEDIATE HYDROCARBON MASS FRACTION.
LPCO	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO CO MASS FRACTION.
LPCO1	STRIDE	INDEX USED TO REFER TO CO MASS FRACTION.
LPCSTR	SOLVE	TEMPORARY USAGE.
LPD	AUX	INDEX USED TO REFER TO DISSIPATION RATE.
LPE	STRIDE	INDEX TO REFER TO X+ LOCATION.
LPF	SOLVE STRIDE STRAD	INDEX FOR REFERING TO VALUE IN F ARRAY.
LPF	FPRINT	DO-LOOP LIMIT FOR PRINTOUT.
LPEAV	AUX STRIDE	INDEX USED TO REFER TO AVERAGE RADIATION FLUX.

TABLE C-1 (CONTD.)

ORIGINAL PUBL.
OF PCC QUALITY

***** FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	***** DEFINITION
LPFU	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO UNBURNT FUEL MASS FRACTION.
LPFUOX	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO MIXTURE FRACTION.
LPFU1	STRIDE	INDEX USED TO REFER TO UNBURNT FUEL MASS FRACTION.
LPF1	SOLVE	=LPF+ISTR1.
LPH	AUX STRIDE	INDEX USED TO REFER TO ENTHALPY.
LPHP	AUX	INDEX USED TO REFER TO ENTHALPY.
LPH2	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO H2 MASS FRACTION.
LPH21	STRIDE	INDEX USED TO REFER TO H2 MASS FRACTION.
LPK	AUX	INDEX USED TO REFER TO TURBULENCE ENERGY.
LPL	FPRINT	DO-LOOP LIMIT FOR PRINTOUT.
LPND	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LPN	ALLMOD	TEMPORARY USAGE.
LPN	STRIDE	INDEX TO REFER TO Y+ LOCATION.
LPN	AUX	INDEX USED TO REFER TO SOOT NUCLEUS CONCENTRATION.
LPNP1	ALLMOD STRIDE	TEMPORARY USAGE.
LPND,LPDP	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LPO2	STRIDE	INDEX USED TO REFER TO O2 MASS FRACTION.
LPPD	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LPRFF	STRIDE MAIN	LOCATION OF REFERENCE PRESSURE NODE.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LPRX	AUX AUXRAD STRIDE	INDEX USED TO REFER TO X DIRECTION RADIATION FLUX.
LPRY	AUX AUXRAD STRIDE	INDEX USED TO REFER TO Y DIRECTION RADIATION FLUX.
LPRZ	AUXRAD STRIDE	INDEX USED TO REFER TO Z DIRECTION RADIATION FLUX.
LPS	AUX	INDEX USED TO REFER TO SOOT CONCENTRATION.
LPS	STRIDE	INDEX TO REFER TO Y- LOCATION.
LPSTR	SOLVE	TEMPORARY USAGE.
LPS1	AUX	INDEX USED TO REFER TO SOOT CONCENTRATION OF SIZE 1.
LPS2	AUX	INDEX USED TO REFER TO SOOT CONCENTRATION OF SIZE 2.
LPT	STRIDE	INDEX TO REFER TO Z+ LOCATION.
LPTE	AUX AUXRAD SPRAY	INDEX USED TO REFER TO TEMPERATURE.
LPW	ALLMOD STRIDE	INDEX TO REFER TO X- LOCATION.
LP1	ALL	NUMBER OF GRID NODES IN AXIAL (X) DIRECTION.
LP11	STRIDE	TEMPORARY USAGE.
LP2	ALLMOD STRIDE	TEMPORARY USAGE.
LREACT	CREK	SEE TABLE C-2.
LVCH	DATA ALLMOD AUX STRIDE	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
LVCH1	DATA STRIDE	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
LVCO	DATA ALLMOD AUX STRIDE	INDEX FOR CO MASS FRACTION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LVC01	DATA STRIDE	INDEX FOR CO MASS FRACTION.
LVC02	DATA	INDEX FOR CO2 MASS FRACTION.
LVO	DATA ALLMOD AUX	INDEX FOR DISSIPATION RATE OF TURBULENCE.
LVFU	DATA ALLMOD AUX STRIDE	INDEX FOR UNBURNT FUEL MASS FRACTION.
LVFUOX	DATA ALLMOD AUX STRIDE	INDEX FOR MIXTURE FRACTION.
LVFU1	DATA STRIDE	INDEX FOR UNBURNT FUEL MASS FRACTION.
LVH	DATA ALLMOD AUX STRIDE	INDEX FOR ENTHALPY.
LVH1	DATA ALLMOD AUX STRIDE	INDEX FOR H ATOM MASS FRACTION.
LVH2	DATA ALLMOD AUX STRIDE	INDEX FOR H2 MASS FRACTION.
LVH20	DATA	INDEX FOR H2O MASS FRACTION.
LVH21	DATA STRIDE	INDEX FOR H2 MASS FRACTION.
LVK	DATA ALLMOD AUX STRIDE	INDEX FOR TURBULENCE KINETIC ENERGY.
LVN	DATA ALLMOD AUX	INDEX FOR SOOT NUCLEUS CONCENTRATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

***** FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	***** DEFINITION *****
LVNO	DATA	INDEX FOR NO MASS FRACTION.
LVNO2	DATA	INDEX FOR NO2 MASS FRACTION.
LVN1	DATA	INDEX FOR N ATOM MASS FRACTION.
LVN2	DATA	INDEX FOR N2 MASS FRACTION.
LVO	DATA	INDEX FOR O ATOM MASS FRACTION.
LVON	DATA STRIDE	INDEX FOR OH MASS FRACTION.
LV02	DATA STRIDE	INDEX FOR O2 MASS FRACTION.
LVRX	DATA ALLMOD STRIDE	INDEX FOR X DIRECTION RADIATION FLUX.
LVRY	DATA ALLMOD	INDEX FOR Y DIRECTION RADIATION FLUX.
LVZ	DATA STRIDE	INDEX FOR Z DIRECTION RADIATION FLUX.
LVS1	DATA ALLMOD AUX	INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 1.
LVS2	DATA ALLMOD AUX	INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 2.
LXM	ALL	INDEX TO REFER TO X- LOCATION.
LXMC	ALLMOD SPRAY	TEMPORARY USAGE.
LXM1	AUX STRIDE	=LXM-NI.
LXP	ALL	INDEX TO REFER TO X+ LOCATION.
LXP1	AUX STRIDE	=LXP-NI.
LYM	ALL	INDEX TO REFER TO Y- LOCATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LYMC	ALLMOD SPRAY	TEMPORARY USAGE.
LYM1	AUX	=LYM-1.
LYP	ALL	INDEX TO REFER TO Y+ LOCATION.
LYP1	AUX STRIDE	=LYP-1.
LZM	ALL	INDEX TO REFER TO Z- LOCATION.
LZMC	ALLMOD SPRAY	TEMPORARY USAGE.
LZM1	AUX	=LZM-1.
LZP	ALL	INDEX TO REFER TO Z+ LOCATION.
LZP1	AUX STRIDE	=LZP-1.
M	ALL	=MP1-1.
MAX	AUX STRIDE	LOCAL VALUE OF JWLO-1.
MCV	STRIDE	NUMBER OF CONTROL VOLUMES IN Y DIRECTION.
MIN	AUX	LOCAL VALUE OF JWLI+1.
MM1	STRIDE	SAME AS MCV.
MM1	ALLMOD	TEMPORARY USAGE.
MNDEL	AUX,MAIN	INDEX FOR TYPE OF VISCOSITY(SEE INPUT).
MNDEN	AUX,MAIN	INDEX FOR TYPE OF DENSITY(SEE INPUT).
MNDR	AUX,MAIN STRIDE	INDEX FOR TYPE OF REACTION RATE(SEE INPUT).
MPART	AUX,MAIN	NUMBER OF SOOT PARTICLE SIZES.
MP1	ALL	NUMBER OF GRID NODES IN RADIAL (Y) DIRECTION.
MW	SPRAY	ARRAY TO STORE MOLECULAR WEIGHTS OF VARIOUS FUELS.
MWCND	SPRAY	CONSTANT USED IN MOLECULAR WEIGHT CALCULATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION

MWT	SPRAY	MOLECULAR WEIGHT OF FUEL VAPORS.
M1,M2	ALLMOD	TEMPORARY USAGE.
N	ALL	=NP1-1.
NA	CREK	SEE TABLE C-2.
NCV	STRIDE	NUMBER OF CONTROL VOLUMES IN Z DIRECTION(=N-1).
NDERUG	CREK	SEE TABLE C-2.
NFNZ	SPRAY PAIN ALLMOD STRIDE INIT	INDEX FOR WHETHER LIQUID FUEL NOZZLE IS PRESENT (SEE INPUT).
NG	SPRAY	NUMBER OF DROPLET SIZE GROUPS.
NGAM	DATA STRIDE AUX	INDEX FOR DIFFUSION COEFFICIENT.
NGLOB	CREK	SEE TABLE C-2.
NGLOP	CREK	SEE TABLE C-2.
NGOTO	STRIDE SOLVE STRAD ALLMOD AUX	INDEX WHICH TAKES VALUES 1,2,3 WHEN U,V,W BEING SOLVED, OTHERWISE IT HAS A VALUE OF 4.
NI	ALL	MAXIMUM NUMBER OF NODES IN X DIRECTION.
NINJ	STRIDE	NI*NJ.
NINJNK	STRIDE	NI*NJ*NK.
NITER	STRIDE	MAXIMUM NUMBER OF CHEMICAL KINETICS ITERATIONS.
NJ	ALL	MAXIMUM NUMBER OF NODES IN Y DIRECTION.
NK	ALL	MAXIMUM NUMBER OF NODES IN Z DIRECTION.
NLM	CREK	SEE TABLE C-2.
NN	SPRAY	DO-LOOP INDEX OVER FUEL NOZZLES.

TABLE C-1 (CONTD.)

OPTIMUM VALUES
OF POOR QUALITY

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
NNOX	MAIN	INDEX FOR NOX SOLUTION(SEE INPUT).
NNV	DATA STRIDE	MAXIMUM NUMBER OF DEPENDENT VARIABLES.
NP	DATA STRIDE	INDEX FOR PRESSURE.
NP1	ALL	NUMBER OF GRID NODES IN TANGENTIAL (Z) DIRECTION.
NQ	CREK	SEE TABLE C-2.
NRHO	DATA AUX	INDEX FOR DENSITY.
NS	ALL	NUMBER OF SPECIES.
NSKIP	FPRINT	TEMPORARY STORAGE FOR IPRINT.
NSL	SPRAY MAIN	NUMBER OF SPRAY CONE RAYS.
NSL2	SPRAY	=NSL(NN).
NSM	CREK	SEE TABLE C-2.
NSOOT	MAIN	INDEX FOR SOOT SOLUTION(SEE INPUT).
NS1,NS2	ALL	TEMPORARY USAGE OF DO-LOOP LIMITS ON SPECIES CONCENTRATIONS.
NTP	OUTPUT	INDEX FOR TAPE NUMBER.
NTPT	STRIDE	=NTP1+NTP2.
NTP1	STRIDE MAIN,INIT AUX	INDEX FOR TAPE NUMBER.
NTP2	STRIDE MAIN,INIT	INDEX FOR TAPE NUMBER.
NTP3	SPRAY MAIN ALLMOD	INDEX FOR TAPE NUMBER.
NUINJ	MAIN,INIT ALLMOD	NUMBER OF COOLING SLOTS.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTTRAN	SUBROUTINE	DEFINITION
VARIABLE	WHERE	
	DEFINED OR	
	USED OFTEN	

NV	ALL	DEPENDENT VARIABLE INDEX.
NVCH	DATA, INIT	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
	ALLMOD	
	STRIDE	
	AUX	
NVCO	DATA, INIT	INDEX FOR CO MASS FRACTION.
	STRIDE	
	AUX	
NVCO2	DATA	INDEX FOR CO2 MASS FRACTION.
NVD	DATA, INIT	INDEX FOR DISSIPATION RATE OF TURBULENCE.
	AUX	
NVE		INDEX FOR EMISSIVE POWER.
NVF	ALL	INDEX FOR IDENTIFYING LOCATION IN F ARRAY.
NVFAV	DATA, INIT	INDEX FOR AVERAGE RADIATION FLUX.
	STRIDE	
	AUX	
NVFF	ALLMOD	=NVF(NV).
NVFU	DATA, INIT	INDEX FOR UNBURNT FUEL MASS FRACTION.
	ALLMOD	
	AUX	
	STRIDE	
NVFUCX	DATA, INIT	INDEX FOR MIXTURE FRACTION.
	ALLMOD	
	STRIDE	
	AUX	
NVM	DATA, INIT	INDEX FOR ENTHALPY.
	STRIDE	
	AUX	
NVHP	AUX	INDEX FOR ENTHALPY.
NVM2	DATA, INIT	INDEX FOR H2 MASS FRACTION.
	STRIDE	
	AUX	
NVM2(I)	DATA	INDEX FOR H2O MASS FRACTION.
NVINJ	MAIN	NUMBER OF RADIAL INJECTION HOLES.
	INIT	
	ALLMOD	

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
NVJM	STRAD	$= JM(J) + NVN(NVRZ),$
NVK	DATA, INIT ALLMOD AUX	INDEX FOR TURBULENCE KINETIC ENERGY.
NVKM	SOLVE STRAD FPRINT	$= KM(K) + NVN(NVF(NV)),$
NVM	ALL	$= (NV-1) * NI * NJ * NK,$
NVN	DATA, INIT AUX	INDEX FOR SOOT NUCLEUS CONCENTRATION.
NVN2	DATA	INDEX FOR N2 MASS FRACTION.
NVNX	DATA	INDEX FOR O2 MASS FRACTION.
NVRX	DATA, INIT STRIDE	INDEX FOR X DIRECTION RADIATION FLUX.
NVRV	DATA, INIT STRIDE	INDEX FOR Y DIRECTION RADIATION FLUX.
NVRZ	DATA, INIT STRIDE ALLMOD	INDEX FOR Z DIRECTION RADIATION FLUX.
NVS1	DATA, INIT AUX	INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 1.
NVS2	DATA, INIT AUX	INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 2.
NVTF	DATA, INIT AUX	INDEX FOR TEMPERATURE.
NVV	FPRINT	DO-LOOP COUNTER.
NVVV	FPRINT	FIRST DEPENDENT VARIABLE TO BE PRINTED ON A CALL TO FPRINT.
N1	CREK	SEE TABLE C-2.
N2	CREK	SEE TABLE C-2.
N3	CREK	SEE TABLE C-2.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
DGPSI	AUX	TEMPORARY USAGE.
DGPSIR	AUX	TEMPORARY USAGE.
P	ALL	PRESSURE.
PA	CREK	PRESSURE.
PATH	AUXRAD	PATH LENGTH FOR RADIATION CALCULATIONS.
PRAR	OUTPUT	TEMPORARY USAGE.
PCO2	AUXRAD	CO2 PARTIAL PRESSURE.
PEXP1	INIT	PRE-EXPONENT FACTOR IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
PEXP2	INIT	PRE-EXPONENT FACTOR IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
PEXP3	INIT	PRE-EXPONENT FACTOR IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
PEXP4	INIT	PRE-EXPONENT FACTOR IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
PHI	INIT AUX	FUEL MASS FRACTION/STOICHIOMETRIC MIXTURE FRACTION.
PH2O	AUXRAD	H2O PARTIAL PRESSURE.
PI	SPRAY	-3.14159.
PJAY	ALLMOD MAIN	PJAY FUNCTION FOR HEAT TRANSFER WALL FUNCTION.
PLAXM1	ALL	IPLAX-1.
PLPREF	STRIDE	PRESSURE AT REFERENCE PRESSURE LOCATION.
P0,P0T	SPRAY	CONSTANTS IN BOILING POINT CALCULATION.
PO2	AUX	OXYGEN PARTIAL PRESSURE.
PP	ALL	PRESSURE CORRECTION.
PPLN	CREK	SEE TABLE C-2.
PR	AUX, MAIN ALLMOD	LAMINAR PRANDTL/SCHMIDT NUMBER.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

***** FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION *****
PRFF	AUX,MAIN ALLMOD	TURBULENT PRANDTL/SCHMIDT NUMBER.
PRESS	MAIN INIT STRIDE AUX	SYSTEM PRESSURE.
PREXP5	AUX,MAIN	PRE-EXPONENT FACTOR IN SOOT OXIDATION RATE (SEE INPUT).
PREXP1	AUX,MAIN INIT	PRE-EXPONENT FACTOR IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP1).
PREXP2	AUX,MAIN INIT	PRE-EXPONENT FACTOR IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP2).
PREXP3	AUX,MAIN INIT	PRE-EXPONENT FACTOR IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP3).
PREXP4	AUX,MAIN INIT	PRE-EXPONENT FACTOR IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP4).
PRRAT	MAIN	RATIO OF LAMINAR AND TURBULENT PRANDTL NUMBERS.
PR3	SPRAY	PRANDTL NUMBER.
PSI	AUX	FRACTION OF FINE STRUCTURES HEATED ENOUGH TO REACT.
PSIC	AUX	TEMPORARY USAGE IN SOOT OXIDATION RATE.
PT2	SPRAY	=2*PI.
QCH	TSOLVE	CONVECTION HEAT TRANSFER.
QDNT	SPRAY	HEAT TRANSFER RATE TO DROPLET.
QRH	TSOLVE	NET RADIATION HEAT TRANSFER FROM WALL.
QD-Q4	CREK	SEE TABLE C-2.
R	ALL	RADIUS.
RAD	TSOLVE	RADIATION HEAT FLUX TO WALL.
RADIN	INIT ALLMOD	INLET RADIATION FLUX.
RADSHR	INIT ALLMOD	RADIATION FLUX AT EACH AXIAL STATION.

TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
RATE	SPRAY	DROPLET EVAPURATION RATE.
RATIO1-9	INIT ALLMOD AUX	CONSTANTS USED IN ELEMENT BALANCE EQUATIONS.
RATIO10-12	INIT ALLMOD AUX	CONSTANTS USED IN ELEMENT BALANCE EQUATIONS.
RDT	STRIDE	ALWAYS EQUAL TO ZERO.
REI	SPRAY	DROPLET REYNOLDS NUMBER.
RELAX	SOLVE MAIN STRIDE AUX	UNDER-RELAXATION FACTORS (SEE INPUT).
RELAXM	SOLVE AUX	=1.-RELAX.
RET	AUX	TURBULENT REYNOLDS NUMBER.
RFUFL	MAIN SPRAY	RADIUS OF FUEL NOZZLE.
RF1,PF2	AUX	SOOT FORMATION RATES.
RGAS	CREK	SEE TABLE C-2.
RGASIN	CREK	SEE TABLE C-2.
RHO	ALL	DENSITY.
RHDA	ALLMOD STRIDE	DENSITY*AREA.
RHOCN	MAIN AUX	PRESSURE DIVIDED BY UNIVERSAL GAS CONSTANT.
RHOIMJ	ALLMOD	DENSITY OF DILUTION JET.
RHOLP	AUX	DENSITY AT NODE LP.
RHOD	AUX	DENSITY OF SURROUNDING FLUID.
RHOP	AUX MAIN INIT	SOOT PARTICLE DENSITY.

TABLE C-1 (CONTD.)

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FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION

RHOPP	STRIDE INIT	DENSITY AT NODE P.
RHOSTR	AUX	DENSITY OF FINE STRUCTURES.
RHOSW	INIT ALLMOD	INLET DENSITY.
RHO4	INIT	DENSITY.
RI	STRIDE PAIN	INNER RADIUS OF COMBUSTOR.
RM	STRIDE	RADIUS AT V-VELOCITY LOCATION.
RMV	STRIDE	RADIUS AT V-VELOCITY CONTROL VOLUME SURFACE.
RNC	AUX	TEMPORARY USAGE.
RNG	SPRAY	NUMBER OF DROPLET SIZE GROUPS.
RNSL	SPRAY PAIN INIT	=NSL2, NUMBER OF SPRAY CONE RAYS.
ROA	ALLMOD	DENSITY*AREA.
ROF	SPRAY	DENSITY OF LIQUID FUEL AT BOILING POINT.
ROFO	SPRAY	INITIAL DENSITY OF LIQUID FUEL.
ROST	SPRAY	GAS DENSITY.
RTCD	INIT ALLMOD AUX	SQUARE ROOT OF CD.
RTCDK	ALLMOD	TURBULENCE ENERGY*SQRT(CD).
RVAV	STRIDE	TEMPORARY USAGE.
RVFCY-2	SPRAY	COORDINATE TRANSFORMATION QUANTITIES.
SBAR	OUTPUT	TEMPORARY USAGE.
SCATR	AUXRAD PAIN INIT	SCATTERING COEFFICIENT (IF ITRAD=2).

ORIGINAL PAGE IS
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TABLE C-1 (CONTD.)

FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION

SCTR	AUXRAD	ARRAY FOR SCATTERING COEFFICIENT.
SC9	SPRAY	SCHMIDT NUMBER.
SECTOR	INIT	ANGULAR SECTOR.
SEXIT	ALLMOD	EXIT MASS FLOW ERROR.
SFAC	AUX	TEMPORARY USAGE IN CO REACTION RATE.
SHRSTR	ALLMOD	SHEAR STRESS.
SIG	TSOLVE	STEFAN-BOLTZMANN CONSTANT.
SIGMA	AUXRAD DATA ALLMOD INIT AUX	STEFAN-BOLTZMANN CONSTANT.
SINA	SPRAY	SINE OF HALF THE NOZZLE CONE ANGLE.
SINB	SPRAY	SINE OF NOZZLE BACK ANGLE.
SIND	SPRAY	SINE OF NOZZLE DOWN ANGLE.
SINT	SPRAY	SINE OF CURRENT SPRAY CONE SEGMENT ANGLE.
SKE	ALLMOD	TURBULENCE ENERGY AT COOLING SLOT.
SLM	ALLMOD	LENGTH SCALE AT COOLING SLOT.
SM	CREK	SEE TABLE C-2.
SMASS	INIT	TEMPORARY USAGE.
SMAY	ALLMOD MAIN	MAXIMUM OF CONTINUITY ERRORS.
SMCONC	OUTPUT	SMOKE CONCENTRATION.
SMD	SPRAY MAIN	SAUTER MEAN DIAMETER.
SMINV	CREK	SEE TABLE C-2.
SMONO	OUTPUT	SMOKE NUMBER.
SMW	CREK	SEE TABLE C-2.

TABLE C-1 (CONTD.)

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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
SMO	CREK	NOT USED.
SNOX	PAIN	NOX SOLUTION STARTED AFTER ERROR FALLS TO SNOX OR AFTER INOX NUMBER OF ITERATIONS.
SOOTH	AUXRAD	SOOT CONCENTRATION.
SOOT1	ALL	MASS FRACTION OF SOOT PARTICLE SIZE 1.
SOOT2	ALL	MASS FRACTION OF SOOT PARTICLE SIZE 2.
SOR	AUX	PART OF SOURCE TERM.
SORCO	AUX	PART OF CO SOURCE TERM.
SOR1	AUX	LAMINAR SOURCE TERM.
SOR2	AUX	TURBULENT SOURCE TERM.
SOR3	AUX	LAMINAR SOURCE TERM.
SOR4	AUX	TURBULENT SOURCE TERM.
SP	ALL	PART OF LINEARIZED SOURCE TERM.
SPCH	AUX	PART OF LINEARIZED SOURCE TERM (SP) FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
SPC1,SPC2	AUX	SOOT OXIDATION RATE.
SPFU	AUX	PART OF LINEARIZED SOURCE TERM (SP) FOR FUEL.
SPF1,SPF2	AUX	TEMPORARY USAGE.
SPF2F	AUX	TEMPORARY USAGE.
SPK	SOLVE	PART OF LINEARIZED SOURCE TERM USED IN CYCLIC TOMA.
SQFK	INIT	SQUARE ROOT OF FK.
SRAD	PAIN	RADIATION SOLUTION STARTED AFTER ERROR FALLS TO SRAD OR AFTER IRAD NUMBER OF ITERATIONS.
SREI	SPRAY	SQUARE ROOT OF REI.
SSOOT	MAIN	SOOT SOLUTION STARTED AFTER ERROR FALLS TO SSOOT OR AFTER ISOOT NUMBER OF ITERATIONS.
SSS	AUX	TEMPORARY USAGE.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION

SSUM	ALLMOD MAIN	SUM OF ABSOLUTE CONTINUITY ERRORS.
STORE	SOLVE STRAD	TEMPORARY USAGE.
ST4	INIT	$-\text{SIGMA} \cdot \text{TEMP} \cdot 0.4$.
SU	ALL	PART OF LINEARIZED SOURCE TERM.
SUCH	AUX	PART OF LINEARIZED SOURCE TERM (SU) FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
SUFU	AUX	PART OF LINEARIZED SOURCE TERM (SU) FOR FUEL.
SUF1,SUF2	AUX	TEMPORARY USAGE.
SUK	SOLVE	PART OF LINEARIZED SOURCE TERM USED IN CYCLIC TDMA.
SUM	AUX	TEMPORARY USAGE.
SUM1	MAIN	TEMPORARY USAGE.
SUM2	MAIN	TEMPORARY USAGE.
SWNO	MAIN	RATIO OF TANGENTIAL TO AXIAL VELOCITY AT DOME INLET.
S1	CREK	SEE TABLE C-2.
S2	CREK	SEE TABLE C-2.
T	INIT AUXRAD AUX	TEMPERATURE.
TAN	INIT	ANNULUS TEMPERATURE.
TAUP	AUX	WALL SHEAR STRESS.
TR	SPRAY	LIQUID FUEL BOILING TEMPERATURE.
TCYLM	ALLMOD MAIN	TEMPERATURE OF CYLINDRICAL PORTION OF COMBUSTOR WALL.
TEMP	ALL	TEMPERATURE.
TEMPW	ALLMOD	TEMPERATURE.
TEMPH	INIT	MASS AVERAGED TEMPERATURE AT EACH AXIAL STATION.

TABLE C-1 (CONTO.)

ORIGINAL PAGE IS
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***** FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN *****	DEFINITION *****
TF	SPRAY	TEMPERATURE OF COMBUSTION PRODUCTS.
TFU	SPRAY	LIQUID DROPLET TEMPERATURE.
TFUEL	MAIN ALLMOD SPRAY	INLET TEMPERATURE OF FUEL.
TGAS	TSOLVE	GAS TEMPERATURE.
THETA	SPRAY	CURRENT SPRAY CONE SEGMENT ANGLE.
THETA1	SPRAY MAIN	INITIAL SPRAY CONE SEGMENT ANGLE.
THETA2	SPRAY MAIN	FINAL SPRAY CONE SEGMENT ANGLE.
TINE	STRIDE	TIME.
TIN	INIT	INITIAL TEMPERATURE AT EACH AXIAL STATION.
TINCP	AUX MAIN	SOOT CALCULATION BYPASSED FOR TEMPERATURE. LE. TINCP.
TINLW	ALLMOD MAIN INIT	TEMPERATURE OF INCLINED WALL PORTION OF COMBUSTOR AND OF DOME.
TITLE	FPRINT MAIN	HEADING FOR DEPENDENT VARIABLE.
TITLE2	OUTPUT MAIN	CASE TITLE CARD.
TK	CREK	SEE TABLE C-2.
TKINV	CREK	SEE TABLE C-2.
TLIP	ALLMOD MAIN	TEMPERATURE OF COOLING SLOT LIP.
TLN	CREK	SEE TABLE C-2.
TMAX	INIT AUX	MAXIMUM TEMPERATURE.
TNEW	INIT	TEMPERATURE ON NEW ITERATION.

TABLE C-1 (CONTO.)

ORIGINAL PAGE IS
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FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION

TNOX	MAIN STRIDE	NOX CALCULATION BYPASSED IF TEMPERATURE.LE.TNOX.
TO	AUX	TEMPERATURE OF SURROUNDING FLUID.
TOUT		OUTLET TEMPERATURE (NOT USED).
TS	AUXRAD	TEMPERATURE.
TST	SPRAY	GAS TEMPERATURE.
TSTR	AUX	TEMPERATURE OF FINE STRUCTURES.
TSW	INIT MAIN	TEMPERATURE AT DOME INLET.
TU:NI	ALLMOD MAIN INIT	COOLING SLOT TEMPERATURE.
TVINJ	MAIN INIT	DILUTION JET TEMPERATURE.
TW	TSOLVE	WALL TEMPERATURE.
TWN	TSOLVE	WALL TEMPERATURE AT NEW ITERATION.
TW2	TSOLVE	=TW**2.
TX,TX1	STRIDE STRAD	DIFFUSION FLUX IN X DIRECTION.
TY,TV1	STRIDE STRAD	DIFFUSION FLUX IN Y DIRECTION.
TZ	STRIDE STRAD	DIFFUSION FLUX IN Z DIRECTION.
TZFAC	STRIDE	FRACTION OF DIFFUSION FLUX IN Z DIRECTION.
T1	SPRAY	AVERAGE OF TS AND TF.
T4	INIT	TEMPORARY USAGE.
U	ALL	U-VELOCITY.
UADP	ALLMOD	CORRECTION TO EXIT VELOCITIES.
UF	SPRAY	DROPLET VELOCITY IN X DIRECTION AT CURRENT LOCATION.

TABLE C-1 (CONTD.)

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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
UFD	SPRAY	DROPLET VELOCITY IN X DIRECTION AT PREVIOUS LOCATION.
UIN	INIT	MEAN U-VELOCITY AT EACH AXIAL STATION.
UINJ	ALLMOD MAIN INIT	COOLING SLOT AXIAL VELOCITY.
ULIM	SPRAY	LIMIT ON DROPLET VELOCITY CHANGE BETWEEN SUCCESSIVE STEPS.
UMASS	INIT	MOMENTUM FLOW THROUGH DOME INLET.
UMEAN	ALLMOD	MEAN EXIT VELOCITY.
UNICON	DATA ALLMOD STRIDE AUX INIT	UNIVERSAL GAS CONSTANT.
UST	SPRAY	GAS VELOCITY IN X DIRECTION.
USW	INIT MAIN	AXIAL VELOCITY OF DOME INLET.
UYN, UYP	AUX	AVERAGE U VELOCITY BETWEEN NEIGHBORING NODES.
UYN, UZP	AUX	AVERAGE U VELOCITY BETWEEN NEIGHBORING NODES.
V	ALL	V-VELOCITY.
VC, VEC	AUX	RESULTANT VELOCITY.
VECX-Z	SPRAY	UNIT VECTORS IN X, Y, Z DIRECTIONS.
VF	SPRAY	DROPLET VELOCITY IN Y DIRECTION AT CURRENT LOCATION.
VFD	SPRAY	DROPLET VELOCITY IN Y DIRECTION AT PREVIOUS LOCATION.
VFU	SPRAY	RESULTANT DROPLET VELOCITY AT CURRENT LOCATION.
VFUEL	SPRAY MAIN	INITIAL FUEL DROPLET VELOCITY.
VINJ	INIT ALLMOD MAIN	RADIAL VELOCITY OF DILUTION JET.
VISC	ALL	VISCOSITY.

TABLE C-1 (CONTD.)

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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION

VISCO	SPRAY	GAS VISCOSITY.
VISCOS	AUX	VISCOSITY.
VMIX	AUX AUXRAD	RECIPROCAL OF AVERAGE MOLECULAR WEIGHT.
VMT2	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
VOL	STRIDE	VOLUME OF ELEMENTARY CONTROL VOLUME.
VP	AUX	RESULTANT VELOCITY.
VPT2	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
VR	SPRAY	RESULTANT RELATIVE VELOCITY BETWEEN GAS AND DROPLET.
VST	SPRAY	GAS VELOCITY IN Y DIRECTION.
VSW	INIT MAIN	RADIAL VELOCITY OF DOME INLET.
VXM,VXP	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
VZM,VZP	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
W	ALL	W-VELOCITY.
WALKE	ALLMOD	WALL TURBULENCE KINETIC ENERGY.
WCH	INIT AUX	MOLECULAR WEIGHT OF INTERMEDIATE HYDROCARBON.
WCO	INIT,DATA AUX	MOLECULAR WEIGHT OF CO.
WCO2	INIT,DATA AUX	MOLECULAR WEIGHT OF CO2.
WC2H4	INIT,DATA	MOLECULAR WEIGHT OF C2H4.
WF	SPRAY	DROPLET VELOCITY IN Z DIRECTION AT CURRENT LOCATION.
WFF	SPRAY MAIN INIT	FUEL FLOW RATE.
WFI	SPRAY	FUEL FLOW RATE ON A PARTICULAR RAY.

TABLE C-1 (CONTD.)

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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
WFN7	INIT	TOTAL LIQUID FUEL FLOW RATE.
WFO	SPRAY	DROPLET VELOCITY IN Z DIRECTION AT PREVIOUS LOCATION.
WFO	INIT, DATA AUX	MOLECULAR WEIGHT OF FUEL.
WN2	INIT, DATA AUX	MOLECULAR WEIGHT OF N2.
WN20	INIT, DATA AUX	MOLECULAR WEIGHT OF H2O.
WIN	ALLMOD	W-VELOCITY THROUGH DOME INLET.
WL7P	STRIDE	TEMPORARY USAGE.
WMNM, WMNP	AUX	AVERAGE W VELOCITY BETWEEN NEIGHBORING NODES.
WN2	INIT, DATA AUX	MOLECULAR WEIGHT OF N2.
W0Y	INIT, DATA AUX	MOLECULAR WEIGHT OF O2.
WST	SPRAY	GAS VELOCITY IN Z DIRECTION.
WSW	INIT ALLMOD	TANGENTIAL VELOCITY OF DOME INLET.
WUINJ	ALLMOD MAIN INIT	COOLING SLOT TANGENTIAL VELOCITY.
WXM, WXP	AUX	AVERAGE W VELOCITY BETWEEN NEIGHBORING NODES.
WYM, WYP	AUX	AVERAGE W VELOCITY BETWEEN NEIGHBORING NODES.
X	ALL	AXIAL DISTANCE.
XDIF	STRIDE	INTERNODAL DISTANCE IN X-DIRECTION.
XF	SPRAY	X LOCATION OF DROPLET.
XH	SPRAY	X LOCATION OF CONTROL VOLUME SURFACES.
XH	AUX	X DISTANCE AT X- LOCATION.
XO	MAIN SPRAY	X LOCATION OF ORIGIN OF FUEL NOZZLE SPRAY.

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TABLE C-1 (CONTD.)

FORTTRAN	SUBROUTINE	DEFINITION
VARIABLE	WHERE DEFINED OR USED OFTEN	

XP	AUX	X DISTANCE AT X+ LOCATION.
XS	STRIDE	MAIN CONTROL VOLUME WIDTH IN X DIRECTION.
XSU	STRIDE	U-VELOCITY CONTROL VOLUME WIDTH IN X DIRECTION.
Y	ALL	RADIAL DISTANCE.
YDIF	STRIDE	INTERNODAL DISTANCE IN Y DIRECTION.
YF	SPRAY	Y LOCATION OF DROPLET.
YM	SPRAY	Y LOCATION OF CONTROL VOLUME SURFACES.
YM	AUX	Y DISTANCE AT Y- LOCATION.
YO	MAIN SPRAY	Y LOCATION OF ORIGIN OF FUEL NOZZLE SPRAY.
YP	AUX	Y DISTANCE AT Y+ LOCATION.
YPLUS	ALLMOD	YPLUS IN WALL FUNCTIONS.
YS	STRIDE	MAIN CONTROL VOLUME WIDTH IN Y DIRECTION.
YSR	STRIDE	MAIN CONTROL VOLUME AREA NORMAL TO X DIRECTION.
YSV	STRIDE	V-VELOCITY CONTROL VOLUME WIDTH IN Y DIRECTION.
YSVR	STRIDE	V-VELOCITY CONTROL VOLUME AREA NORMAL TO X DIRECTION.
Y1,Y2	INIT	TEMPORARY USAGE.
Z	ALL	TANGENTIAL DISTANCE.
ZDIF	STRIDE	INTERNODAL DISTANCE IN Z DIRECTION.
ZF	SPRAY	Z LOCATION OF DROPLET.
ZM	SPRAY	Z LOCATION OF CONTROL VOLUME SURFACES.
ZM	AUX	Z DISTANCE AT Z- LOCATION.
ZO	MAIN SPRAY	Z LOCATION OF ORIGIN OF FUEL NOZZLE SPRAY.
ZP	AUX	Z DISTANCE AT Z+ LOCATION.
ZS	STRIDE	MAIN CONTROL VOLUME WIDTH IN Z DIRECTION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION

ZSHALL	SPRAY	ONE HUNDRETH OF AVERAGE ANGULAR GRID SPACING.
ZSW	STRIDE	W-VELOCITY CONTROL VOLUME WIDTH IN Z DIRECTION.

TABLE C-2. LIST OF FORTRAN VARIABLES IN THE CHEMICAL KINETICS PROGRAM CREK.

This list is adapted from Ref. 48 to which the reader is referred for further details.

Fortran Variable	Routines Where Defined Or Used Often	Definition
A	CALC	Elements of Newton-Raphson correction matrix.
AL	CREKO SPECE CALC	Atomic stoichiometric coefficients, AL(I,J) = the number of kg-atoms of element I per kg-mole of species J.
ATOM	ERATIO (SPECE) CREKO	ATOM (1,K) = atomic symbol for element K. ATOM (2,K) = atomic weight of element K. ATOM (3,K) = valence or oxidation state of element K.
ASUB	CREKO	Molecular symbol of each NS species (e.g., CO, H ₂ O, etc.).
BO	SPECE CALC	Atom numbers for reactant mixture, BO(I) = kg-atoms element I per kg reactant mixture.
BX	CREKO CALC	Exponent-on 10 on pre-exponential term of extended Arrhenius forward rate expression, when read from MECHANISM data cards. Later, BX is set = BX*(log _e 10) to avoid repetitive exponentiation on ten.
BX2	CREKO CALC	Same as BX for reverse rate expression.
CPSUM	CALC CREKO HCPS	Non-dimensional mixture constant pressure specific heat capacity.
EMV	CREK CALC	Total convective and diffusive mass inflow rate to the control volume, kg m ⁻³ s ⁻¹ .
ER	CREK ERATIO (SPECE)	Fuel/air equivalence ratio.

TABLE C-2 (Continued).

Fortran Variable	Routines Where Defined Or Used Often	Definition
ETA	SPECE	Self-adjusting under-relaxation parameter.
FQ	CREK CALC	Scaling parameter for Q.
HO	CREKO CALC HCPS	Non-dimensional, ideal-gas enthalpy of each chemical species at given temperature.
HSUBO	CREKO CALC	Convective and diffusive net enthalpy influx rate to the control volume, divided by EMV (i.e., mass-averaged specific enthalpy of reactants entering the control volume), J/kg. HSUBO must be set by the calling program.
HSUM	CREKO CALC	Working variable wherever used.
ID	CREKO CALC	ID(K,J) is the species index number (i=1, NS) of the K-th species (K=1,4) in the J-th reaction (J=1, JJ).
IDCO, IDC02 IDH2, IDH20 IDN2, ID02	CALC	Index number (i=1,NS) of the particular species in the variable name.
IHCPS	CREKO CALC HCPS	Value of IHCPS controls whether or not subroutine HCPS calculates values of non-dimensional one-atmosphere entropy for each species.
ILC, ILH	CREKO CALC	Index number of the elements carbon and hydrogen, respectively.
IMAT	SPECE CALC	Number of rows in Newton-Raphson correction matrix; set in CALC. IMAT=N2 if LEQUIL=.TURE.: IMAT=NQ if LEQUIL=.FALSE.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
ITER	SPECE	Current value of iteration counter.
ITMAX	SPECE	Controls the maximum number of iterations permitted by each call to CREK. Set by DATA statement in SPECE.
JJ	CREKO CALC	Number of distinct forward reactions considered in reaction mechanism; must be less than or equal to the dimensions of labeled COMMON block REACTS.
LADIAB	CREK CALC	LADIAB must be set by program calling CREK. If = .FALSE., enthalpy source term Q is non-zero, and calling program must specify values of Q0, Q1, Q2, Q3 and Q4 in enthalpy source term.
LCONVG	CREK SPECE	Initially = .FALSE.; set = .TRUE. in SPECE if convergent solution achieved. Controls solution strategy in CREK.
LDEBUG	SPECE CALC	If LDEBUG is set = .TRUE. by the calling program, intermediate output is written on the output record. Default value is .FALSE.
LEQUIL	CREK SPECE CALC	LEQUIL must be set by calling program. If = .TRUE., equilibrium states are calculated; if = .FALSE., kinetic stationary states are calculated.
LNRG	CREK CALC	For LEQUIL = .FALSE. problems only. If = .TRUE., fully coupled energy equation is used.
LREACT	CREK	LREACT = .FALSE. on entry to CREK suppresses calculation of combustion reaction. Default value is .TRUE.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
NDEBUG	CREK SPECE CALC	When LDEBUG = .TRUE., NDEBUG set from 1 to 5 controls increasing detail of debug output. Default value of NDEBUG = 5.
NGLOB	CREKO CALC	Number of finite-rate global hydrocarbon pyrolysis steps considered.
NGLOBP	CREKO CALC	NGLOB + 1.
NLM	CREKO SPECE CALC	The number of distinct elements considered. Must be less than or equal to corresponding dimensions of labeled COMMON block CEQUIL.
N1,N2,N3	CREKO CALC	N1 = NLM + 1, N2 = NLM + 2, N3 = NLM + 3.
NS	CREKO SPECE CALC	Number of distinct species considered. Must be less than appropriate dimensions in labeled COMMON blocks CEQUIL, CMATRI, CPARAM and CSPECE.
NSM, NQ, NA	CREKO CALC	NSM = NS + 1, NQ = NS + 2, NA = NS + 3.
PA	CREK SPECE CALC	Pressure within control volume, $N\ m^{-2}$. Must be set by program calling CREK.
PI	CALC	Lagrange multipliers in reduced Gibbs iteration correction equations.
PPLN	CREK CALC	$\log_e (P/P_0)$.
Q	CALC	Negative of non-dimensional enthalpy source term, determined by values of Q0, Q1, Q2, Q3 and Q4 set by the calling program.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
Q0, Q1, Q2, Q3, Q4	CALC	Coefficients for enthalpy source term, $-S_H = Q_0 + Q_1T + Q_2T^2 + Q_3T^3 + Q_4T^4$, $Jm^{-3} s^{-1}$. These values must be set whenever LADIAB = .FALSE. is set by the calling program.
RGAS	CREKO CALC	Universal gas constant, 8314.4 J/(kg-mole) (K).
RGASIN	CREKO CALC	Inverse of RGAS.
RHOP	CREKO CALC	Mass density , $kg m^{-3}$.
RT	CALC	$\frac{\partial f_i}{\partial \log T}$
SO	CREKO CALC HCPS	One-atmosphere, ideal-gas entropy of species i.
S1	CREKO CALC	Inlet mole numbers of species i.
S2	CREKO CALC	Mole numbers of species i, kg-moles i/kg. Calling program must set these values as estimates; on return they are solution values.
SM	ALL	Reciprocal mixture molecular weight.
SMINV	CREK CALC	Reciprocal of SM, therefore the mixture molecular weight, kg/(kg-mole).
SMW	CREKO	Molecular weight of species i.
SSAVE	CREK	Array for saving current values of S2.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
TACT, TACT2	CREKO CALC	Activation temperature (activation energy divided by gas constant) for forward and reverse reactions respectively, degrees K.
TEN, TEN2	CREKO CALC	Exponent-on-temperature in pre-exponential term of rate constant in forward and reverse reactions respectively.
TK	ALL	Temperature T, deg K. Estimate on calling CREK, solution on return. If set equal to zero by program calling CREK, causes CREK to establish estimates for T and S2.
TKINV	CREK CALC	Reciprocal of TK.
TLN	CREKO CALC HCPS	Logarithm of the temperature.
X	CREKO CALC	Current values of the correction variables: Also used as working variable in subroutine CREKO.
X1, X2	CALC	Contact index for forward and reverse reactions j. Dimensionless.
Y	CREKO CALC	Logarithms of variables. Also used as working variable in subroutine CREKO.
Z	CREKO HCPS	Coefficients for calculation of thermochemical data.

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APPENDIX D
LISTING OF THE 3-D COMBUSTOR
PERFORMANCE PROGRAM

APPENDIX D

LISTING OF THE 3-D COMBUSTOR PERFORMANCE PROGRAM

This appendix contains a listing of the 3-D combustor performance program. In order to identify the changes made to the original program of Ref. 1, various correction idents appear at the ends of the changed or newly inserted statements. The meanings of these correction idents are given below:

CREK	}	- Chemical kinetics program CREK
CALC		
SPEC		
CRKO		
HCPS		
ABSOR	-	Radiation-property subroutine
SOOT	-	Soot-emissions updates
NASAX	-	Corrections to the original program
CTDMA	-	Cyclic TDMA updates
NOXXX	-	Updates to make the chemical kinetics program CREK CYBER-Compatible
RAD	}	- Radiation updates
TS0		
NOX	-	NO _x -emissions updates for 3-D program
NOXX	-	NO _x -emissions updates for CREK program
4STEP	-	4-Step-mechanism updates
COMMENT	-	Comment cards
JAN14	}	- Some additional modifications
JAN18		
FEB2		
MAR2		

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PROGRAM MAIN(INPUT,OUTPUT,TAPE5=INPUT,TAPF6=OUTPUT,TAPE9,TAPE9,	NASAX	1
1 TAPF11)	NASAX	2
COMMON F(500,7),NU(10,10,5),DV(10,10,5),DW(10,10,5),	COMFA	2
1 AMUC(10,10,5),SQU1(10,10,5),SQU2(10,10,5),FCH(10,10,5),	4STEP	1
2 F42(10,10,5),FS(500,14),	4STEP	2
1 RHO(10,10,5),VISC(10,10,5),ABSR(10,10,5),SCTR(10,10,5),	RAD	1
1 SU(10,10),SP(10,10),DRHONP(10,10,5),	RAD	2
1 AXP(10,10),AXM(10,10),AYP(10,10),AYM(10,10),AZP(10,10),	COMFA	4
2 AZM(10,10),C7(10,10),CY(10,10),CZU(10,10),CYU(10,10),	COMFA	5
3 CZP(10,10),CYP(10,10),DIVG(10,10),NTP1,NTP2	COMFA	6
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),	CTOMA	1
2 SUK(192),SPK(192)	CTOMA	2
DIMENSION U(10,10,5),V(10,10,5),W(10,10,5),PP(10,10,5)	COMFA	7
DIMENSION P(10,10,5),TEMP(10,10,5),GAM(10,10,5)	COMFA	8
EQUIVALENCE (F(1,1),U(1,1,1)),(F(1,2),V(1,1,1)),(F(1,3),W(1,1,1))	COMFA	9
EQUIVALENCE (F(1,4),PP(1,1,1)),(F(1,5),P(1,1,1))	COMFA	10
EQUIVALENCE (F(1,6),TEMP(1,1,1)),(F(1,7),GAM(1,1,1))	COMFA	11
COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX	COMMON	2
COMMON/GR10/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),	COMMON	3
1 YSV(30),ZSV(30),XOIF(40),YOIF(30),ZOIF(30),FXP(40),FXM(40),	COMMON	4
2 FYP(30),FYM(30),F7P(30),F7M(30),OT,TIME	COMMON	5
COMMON	NOX	2
1/CINDEX/IDCC,IOFU,IOO2,ION2,IOH2O,IOCO2,IOH1,IOH2,ION1,IONO,IONO2	NOX	3
2,ION,IOOH,IOHPS,ILC,ILH,IMAT,ITER,JJ,N1,N2,N3,NA,NGL0B,NGL0BP,	NOX	4
1 NLN,NO,NSP,NS1,NS2,IOCH	4STEP	3
3/CCHEMI/CPSUP,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG	NOX	6
4/CPARAM/ASUB(30,3),EMV,ER,HSUBO,NOERUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOPP,	NOX	7
4 SM,SNW(30),SMO,S1(30),S2(30),TK,LA0IAB,LDEB0G,LFOUIL,LPEACT,	NOX	8
4 LENER,ENKIJ,LCONVG	NOX	9
DOUBLE PRECISION CPSUM,EMV,ER,FQ,HSUBO,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOPP,SM,SHINV,SNW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FIIT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CERU1,CERU2,	4STEP	5
1 CERU3,CERU4,AXP1,AXP2,AXP3,AXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FIIT,FST	4STEP	7
LOGICAL LADIA0,LCONVG,LDERUG,LEQUIL,LNRG,LREACT,LENER	NOX	12
COMMON/INT/L,N,N,LCV,MCV,NCV,LPI,MP1,MP1,NI,NJ,NK,NINJ,NINJNK,NV,	COMMON	6
1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KM(30),JM(30),ISTEP,	4STEP	8
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISMP,J5MP,RELAX(35),NP,	4STEP	9
3 VRHO,NGAM,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWFI,	COMMON	9
4 IWFO,MH1,JW11,JW10,JW01,JW00,ION,JKIN(30,30),IKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LPRFF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVR2,JPLANE	COMMON	11
1,PLAXM1,LVK,LVD,LVFUOX,LVFO,LVCO,LVH,LVRX,LVR2,NVF(32),	4STEP	10
2 IJUMP,IRFS,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH2O,NVCO2,	COMMON	13
1 NVN2,NVCH,NVM2	4STEP	11
COMMON/CHOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVNH,LVH2O,LVN2,LVO2,	NOX	16
1 LVCO2,LVFU1,LVCO1,MNOX,INOX,ITNOX,SNMX,TNOX	NOX	17
COMMON/TEMP/NVM,NVFU,NVQX,NVFUOX,NVTE,MODEN,IOK,FSTOIC,HFU,CP,	COMMON	15
1 GASCON,RHOCN,UNICCN,PRESS,NVFAY,TCYLV,TINLV,TLIP,ACDEF(4),	COMMON	16
2 T4,OFAC,HFU,WCO2,WCO,WDX,WH2O,WN2,HVY,CXX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,HCO,TAN,ITWALL	COMMON	18
COMMON/CTDPA/REND,ICTDMA(32)	4STEP	12
COMMON/MIS/AMU,DEF,SMAX,SSUM,LASTEP,HTCENT,CFR,EMISW,EMTSIN,	COMGEN	2
1 EMISR,TOUT,RTCO,EMI,RADIN,RADSUR,FMA,FK,SQFK,	COMGEN	3
2 FKFU,FDFU,TFUEL,MFNZ,FLO(40),TENTM(40),H(40),FUEL(40),FUOX(40),	COMGEN	4
2 UIN(40),TIN(40),FUELS(40),SEKIT,IGAM1(29),IGAM2(29)	4STEP	13
COMMON/THRR/NVK,NVO,C1,C2,C0,AK,OUIONJ(3,3),AKFAC,ALFAC,	COMGEN	6
1 MODEL,PR(32),PREF(32),PJAY(32),E	4STEP	14
COMMON/RAD/NVE,SIGMA,ANSOR,SCATR	COMGEN	8
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	COMGEN	9
COMMON/DRDP1/EVAP(192),NTP4,MFN2,XO(3),YQ(3),ZO(3),ALFA(3),	COMGEN	10
1 RETA(3),DELTA(3),THETA1(3),THETA2(3),MSL(3),WFF(3),SMO(3),	COMGEN	11
2 VFUEL(3),RFUEL(3),FVSI(64),HEVAP	COMGEN	12
COMMON/INJEC/FLOWIN,IUTNJ(20),JUINJ(20),UINJ(20),WUINJ(20),	COMGEN	13

1	AVINJ(20),TVINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	COMGEN	14
2	FVINJ(20),OVINJ(20),AVINJ(20),TVINJ(20),NUINJ,NVINJ,JSW1,JSW2,	COMGEN	15
3	USW,VSW,AFSW,FSW,TSW,WSW,SWND,RHDSW	COMGEN	16
	COMMON/CSOOT/NVN,NVS1,NVS2,TSOOT,SSOOT,MSOOT,AD,ARCONN,AAA,BB8,FMG	SOOT	8
1	GO,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BBS,DHR	SOOT	9
2	LVN,LVS1,LVS2,CINCP,TINCP,FUTDT	SOOT	10
	COMMON/CRAD/IPAD,SRAD	SOOT	11
	COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,A=1,BB1,CC1,	4STEP	15
1	AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2	RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,MCH,MH2,MC2H4,LVCH,LVCH1,LVH21	4STEP	17
	DIMENSION CLEND(2),CLENV(2),CENER(2),CMASS(2),CTEMP(2),CPRESS(2)	MA	7
	DIMENSION CANG(2)	MA	8
	DATA CLEND/1.0,.0254/,CLENV/1.0,.3048/,CENER/1.0,1095./	MA	9
	DATA CMASS/1.0,.4536/,CTEMP/1.0,.5555/,CPRESS/1.0,101329./	MA	10
	DATA CANG/1.0,.01745/	MA	11
CHAPTER 1 -----PARAMETERS AND CONTROL INDICES-----		MA	12
	NT01=0	MA	13
	NT02=0	MA	14
	NT04=11	MA	15
	READ (5,30) TITLE	MA	16
	READ (5,31) TITLE2	MA	17
31	FORMAT (20A4)	MA	18
30	FORMAT (10A4)	MA	19
	READ (5,100) LP1,MP1,NP1,IPLAX,MODEL,MODEE,IPAR,ITRAD	MA	20
	READ (5,100) IU,MODEN,INTAPE,IDW,IRES	MA	21
100	FORMAT (8(I2,0X))	MA	22
	READ (5,100) ISOLVE	MA	23
	READ (5,100) ICTDMA	MA	24
	READ (5,100) IPRINT	MA	25
	READ (5,101) RELAX	MA	26
	READ (5,101) PR	MA	27
	READ (5,101) PREF	MA	28
101	FORMAT (RE10.4)	MA	29
	PLAXM1=FLOAT(IPLAX-1)	MA	30
CHAPTER 2 -----GRID AND GEOMETRY-----		MA	31
C-----		MA	32
	CALL STRIOO	MA	33
C-----		MA	34
	READ (5,101) (X(I),I=1,LP1)	MA	35
	READ (5,101) (Y(J),J=1,MP1)	MA	36
	READ (5,101) (Z(K),K=1,NP1)	MA	37
	DO 200 I=1,LP1	MA	38
200	X(I)=X(I)*CLEND(IU)	MA	39
	DO 205 J=1,MP1	MA	40
205	Y(J)=Y(J)*CLEND(IU)	MA	41
	DO 220 K=1,NP1	MA	42
	GO TO (210,215), IPLAX	MA	43
210	Z(K)=Z(K)*CLEND(IU)	MA	44
	GO TO 220	MA	45
215	Z(K)=Z(K)*CANG(IU)	MA	46
220	CONTINUE	MA	47
	R1=Y(1)	MA	48
	Y(1)=0.0	MA	49
C	----- INCLINED WALL DATA	MA	50
	DO 22 J=1,MP1	MA	51
	IWL(I,J,4)=2	MA	52
22	IWLO(J,4)=L	MA	53
	DO 26 J=1,LP1	MA	54
	JWL(I,J,4)=1	MA	55
26	JWLO(J,4)=NP1	MA	56
	IWFO=L	MA	57
	JWFI=1	MA	58
	JWFI=1	MA	59
	JWFO=NP1	MA	60

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RFAD(5,100)IWEI,JWID,IWEO,JWNO	NASAX	3
IF (IWEI.EQ.2) GO TO 82	NA	62
RFAD (5,100) (IWI(J,4),J=JWID,MP1)	NA	63
RFAD (5,100) (JWLO(I,4),I=1,IWEI)	NA	64
02 CONTINUE	NA	65
IF(IWEO.EQ.L)GO TO 82	NASAX	4
RFAD(5,100)(IWI(J,4),J=JWNO,MP1)	NASAX	5
RFAD(5,100)(JWLO(I,4),I=IWEO,LP1)	NASAX	6
03 CONTINUE	NASAX	7
GO TO (23,24),IPAR	NA	66
24 IREF=L	NA	67
JREF=M	NA	68
KREF=N	NA	69
LPREF=KM(KREF)+JM(JREF)+IREF	NA	70
23 CONTINUE	NA	71
DO 25 J=1,MP1	NA	72
GO TO (260,265), IPLAX	NA	73
260 R(J)=1.0	NA	74
GO TO 25	NA	75
265 R(J)=RI+Y(J)	NA	76
25 CONTINUE	NA	77
C-----CALL STRID1	NA	78
C-----	NA	79
CHAPTER 3 -----DEPENDENT VARIABLES-----	NA	80
READ (5,101) PRESS,OEN,ANSOR,SCATR,AKFAC,ALFAC	NA	81
READ (5,101) CKX,MYY,MFU,FUMCO	NA	82
READ (5,101) PREXP1,ARCON1,CR1,PREXP2,ARCON2,CR2	NA	83
READ(5,101)PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4	NA	84
READ(5,101)AA1,BB1,CC1,AA2,BB2,CC2	4STEP	19
READ(5,101)AA3,BB3,CC3,AA4,BB4,CC4	4STEP	20
READ (5,101) C1,C2,CD,AMU,ERROR,TCYLM,TINLW,TLIP	4STEP	21
READ (5,103) LASTEP,IJUMP,JSW1,JSW2,MUINJ,MVINJ	NA	85
103 FORMAT (2(I3,7X),6(I2,8X))	NA	86
READ (5,101) USW,VSW,SWNO,AFSW,FSW,TSW	NA	87
C-----FUEL INJECTION DATA.	NA	88
READ (5,102) MFMZ,ISPRAY,TFUEL	COMMENT	1
102 FORMAT (2(I2,8X),6E10.4)	NA	89
IF (MFMZ.LE.C) GO TO 110	NA	90
DO 115 I=1,MFMZ	NA	91
READ (5,101) XO(I),YO(I),ZO(I),ALFA(I),BETA(I),DELTA(I),THETA1(I),	NA	92
1 THETA2(I),RMSL,MFF(I),SMD(I),VFUEL(I),RFUEL(I)	NA	93
115 NSL(I)=FIX(RMSL)	NA	94
DO 120 II=1,MFMZ	NA	95
YO(II)=XO(II)*CLEND(IU)	NA	96
YO(II)=YO(II)*CLEND(IU)	NA	97
GO TO (125,130), IPLAX	NA	98
125 ZO(II)=ZO(II)*CLEND(IU)	NA	99
GO TO 135	NA	100
130 ZO(II)=ZO(II)*CANG(IU)	NA	101
135 ALFA(II)=ALFA(II)*CANG(IU)	NA	102
BETA(II)=BETA(II)*CANG(IU)	NA	103
DELTA(II)=DELTA(II)*CANG(IU)	NA	104
THETA1(II)=THETA1(II)*CANG(IU)	NA	105
THETA2(II)=THETA2(II)*CANG(IU)	NA	106
MFF(I)=MFF(II)*CMASS(IU)	NA	107
RFUEL(II)=RFUEL(II)*CLEND(IU)	NA	108
120 VFUEL(II)=VFUEL(II)*CLEND(IU)	NA	109
110 CONTINUE	NA	110
TFUEL=TFUEL*CTEMP(IU)	NA	111
AMU=AMU*CMASS(IU)/CLEND(IU)	NA	112
PRESS=PRESS*CPRESS(IU)	NA	113
OEN=OEN*CMASS(IU)/CLEND(IU)/CLEND(IU)/CLEND(IU)	NA	114
TCYLM=TCYLM*CTEMP(IU)	NA	115
	NA	116

TINLW=TINLW*CTEMP(IU)	MA	117
TLIP=TLIP*CTEMP(IU)	MA	118
USW=USW*CLENV(IU)	MA	119
VSW=VSW*CLENV(IU)	MA	120
AFSW=AFSW*CHASS(IU)	MA	121
FSW=FSW*CHASS(IU)	MA	122
TSW=TSW*CTEMP(IU)	MA	123
C-----FILM COOLING DATA.	COMMENT	2
IF (NUINJ.LE.0) GO TO 85	MA	124
RFAD (5,100) (IUINJ(I),I=1,NUINJ)	MA	125
RJAD (5,100) (JUINJ(I),I=1,NUINJ)	MA	126
READ (5,101) (UINJ(I),I=1,NUINJ)	MA	127
READ (5,101) (WUINJ(I),I=1,NUINJ)	MA	128
READ (5,101) (AUINJ(I),I=1,NUINJ)	MA	129
RJAD (5,101) (TUINJ(I),I=1,NUINJ)	MA	130
DO 235 II=1,NUINJ	MA	131
UINJ(II)=UINJ(II)*CLENV(IU)	MA	132
WUINJ(II)=WUINJ(II)*CLENV(IU)	MA	133
AUINJ(II)=AUINJ(II)*CHASS(IU)	MA	134
235 TUINJ(II)=TUINJ(II)*CTEMP(IU)	MA	135
C-----DILUTION JET DATA.	COMMENT	3
85 IF (NVINJ.LE.0) GO TO 88	MA	136
READ (5,100) (IUVINJ(I),I=1,NVINJ)	MA	137
READ (5,100) (JUVINJ(I),I=1,NVINJ)	MA	138
READ (5,100) (KVINJ(I),I=1,NVINJ)	MA	139
READ (5,101) (VINJ(I),I=1,NVINJ)	MA	140
READ (5,101) (EUVINJ(I),I=1,NVINJ)	MA	141
RJAD (5,101) (DUVINJ(I),I=1,NVINJ)	MA	142
READ (5,101) (AVINJ(I),I=1,NVINJ)	MA	143
READ (5,101) (TVINJ(I),I=1,NVINJ)	MA	144
DO 240 II=1,NVINJ	MA	145
VINJ(II)=VINJ(II)*CLENV(IU)	MA	146
EUVINJ(II)=EUVINJ(II)*CLENV(IU)*CLENV(IU)	MA	147
DUVINJ(II)=DUVINJ(II)*CLENV(IU)	MA	148
AVINJ(II)=AVINJ(II)*CHASS(IU)	MA	149
240 TVINJ(II)=TVINJ(II)*CTEMP(IU)	MA	150
88 READ(5,100) NSOOT, ISOOT, MPART	SOOT	13
C-----SOOT DATA.	COMMENT	4
IF(NSOOT.EQ.0)GO TO 910	SOOT	14
READ(5,101)SSOOT,AD,ARCONH,AAA,BBB,FHG,GO,HOP	SOOT	15
READ(5,101)PREXPS,ARCONS,ALPHA,AAS,BBS,DHR,CINCP,TINCP	SOOT	16
READ(5,101)(DPART(I),I=1,MPART)	SOOT	17
READ(5,101)(FRACP(I),I=1,MPART)	SOOT	18
RHOP=RHOP*CHASS(IU)/(CLEND(IU)**3)	SOOT	19
DHR=DHR*CFNER(IU)/CHASS(IU)	SOOT	20
910 CONTINUE	SOOT	21
C-----RADIATION DATA.	COMMENT	5
IF(ITRAD.NE.1)READ(5,105)IRAD,SRAD	RAD	5
105 FORMAT(I2,8X,E10.4)	RAD	6
C-----NOX DATA.	COMMENT	6
RFAD(5,104)NNOX,INOX,ITNOX,SNOX,TNOX	NOX	22
104 FORMAT(3(I2,8X),2E10.4)	NOX	23
TNOX=TNOX*CTEMP(IU)	NOX	24
CALL CREKO	NOX	25
WPU=12.*CXX*WVY	MA	152
ISTEP=IRES	MA	153
DFAC=1.0	MA	154
SUM1=.01	MA	155
SUM2=.05	MA	156
CHAPTER 4 -----MATERIAL CONSTANTS-----	MA	157
PRFF(LVD)=AK*AK/(C2-C1)/SORT(CD)	MA	158
DO 93 NV=1,NV	MA	159
PRRAT=PR(NV)/PRF(NV)	MA	160
93 PJAY(NV)=E0(PRRAT-1.)/PRRAT*.25	MA	161

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RHOCON=PRESS/UNICON	MA	162
GASCON=UNICON*(0.232/MOX+0.768/MM2)	NASAX	8
CHAPTER 5 ----- INITIAL VALUES -----	MA	164
CALL START	MA	165
IF (INTAPE.NF.C) CALL OUTPUT (INTAPE)	NASAX	9
JTRAD=ITRAD	SOOT	22
ITRAD=1	SOOT	23
JNOX=1	NOX	26
SSUM=1.0E30	SOOT	24
C----- MAIN LOOP STARTS -----	MA	167
60 CONTINUE	MA	168
IF (NSOOT.EQ.0) GO TO 64	SOOT	25
C----- START SOOT CALCULATION.	COMMENT	7
IF (ISTEP.LT.ISOOT.AND.SSUM.GT.SSOOT) GO TO 64	SOOT	26
DO 66 II=1,MPART	SOOT	27
ISOLVE(LVS1+II-1)=1	SOOT	28
66 IPRINT(23+II)=1	SOOT	29
ISOLVE(LVN)=1	SOOT	30
GO TO 63	SOOT	31
64 DO 67 II=1,MPART	SOOT	32
ISOLVE(LVS1+II-1)=0	SOOT	33
67 IPRINT(23+II)=0	SOOT	34
ISOLVE(LVN)=0	SOOT	35
IPRINT(23)=0	SOOT	36
63 IF (JTRAD.EQ.1) GO TO 65	RAD	7
C----- START RADIATION CALCULATION.	COMMENT	8
IF (ISTEP.GE.ITRAD.OR.SSUM.LE.SRAD) ITRAD=JTRAD	SOOT	38
IF (ITRAD.EQ.1) GO TO 65	RAD	8
ISOLVE(LVRX)=1	RAD	9
ISOLVE(LVRY)=1	RAD	10
ISOLVE(LVRZ)=1	RAD	11
IPRINT(11)=1	RAD	12
IPRINT(12)=1	RAD	13
IPRINT(13)=1	RAD	14
IPRINT(14)=1	RAD	15
GO TO 69	RAD	16
69 CONTINUE	SOOT	39
ISOLVE(LVRX)=0	RAD	17
ISOLVE(LVRY)=0	RAD	18
ISOLVE(LVRZ)=0	RAD	19
IPRINT(11)=0	RAD	20
IPRINT(12)=0	RAD	21
IPRINT(13)=0	RAD	22
IPRINT(14)=0	RAD	23
69 CONTINUE	RAD	24
IF (JNOX.EQ.0) GO TO 70	NOX	27
C----- START NOX CALCULATION.	COMMENT	9
IF (INNOX.EQ.0) GO TO 68	NOX	28
IF (ISTEP.LT.INOX.AND.SSUM.GT.SNOX) GO TO 68	NOX	29
ISOLVE(LVFU)=0	NOX	30
ISOLVE(LVCO)=0	NOX	31
ISOLVE(LVCH)=0	4STEP	22
ISOLVE(LVH2)=0	4STEP	23
ISOLVE(LVH1)=1	NOX	32
JNOX=0	NOX	33
INOX=ISTEP	NOX	34
GO TO 70	NOX	35
68 ISOLVE(LVH1)=0	NOX	36
70 CONTINUE	NOX	37
C-----	MA	169
IF (ISTEP.EQ.100) ISOLVE(LVK)=9	MA	170
IF (ISTEP.EQ.100) ISOLVE(LVO)=9	MA	171
CALL DENS	MA	172
ISP=ISPRAY	MA	173

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IF (ISTEP-IRFS,LF,5) ISP=1		MA	174
IF (MOD(ISTEP-IRFS,ISP),EQ,0) CALL SPRAY		MA	175
CALL VISCO		MA	176
C-----		MA	177
CHAPTER 5 -----SINGLE LINE PRINTOUT-----		MA	178
IF (ISTEP,FQ,IRFS) GO TO 16		MA	179
WRITE (6,10) ISTEP,SMAX,SSUM,SEXIT,P(2,M,2),P(L,M,2),		MA	180
1 U(IMAX,JMAX,KMAX),V(IMAX,JMAX,KMAX),W(IMAX,JMAX,KMAX),		MA	181
2 TEMP(IMAX,JMAX,KMAX),RHO(IMAX,JMAX,KMAX),IMAX,JMAX,KMAX		MA	182
10 FORMAT (1X,I4,10(1PE11.3),1X,3I3)		MA	183
16 CONTINUE		MA	184
C-----		MA	185
CALL STPID2		MA	186
C-----		MA	187
CHAPTER 7 -----OUTPUT-----		MA	188
IF (ERRCR,GT,SSUM) ISTEP=LASTEP		MA	189
DFAC=AMAX1(0.0,(SUM2-SSUM)/(SUM2-SUM1))		MA	190
DFAC=APIN1(1.0,DFAC)		MA	191
CALL OUTPUT (NTP1)		MA	192
CHAPTER 8 -----TERMINATION -----		MA	193
IF (ISTEP=LASTEP) 60,80,80		MA	194
80 WRITE (6,10) ISTEP,SMAX,SSUM		MA	195
C-----		MA	196
STOP		MA	197
END		MA	198
BLCK DATA		MA	199
COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX	COMMON	2	
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),	COMMON	3	
1 YSV(30),ZSW(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXN(40),	COMMON	4	
2 FYP(30),FYM(30),FZP(30),FZN(30),DT,TIME	COMMON	5	
COMMON	NOX	2	
1/CINDEF/IDCO,IOFU,IDO2,ION2,ION2O,IDCO2,ION1,ION2,ION1,IONO,IONO2	NOX	3	
1,IDO,IOOH,IOCP5,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NGLOR,NGLORP,	NOX	4	
2 NLM,NO,NSM,NS1,NS2,IOCH	4STEP	3	
3/CHEMI/CPSUP,MSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG	NOX	6	
4/CPARAM/ASUB(30,3),ENV,ER,HSUBO,NDEBUE,NS,PA,QO,Q1,Q2,Q3,Q4,RHOP,	NOX	7	
4 S,SMW(30),SPO,S1(30),S2(30),TK,LADTAB,LDEBUE,LEQUIL,LREACT,	NOX	8	
4 LENER,FONIJ,LCONVG	NOX	9	
DIRLE PRECISION CPSUM,ENV,ER,FQ,HSUBO,MSUM,PA,PPLN,QO,Q1,Q2,Q3,	NOX	10	
1 Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11	
2,FIIT,FST	4STEP	4	
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CERU1,CERU2,	4STEP	5	
1 CERU3,CERU4,AEXP1,AEXP2,AEXP3,AEXP4,DEXP1,DEXP2,DEXP3,DEXP4,	4STEP	6	
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7	
LOGICAL LADTAB,LCONVG,LDERUG,LEQUIL,LNRG,LREACT,LENER	NOX	12	
COMMON/INT/L,M,N,LCV,MCV,KCV,L01,NP1,NP1,N1,NJ,NK,NINJ,NINJNK,NV,	COMMON	6	
1 NNV,NROTO,K,ISTR,KSTR,NVM(33),KM(30),JM(30),ISTEP,	4STEP	8	
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(33),NP,	4STEP	9	
3 NRMN,NGAM,IWL1(30,3),IWL0(30,3),JWL0(40,3),JNL1(40,3),IWE1,	COMMON	9	
4 IWE0,PP1,JW11,JW10,JW11,JW00,ION,JKIN(30,30),IKIN(40,30)	COMMON	10	
COMMON/INDEX/IPAR,LPREF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11	
1,PLAXM1,LVM,LVD,LVFHDX,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10	
2 IJUMP,IRFS,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH2O,NVCO2,	COMMON	13	
3 NVN2,NVCH,NVH2	4STEP	11	
COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVON,LVH2O,LVN2,LVQ2,	NOX	16	
1 LVCO2,LVFU1,LVCO1,NNOX,INOX,ITNOX,SMOX,TNOX	NOX	17	
COMMON/TEMP/NVH,NVFU,NVQX,NVFUQX,NVTE,NODEN,ION,FSTQIC,HFU,CP,	COMMON	15	
1 GASCON,RHCCCN,UNICCN,PRESS,NVFAY,TCYLV,TINLV,TLIP,ACDEF(4),	COMMON	16	
2 T4,DFAC,WFO,WCO2,WCO,WDX,WH2O,WN2,HVY,CXX,RATIN1,RATIO2,	COMMON	17	
3 RATIO3,RATIO4,MCO,TAN,ITWALL	COMMON	18	
COMMON/CTOMA/RENO,ICTOMA(32)	4STEP	12	
COMMON/MIS/AMU,DEN,SMAX,SSUM,LASTEP,HTCEXT,CFR,EMISM,EMISIN,	COMGEN	2	
1 EMISW,TOUT,RTCO,FMI,RADIN,RADSUR,FPA,FR,SQFN,	COMGEN	3	
2 FNFU,FDFU,TFUFL,WFM7,FLO(40),TENTM(40),M(40),FUEL(40),FUOX(40),	COMGEN	4	

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2 UIN(40), TIN(40), FUELS(40), SEXIT, IGAM1(29), IGAM2(29)
COMMON/TURN/NM, NVD, C1, C2, CD, AK, DUIDXJ(3,3), AKFAC, ALFAC,
1 MODEL, PR(32), PRFF(32), PJAY(32), E
COMMON/RAD/NVE, SIGMA, ABSOR, SCATR
COMMON/REACT/ARCON1, PREXP1, CR1, ARCON2, PREXP2, CR2, MODER
COMMON/DROPL/EVAP(192), NTP4, NFN2, XO(3), YO(3), ZO(3), ALFA(3),
1 RETA(3), DELTA(3), THETA1(3), THETA2(3), NSL(3), WFF(3), SMD(3),
2 VFUFL(3), RFUEL(3), EVSU(64), MEVAP
COMMON/INJEC/FLNWIN, IUINJ(20), JUINJ(20), UIIJ(20), WUIIJ(20),
1 AUTIJ(20), TUIIJ(20), IVIJ(20), JVIJ(20), KVIJ(20), VINIJ(20),
2 EVIJ(20), DVIJ(20), AVIJ(20), TVIJ(20), NUIIJ(20), JSW1, JSW2,
3 USW, VSW, AFSW, FSW, TSW, MSW, SWND, RHQSW
COMMON/CSOOT/AVN, NVS1, NVS2, ISOOT, SSOOT, NSOOT, AD, ARCONN, AAA, BBB, FNG
1, GD, MPART, DPART(2), FRACP(2), RHQP, ARCONS, PREXPS, ALPHA, AAS, BBS, DMR
2, LVN, LVS1, LVS2, CINC, TINC, FUTOT
COMMON/CRAO/IRAD, SRAD
COMMON/CFDUR/PREXP3, ARCON3, CR3, PREXP4, ARCON4, CR4, AA1, BB1, CC1,
1 AA2, BB2, CC2, AA3, BB3, CC3, AA4, BB4, CC4, RATIO5, RATIO6, RATIO7,
2 RATIO8, RATIO9, RATIO10, RATIO11, RATIO12, WCH, WH2, WC2H4, LVCH, LVCH1, LVH21
DATA NI, NJ, NK, NNV/10, 10, 5, 29/
DATA AK, E/, 43, 9, /
DATA UNICON, SIGMA/8314., 5.669E-08/
DATA NVK, NVD, NVFUOX, NVFU, NVCH, NVCO, NVH2, NVTE, NVH, NVN, NVS1, NVS2
1/4, 5, 4, 5, 14, 8, 15, 6, 9, 11, 12, 13/
DATA NVFAV, NVRX, NVRY, NVRZ/10, 1, 2, 3/
DATA IDFU, IDC2, IDN2, IDCQ, IDCH, IDH2, IDH2Q, IDCQ2, IDH1, IDN1, IDNO,
1 IDNO2, IDQ, IDQH/1, 2, 3, 4, 5, 6, 7, 8, 9, 10, 11, 12, 13, 14/
DATA NVF/1, 2, 3, 4, 5, 4, 5, 14, 8, 15, 9, 11, 12, 13, 16, 17, 18, 19, 20, 21, 22,
1 23, 24, 25, 26, 27, 28, 29, 1, 2, 3/
DATA LVK, LVD, LVFUOX, LVFU, LVCH, LVCO, LVH2, LVH, LVN, LVS1, LVS2/5, 6,
1 7, 8, 9, 10, 11, 12, 13, 14, 15/
DATA LVFU1, LVCO2, LVN2, LVCO1, LVCH1, LVH21, LVH2Q, LVCO2, LVH1, LVN1,
1 LVNO, LVNO2, LVQ, LVQH/16, 17, 18, 19, 20, 21, 22, 23, 24, 25, 26, 27, 28, 29/
DATA LVRY, LVRY, LVRY/30, 31, 32/
DATA NVH2Q, NVEX, NVCO2, NVN2/1, 2, 3, 4/
DATA NP, NRHO, NGAM/33, 34, 35/
DATA WCO2, WCO, WOX, WH2Q, WN2, WH2, WC2H4/44., 28., 32., 18., 28., 2., 28./
DATA IGSP1, IGAM2/1, 0, 3+1, 24*0, 0, 4+1, 24*0/
DATA ACDEF/-1306, 01, 8620, 37, -6167, 08, 1336, 65/
END
SUBROUTINE INIT
COMMON F(500,7), DU(10,10,5), DV(10,10,5), DW(10,10,5),
1 ANUC(10,10,5), SDO1(10,10,5), SDO2(10,10,5), FCH(10,10,5),
2 FH2(10,10,5), FS(500,14),
1 RHQ(10,10,5), VISC(10,10,5), ABSR(10,10,5), SCTR(10,10,5),
2 SU(10,10), SP(10,10), DRHNDP(10,10,5),
1 AXP(10,10), AXF(10,10), AYP(10,10), AYH(10,10), AZP(10,10),
2 AYH(10,10), CZ(10,10), CY(10), CZU(10,10), CYU(10),
3 CZP(10,10), CYP(10), DIVG(10,10), NTP1, NTP2
1, AXPK(192), AXPK(192), AYMK(192), AYPK(192), AZMK(192), AZPK(192),
2 SHK(192), SPK(192)
DIMENSION U(10,10,5), V(10,10,5), W(10,10,5), PP(10,10,5)
DIMENSION P(10,10,5), TEMP(10,10,5), GAM(10,10,5)
EQUIVALENCE (F(1,1), U(1,1,1)), (F(1,2), V(1,1,1)), (F(1,3), W(1,1,1))
EQUIVALENCE (F(1,4), PP(1,1,1)), (F(1,5), P(1,1,1))
EQUIVALENCE (F(1,6), TEMP(1,1,1)), (F(1,7), GAM(1,1,1))
COMMON/CYL/R(30), RM(30), RMV(30), YSR(30), YSVR(30), IPLAX
COMMON/GRIN/X(40), Y(30), Z(30), XS(40), YS(30), ZS(30), XSU(40),
1 YSV(30), ZSV(30), XDIF(40), YDIF(30), ZDIF(30), FXP(40), FXM(40),
2 FYP(30), FYP(30), FZP(30), FZM(30), DT, TIME
COMMON
1/CINDEX/IDCF, IDFU, IDQ2, IDN2, IDH2Q, IDCQ2, IDH1, IDH2, IDN1, IDNO, IDNO2
1, IDQ, IDQH, IMCP5, ILC, ILH, IMAT, ITER, JJJ, N1, N2, N3, NA, NGL08, NGL08P,
2 NLM, NQ, NSM, NS1, NS2, IOCH
4STEP 13
COMGEN 6
4STEP 14
COMGEN 8
COMGEN 9
COMGEN 10
COMGEN 11
COMGEN 12
COMGEN 13
COMGEN 14
COMGEN 15
COMGEN 16
SOOT 8
SOOT 9
SOOT 10
SOOT 11
4STEP 15
4STEP 16
4STEP 17
4STEP 24
MA 203
MA 204
4STEP 25
4STEP 26
MA 206
4STEP 27
4STEP 28
4STEP 29
4STEP 30
4STEP 31
4STEP 32
4STEP 33
4STEP 34
4STEP 35
MA 210
4STEP 36
4STEP 37
4STEP 38
MA 214
MA 215
NASAX 10
COMFA 2
4STEP 1
4STEP 2
RAD 1
RAD 2
COMFA 4
COMFA 5
COMFA 6
CTOMA 1
CTOPA 2
COMFA 7
COMFA 8
COMFA 9
COMFA 10
COMFA 11
COMMON 2
COMMON 3
COMMON 4
COMMON 5
NOX 2
NOX 3
NOX 4
4STEP 3

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3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG	NOX	6
4/CPARAM/ASUB(30,3),EMV,ER,HSUBO,NDEBUB,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOPP,	NOX	7
4 SM,SMW(30),SPO,S1(30),S2(30),TK,LADIAB,LOEBUG,LEQUIL,LREACT,	NOX	8
4 LENER,FODIJ,LCONVG	NOX	9
DOUBLE PRECISION CPSUM,EMV,ER,FQ,HSUBO,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOPP,SM,SHINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FUT,FST	4STEP	4
COMMON/STFP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,	4STEP	5
1 CFBUS,CERU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADIAB,LCONVG,LOFRUG,LEQUIL,LNRG,LREACT,IENER	NOX	12
COMMON/INT/L,P,N,LCV,NCV,NCV,LP1,MP1,MP1,NI,NJ,MK,NINJ,NINJNK,NV,	COMMON	6
1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVN(35),KH(30),JM(30),ISTEP,	4STEP	8
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,	4STEP	9
3 NRHO,NGAM,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWF1,	COMMON	9
4 TVEO,NM1,JWIT,JWIO,JWOT,JWOO,IOW,JKIN(30,30),TKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LREF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVZ2,JPLANE	COMMON	11
1,PLAXM1,LVK,LVD,LVFUOX,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
2 IJUMP,IRES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH2O,NVCO2,	COMMON	13
3 NVN2,NVCH,NVH2	4STEP	11
COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVD,LVON,LVH2O,LVN2,LVD2,	NOX	16
1 LVCO2,LVFU1,LVCO1,NNOX,INOX,ITNOX,SNOX,TNOX	NOX	17
COMMON/THERM/NVH,NVFU,NVOX,NVFUOX,NVTE,NODEN,IOK,FSTOIC,HFU,CP,	COMMON	15
1 GASCON,RHOCON,UNICON,PRESS,NVFAV,TCYLN,TINLN,TLIP,ACDEF(4),	COMMON	16
2 T4,DFAC,WFU,WCO2,WCO,WDX,WZD,WZ2,HVY,CXX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,WCO,TAN,ITWALL	COMMON	18
COMMON/CTOMA/KEND,ICTOMA(32)	4STEP	12
COMMON/MIS/AMU,DEF,SMAX,SSUM,LASTEP,HTCEXT,CFR,EMISW,EMISIN,	COMGEN	2
1 ENISR,TOUT,RTCD,ONI,RADIN,RADSUR,FMA,FK,SQFK,	COMGEN	3
2 KKFU,FOFU,TFUEL,WFNZ,FLO(40),TENTM(40),H(40),FUEL(40),FUOX(40),	COMGEN	4
2 UIN(40),TIN(40),FUELS(40),SEXIT,IGAM1(29),IGAM2(29)	4STEP	13
COMMON/TURB/NVK,NVD,C1,C2,CO,AK,DUIDX(3,3),AKFAC,ALFAC,	COMGEN	6
1 MODEL,PR(32),PREF(32),PJAY(32),E	4STEP	14
COMMON/RAD/NVE,SIGMA,ABSOR,SCATR	COMGEN	8
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	COMGEN	9
COMMON/DRDPL/EVAP(192),NTP4,NFM7,XO(3),YO(3),ZO(3),ALFA(3),	COMGEN	10
1 BETA(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SND(3),	COMGEN	11
2 VFUEL(3),RFUEL(3),EVSU(64),HEVAP	COMGEN	12
COMMON/INJEC/FLOWIN,TUINJ(20),JUINJ(20),UINJ(20),WUINJ(20),	COMGEN	13
1 AUTNJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	COMGEN	14
2 FVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),WUINJ,NVINJ,JSW1,JSW2,	COMGEN	15
3 USW,VSW,AFSW,FSW,TSW,MSW,SWND,RHOSW	COMGEN	16
COMMON/CSOOT/NVN,NVS1,NVS2,ISOOT,SSOOT,NSOOT,AD,ARCONN,AAA,BBB,FMG	SOOT	8
1,G0,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BBS,OMR	SOOT	9
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT	SOOT	10
COMMON/CRAD/IRAD,SRAD	SOOT	11
COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CF4,AA1,BB1,CC1,	4STEP	15
1 AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2 RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,WZ2,WCH4,LVCH,LVCH1,LVH21	4STEP	17
C ** ** ** **	AL	7
ENTRY START	AL	8
C-----SURROUTINE INIT(ENTRY START) IS USED FOR INITIALIZATION PURPOSES.	COMMENT	10
C-----SOME PRELIMINARY VALUES -----	AL	9
WCO=1.0112E+7	AL	10
RATIO1=WDX*(CXX+HVY/4.)/WFU	AL	11
RATIO2=.232	AL	12
RATIO3=WDX*0.5/WCO	AL	13
RATIO4=WCO*CXX/WFU	AL	14
WCH=12.01*CXX+1.005*(HVY-2.0)	4STEP	39
SMW(INCH)=WCH	4STEP	40
RATIO5=(CXX*(HVY-2.0)+.291*WDX/WCH	4STEP	41
RATIO6=0.25*WCH	4STEP	42
RATIO7=(HVY-2.0)/WCH	4STEP	43
RATIO8=WCH/WFU	4STEP	44

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RATIO9=HYY*WH2/(2.0*WFI)
RATIO10=(HYY-2.0)*WH2/(2.0*WCH)
PATIO1=CXX*WCD/WCH
RATIO12=WH2/WFI
FSTOIC=RATIO2/(RATIO1+RATIO2)
HFU=HFU/1.987
CFR=.003
EMISW=.8
EMISIN=1.
EMISR=1.
UMASS=0.
SMASS=1.E-30
ASW=AFSW-FSW
FUMSW=FSW/AFSW
FUXSW=FUMSW
WSW=SWND*USW
UMASS=AFSW*USW
SPASS=AFSW
FK=ANAX1(10.,AKFAC*(UMASS/SMASS)**2)*FLOAT(MODEL-1)
SQFK=SQRT(FK)
ASWRLR=0.
DO 10 J=JSW1,JSW2
10 ASWRLR=ASWRLR+YSP(J)*(Z(NP1)-Z(1))
ALIN=.9*ALFAC*(Y(JSW2)+Y(JSW2+1)-Y(JSW1)+Y(JSW1-1))
RHOSW=AFSW/ASWRLR/USW
RTCD=SQRT(CD)
DO 40 I=1,LP1
40 FUELS(I)=0.
C-----FUEL INJECTION.
IF (NFMZ.LE.0) GO TO 40
DO 165 II=1,NFMZ
DO 165 I=2,L
IF (XO(II).GT.0.5*(X(II)+X(II+1))) GO TO 165
FUELS(I)=FUELS(I)+WFF(II)
165 CONTINUE
4A FUELS(LP1)=FUELS(L)
WFMZ=FUELS(LP1)
C-----BOUNDARY CONDITIONS.
DO 80 K=1,NP1
DO 82 J=1,MP1
82 JKIN(J,K)=0
DO 90 I=1,LP1
90 IKIN(I,K)=0
DO 86 K=1,NP1
DO 86 J=JSW1,JSW2
86 JKIN(J,K)=1
84 CONTINUE
C-----DILUTION JETS.
9A IF (NVIJ.LE.0) GO TO 92
DO 94 II=1,NVIJ
I=IVIJ(II)
J=JVIJ(II)
K=KVIJ(II)
IF (J.EQ.JMLI(I,4)) GO TO 96
IKIN(I,K)=IKIN(I,K)+2
GO TO 94
96 IKIN(I,K)=IKIN(I,K)+1
94 CONTINUE
C-----FILM COOLING SLOTS.
97 IF (NUIJ.LE.0) GO TO 199
DO 198 II=1,NUIJ
I=IUIJ(II)-1
J=JUJ(II)
IF (J.EQ.JMLI(I,4)+1) GO TO 197

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4STEP	45
4STEP	46
4STEP	47
4STEP	48
AL	15
NOX	48
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COMMENT	11
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COMMENT	12
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COMMENT	13
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COMMENT	14
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AL	71

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      DD 196 K=1,NP1
196 IKIN(I,K)=IKIN(I,K)+2
      GO TO 198
197 DD 195 K=1,NP1
195 IKIN(I,K)=IKIN(I,K)+1
198 CONTINUE
199 CONTINUE
C ----- COMPUTE TOTAL FLOW RATE -----
      94 DD 499 I=1,LP1
        FLO(I)=0.
        FUEL(I)=0.
499 TENTM(I)=0.
        FLQ(I)=AFSW
        FUEL(I)=FSW
        TENTM(I)=AFSW*TSW
C ----- AXIAL INJECTION
        IF (NUINJ.LE.0) GO TO 104
      DD 106 II=1,NUINJ
        I=I+1
        FLO(I)=FLO(I)+AUINJ(II)
106 TENTM(I)=TENTM(I)+TUINJ(II)+AUINJ(II)
C ----- RADIAL INJECTION
      104 IF (NWINJ.LE.0) GO TO 108
      DD 110 II=1,NWINJ
        I=I+1
        FLO(I)=FLO(I)+AVINJ(II)
110 TENTM(I)=TENTM(I)+TVINJ(II)+AVINJ(II)
108 CONTINUE
C ----- FLOW RATE AT EACH I-STATION
      DD 135 I=2,LP1
        FLO(I)=FLO(I-1)+FLO(I)
        FUEL(I)=FUEL(I-1)+FUEL(I)
135 TENTM(I)=TENTM(I-1)+TENTM(I)
        FLOWIN=FLO(LP1)+WFNZ
      DD 145 I=1,LP1
145 FUEL(I)=FUEL(I)/FLO(I)
        FUTOT=FUEL(LP1)+WFNZ
        AMASS=FLO(LP1)-FUEL(LP1)
        FUARAT=FUTOT/AMASS
      DD 150 I=1,LP1
        FUEL1=(FUEL(I)+FUELS(I))/(FLO(I)+FUELS(I))
        FUELF=AMAX1(FUEL1-RATIO2*(1.-FUEL1)/RATIO1,0.)
        PHI=FUEL1/FSTCIC
        IMCPS=3
        NS1=IDFU
        NS2=IDN2
        TK=TSW
        TKINV=1.000/TK
        S2(IDFU)=FUEL1/SMW(IDFU)
        S2(IDO2)=(1.-FUEL1)*RATIO2/SMW(IDO2)
        S2(IDN2)=(1.-FUEL1)*(1.-RATIO2)/SMW(IDN2)
        CALL MCPS
        H1=MSUM*UNICCN*TK
        TIN(I)=TSW
        FUB=FUEL1-FUELF
        FLPCD2=WC02*(CXX*FUB/WFU-CXX*FUNCO/MCH-FUNCO/MCO)
        FLPOX=RATIO1*FUELF+RATIO3*FUNCO+RATIO2*(RATIO1+RATIO2)*FUEL1
1+(RATIO3+RATIO6)*FUNCO
        FLPOX=AMAX1(FLPOX,0.)
        FLPH20=C.9*MH20*(HTY*FUB/WFU-(RATIO7+1.0)*FUNCO)
        FLPH2=1.0-FUELF-FLPCD2-3.0*FUNCO-FLPOX-FLPH20
        IMCPS=4
        NS1=IDFU
        NS2=IDN2

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AL	72
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AL	110
AL	111
AL	112
AL	113
AL	114
NOX	49
NOX	50
NOX	51
NOX	52
NOX	53
NOX	54
NOX	55
NOX	56
NOX	57
NOX	58
AL	117
AL	118
4STEP	49
AL	120
4STEP	50
AL	121
4STEP	51
4STEP	52
NOX	59
NOX	60
NOX	61

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S2(I0FU)=FUELF/SMW(I0FU)
S2(I0O2)=FLPH2/SMW(I0O2)
S2(I0N2)=FLPH2/SMW(I0N2)
S2(I0CC)=FUMCO/SMW(I0CC)
S2(I0CH)=FUMCO/SMW(I0CH)
S2(I0M2)=FUMCO/SMW(I0M2)
S2(I0H2O)=FLPH2O/SMW(I0H2O)
S2(I0CO2)=FLPHCO2/SMW(I0CO2)
C-----IGNITION SEQUENCE.
DO 191 I=1,10
  T=TIN(I)
  TK=T
  TKINV=1.000/TK
  CALL HCPS
  H2=H2SUM*UNICOM*TK
  CPI=CPSUM*UNICOM
  TNEW=T+(H1-H2)/CPI
  TMAX=ACDEF(1)+PHI*(ACDEF(2)+PHI*(ACDEF(3)+PHI*ACDEF(4)))
  TMAX=AMAX1(TMAX,2000.)
  TNEW=AMIN1(TNEW,TMAX)
  IF (ABS(TIN(I)-TNEW).LT.10.) GO TO 190
191 TIN(I)=TNEW
  WRITE (6,196)
196 FORMAT (' **ERROR-100')
190 CONTINUE
  T4=TIN(I*1)
  IMCPS=1
  NS1=I0O2
  NS2=I0N2
  TK=T4
  TKINV=1.000/TK
  S2(I0O2)=RATIO2/SMW(I0O2)
  S2(I0N2)=(1.0-RATIO2)/SMW(I0N2)
  CALL HCPS
  CP=CPSUM*UNICOM
C-----AVERAGE U-VELOCITY AT EACH I-SECTION.
DO 231 I=3,LPI
  J1=JWLI(I,1)
  J2=JWLI(I,1)
  RHO4=PRESS/GASCON/TIN(I-1)
  A4=.5*(Z(NP1)-Z(1))*(RN(J2)**2-RN(J1+1)**2)
  IF (IPLAX.EQ.2) GO TO 231
  Y1=.5*(Y(J1)+Y(J1+1))
  IF (J1.EQ.1) Y1=Y(J1)
  Y2=.5*(Y(J2)+Y(J2-1))
  IF (J2.EQ.MPI) Y2=Y(J2)
  A4=(Z(NP1)-Z(1))*(Y2-Y1)
231 UIN(I)=FLO(I-1)/RHO4/A4
  EMI=EMISW/(2.-EMISW)
  RADIN=EMISIN*SIGMA*TSW**4
  RADSUR=EMISR*SIGMA*T4**4
C-----PRINTOUT INPUT DATA -----
  WRITE (6,1004) TITLE2
1004 FORMAT(1H1,24X,20A4/25X,80(1H-))
  HCRAT=H2Y/CXX
  WRITE (6,2010) HCRAT,MFU,MFU
2010 FORMAT (2X,'1. PHYSICAL INPUT',8X,14(1H-)/10X,'1.FUEL-' /
  4 30X,'HYDROGEN-CARBON RATIO -----',1PE12.4, /
  2 30X,'MOLECULAR WEIGHT-----',1PE12.4,' (KG/KMOLE)' /
  3 30X,'HEAT OF FORMATION-----',1PE12.4,' (CAL/KMOLE)' /
  JJ=1
  WRITE (6,2014) JJ,FSW
2014 FORMAT (30X,'INLET-',11,' MASS FLOW RATE-----',1PE12.4,
  1 ' (KG/S)')
158

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NOX	62
NOX	63
NOX	64
NOX	65
4STEP	53
4STEP	54
NOX	66
NOX	67
COMMENT	19
AL	124
AL	125
NOX	68
NOX	69
NOX	70
NOX	71
NOX	72
AL	130
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NOX	73
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NOX	81
COMMENT	16
AL	141
AL	142
AL	143
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FEB2	1
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WRITE (6,2020) PRESS
2020 FORMAT (10X,'2.AIR -')
3 30X,'PRESSURE-----',1PE12.4,' (NEW/SQ.M)')
WRITE (6,2024) JJ,ASM,JJ,USW,JJ,SWND
2024 FORMAT (30X,'INLET-',I1,' MASS FLOW RATE-----',1PE12.4,
1 ' (KG/S)/30X,'INLET-',I1,' AXIAL VELOCITY-----',1PE12.4,
2 ' (M/S)/30X,'INLET-',I1,' SWIRL NUMBER-----',
3 1PE12.4)
HEIGHT=2.0*(Y(MP1)-Y(1))
ALNGHT=X(LP1)-X(1)
SECTOR=2(MP1)-2(1)
WRITE (6,2025) HEIGHT,ALNGHT,SECTOR
2025 FORMAT (2X,'II. GEOMETRICAL INPUT'/8X,10(1H-)/
1 30X,'CHANNEL HEIGHT OF COMBUSTOR-----',1PE12.4,' (M)'/
2 30X,'LENGTH OF COMBUSTOR-----',1PE12.4,' (M)'/
2 30X,'ANGULAR SECTOR-----',1PE12.4,' (RAD-M)')
WRITE (6,2029) JJ,ASWRLR
2029 FORMAT (30X,'INLET-',I1,' FLOW AREA-----',1PE12.4,
1 ' (SQ.M)')
IF (NUINJ+NVINJ+NFNZ.GT.0) WRITE (6,2130)
2030 FORMAT (2X,'III. AIR INJECTIONS'/8X,14(1H-))
IF (NUINJ.LE.0) GO TO 770
WRITE (6,2031)
2031 FORMAT (10X,'1.FILM COOLING AIR-')
WRITE (6,2033)
2033 FORMAT (25X,'SLOT NO',4X,'I',5X,'J',4X,'K',8X,'U-VELOCITY',
1 5X,'V-VELOCITY',5X,'W-VELOCITY',6X,'MASS FLOW',6X,'FUEL FLOW'/
2 50X,'(M/S)',10X,'(M/S)',10X,'(M/S)',10X,'(KG/S)',9X,'(KG/S)')
DO 772 II=1,NUINJ
I=IUINJ(II)
J=JVINJ(II)
772 WRITE (6,2090) II,I,J,K,UEF,VINJ(II),UEF,AVINJ(II)
770 IF (NVINJ.LE.0) GO TO 774
WRITE (6,2034)
2034 FORMAT (/10X,'2.DILUTION AND SECONDARY AIR-')
WRITE (6,2033)
DO 776 II=1,NVINJ
I=IVINJ(II)
K=KVINJ(II)
J=JVINJ(II)
776 WRITE (6,2090) II,I,J,K,UEF,VINJ(II),UEF,AVINJ(II)
774 CONTINUE
2090 FORMAT (27X,13,4X,13,3X,13,2X,13,8X,1PE10.3,4(5X,1PE10.3))
*10 IF (NFNZ.LE.0) GO TO 813
WRITE (6,816)
*11 FORMAT (/10X,'3.FUEL NOZZLES-'/12X,'XD',8X,'YO',8X,'ZO',6X,'ALFA',
1 5X,'BETA',5X,'DELTA',4X,'THETA1',4X,'THETA2',7X,'NSL',8X,'WFF',
2 7X,'SMD',5X,'VFUEL'/11X,'(M)',7X,'(M)',6X,'(M-R)',4X,'(RAD)',
3 5X,'(RAD)',5X,'(RAD)',5X,'(RAD)',5X,'(RAD)',8X,'-',6X,'(KG/S)',
4 3X,'(MICRON)',2X,'(M/S)')
DO 818 I=1,NFNZ
*NSL=FLOAT(NSL(I))
*11 WRITE (6,819) XD(I),YO(I),ZO(I),ALFA(I),BETA(I),DELTA(I),
1 THETA1(I),THETA2(I),NSL,WFF(I),SMD(I),VFUEL(I)
*119 FORMAT (5X,1P12E10.2)
*113 CONTINUE
WRITE (6,2037) FUTCY,AMASS,FUARAT
2037 FORMAT (/2X,'IV. AIR-FUEL BALANCE'/8X,16(1H-)/
1 30X,'TOTAL FUEL FLOW RATE-----',1PE12.4,' (KG/S)'/
2 30X,'TOTAL AIR FLOW RATE-----',1PE12.4,' (KG/S)'/
3 30X,'FUEL TO AIR RATIO-----',1PE12.4,/)
WRITE (6,2040) CP,ARCON1,PREXP1,CRI,ARCON2,PREXP2,CR2,
1 C1,C2,CD
2040 FORMAT (2X,'V. SOME IMPORTANT QUANTITIES'/8X,24(1H-)/

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SQDT 49
AL 232

1	30X,'SPECIFIC HEAT-----',1PE12.4,' (J/KG-K)'/	AL	233
2	30X,'ACTIVATION ENERGY (1ST) -----',1PE12.4,' (K)'/	AL	234
3	30X,'PRE-EXPONENT (1ST) -----',1PE12.4,/	AL	235
3	30X,'EDDY BREAKUP CONSTANT (1ST) -----',1PE12.4,/	AL	236
7	30X,'ACTIVATION ENERGY (2ND) -----',1PE12.4,' (K)'/	AL	237
8	30X,'PRE-EXPONENT (2ND) -----',1PE12.4,/	AL	238
9	30X,'EDDY BREAKUP CONSTANT (2ND) -----',1PE12.4,/	AL	239
4	30X,'TURB. CONSTANT (C1) -----',1PE12.4,/	AL	240
4	30X,'TURB. CONSTANT (C2) -----',1PE12.4,/	AL	241
4	30X,'TURB. CONSTANT (CD) -----',1PE12.4,/))	SOOT	50
	WRITE(6,2062)PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4	4STEP	55
2062	FORMAT(30X,'PRE-EXPONENT (3RD) -----',1PE12.4/	4STEP	56
1	30X,'ACTIVATION ENERGY (3RD) -----',1PE12.4/	4STEP	57
1	30X,'EDDY BREAKUP CONSTANT (3RD) -----',1PE12.4/	4STEP	58
1	30X,'PRE-EXPONENT (4TH) -----',1PE12.4/	4STEP	59
1	30X,'ACTIVATION ENERGY (4TH) -----',1PE12.4/	4STEP	60
1	30X,'EDDY BREAKUP CONSTANT (4TH) -----',1PE12.4/	4STEP	61
	WRITE(6,2064)AA1,BB1,CC1,AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4	4STEP	62
2064	FORMAT(30X,'SPECIES EXPONENTS,A,B,C(1ST) ---',1P3E12.4/	4STEP	63
1	30X,'SPECIES EXPONENTS,A,B,C(2ND) ---',1P3E12.4/	4STEP	64
1	30X,'SPECIES EXPONENTS,A,B,C(3RD) ---',1P3E12.4/	4STEP	65
1	30X,'SPECIES EXPONENTS,A,B,C(4TH) ---',1P3E12.4/	4STEP	66
	C-----UNIT CONVERSION FOR 4-STEP RATE CONSTANTS.	COMMENT	17
	PREXP1=PREXP1*(WFU**((1.0-AA1)/((WOX**BB1)*(WC2H4**CC1))	4STEP	67
	1*(1.0-0**(-3.0*(AA1+BB1+CC1)))	4STEP	68
	PREXP2=PREXP2*(WC2H4**((1.0-AA2)/((WOX**BB2)*(WFU**CC2))	4STEP	69
	1*(1.0-0**(-3.0*(AA2+BB2+CC2)))	4STEP	70
	PREXP3=PREXP3*(WC2H4**((1.0-AA3)/((WOX**BB3)*(WH2O**CC3))	4STEP	71
	1*(1.0-0**(-3.0*(AA3+BB3+CC3)))	4STEP	72
	PREXP4=PREXP4*(WH2O**((1.0-AA4)/((WOX**BB4)*(WC2H4**CC4))	4STEP	73
	1*(1.0-0**(-3.0*(AA4+BB4+CC4)))	4STEP	74
	PEXP1=ALOG(PREXP1*(WFU**((AA1-1.0)/(WOX**BB1)*(WC2H4**CC1))	4STEP	75
	PEXP2=ALOG(PREXP2*(WC2H4**((AA2-1.0)/(WOX**BB2)*(WFU**CC2))	4STEP	76
	PEXP3=ALOG(PREXP3*(WC2H4**((AA3-1.0)/(WOX**BB3)*(WH2O**CC3))	4STEP	77
	PEXP4=ALOG(PREXP4*(WH2O**((AA4-1.0)/(WOX**BB4)*(WC2H4**CC4))	4STEP	78
	ER1=ARCON1	4STEP	79
	ER2=ARCON2	4STEP	80
	ER3=ARCON3	4STEP	81
	ER4=ARCON4	4STEP	82
	CFBU1=CR1	4STEP	83
	CFBU2=CR2	4STEP	84
	CFBU3=CR3	4STEP	85
	CFBU4=CR4	4STEP	86
	AEXP1=AA1	4STEP	87
	AEXP2=AA2	4STEP	88
	AEXP3=AA3	4STEP	89
	AEXP4=AA4	4STEP	90
	BEXP1=BB1	4STEP	91
	BEXP2=BB2	4STEP	92
	BEXP3=BB3	4STEP	93
	BEXP4=BB4	4STEP	94
	CEXP1=CC1	4STEP	95
	CEXP2=CC2	4STEP	96
	CEXP3=CC3	4STEP	97
	CEXP4=CC4	4STEP	98
	FST=FSTOIC	4STEP	99
	IF(ITRAD.EQ.2)WRITE(6,2041)ARCON,SCATR	SOOT	51
2041	FORMAT(SOOT	52
3	30X,'ABSORPTION COEFFICIENT-----',1PE12.4,/	AL	243
4	30X,'SCATTERING COEFFICIENT-----',1PE12.4,/))	AL	244
	IF(ITRAD.EQ.3)WRITE(6,2043)	SOOT	53
2043	FORMAT(30X,'ABSORPTION AND SCATTERING COEFFICIENTS CALCULATED'))	SOOT	54
	IF(NSOOT.EQ.0)GO TO 401	SOOT	55
	WRITE(6,2045)(OPART(I),I=1,MPART)	SOOT	56

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      DO 203 J=1,MP1
      DO 203 I=1,LP1
      ABSR(I,J,K)=ABSOR
203  SCTR(I,J,K)=SCATR
      RETURN
C ----- ZERO ARRAYS
201  DO 204 NV=1,N1
      DO 204 K=1,NP1
      DO 204 J=1,MP1
      KJM=KN(K)+JM(J)
      DO 204 I=1,LP1
      ABSR(I,J,K)=ABSOR
      SCTR(I,J,K)=SCATR
      LP=KJM+I
204  F(LP,NV)=0.
      DO 205 K=2,N
      DO 205 J=2,M
      KJM=KN(K)+JP(J)
      DO 205 I=2,L
      LP=KJM+I
C-----SPECIES CONCENTRATIONS.
      DO 207 INV=LV02,LV0M
207  F(LP,INV)=1.E-15
      F(LP,NVS1)=1.E-5
      F(LP,NVS2)=1.E-6
209  F(LP,NVN)=1.E0
C +-----+-----+-----+-----+-----+-----+-----+-----+-----+
      DO 451 K=1,NP1
      DO 451 J=2,M
      IS=IWL(I,J,4)
      IE=IWL(I,J,4)
      DO 451 I=IS,IE
      IF (I.EQ.IS) GO TO 452
      U(I,J,K)=UIN(I)
452  W(I,J,K)=0.0
      IF (J.EQ.JWLI(I,4)+1) GO TO 451
      V(I,J,K)=0.0
451  CONTINUE
      IF (IPAR.EQ.2) GO TO 255
      DO 209 K=1,NP1
      DO 209 J=1,MP1
      IS=IWL(I,J,5)
      IE=IWL(I,J,5)
      DO 209 I=IS,IE
209  P(I,J,K)=PRESS
C ----- ROUNDUP NC0ES
255  DO 240 K=1,NP1
      IF (IDW.EQ.1) GO TO 241
      DO 242 I=3,LP1
      J=JWLI(I,4)
      U(I,J,K)=UIN(I)
242  CONTINUE
241  CONTINUE
      DO 244 J=JSM1,JSM2
      I=IWL(I,J,4)+1
      U(I+1,J,K)=USW
      V(I,J,K)=VSW
244  V(I,J+1,K)=VSW
247  CONTINUE
      DO 245 J=1,MP1
      I=IWL(I,J,4)+1
      IF (J.LE.JW01.OR.J.GE.JW00) GO TO 245
      U(I,J,K)=U(I-1,J,K)
245  CONTINUE

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RAD	26
RAD	27
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AL	272
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4STEP	104
AL	275
AL	276
AL	277
AL	278
RAD	30
RAD	31
AL	279
AL	280
SOOT	90
SOOT	91
SOOT	92
SOOT	93
SOOT	94
COMMENT	19
NOX	91
NOX	92
SOOT	95
SOOT	96
SOOT	97
AL	201
AL	202
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AL	207
AL	208
SOOT	98
AL	290
SOOT	99
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AL	319
COMMENT	20
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COMMENT	2
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COMMENT	22
COMMENT	23
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COMMENT	24
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DO 404 J=1,MP1	AL	378
KJM=KM(K)+JM(J)	AL	379
IS=IWL(I,J,5)	AL	380
IE=IWL(I,J,9)	AL	381
DO 406 I=IS,IE	AL	382
LP=KJM+I	AL	383
406 F(LP,NVTE)=TIN(I)	AL	384
IS=IWL(I,J,4)	AL	385
IE=IWL(I,J,4)	AL	386
DO 404 I=IS,IE	AL	387
LP=KJM+I	AL	388
F(LP,NVFUOX)=FUOX(I)	AL	389
F(LP,NVFU)=AMAX1(0.,F(LP,NVFUOX)-RATIO2*(1.-F(LP,NVFUOX))/RATIO1)	AL	390
F(LP,NVCH)=FUPCO	4STEP	105
F(LP,NVH2)=FUPCO	4STEP	106
404 F(LP,NVCC)=FUPCO	AL	391
C -----BOUNDARY NODES	AL	392
DO 495 K=1,MP1	AL	393
DO 206 I=1,LP1	AL	394
J=JWL(I,4)	AL	395
LP=KM(K)+JM(J)+I	AL	396
IF (IDW.EQ.0) GO TO 217	AL	397
TEMP(I,J,K)=TCYLV	AL	398
IF (J.EQ.1) GO TO 208	AL	399
TEMP(I,J,K)=TINLV	AL	400
208 F(LP,NVFUOX)=0.	AL	401
F(LP,NVFU)=0.	AL	402
F(LP,NVCO)=0.	AL	403
F(LP,NVCH)=0.0	4STEP	107
F(LP,NVH2)=0.0	4STEP	108
GO TO 216	AL	404
217 TEMP(I,J,K)=TIN(I)	AL	405
F(LP,NVFUOX)=FUOX(I)	AL	406
FEXIT=FUOX(I)-RATIO2*(1.-FUOX(I))/RATIO1	AL	407
F(LP,NVFU)=AMAX1(FEXIT,0.)	AL	408
F(LP,NVCC)=0.	AL	409
F(LP,NVCH)=0.0	4STEP	109
F(LP,NVH2)=0.0	4STEP	110
216 J=JWL(I,4)	AL	410
LP=KM(K)+JM(J)+I	AL	411
TEMP(I,J,K)=TCYLV	AL	412
IF (J.EQ.MP1) GO TO 444	AL	413
TEMP(I,J,K)=TINLV	AL	414
444 F(LP,NVFU)=0.	AL	415
F(LP,NVCO)=0.	AL	416
F(LP,NVCH)=0.0	4STEP	111
F(LP,NVH2)=0.0	4STEP	112
206 F(LP,NVFUOX)=0.	AL	417
DO 210 J=1,MP1	AL	418
I=IWL(I,J,4)-1	AL	419
LP=KM(K)+JM(J)+I	AL	420
IF (J.GF.JSW1.AND.J.LE.JSW2) GO TO 212	AL	421
TEMP(I,J,K)=TINLV	AL	422
F(LP,NVFUOX)=0.	AL	423
F(LP,NVFU)=0.	AL	424
F(LP,NVCO)=0.	AL	425
F(LP,NVCH)=0.0	4STEP	113
F(LP,NVH2)=0.0	4STEP	114
GO TO 213	AL	426
212 TEMP(I,J,K)=TSW	AL	427
F(LP,NVFUOX)=FUOXSW	AL	428
F(LP,NVFU)=FUMSW	AL	429
F(LP,NVCO)=0.	AL	430
F(LP,NVCH)=0.0	4STEP	115

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      F(LP,NVH2)=0.0
213 I=IWL0(J,4)+1
      LP=KN(K)+JM(J)+I
      IF (J.EY.JW01.AND.J.LY.JW00) GO TO 214
      TEMP(I,J,K)=TINLW
      F(LP,NVFUOX)=0.
      F(LP,NVFU)=0.
      F(LP,NVCO)=0.
      F(LP,NVCH)=0.0
      F(LP,NVH2)=0.0
      GO TO 210
214 F(LP,NVFUOX)=FUOX(LP1)
      FEXIT=FUOX(LP1)-RATIO2*(1.-FUOX(LP1))/RATIO1
      F(LP,NVFU)=AMAX1(FEXIT,0.)
      F(LP,NVTE)=TIN(I)
      F(LP,NVCO)=0.
      F(LP,NVCH)=0.0
      F(LP,NVH2)=0.0
210 CONTINUE
C -----INJECTION POINTS
C-----FILM COOLING SLOTS.
      IF (NUNJ.LE.0) GO TO 495
      DO 218 II=1,NUNJ
      I=IUNJ(II)-1
      J=JUNJ(II)
      LP=KN(K)+JM(J)+I
      F(LP,NVFUOX)=0.
      F(LP,NVFU)=0.
      F(LP,NVCO)=0.
      F(LP,NVCH)=0.0
      F(LP,NVH2)=0.0
218 TEMP(I,J,K)=TUNJ(II)
495 CONTINUE
C-----DILUTION JETS.
      IF (NVINJ.LE.0) GO TO 220
      DO 222 II=1,NVINJ
      I=IVINJ(II)
      J=JVINJ(II)
      K=KVINJ(II)
      LP=KN(K)+JM(J)+I
      F(LP,NVFUOX)=0.
      F(LP,NVFU)=0.
      F(LP,NVCO)=0.
      F(LP,NVCH)=0.0
      F(LP,NVH2)=0.0
222 TEMP(I,J,K)=TVINJ(II)
220 CONTINUE
C ----- HERE PP IS PHI, P IS MFU AND DU IS MCD
      WRITE (NTP1) PP,P,DU
C +-----+-----+-----+-----+-----+-----+-----+-----+-----+
      DO 276 K=1,NP1
      DO 276 J=1,NP1
      IS=IWL1(J,5)
      IE=IWL0(J,5)
      KJM=KN(K)+JM(J)
      DO 276 I=IS,IE
      LP=KJM+I
      T=TEMP(I,J,K)
      FUR=F(LP,NVFUOX)-F(LP,NVFU)
      FLPOX=RATIO1*(F(LP,NVFU)+RATIO3*(F(LP,NVCO)+RATIO2*(RATIO1+RATIO2)*
1 F(LP,NVFUOX)+RATIO5*(F(LP,NVCH)+RATIO6*(F(LP,NVH2)
      FLPOX=AMAX1(FLPOX,0.)
      FLPH20=0.5*(H20*(HYY*FUR/MFU-RATIO7*(F(LP,NVCH)-F(LP,NVH2))
      FLPC02=MCD02*(CXX*FUR/MFU-CXX*(F(LP,NVCH)/MCH-F(LP,NVCO)/MCD)

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2 FYP(30),FYM(30),F7P(30),F2M(30),DT,TIME	COMMON	5
COMMON	NOX	2
1/CINDFX/IDCO,IOFU,IOO2,ION2,IOH2O,IOCO2,IONH,IOH2,ION1,IONO,IONO2	NOX	3
1,IOO,IOCH,INCP3,ILC,ILH,IMAT,ITER,JJJ,M1,M2,M3,MA,NGLON,NGLNAP,	NOX	4
2 NLM,NO,NSP,NS1,NS2,IOCH	4STEP	3
3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRC	NOX	6
4/CPARAM/ASUB(30,3),ENV,ER,HSUBO,MODRUG,MS,PA,QO,Q1,Q2,Q3,Q4,RHOPP,	NOX	7
4 SM,SMW(30),SMO,Q1(30),S2(30),TK,LADIAB,LOFBUG,LEQUIL,LREACT,	NOX	8
4 LENER,EDFIJ,LCONVG	NOX	9
DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUBO,HSUM,PA,PPLN,QO,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOPP,SM,SHINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FUT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,	4STEP	5
1 CFBUS,CEBU4,AEXP1,AEXP2,AEXP3,AEXP4,DEXP1,DEXP2,DEXP3,DEXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADIAB,LCONVG,LODRUG,LEQUIL,LNRC,LREACT,LENER	NOX	12
COMMON/INT/L,P,N,LCV,MCV,NCV,LP1,MP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,	COMMON	6
1 NVV,NGDO,K,ISTR,JSTR,KSTR,NVM(30),NM(30),JM(30),ISTEP,	4STEP	8
2 ISOLVF(32),IPPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(33),NP,	4STEP	9
3 NRHO,NGAM,INLX(30,5),INLO(30,5),JWLO(40,5),JWLI(40,5),IWI(1,	COMMON	9
4 IWEQ,PM1,JWIT,JWIO,JWOT,JWOO,IDW,JKTIN(30,30),IKIN(40,32,	COMMON	10
COMMON/INDEX/IPAR,LPRFF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1,PLXN1,LVK,LVD,LVFUOX,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
2 TJUMP,IRFS,TITLF2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH2O,NVCO2,	COMMON	13
3 NVN2,NVCH,NVH2	4STEP	11
COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVON,LVH2O,LVN2,LVO2,	NOX	16
1 LVCO2,LVFU1,LVCO1,NNOX,INOX,ITNOX,SNOK,TNOX	NOX	17
COMMON/THERM/NVH,NVFU,NVOX,NVFOUX,NVTE,MODEN,IOK,FSTOIC,HFU,CP,	COMMON	15
1 GASCON,RHOCN,UNICON,PRESS,NVFAV,TCYLW,TINLW,TLIP,ACOE(4),	COMMON	16
2 T4,OFAC,MFU,WCO2,WCO,WDX,WH2O,WN2,HVY,CXX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,HCO,TAN,ITWALL	COMMON	18
COMMON/CTOMA/KEND,ICTOMA(32)	4STEP	12
COMMON/MIS/AMU,DEN,SNAX,SSUM,LASTEP,HTCEXT,CFR,EMISW,EMISIN,	CONGEN	2
1 EMISR,TOUT,RTCO,EMI,RADIN,RANSUR,FMA,FK,SQFK,	CONGEN	3
2 KFU,FDFU,TFUEL,WFN7,FLO(40),TENTH(40),H(40),FUEL(40),FUOX(40),	CONGEN	4
2 UIN(40),TIN(40),FUELS(40),SEXIT,IGAM1(29),IGAM2(29)	4STEP	13
COMMON/TURB/NVK,NVD,C1,C2,C0,AK,QUIDXJ(3,3),AKFAC,ALFAC,	CONGEN	6
1 MODEL,PR(32),PREF(32),PJAY(32),E	4STEP	14
COMMON/RAD/NVE,SIGMA,ABSOR,SCATR	CONGEN	8
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	CONGEN	9
COMMON/DROPL/EVAP(192),NTP4,NFNZ,XO(3),YO(3),ZO(3),ALFA(3),	CONGEN	10
1 BETA(3),DELTA(3),THETA1(3),THETA2(3),MSL(3),WFF(3),TMD(3),	CONGEN	11
2 VFUEL(3),RFUEL(3),EVSU(64),HEVAP	CONGEN	12
COMMON/INJEC/FLOWIN,IUINJ(20),JUINJ(20),UTNJ(20),WUINJ(20),	CONGEN	13
1 AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	CONGEN	14
2 EVINJ(20),OVINJ(20),AVINJ(20),TVINJ(20),NUINJ,NVINJ,JSW1,JSW2,	CONGEN	15
3 USW,VSW,AFSW,FSW,TSW,VSW,SAND,RHOSW	CONGEN	16
COMMON/CSOOT/NVM,NVS1,NVS2,ISOOT,SSOOT,MSOOT,AD,ARCONN,AAA,BBB,FMG	SOOT	8
1,GO,MPART,DPART(2),FRACP(2),RHOP,PREXPS,ALPHA,AAS,ABS,DHR	SOOT	9
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT	SOOT	10
COMMON/CRAD/TRAD,SRAD	SOOT	11
COMMON/CEBUR/PEXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BB1,CC1,	4STEP	15
1 AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2 RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,WH2,WC2H4,LVCH,LVCH1,LVH21	4STEP	17
C ** ** ** **	AL	512
ENTRY FMOD	AL	513
C-----ENTRY FMOD IS USED TO UPDATE BOUNDARY VALUES AND TO LIMIT	COMMENT	28
C SPECIES MASS FRACTIONS TO LIE BETWEEN 0.0 AND 1.0.	COMMENT	29
NVFF=NVF(INV)	AL	514
IF(NV,ME,LVN)GO TO 1210	SOOT	102
C-----NUCLEI CONCENTRATION.	COMMENT	30
DO 1211 K=2,N	SOOT	103
DO 1211 J=2,M	SOOT	104
KJM=KM(K)+JM(J)	SOOT	105

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DO 1211 I=2,L	SQOT	106
LP=KJM+1	SQOT	107
1211 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0)	SQOT	108
1210 IF(NV.LT.LVS1.OR.NV.GT.LVS2)GO TO 1310	SQOT	109
C-----SOOT CONCENTRATION.	COMMENT	31
DO 1311 K=2,N	SQOT	110
DO 1311 J=2,N	SQOT	111
KJM=KM(K)+JM(J)	SQOT	112
DO 1311 I=2,L	SQOT	113
LP=KJM+1	SQOT	114
F(LP,NVFF)=AMAX1(F(LP,NVFF),1.E-30)	SQOT	115
1311 F(LP,NVFF)=AMIN1(F(LP,NVFF),1.0)	SQOT	116
1310 CONTINUE	SQOT	117
C-----SYMMETRY AXIS UPDATING.	COMMENT	32
IF(NV.EQ.2)GO TO 1044	NASAX	11
DO 1005 J=1,NP1	NASAX	12
DO 1005 K=2,N	NASAX	13
LP=LP1+JM(J)+KM(K)	NASAX	14
LPN=LP-1	NASAX	15
1005 F(LP,NVFF)=F(LP,NVFF)	NASAX	16
IF(IDW.NE.0)GO TO 1044	NASAX	17
DO 1006 I=2,LP1	NASAX	18
DO 1006 K=2,N	NASAX	19
LP=I+KM(K)	NASAX	20
LPN=LP+JM(2)	NASAX	21
1006 F(LP,NVFF)=F(LP,NVFF)	NASAX	22
C-----CYCLIC BOUNDARY CONDITIONS	AL	515
1044 DO 1002 J=1,NP1	AL	516
DO 1002 I=1,LP1	AL	517
LIJ=I+JM(J)	AL	518
LP2=I+JM(J)+KM(2)	AL	519
LPN=LIJ+KM(N)	AL	520
LPNP1=LIJ+KM(NP1)	AL	521
F(LIJ,NVFF)=F(LP,NVFF)	AL	522
F(LPNP1,NVFF)=F(LP2,NVFF)	AL	523
1002 CONTINUE	AL	524
1001 CONTINUE	AL	525
IF(NV.NE.LVFUOX)GO TO 1010	4STEP	132
C-----MIXTURE FRACTION.	COMMENT	33
DO 1020 K=1,NP1	AL	527
DO 1020 J=1,NP1	AL	528
KJM=KM(K)+JM(J)	AL	529
DO 1020 I=1,LP1	AL	530
LP=KJM+1	AL	531
F(LP,NVFF)=AMAX1(F(LP,NVFF),0.)	AL	532
F(LP,NVFF)=AMIN1(F(LP,NVFF),1.0)	4STEP	133
1020 CONTINUE	AL	534
GO TO 1036	4STEP	134
1010 IF(NV.NE.LVFU)GO TO 1030	4STEP	135
C-----FUEL CONCENTRATION.	COMMENT	34
DO 1031 K=1,NP1	4STEP	136
DO 1031 J=1,NP1	4STEP	137
KJM=KM(K)+JM(J)	4STEP	138
DO 1031 I=1,LP1	4STEP	139
LP=KJM+1	4STEP	140
F(LP,NVFF)=AMIN1(F(LP,NVFF),F(LP,NVFUOX))	4STEP	141
1031 F(LP,NVFF)=AMAX1(F(LP,NVFF),0.0)	4STEP	142
GO TO 1036	4STEP	143
1030 IF(NV.NE.LVCHI)GO TO 1032	4STEP	144
C-----INTERMEDIATE HYDROCARBON CONCENTRATION.	COMMENT	35
DO 1033 K=1,NP1	4STEP	145
DO 1033 J=1,NP1	4STEP	146
KJM=KM(K)+JM(J)	4STEP	147
DO 1033 I=1,LP1	4STEP	148

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LP=KJM+1	4STEP	149
F(LP,NVFF)=AMIN1(F(LP,NVFF),RATIO8*(F(LP,NVFUOX)-F(LP,NVFU)))	4STEP	150
1033 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0E-5)	MAR2	1
GO TO 1036	4STEP	152
1032 IF(NV.NE.LVCG)GO TO 1034	4STEP	153
C-----C1 CONCENTRATION.	COMMENT	36
DO 1035 K=1,NP1	4STEP	154
JO 1035 J=1,MP1	4STEP	155
KJM=KM(K)+JM(J)	4STEP	156
JO 1035 I=1,LP1	4STEP	157
LP=KJM+1	4STEP	158
F(LP,NVFF)=AMIN1(F(LP,NVFF),RATIO4*(F(LP,NVFUOX)-F(LP,NVFU)))	4STEP	159
I=RATIO10*(F(LP,NVCH))	4STEP	160
1035 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0E-5)	MAR2	2
GO TO 1036	4STEP	162
1034 IF(NV.NE.LVMZ)GO TO 1036	4STEP	163
C-----C2 CONCENTRATION.	COMMENT	37
DO 1037 K=1,NP1	4STEP	164
JO 1037 J=1,MP1	4STEP	165
KJM=KM(K)+JM(J)	4STEP	166
JO 1037 I=1,LP1	4STEP	167
LP=KJM+1	4STEP	168
F(LP,NVFF)=AMIN1(F(LP,NVFF),RATIO9*(F(LP,NVFUOX)-F(LP,NVFU)))	4STEP	169
I=RATIO10*(F(LP,NVCH))	4STEP	170
1037 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0E-5)	MAR2	3
1036 CONTINUE	4STEP	172
RETURN	AL	536
C ** ** ** **	AL	537
ENTRY VELMOD	AL	538
C-----ENTRY VELMOD IS USED FOR VELOCITY MODIFICATIONS.	COMMENT	38
C	COMMENT	39
C-----INTRODUCE SWIRL GRADUALLY.	COMMENT	40
DO 1000 K=1,NP1	AL	539
JO 1000 J=JSH1,JSH2	AL	540
WIN=WSW*(J)/K(JSH2)	AL	541
I=INLI(J,4)-1	AL	542
W(I,J,K)=W(I,J,K)+0.05*WIN	AL	543
IF (ABS(W(I,J,K)).GT.ABS(WIN)) W(I,J,K)=WIN	AL	544
1000 CONTINUE	AL	545
1003 CONTINUE	AL	546
DO 2005 J=2,M	AL	547
DO 2005 I=2,L	AL	548
W(I,J,2)=W(I,J,NP1)	AL	549
2007 DW(I,J,2)=DW(I,J,NP1)	AL	550
2005 CONTINUE	AL	551
C ----- SATISFY CONTINUITY AT EXIT PLANE	AL	552
RHUA=0.0	AL	553
FLJWOT=0.0	AL	554
INJX=0	AL	555
DO 755 K=2,N	AL	556
JS=JMLI(LP,4)+1	AL	557
JL=JMLI(LP1,4)-1	AL	558
DO 755 J=JS,JL	AL	559
RHJ(LP,J,K)=RHQ(L,J,K)	AL	560
RUA=YSH(J)*ZS(K)*RHQ(LP1,J,K)	AL	561
RHJA=RHUA+ROA	AL	562
FLJWOT=FLJWOT+U(L,J,K)*ROA	AL	563
IF (U(L,J,K).GE.0.0) GO TO 755	AL	564
INJX=1	AL	565
755 CONTINUE	AL	566
QADD=(FLJWOT-FLJWOT)/RHUA	AL	567
SXIT=1.-FLJWOT/FLJWOT	AL	568
QMEAN=FLJWOT/RUA	AL	569
DO 755 K=2,N	AL	570

JS=JWLI(LP1,4)+1	AL	571
JE=JWLO(LP1,4)-1	AL	572
DO 756 J=JS,JE	AL	573
U(LP1,J,K)=AFAX1(0.0,U(L,J,K)+UADD)	NASAX	21
756 CONTINUE	AL	570
RETURN	AL	579
C ** ** ** **	AL	580
ENTRY DENMOD	AL	581
C-----ENTRY DENMOD IS USED FOR MODIFYING DENSITIES AT RADIAL	COMMENT	41
C INJECTION HOLES, INLET SWIRLER, AND FILM COOLING SLOTS.	COMMENT	42
C	COMMENT	43
IF (NVINJ.LE.0) GO TO 750	AL	582
C-----RADIAL INJECTION.	COMMENT	44
DO 749 II=1,NVINJ	AL	583
I=IVINJ(II)	AL	584
K=KVINJ(II)	AL	585
J=JVINJ(II)	AL	586
M1=J	AL	587
IF (J.FQ.JWLI(I,4)) M1=J+1	AL	588
AREA=XS(I)*RM(M1)*ZS(K)	AL	589
RHOINJ=AVINJ(II)/ABS(VINJ(II))/AREA	AL	590
749 RHO(I,J,K)=RHOINJ	AL	591
750 CONTINUE	AL	592
C-----CYCLIC BOUNDARY CONDITIONS.	COMMENT	45
DO 2060 J=2,M	AL	593
DO 2060 I=2,L	AL	594
RHO(I,J,NP1)=.5*(RHO(I,J,2)+RHO(I,J,M))	AL	595
RHO(I,J,1)=RHO(I,J,NP1)	AL	596
2060 CONTINUE	AL	597
C-----INLET SWIRLER.	COMMENT	46
DO 760 K=1,NP1	AL	598
DO 2061 J=JSW1,JSW2	AL	599
I=IWL(I,J,4)-1	AL	600
2061 RHO(I,J,K)=RHOISW	AL	601
2099 CONTINUE	AL	602
C-----FILM COOLING SLOTS.	COMMENT	47
2064 IF (NUINJ.LE.0) GO TO 760	AL	603
DO 759 II=1,NUINJ	AL	604
I=IUINJ(II)-1	AL	605
J=JUINJ(II)	AL	606
AREA=YSR(J)*(Z(NP1)-Z(1))	AL	607
759 RHO(I,J,K)=2.*AUINJ(II)/AREA/UNJ(II)-RHO(I+1,J,K)	AL	608
760 CONTINUE	AL	609
RETURN	AL	610
C ** ** **	AL	611
ENTRY GAMOD	AL	612
C-----ENTRY GAMOD IS USED TO CALCULATE WALL GAMAS FROM THE WALL	COMMENT	48
C FUNCTIONS.	COMMENT	49
C	COMMENT	50
DO 3000 K=1,NP1	AL	613
DO 3007 I=1,LP1	AL	614
J=JWLO(I,4)	AL	615
IF (IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3) GO TO 3003	AL	616
IF (IGAM1(NV).EQ.0) GO TO 3003	AL	617
VPLUS=VISC(I,J,K)	AL	618
IF (YPLUS.GT.11.5) GO TO 3001	AL	619
GAM(I,J,K)=AMU/PR(NV)	AL	620
GO TO 3002	AL	621
3001 GAM(I,J,K)=AMU*VPLUS/PREF(NV)/(ALOG(E*VPLUS)/AK+PJAY(NV))	AL	622
GO TO 3002	AL	623
3003 GAM(I,J,K)=0.	AL	624
3002 J=JWLI(I,4)	AL	625
IF (IDW.EQ.0.OR.IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3) GO TO 3004	AL	626
IF (IGAM1(NV).EQ.0) GO TO 3004	AL	627

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YPLUS=VISC(I,J,K)	AL	628
IF (YPLUS.GT.11.5) GO TO 3006	AL	629
GAM(I,J,K)=AMU/PR(NV)	AL	630
GO TO 3007	AL	631
3006 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E+YPLUS)/AK+PJAY(NV))	AL	632
GO TO 3007	AL	633
3004 GAM(I,J,K)=0.	AL	634
3007 CONTINUE	AL	635
DO 3000 J=2,M	AL	636
I=IWL(I(J,4))-1	AL	637
IF (JKIN(J,K).EQ.1) GO TO 3009	AL	638
IF (IGAM2(NV).EQ.0) GO TO 3009	AL	639
YPLUS=VISC(I,J,K)	AL	640
IF (YPLUS.GT.11.5) GO TO 3019	AL	641
GAM(I,J,K)=AMU/PR(NV)	AL	642
GO TO 3011	AL	643
3019 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E+YPLUS)/AK+PJAY(NV))	AL	644
GO TO 3011	AL	645
3009 GAM(I,J,K)=0.	AL	646
3011 I=IWL(I(J,4))+1	AL	647
IF (J.GT.JWCI.AND.J.LT.JWCO) GO TO 3012	AL	648
IF (IGAM2(NV).EQ.0) GO TO 3012	AL	649
YPLUS=VISC(I,J,K)	AL	650
IF (YPLUS.GT.11.5) GO TO 3013	AL	651
GAM(I,J,K)=AMU/PR(NV)	AL	652
GO TO 3000	AL	653
3013 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E+YPLUS)/AK+PJAY(NV))	AL	654
GO TO 3000	AL	655
3012 GAM(I,J,K)=0.	AL	656
3000 CONTINUE	AL	657
CYCLIC BOUNDARY CONDITIONS.	COMMENT	51
DO 3014 I=2,L	AL	658
DO 3014 J=2,M	AL	659
GAM(I,J,1)=.5*(GAM(I,J,2)+GAM(I,J,N))	AL	660
GAM(I,J,NP1)=GAM(I,J,1)	AL	661
IF (NV.EQ.3) GAM(I,J,NP1)=GAM(I,J,2)	AL	662
3014 CONTINUE	AL	663
RETURN	AL	664
C ** ** ** **	AL	665
ENTRY SONAS	AL	666
C-----ENTRY SONAS IS USED TO INCLUDE THE SPRAY EVAPORATION TERM	COMMENT	52
C IN THE VARIOUS EQUATIONS.	COMMENT	53
C	COMMENT	54
DO 124 I=1,LP1	AL	667
DO 124 J=1,NP1	AL	668
124 DIVG(I,J)=0.	AL	669
GO TO (266,267,268,269), NGOTO	AL	670
C ----- U-VELOCITY	AL	671
266 CONTINUE	AL	672
270 IF (MFNZ.LE.0) GO TO 271	AL	673
DO 273 J=2,M	AL	674
KJK=(K-2)*(N)-2*(NJ-2)+(J-2)*(NI-2)	AL	675
IS=IWL(I,J,NGOTO)	AL	676
IE=IWL(I,J,NGCTO)	AL	677
DO 273 I=IS,IE	AL	678
LPC=KJK+(I-1)	AL	679
LYMC=LPC-1	AL	680
DIVG(I,J)=DIVG(I,J)-FKM(I-1)*EVAP(LXMC)-FKP(I)*EVAP(LPC)	AL	681
IF (I.EQ.3) DIVG(I,J)=DIVG(I,J)-FXP(2)*EVAP(LXMC)	AL	682
IF (I.EQ.L) DIVG(I,J)=DIVG(I,J)-FKM(L)*EVAP(LPC)	AL	683
273 CONTINUE	AL	684
271 CONTINUE	AL	685
RETURN	AL	686
C ----- V-VELOCITY	AL	687

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267 CONTINUE	AL	688
274 IF (NFN7.LE.0) GO TO 276	AL	689
DO 277 J=2,M	AL	690
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	691
IS=IWL1(J,NGOTO)	AL	692
IE=IWL0(J,NGOTO)	AL	693
DO 277 I=IS,IE	AL	694
LPC=KJK+(I-1)	AL	695
LYMC=LPC-(NI-2)	AL	696
DIVG(I,J)=DIVG(I,J)-FYM(J-1)*EVAP(LYMC)-FYP(J)*EVAP(LPC)	AL	697
IF (J.EQ.3) DIVG(I,J)=DIVG(I,J)-FYP(2)*EVAP(LYMC)	AL	698
IF (J.EQ.M) DIVG(I,J)=DIVG(I,J)-FYM(M)*EVAP(LPC)	AL	699
277 CONTINUE	AL	700
276 CONTINUE	AL	701
RETURN	AL	702
C ----- W-VELOCITY	AL	703
268 CONTINUE	AL	704
278 IF (NFN2.LE.0) GO TO 281	AL	705
DO 282 J=2,M	AL	706
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	707
IS=IWL1(J,NGOTO)	AL	708
IE=IWL0(J,NGOTO)	AL	709
DO 282 I=IS,IE	AL	710
LPC=KJK+(I-1)	AL	711
LZMC=LPC-(NI-2)*(NJ-2)	AL	712
LIJ=(J-2)*(NI-2)+(I-1)	AL	713
DIVG(I,J)=DIVG(I,J)-FZMK-1)*EVAP(LZMC)	AL	714
IF (K.LT.NP1) DIVG(I,J)=DIVG(I,J)-FZP(K)*EVAP(LPC)	AL	715
IF (K.EQ.NP1) DIVG(I,J)=DIVG(I,J)-FZP(2)*EVAP(LIJ)	AL	716
282 CONTINUE	AL	717
281 CONTINUE	AL	718
RETURN	AL	719
C ----- OTHER VARIABLES	AL	720
269 CONTINUE	AL	721
283 IF (NFN7.LE.0) GO TO 285	AL	722
DO 286 J=2,M	AL	723
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)	AL	724
IS=IWL1(J,NGOTO)	AL	725
IE=IWL0(J,NGOTO)	AL	726
DO 286 I=IS,IE	AL	727
LPC=KJK+(I-1)	AL	728
DIVG(I,J)=DIVG(I,J)-EVAP(LPC)	AL	729
286 CONTINUE	AL	730
285 CONTINUE	AL	731
RETURN	AL	732
C ** ** ** **	AL	733
ENTRY SOMOD	AL	734
C-----ENTRY SOMOD IS USED TO INTRODUCE THE BOUNDARY CONDITIONS	COMMENT	95
C BY MODIFYING THE SOURCE TERMS.	COMMENT	96
C	COMMENT	97
COME HERE FOR SLOT COEFFICIENT MODS.	AL	735
94 IF (NUINJ.LE.0) GO TO 92	AL	736
DO 49 II=1,NUINJ	AL	737
I=IUINJ(II)	AL	738
J=JUINJ(II)	AL	739
IF (J.EQ.JWLI(I,4)+1) GO TO 149	AL	740
M1=J-1	AL	741
IF (NV.EQ.1) AYP(I,M1)=.5*AYP(I,M1)	AL	742
IF (NV.EQ.1) AYP(I-1,M1)=.5*AYP(I-1,M1)	AL	743
IF (NV.GT.2) AYP(I-1,M1)=0.	AL	744
IF (NV.NF.1) AYP(I-2,J)=0.	AL	745
IF (NV.FQ.LVRX) AXM(I,J)=0.	AL	746
GO TO 49	AL	747
149 M1=J+1	AL	748


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S2(IDN2)=(1.0-RATIO2)/SMW(IDN2)
CALL HCPS
HPI=HSUM*UNICON*TK
SU(I,J)=1.E30*HPI
736 SP(I,J)=1.E30
802 CONTINUE
COME HERE FOR INLET WALL SOURCE TERMS
DO 803 J=2,M
I=IWL(I,J,NGOTO)
IF (JKIN(I,J,K).EQ.1) GO TO 1003
HTC=.5*(W(I,J,K)+W(I,J,K+1))*RHO(I,J,K)*CFR
HTC=ABS(HTC)
AREA=YSR(J)*ZS(K)
SU(I,J)=SU(I,J)+HTC*AREA*CP*(TINLW-TEMP(I,J,K))
1003 I=IWL(I,J,NGOTO)
IF (J.GT.JWOL.AND.J.LT.JWOD) GO TO 803
LP=I+JW(J)+KN(K)
HTC=.5*(W(I,J,K)+W(I,J,K+1))*RHO(I,J,K)*CFR
HTC=ABS(HTC)
AREA=YSR(J)*ZS(K)
SU(I,J)=SU(I,J)+HTC*AREA*CP*(TINLW-TEMP(I,J,K))
803 CONTINUE
COME HERE FOR DROPLET EVAPORATION TERMS
IF (NPNZ.LE.0) GO TO 319
DO 316 J=2,M
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)
IS=IWL(I,J,NGOTO)
IE=IWL(I,J,NGOTO)
DO 316 I=IS,IE
LPC=KJK*(I-1)
IHCP5=3
NS1=IDFU
NS2=IDFU
TK=TFUEL
TKINV=.000/TK
S2(IDFU)=1.000/SMW(IDFU)
HDFU=HSUM*UNICON*TK
SU(I,J)=SU(I,J)+EVAP(LPC)*HDFU
316 SP(I,J)=SP(I,J)-EVAP(LPC)
319 CONTINUE
C +---+---+---+---+---+---+ PHI (TOTAL FUEL) +---+---+---+---+---+---+
800 IF (INV.NE.LVFUOX) GO TO 850
COME HERE FOR SLOT MODIFICATIONS
IF (NUINJ.LE.0) GO TO 851
DO 737 II=1,NUINJ
I=IUINJ(II)-1
J=JUINJ(II)
SU(I,J)=0.
737 SP(I,J)=1.E30
851 CONTINUE
COME HERE FOR DROPLET EVAPORATION TERMS
IF (NPNZ.LE.0) GO TO 317
DO 318 J=2,M
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)
IS=IWL(I,J,NGOTO)
IE=IWL(I,J,NGOTO)
DO 318 I=IS,IE
LPC=KJK*(I-1)
SU(I,J)=SU(I,J)+EVAP(LPC)
318 SP(I,J)=SP(I,J)-EVAP(LPC)
317 CONTINUE
C +---+---+---+---+---+---+ FUEL +---+---+---+---+---+---+
890 IF (INV.NE.LVFU) GO TO 941
COME HERE FOR SLOT MODIFICATIONS

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NOX	115
NOX	116
NOX	117
AL	998
AL	999
AL	1000
AL	1001
AL	1002
AL	1003
AL	1004
AL	1005
AL	1006
AL	1007
AL	1008
AL	1009
AL	1010
AL	1011
AL	1012
AL	1013
AL	1014
AL	1015
AL	1016
AL	1017
AL	1018
AL	1019
AL	1020
AL	1021
AL	1022
AL	1023
AL	1024
NOX	118
NOX	119
NOX	120
NOX	121
NOX	122
NOX	123
NOX	124
NOX	125
AL	1026
AL	1027
AL	1028
AL	1029
AL	1030
AL	1031
AL	1032
AL	1033
AL	1034
AL	1035
AL	1036
AL	1037
AL	1038
AL	1039
AL	1040
AL	1041
AL	1042
AL	1043
AL	1044
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AL	1046
AL	1047
AL	1048
AL	1049
AL	1050
AL	1051

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      SU(I,J)=0.0
1308 SP(I,J)=-1.0E30
C----- HERE FOR DRCLFT EVAPORATION TERMS
1303 IF (NFWZ.LE.C) GO TO 1305
      DO 1306 J=2,M
      KJK=(K-2)*(NI-2)*(NJ-2)*(J-2)*(MI-2)
      IS=IWL(I,J,NGOTD)
      IE=IWL(I,J,NGOTD)
      DO 1306 I=IS,IE
      LPC=KJK+I-1
1306 SP(I,J)=SP(I,J)-EVAP(LPC)
1305 CONTINUE
      RETURN
C +---+---+---+---+---+---+ X-DIRECTION RADIATION +---+---+---+---+---+---+
1300 IF (NV.NE.LVRX) GO TO 910
C----- INLET BOUNDARY.
      DO 901 J=2,M
      I=IWL(I,J,NGOTC)
      IF (JKIN(I,K).EQ.1) GO TO 902
      TEMPW=TEMP(I-1,J,K)
      SU(I,J)=SU(I,J)+EMI*SIGNA*TEMPW**4
      SP(I,J)=SP(I,J)-EMI
      GO TO 1901
902 CONTINUE
      SU(I,J)=SU(I,J)+RADIN
      SP(I,J)=SP(I,J)-1.
C----- OUTLET BOUNDARY.
1901 I=JWL(I,J,NGOTC)
      IF (J.GT.JMOI.AND.J.LT.JMOO) GO TO 1902
      TEMPW=TEMP(I+1,J,K)
      SU(I,J)=SU(I,J)+EMI*SIGNA*TEMPW**4
      SP(I,J)=SP(I,J)-EMI
      GO TO 901
1902 CONTINUE
      SU(I,J)=SU(I,J)+RADSR
      SP(I,J)=SP(I,J)-1.
901 CONTINUE
C----- HERE FOR SLOT MODIFICATIONS
      IF (NUINJ.LE.C) GO TO 903
      DO 743 II=1,NUINJ
      I=IUIINJ(II)-1
      J=JUINJ(II)
      SU(I+1,J)=SU(I+1,J)+EMISR*SIGNA*TEMP(I,J,K)**4
      SP(I+1,J)=SP(I+1,J)-1
      TEMPW=TLIP
      SU(I-1,J)=SU(I-1,J)+EMI*SIGNA*TEMPW**4
      SP(I-1,J)=SP(I-1,J)-EMI
743 CONTINUE
C +---+---+---+---+---+---+ Y-DIRECTION RADIATION +---+---+---+---+---+---+
910 IF (NV.NE.LVRY) GO TO 920
      DO 911 I=2,L
C----- TOP WALL.
      J=JWL(I,NGOTC)-1
      IF (IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3) GO TO 904
      TEMPW=TEMP(I,J+1,K)
      SU(I,J)=SU(I,J)+EMI*SIGNA*TEMPW**4*RN(J+1)
      SP(I,J)=SP(I,J)-EMI*RN(J+1)
      GO TO 905
904 SU(I,J)=SU(I,J)+RADIN*RN(J+1)
      SP(I,J)=SP(I,J)-RN(J+1)
905 IF (IDW) 911,911,1911
C----- BOTTOM WALL.
1911 J=JWL(I,NGOTC)+1
      IF (IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3) GO TO 906

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SOOT	145
SOOT	146
SOOT	147
SOOT	148
SOOT	149
SOOT	150
SOOT	151
SOOT	152
SOOT	153
SOOT	154
SOOT	155
SOOT	156
SOOT	157
AL	1089
SOOT	158
COMMENT	60
AL	1091
AL	1092
AL	1093
AL	1094
AL	1095
AL	1096
AL	1097
AL	1098
AL	1099
AL	1100
COMMENT	61
AL	1101
AL	1102
AL	1103
AL	1104
AL	1105
AL	1106
AL	1107
AL	1108
AL	1109
AL	1110
AL	1111
AL	1112
AL	1113
AL	1114
AL	1115
AL	1116
AL	1117
AL	1118
AL	1119
AL	1120
AL	1121
AL	1122
AL	1123
AL	1124
COMMENT	62
AL	1125
AL	1126
AL	1127
AL	1128
AL	1129
AL	1130
NASAX	24
NASAX	25
AL	1133
COMMENT	63
AL	1134
AL	1135

TEMPW=TEMP(I,J-1,K)	AL	1136
SU(I,J)=SU(I,J)+EMI*SIGMA*TEMPW**4*RM(J)	AL	1137
SP(I,J)=SP(I,J)-EMI*RM(J)	AL	1138
GO TO 911	AL	1139
906 SU(I,J)=SU(I,J)+RADIN*RM(J)	MASAX	26
SP(I,J)=SP(I,J)-RM(J)	MASAX	27
911 CONTINUE	AL	1142
C-----SLOT MODIFICATIONS.	COMMENT	64
IF (NUINJ.LE.0) GO TO 912	AL	1143
DO 744 II=1,NUINJ	AL	1144
I=IUIINJ(II)-1	AL	1145
J=JUIINJ(II)	AL	1146
M1=J-1	AL	1147
IF (J.EQ.JWLI(I,NGOTO)+1) M1=J+1	AL	1148
M2=MAX0(J,M1)	AL	1149
TC 'W=TLIP	AL	1150
SU(I,M1)=SU(I,M1)+EMI*SIGMA*TEMPW**4*RM(M2)	AL	1151
744 SP(I,M1)=SP(I,M1)-EMI*RM(M2)	AL	1152
912 CONTINUE	AL	1153
920 CONTINUE	AL	1154
RETURN	AL	1155
C ** ** ** **	AL	1156
C -+--+--+--+--+--+--+ Z-DIRECTION RADIATION -+--+--+--+--+--+	AL	1157
ENTRY SQM00Z	AL	1158
C-----SLOT MODIFICATIONS.	COMMENT	65
IF (NUINJ.LE.0) GO TO 1100	AL	1159
DO 1102 II=1,NUINJ	AL	1160
IF (JUIINJ(II).NE.JPLANE) GO TO 1102	AL	1161
I=IUIINJ(II)-1	AL	1162
DO 1104 K=2,N	AL	1163
SU(I,K)=0.	AL	1164
1104 SP(I,K)=-1.E30	AL	1165
1102 CONTINUE	AL	1166
1100 CONTINUE	AL	1167
C-----CYCLIC BOUNDARY CONDITIONS.	COMMENT	66
DO 921 I=2,L	AL	1168
LP2=I+JM(JPLANE)+KM(2)	AL	1169
LPN=I+JM(JPLANE)+KM(N)	AL	1170
GAMDDL=.5*(GAM(I,JPLANE,2)+GAM(I,JPLANE,N))/R(JPLANE)/(2DIF(NP1)+	AL	1171
1 2DIF(2))	AL	1172
SU(I,2)=SU(I,2)+GAMDDL*F(LP2,NVRZ)	AL	1173
SP(I,2)=SP(I,2)-GAMDDL	AL	1174
SU(I,N)=SU(I,N)+GAMDDL*F(LP2,NVRZ)	AL	1175
SP(I,N)=SP(I,N)-GAMDDL	AL	1176
921 CONTINUE	AL	1177
RETURN	AL	1178
END	AL	1179
SUBROUTINE OUTPUT(NTP)	OU	2
COMMON F(500,7),DU(10,10,5),DV(10,10,5),DW(10,10,5),	COMFA	2
1 ANUC(10,10,5),SOUT1(10,10,5),SOUT2(10,10,5),FCV(10,10,5),	4STEP	1
2 F42(10,10,5),FS(500,14),	4STEP	2
1 P4N(10,10,5),VISC(10,10,5),ABSR(10,10,5),SCTR(10,10,5),	RAD	1
1 SU(10,10),SP(10,10),DRHODP(10,10,5),	RAD	2
1 AXP(10,10),AXM(10,10),AYP(10,10),AYM(10,10),AZP(10,10),	COMFA	4
2 AZM(10,10),C7(10,10),CY(10),CZU(10,10),CYU(10),	COMFA	5
3 C7P(10,10),CYP(10),DIVG(10,10),NTP1,NTP2	COMFA	6
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),	CTOMA	1
2 SUK(192),SPK(192)	CTOMA	2
DIMENSION U(10,10,5),V(10,10,5),W(10,10,5),PP(10,10,5)	COMFA	7
DIMENSION P(10,10,5),TEMP(10,10,5),GAM(10,10,5)	COMFA	8
EQUIVALENCE (F(1,1),U(1,1,1)),(F(1,2),V(1,1,1)),(F(1,3),W(1,1,1))	COMFA	9
EQUIVALENCE (F(1,4),PP(1,1,1)),(F(1,5),P(1,1,1))	COMFA	10
EQUIVALENCE (F(1,6),TEMP(1,1,1)),(F(1,7),GAM(1,1,1))	COMFA	11
COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX	COMMON	2

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COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSV(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXH(40),
2 FYP(30),FYM(30),FZP(30),FZH(30),DT,TIME
COMMON
1/CINDEF/INCC,INFU,IND2,IND1,IND20,INDQ2,IND1,IND2,IND1,INDQ,INDQ2
1,IND,INDH,INCP5,ILC,ILH,INAT,ITER,JJJ,M1,M2,M3,NA,NGLOR,NGLORP,
2 NLN,NQ,NSH,NS1,NS2,IOCH
3/CCHEM/CPSUP,MSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG
4/CPARAN/ASUB(30,3),EMV,FR,HSURQ,NDEBUD,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOPP,
4 SM,SMW(30),SMO,S1(30),S2(30),TK,LADIAB,LDERUG,LEQUIL,LREACT,
4 LENER,FDKIJ,LCONVG
DOUBLE PRECISION CPSUM,EMV,ER,FQ,HSURQ,MSUM,PA,PPLN,Q0,Q1,Q2,Q3,
1 Q4,NGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO
2,FUT,FST
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CERU1,CERU2,
1 CERU3,CERU4,AFXP1,AEXP2,AEXP3,AEXP4,REXP1,REXP2,REXP3,REXP4,
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST
LOGICAL LADIAB,LCONVG,LDERUG,LEQUIL,LNRG,LREACT,LENER
COMMON/INT/L,M,N,LCV,MCV,NCV,LP1,MP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,
1 NVV,NGOTO,K,ISTR,JSTR,KSTR,NVN(30),KM(30),JM(30),ISTEP,
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,
3 NRMH,NGAM,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWEI,
4 IWFO,PM1,JWII,JWIO,JWOI,JWOO,IWV,JKIN(30,30),IKIN(40,30)
COMMON/INDEX/IPAR,LPRF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE
1,PLAXM1,LVA,LVD,LVFUDX,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),
2 IJUMP,IPRES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH20,NVCH2,
3 NVH2,NVCH,NVH2
COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVCH,LVH20,LVN2,LVO2,
1 LVCO2,LVFU1,LVCO1,NNOX,INOX,ITNOX,SNNOX,TNOX
COMMON/THERM/NVH,NVFU,NVCH,NVFUDX,NVTE,NODEN,IOK,FSTOIC,MFU,CP,
1 GASCON,RHOCOM,UNICOM,PRESS,NVFAV,TCYLW,TINLW,TLIP,ACOF(4),
2 T4,DFAC,MFU,WC2,WC0,WCX,WH20,WH2,HYY,CXX,RATIO1,RATIO2,
3 RATIO3,RATIO4,WC0,TAN,ITWALL
COMMON/CTDMA/END,ICTDMA(32)
COMMON/MIS/AMU,DEN,SMAX,SSUM,LASTEP,HTCEXT,CFR,EMISW,EMISIN,
1 EMISR,TOUT,RTCD,EMI,RADIN,RADSUR,FMA,FK,SQFK,
2 FKFU,FDFU,TFUEL,NFZ,FLD(40),TENTH(40),M(40),FUEL(40),FUDX(40),
2 UIN(40),TIN(40),FUELS(40),SEKIT,IGAN1(29),IGAN2(29)
COMMON/TURR/NVK,NVD,C1,C2,CD,AK,NUIDXJ(3,3),AKFAC,ALFAC,
1 MODEL,PR(32),PREF(32),PJAY(32),E
COMMON/RAD/NVE,SIGMA,ABSOR,SCATR
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER
COMMON/DROPL/EVAP(192),NTP4,NFZ,XO(3),YO(3),ZO(3),ALFA(3),
1 BETA(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SMD(3),
2 VFUEL(3),RFUEL(3),EVSU(64),HEVAP
COMMON/INJEC/FLOWIN,TUINJ(20),JUINJ(20),UINJ(20),WUINJ(20),
1 AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),
2 EVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),NUINJ,NVINJ,JSW1,JSW2,
3 USW,VSW,AFSW,FSW,TSW,WSW,SWNO,RHOSW
COMMON/CSOOT/NVN,NVS1,NVS2,ISOOT,SSOOT,AD,ARCONN,AAA,ABB,FMG
1,G0,MPART,CPART(2),FRACP(2),RHOP,ACCONS,PREXPS,ALPHA,AAS,ABS,DHR
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT
COMMON/CRAD/IRAD,SRAD
COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,AB1,CC1,
1 AA2,AB2,CC2,AA3,AB3,CC3,AA4,AB4,CC4,RATIO5,RATIO6,RATIO7,
2 RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,WH2,WC2H4,LVCH,LVCH1,LVH21
C-----SURROUTINE OUTPUT IS USED FOR PRINTOUT PURPOSES.
C
IF (NTP.LE.0) GO TO 16
IF (ISTEP.EQ.LASTEP) GO TO 11
IF (MOD(ISTEP,IJUMP)) 20,11,20
11 CONTINUE
REWIND NTP
READ (NTP) U,V,W,P

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COMMON 3
COMMON 4
COMMON 4
NOX 2
NOX 3
NOX 4
4STEP 3
NOX 6
NOX 7
NOX 8
NOX 9
NOX 10
NOX 11
4STEP 4
4STEP 5
4STEP 6
4STEP 7
NOX 12
COMMON 6
4STEP 8
4STEP 9
COMMON 9
COMMON 10
COMMON 11
4STEP 10
COMMON 13
4STEP 11
NOX 16
NOX 17
COMMON 19
COMMON 16
COMMON 17
COMMON 18
4STEP 12
COMMON 2
COMMON 3
COMMON 4
4STEP 13
COMMON 6
4STEP 14
COMMON 8
COMMON 9
COMMON 10
COMMON 11
COMMON 12
COMMON 13
COMMON 14
COMMON 15
COMMON 16
SOOT 8
SOOT 9
SOOT 10
SOOT 11
4STEP 15
4STEP 16
4STEP 17
COMMENT 67
COMMENT 68
OU 6
OU 7
OU 8
OU 9
OU 10
OU 11

```

```

CALL FPRINT (1,3,1)
CALL FPRINT (3,5,4)
IF (ISTEP.EQ.0) GO TO 300
IF (MSOOT.EQ.0) GO TO 227
C-----SOOT EMISSIONS INDEX AND SMOKE NUMBER.
FLOW=0.0
PBAR=0.0
SBAR=0.0
DO 225 K=2,N
DO 225 J=2,M
LP=KM(K)+JP(J)+L
OMDOT=PHO(LP,J,K)*YSR(J)*ZS(K)*U(LP,J,K)
FLOW=FLOW+OMDOT
OSOOT=OMDOT*(SOOT1(L,J,K)+SOOT2(L,J,K))
SBAR=SBAR+OSOOT
225 PBAR=PBAR+OSOOT*PHO(LP,J,K)
PBAR=PBAR+1.0E-30
FLOW=FLOW+1.0E-30
CSMO=1000.0*SBAR/FUTOT
SMCONC=1.0E6*PBAR/FLOW
SMONQ=12.5847*ALOG(SMCONC)+12.045
SMONO=AMAX1(SMONQ,0.0)
227 IF (NMOX.EQ.0) GO TO 300
C-----NOX EMISSIONS INDEX.
PBAR=0.0
DO 301 K=2,N
DO 301 J=2,M
LP=KM(K)+JP(J)+L
301 PBAR=PBAR+RHC(LP,J,K)*YSR(J)*ZS(K)*U(LP,J,K)*(F(LP,LVNO)+46./30.
1+F(LP,LVNO2))
CMN=1000.0*PBAR/FUTOT
300 CONTINUE
C ----- HERE PP IS ACTUALLY KE, P IS ACTUALLY DISSIPATION
READ (NTP) PP,P
DO 25 K=1,NP1
DO 25 J=1,MP1
KJM=KM(K)+JM(J)
DO 25 I=1,LP1
LP=KJM+I
25 F(LP,NVK)=CD*F(LP,NVK)**1.5/(F(LP,NVD)+1.0E-30)
CALL FPRINT (NVK,NVD,5)
C ----- HERE PP IS PHI, P IS MFU, OU IS MCO
READ (NTP) PP,P,OU
CALL FPRINT (NVFUOX,NVTE,7)
CALL FPRINT (NVCO,NVCO,15)
DO 50 K=1,NP1
DO 50 J=1,MP1
KJM=KM(K)+JM(J)
DO 50 I=1,LP1
LP=KJM+I
FUR=F(LP,NVFUOX)-F(LP,NVFU)
F(LP,NVCO2)=FS(LP,IOCO2)
F(LP,NVCOX)=FS(LP,IOO2)
F(LP,NVH2O)=FS(LP,IOH2O)
F(LP,NVN2)=FS(LP,ION2)
50 CONTINUE
CALL FPRINT (NVH2O,NVN2,16)
IF (MFM7.(F,C) GO TO 35
DO 37 K=1,NP1
DO 37 J=1,MP1
KJM=KM(K)+JM(J)
DO 37 I=1,LP1
LP=KJM+I
37 F(LP,NVFUOX)=C.

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OU      12
OU      13
NOX     127
SOOT    139
COMMENT 69
SOOT    160
SOOT    161
SOOT    162
SOOT    163
SOOT    164
SOOT    165
SOOT    166
SOOT    167
SOOT    168
SOOT    169
SOOT    170
SOOT    171
SOOT    172
SOOT    173
SOOT    174
SOOT    175
SOOT    176
NOX     128
COMMENT 70
NOX     129
NOX     130
NOX     131
NOX     132
NOX     133
NOX     134
NOX     135
NOX     136
OU      14
OU      15
OU      16
OU      17
OU      18
OU      19
OU      20
OU      21
OU      22
OU      23
OU      24
OU      25
OU      26
OU      27
OU      28
OU      29
OU      30
OU      31
OU      32
NOX     137
NOX     138
NOX     139
NOX     140
OU      40
OU      41
OU      42
OU      43
OU      44
OU      45
OU      46
OU      47
OU      48

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C-----	SPRAY EVAPORATION RATES.	COMMENT	71
	DO 39 K=2,N	OU	49
	DO 39 J=2,M	OU	50
	KJM=KM(K)+JM(J)	OU	51
	KJK=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)	OU	52
	DO 39 I=2,L	OU	53
	LP=KJM+I	OU	54
	LPC=KJK+(I-1)	OU	55
39	F(LP,MVFUX)=EVAP(LPC)	OU	56
	CALL FPRINT (MVFUX,MVFUX,22)	OU	57
35	CONTINUE	OU	58
C-----	HERE DV IS ENTHALPY, DW IS FAV	OU	59
	READ (NTP) DV,DW	OU	60
	CALL FPRINT (NVH,MVFAV,10)	OU	61
C-----	HERE U IS FX, V IS FY, W IS FZ	OU	62
	READ (NTP) U,V,W	OU	63
	CALL FPRINT (NVFX,MVFX,12)	OU	64
C-----	RHO AND VISCOSITY	OU	65
	CALL FPRINT(30,30,20)	4STEP	175
	NV=4	OU	67
	DO 56 K=1,NP1	OU	68
	DO 56 J=1,MP1	OU	69
	KJM=KM(K)+JM(J)	OU	70
	DO 56 I=1,LP1	OU	71
	LP=KJM+I	OU	72
56	F(LP,7)=0.	OU	73
	CALL GAMMA	OU	74
	CALL FPRINT (7,7,21)	OU	75
	REWIND NTP1	OU	76
	DO 46 II=1,2	OU	77
46	READ (NTP1)	OU	78
C-----	HERE PP IS PHI, P IS MFU, DU IS MCO	OU	79
	READ (NTP1) PP,P,DU	OU	80
	CALL FPRINT(11,13,23)	SOOT	179
	CALL FPRINT(24,29,26)	4STEP	176
	CALL FPRINT(14,15,32)	4STEP	177
	IF(ISTEP.GT.0.AND.NSOOT.NE.0)WRITE(6,226)SMONO,SMCONC,CSMO	SOOT	180
226	FORMAT(1H,10(1H),5X,*SMOKE NUMBER = *,E10.2,5X,10(1H)/1H,	SOOT	181
1	10(1H),5X,*SMOKE CONCENTRATION = *,E10.2,1X,*MG/M3, OR*,E10.2,	SOOT	182
2	1X,*GM,OF SMOKE/KG,OF FUEL*,5X,10(1H)/)	SOOT	183
	IF(ISTEP.GT.0.AND.NNOX.NE.0)WRITE(6,302)CNO	NOX	143
302	FORMAT(1H,10(1H),5X,*NOX EMISSIONS INDEX = *,E10.2,1X,	NOX	144
1	*GM,OF NO2/KG,OF FUEL*,5X,10(1H)/)	NOX	145
14	CONTINUE	OU	81
	WRITE(6,19)	OU	82
19	FORMAT (1H,4HSTEP,5X,4HSMAX,7X,4HSSUM,6X,5HSEKIT,5X,	OU	83
1	8HP(2,M,2),3X,8HP(L,M,2),3X,8HU(I,J,K),3X,8HV(I,J,K),3X,	OU	84
2	8HW(I,J,K),2X,8HT(I,J,K),2X,10HRHO(I,J,K),2X,7HI J K)	OU	85
20	CONTINUE	OU	86
	RETURN	OU	87
	END	OU	88
	SUBROUTINE AUX	AU	2
	COMMON F(3500),DU(500),DV(500),DW(500),	CONF8	2
1	ANUC(500),SOCT1(500),SOCT2(500),FCH(500),FH2(500),FS(500,14),	4STEP	18
1	RHO(500),VISC(500),ABSR(500),SCTR(500),SU(100),SP(100),	RAD	3
1	DRHODP(500),	RAD	4
1	AXP(100),AXP(100),AYP(100),AYH(100),AZP(100),	CONF8	4
2	A7M(100),C7(100),CY(10),CZU(100),CYU(10),	CONF8	5
3	C7P(100),C7P(10),DIVG(100),NTP1,NTP2	CONF8	6
1	AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),	CTOMA	3
2	SUK(192),SPK(192)	CTOMA	4
	DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)	CONF8	7
	DIMENSION GAM(500)	CONF8	8
	EQUIVALENC F(1),U(1), (F(501),V(1)), (F(1001),W(1))	CONF8	9

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EQUIVALENCE (F(1901),PP(1)),(F(2001),P(1)),(F(2901),TEMP(1))
EQUIVALENCE (F(3001),GAM(1))
COMMON/CYL/R(30),PM(30),RMV(30),YSR(30),YSVR(30),IPLAX
COMMON/GRIN/X(40),Y(30),Z(30),XS(40),YS(30),ZS(40),XSU(40),
1 YSV(30),ZSV(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXM(40),
2 FYP(30),FYM(30),F7P(30),F7M(30),DT,TIME
COMMON
1/CINDEF/IDCC,INFU,IND2,INDZ,IND20,IDCQ2,IND1,IND2,IND1,IND0,IND12
1,IND0,INDM,IHCPS,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NGL0B,NGL0BP,
2 NLM,NQ,NSM,NS1,NS2,IOCH
3/CCHEMI/CPSUM,MSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
4/CPARAM/ASUB(30,3),ENV,ER,HSUB0,NDEB0G,MS,PA,Q0,Q1,Q2,Q3,Q4,RHOP,
4 SM,SMW(30),SPO,S1(30),S2(30),TK,LADIAB,LDEB0G,LEQUIL,LREACT,
4 LENER,FDKIJ,LCONVG
DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUB0,MSUM,PA,PPLN,Q0,Q1,Q2,Q3,
1 Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO
2,FIIT,FST
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,
1 CEBU3,CEBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST
LOGICAL LADIAB,LCONVG,LDEB0G,LEQUIL,LNRG,LREACT,LENER
COMMON/INT/L,P,N,LCV,MCV,N,V,LP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,
1 NNV,NGOTO,K,ISTR,KSTR,NVM(35),KN(30),JM(30),ISTEP,
2 ISOLVF(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,
3 NRHO,NGAM,IWLI(30,5),IWL0(30,5),JWL0(40,5),JWLI(40,5),IWET,
4 IWFO,NM1,JWII,JWIO,JWOI,JWOO,IOW,JKIN(30,30),IKIN(40,30)
COMMON/INDEX/IPAR,LPRF,ISTUN,INCOMP,ITRAO,NVRX,NVRY,NVRZ,JPLANE
1,PLAXM1,LVK,LVD,LVFUOX,LVFU,LVC0,LVH,LVRX,LVRY,LVRZ,NVF(32),
2 IJUMP,IRFS,TITLF2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH20,NVCO2,
3 NVN2,NVCH,NVW2
COMMON/CNOX/LVH1,LVH2,LVN1,LVND,LVND2,LVD,LVDH,LVH20,LVN2,LVO2,
1 LVC02,LVFU1,LVC01,MNOX,INDX,ITNOX,SMOX,TNOX
COMMON/THERP/NVH,NVFU,NVOX,NVFUOX,NVTE,NODEN,IOK,FSTOIC,HFU,CP,
1 GASCCN,RHCCCN,UNICCN,PRESS,NVFAY,TCYLV,TIMLV,TLIP,ACDEF(4),
2 T4,DFAC,WFU,WC02,MC0,W0X,WH20,WN2,HVY,CXX,RATIO1,RATIO2,
3 RATIO3,RATIO4,HCO,TAN,ITWALL
COMMON/CTOMA/KEND,ICTOMA(32)
COMMON/MIS/AMU,DEN,SHAX,SSUM,LASTEP,HTCEXT,CFR,EMISW,EMISIN,
1 EMISR,TOUT,RTCO,EMI,RADIN,RADSUR,FMA,FK,SQFK,
2 FKFU,FDFU,TFUEL,WFNZ,FLO(40),TEMTH(40),H(40),FUEL(40),FUOX(40),
2 UIN(40),TIN(40),FUELS(40),SEXIT,IGAM1(29),IGAM2(29)
COMMON/TURB/NVK,NVO,C1,C2,C0,AK,DUIDX(3,3),AKFAC,ALFAC,
1 M0DFL,PR(32),PRF(32),PJAY(32),E
COMMON/RAD/NVE,SIGMA,ABSOR,SCATR
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER
COMMON/DRDPL/EVAP(192),NTP4,MFNZ,KO(3),YO(3),ZO(3),ALFA(3),
1 AETA(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SMO(3),
2 VFUEL(3),RFUEL(3),EVSU(64),HEVAP
COMMON/INJEC/FLOWIN,IUINJ(20),JUINJ(20),UINJ(20),WUINJ(20),
1 AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),
2 EVINJ(20),QVINJ(20),AVINJ(20),TVINJ(20),NUINJ,NVINJ,JSW1,JSW2,
3 USW,VSU,AFSW,FSW,TSW,WSW,SWND,RHOSW
COMMON/CSOOT/NVN,NVS1,NVS2,ISOOT,SSOOT,MSOOT,A0,ARCONN,AAA,B0B,FMG
1,G0,MPART,OPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BRS,DHR
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT
COMMON/CRAD/IRAO,SRAD
COMMON/CFQUP/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BR1,CC1,
1 AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,
2 RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,MCH,MH2,MC2M,LVCH,LVCH1,LVH21
COMMON/CDK/EDK(192)
DIMENS DM GENR(900),SUFU(900),SPFU(900),EDK2(192)
DIMENS DM SUCH(900),SPCH(900)
C ***** REWARE OF EQUIVALENCE STATEMENTS *****
EQUIVALENCE (GENR(1),DU(1)),(SUFU(1),DV(1)),(SPFU(1),DM(1))

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CONF8 10
CONF8 11
COMMON 2
COMMON 3
COMMON 4
COMMON 5
NOX 2
NOX 3
NOX 4
4STEP 3
NOX 6
NOX 7
NOX 8
NOX 9
NOX 10
NOX 11
4STEP 4
4STEP 5
4STEP 6
4STEP 7
NOX 12
COMMON 6
4STEP 8
4STEP 9
COMMON 9
COMMON 10
COMMON 11
4STEP 10
COMMON 13
4STEP 11
NOX 16
NOX 17
COMMON 19
COMMON 16
COMMON 17
COMMON 18
4STEP 12
COMGEN 2
COMGEN 3
COMGEN 4
4STEP 13
COMGEN 6
4STEP 14
COMGEN 8
COMGEN 9
COMGEN 10
COMGEN 11
COMGEN 12
COMGEN 13
COMGEN 14
COMGEN 15
COMGEN 16
SOOT 8
SOOT 9
SOOT 10
SOOT 11
4STEP 15
4STEP 16
4STEP 17
NOX 146
NOX 147
4STEP 178
AU 7
AU 8

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C	-----FENTRY DEMS	AU	9
	FENTRY DEMS IS USED TO CALCULATE TEMPERATURE AND DENSITY.	AU	10
C		COMMENT	72
	RELAXM=1.-RELAX(MRHO)	COMMENT	73
	KONTR0=2	AU	11
	IF(ISTEP.EQ.IRFS)KONTR0=1	AU	12
	NVHP=7	NASAX	20
C	-----FNTALPY.	AU	17
	DO 1040 K=1,NP1	COMMENT	74
	DO 1040 J=1,MP1	AU	18
	KJM=KM(K)+JM(J)	AU	19
	DO 1040 I=1,LP1	AU	20
	LP=KJM+I	AU	21
	LPH=(LP+NVH(NVH))	AU	22
	LPHP=(LP+NVH(NVHP))	AU	23
1040	F(LPHP)=F(LPH)	AU	24
	IF(ISOLVE(LVFU).EQ.0)GO TO 1034	AU	25
	GO TO (1034,1044,1034), MODEN	NOX	140
1044	DO 1050 K=1,NP1	AU	26
	CALCULATE GAS TEMPERATURE.	AU	27
	DO 1050 J=2,M	COMMENT	75
	KJM=KM(K)+JM(J)	AU	28
	IS=IWL1(J,4)	AU	29
	IE=IWL0(J,4)	AU	30
	DO 1050 I=IS,IE	AU	31
	LP=KJM+I	AU	32
	LPHP=(LP+NVH(NVHP))	AU	33
	LPHU=(LP+NVH(NVHU))	AU	34
	LPHC=(LP+NVH(NVHC))	AU	35
	LPHM=(LP+NVH(NVHM))	AU	36
	LPH2=(LP+NVH(NVH2))	4STEP	179
	LPHUX=(LP+NVH(NVHUX))	4STEP	180
	T=TEMP(LP)	AU	37
	F(LPHU)=AMIN1(F(LPHU),F(LPHUX))	AU	38
	FUA=F(LPHUX)-F(LPHU)	NOX	149
	FLPC02=WCO2*(CXX*FUB/WFU-CXX*F(LPHC)/WCH-F(LPC0)/WCO)	AU	39
	FLPOX=RATIO1*F(LPHU)+RATIO3*F(LPC0)+RATIO2*(RATIO1+RATIO2)*	4STEP	181
	1 F(LPHUX)+RATIO5*F(LPHC)+RATIO6*F(LPH2)	AU	41
	FLPOX=AMAX1(FLPOX,0.)	4STEP	182
	FLPH20=0.9*WCH20*(HYY*FUB/WFU-RATIO7*F(LPHC)-F(LPH2))	AU	43
	FLPH2=1.0-F(LPHU)-FLPC02-F(LPC0)-FLPOX-FLPH20-F(LPHC)-F(LPH2)	4STEP	183
	FS(LP,IOFU)=F(LPHU)	4STEP	184
	FS(LP,IOC2)=AMIN1(FLPOX,RATIO2)	NOX	150
	FS(LP,ION2)=AMAX1(1.E-15,FLPH2)	NOX	151
	FS(LP,IOC0)=F(LPC0)	NOX	152
	FS(LP,IOCH)=F(LPHC)	NOX	153
	FS(LP,IOH2)=F(LPH2)	4STEP	185
	FS(LP,IOH20)=FLPH20	4STEP	186
	FS(LP,IOC02)=AMAX1(1.E-15,FLPC02)	NOX	154
	IMCPS=4	NOX	155
	NS1=IOFU	NOX	156
	NS2=IOC02	NOX	157
	TK=T	NOX	158
	TKINV=1.000/TK	NOX	159
	DO 1011 II=NS1,NS2	NOX	160
1011	S2(II)=FS(LP,II)/SMW(II)	NOX	161
	CALL MCPS	NOX	162
	HPI=MSUM*UNICCH*TK	NOX	163
	CPI=CPSUM*UNICCH	NOX	164
	T=TEMP(LP)+(F(LPHP)-HPI)/CPI	NOX	165
	TEMP(LP)=(1.-RELAX(NVH))*TEMP(LP)+RELAX(NVH)*T	AU	50
	PHI=F(LPHUX)/FSTOIC	AU	51
	THAX=ACOFF(1)+PHI*(ACOFF(2)+PHI*(ACOFF(3)+PHI*ACOFF(4)))	AU	52
		AU	53

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      THAX=AMAX1(THAX,2000.)
      TEMP(LP)=AMIN1(TEMP(LP),THAX)
1050 TEMP(LP)=AMAX1(TEMP(LP),100.)
C ----- HERE DU IS U, DV IS V, DW IS W
1034 REWIND NTP1
      READ (NTP1) DU,DV,DW,P
1048 READ (NTP1)
C ----- HERE PP IS PHI, DU IS MFU, DV IS MCO
      READ (NTP1) PP,DU,DV
      READ(NTP1)
      READ(NTP1)DW,P
      REWIND NTP1
      READ(NTP1)U,V,W
CALCULATE WALL TEMPERATURE.
      DO 1052 K=2,N
      DO 1058 I=2,L
      IF(IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3)GO TO 1054
      J=JWL(I,4)+1
      LP=I+JM(J)+KM(K)
      LPRY=LP+NYM(5)
      VEC=0.25*((U(LP)+U(LP+1))*2+(W(LP)+W(LP+NYM(J)))*2)
      HTC=CFR*RHQ(LP)*CP*SORT(VEC)
      TEMP(LP+NI)=TSOLVE(TEMP(LP+NI),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,
1 ITRAD)
C
1054 IF(IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3)GO TO 1058
      IF(IDW.EQ.0)GO TO 1058
      J=JWL(I,4)+1
      LP=I+JM(J)+KM(K)
      LPRY=LP+NYM(5)
      VEC=0.25*((U(LP)+U(LP+1))*2+(W(LP)+W(LP+NYM(J)))*2)
      HTC=CFR*RHQ(LP)*CP*SORT(VEC)
      TEMP(LP+NI)=TSOLVE(TEMP(LP+NI),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,
1 ITRAD)
1058 CONTINUE
      DO 1052 J=2,M
      IF(JKIN(J,K).EQ.1)GO TO 1059
      LP=IWL(J,4)+JM(J)+KM(K)
      LPRY=LP+NYM(10)
      VEC=0.25*((V(LP)+V(LP+NI))*2+(W(LP)+W(LP+NYM(J)))*2)
      HTC=CFR*RHQ(LP)*CP*SORT(VEC)
      TEMP(LP+1)=TSOLVE(TEMP(LP+1),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,ITRAD)
1059 IF(J.GT.JWCI.AND.J.LT.JWCI)GO TO 1052
      LP=IWL(J,4)+JM(J)+KM(K)
      LPRY=LP+NYM(10)
      VEC=0.25*((V(LP)+V(LP+NI))*2+(W(LP)+W(LP+NYM(J)))*2)
      HTC=CFR*RHQ(LP)*CP*SORT(VEC)
      TEMP(LP+1)=TSOLVE(TEMP(LP+1),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,ITRAD)
1062 CONTINUE
      REWIND NTP1
      READ(NTP1)U,V,W,P
      IF(ISOLVE(LVFU).EQ.0)GO TO 1200
      GO TO (1060,1062,1064), MODEN
1060 DO 1061 K=1,NP1
C-----DENSITY=CONSTANT. MODEN=1.
      DO 1061 J=1,NP1
      KJM=KM(K)+JM(J)
      IS=IWL(J,5)
      IE=IWL(J,5)
      DO 1061 I=IS,IE
      LP=KJM+I
      RHQ(LP)=DFN
1061 CONTINUE
      GO TO 1200

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AU      54
AU      55
AU      56
AU      57
AU      58
AU      59
AU      60
AU      61
AU      62
RAD     32
RAD     33
AU      63
RAD     34
COMMENT 76
RAD     35
RAD     36
RAD     37
RAD     38
RAD     39
RAD     40
RAD     41
RAD     42
RAD     43
RAD     44
FEB2    2
RAD     46
RAD     47
RAD     48
RAD     49
RAD     50
RAD     51
RAD     52
RAD     53
RAD     54
RAD     55
RAD     56
RAD     57
RAD     58
RAD     59
RAD     60
RAD     61
RAD     62
RAD     63
RAD     64
RAD     65
RAD     66
RAD     67
RAD     68
RAD     69
RAD     70
RAD     71
MODX    166
AU      65
AU      66
COMMENT 77
AU      67
AU      68
AU      69
AU      70
AU      71
AU      72
AU      73
AU      74
AU      75

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1062 DO 1063 K=1,NP1	AU	76
C-----DENSITY=FUNCTION(COMPOSITION,TEMPERATURE), MODEN=2.	COMMENT	78
DO 1063 J=1,NP1	AU	77
KJM=KM(K)+JM(J)	AU	78
IS=IWL1(J,5)	AU	79
IE=IWL2(J,5)	AU	80
DO 1063 I=IS,IE	AU	81
LP=KJM+I	AU	82
LPTE=LP+NVH(NVTE)	AU	83
LPFUOX=LP+NVH(NVFUOX)	AU	84
C ----- CAUTION HERE	AU	85
LPFU=LP+NVH(NVFU+3)	AU	86
LPCO=LP+NVH(NVCO+1)	AU	87
LPCN=LP+NVH(NVCH)	4STEP	187
LPH2=LP+NVH(NVH2)	4STEP	188
FUB=F(LPFUOX)-F(LPFU)	AU	88
FLPH2O=0.5*WH2O*(HYV*FUB/WFU-RATIO7*F(LPCN)-F(LPH2))	4STEP	189
FLPCO2=WC02*(CXX*FUB/WFU-CXX*F(LPCN)/WCH-F(LPCO)/WCO)	4STEP	190
FLPOX=RATIO1*F(LPFU)+RATIO3*F(LPCO)+RATIO2*(RATIO2+RATIO1)*	AU	91
1 F(LPFUOX)+RATIO5*F(LPCN)+RATIO6*F(LPH2)	4STEP	191
FLPOX=AMAX1(FLPOX,0.)	AU	93
FLPH2=1.0-F(LPFU)-FLPCO2-F(LPCO)-FLPOX-FLPH2O-F(LPCN)-F(LPH2)	4STEP	192
1008 CONTINUE	AU	95
FLPTE=F(LPTE)	AU	96
FLPTE=AMAX1(FLPTE,100.)	AU	97
VMIX=F(LPFU)/WFU+FLPCO2/WCO2+F(LPCO)/WCO+FLPOX/WOX+FLPH2O/WH2O+	AU	98
1 FLPH2/WH2+F(LPCN)/WCH+F(LPH2)/WH2	4STEP	193
DENST=RHOCON/(VMIX*FLPTE)	AU	100
GO TO (1009,1010),KONTRD	AU	101
1009 RHO(LP)=DENST	AU	102
1010 RHO(LP)=RELAX(NRHO)*DENST+RELAXN*RHO(LP)	AU	103
1063 CONTINUE	AU	104
1064 CONTINUE	AU	105
1700 CONTINUE	AU	106
CALL DENMOD	AU	107
RETURN	AU	108
C ** ** ** **	AU	109
ENTRY VISC	AU	110
C-----ENTRY VISCO IS USED TO CALCULATE THE EFFECTIVE VISCOSITY	COMMENT	79
C AND YPLUS AT WALL BOUNDARIES.	COMMENT	80
C	COMMENT	81
C ----- HERE DU IS KE, DV IS DISS	AU	111
READ (INTP1) DU,DV	AU	112
RELAXM=1.-RELAX(NGAM)	AU	113
KONTRD=2	AU	114
IF (ISTEP,E0,IPES) KONTRD=1	AU	115
DO 2000 K=1,NP1	AU	116
DO 2000 J=2,N	AU	117
KJM=KM(K)+JM(J)	AU	118
IS=IWL1(J,4)	AU	119
IE=IWL2(J,4)	AU	120
DO 2000 I=IS,IE	AU	121
LP=KJM+I	AU	122
GO TO (2001,2002),MODEL	AU	123
2001 CONTINUE	AU	124
C-----CONSTANT VISCOSITY, MODEL=1, LAMINAR.	COMMENT	92
VISC(LP)=AMU	AU	125
GO TO 2000	AU	126
2002 CONTINUE	AU	127
LPM=LP+NVH(NVK+4)	AU	128
LPO=LP+NVH(NVO+4)	AU	129
C-----VISCOSITY FROM K-E MODEL, MODEL=2, TURBULENT.	COMMENT	83
VISCO=RHO(LP)*CO*F(LPM)**2/(F(LPO)+1.E-30)	AU	130
GO TO (2003,2004),KONTRD	AU	131

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2003 VISC(LP)=VISCOS	AU	132
2004 VISC(LP)=RELAX(NGAM)*VISCOS+RELAXM*VISC(LP)	AU	133
2000 CONTINUE	AU	134
C----- CALCULATE YPLUS	AU	135
DO 2020 K=1,NP1	AU	136
DO 2022 I=1,LP1	AU	137
J=JWLO(I,4)	AU	138
LP=KN(K)+JM(J)+I	AU	139
LPK=LP+NVN(NVK+4)	AU	140
DIST=.5*YDIF(J)	AU	141
IF (J.EQ.NP1) DIST=YDIF(NP1)	AU	142
YPLUS=RHO(LP-NI)*SORT(F(LPK-NI)*RTCD)*DIST/AMU	AU	143
VISC(LP)=YPLUS	AU	144
J=JWLI(I,4)	AU	145
LP=KN(K)+JM(J)+I	AU	146
LPK=LP+NVN(NVK+4)	AU	147
DIST=.5*YDIF(J+1)	AU	148
IF (J.EQ.1) DIST=YDIF(2)	AU	149
YPLUS=RHO(LP+NI)*SORT(F(LPK+NI)*RTCD)*DIST/AMU	AU	150
VISC(LP)=YPLUS	AU	151
2022 CONTINUE	AU	152
DO 2024 J=2,M	AU	153
I=IWL1(J,4)-1	AU	154
LP=KN(K)+JM(J)+I	AU	155
LPK=LP+NVN(NVK+4)	AU	156
DIST=.5*YDIF(I+1)	AU	157
IF (I.EQ.1) DIST=XDIF(2)	AU	158
YPLUS=RHO(LP+1)*SORT(F(LPK+1)*RTCD)*DIST/AMU	AU	159
VISC(LP)=YPLUS	AU	160
I=IWL0(J,4)+1	AU	161
LP=KN(K)+JM(J)+I	AU	162
LPK=LP+NVN(NVK+4)	AU	163
DIST=.5*XDIF(I)	AU	164
IF (I.EQ.LP1) DIST=XDIF(LP1)	AU	165
YPLUS=RHO(LP-1)*SORT(F(LPK-1)*RTCD)*DIST/AMU	AU	166
VISC(LP)=YPLUS	AU	167
2024 CONTINUE	AU	168
2020 CONTINUE	AU	169
DO 3003 K=2,N	AU	170
DO 3005 J=2,M	AU	171
KJM=KN(K)+JM(J)	AU	172
IS=IWL1(J,4)	AU	173
IE=IWL0(J,4)	AU	174
DO 3009 I=IS,IE	AU	175
LP=KJM+I	AU	176
LPK=LP+NVN(NVK+4)	AU	177
LPD=LP+NVN(NVD+4)	AU	178
LPC=I-1+(J-2)*(NI-2)+(K-2)*(NI-2)*(NJ-2)	AU	179
ENK2(LPC)=F(LPD)/(F(LPK)*2+1.0E-30)	AU	180
3009 FOK(LPC)=F(LPD)/(F(LPK)+1.0E-30)	SDOT	181
RETURN	AU	182
C ** ** ** **	AU	183
ENTRY GAMMA	AU	184
C-----ENTRY GAMMA IS USED TO CALCULATE THE DIFFUSION COEFFICIENTS.	COMMENT	84
C	COMMENT	85
DO 3000 K=1,NP1	AU	186
DO 3000 J=2,M	AU	187
KJM=KN(K)+JM(J)	AU	188
IS=IWL1(J,4)	AU	189
IE=IWL0(J,4)	AU	190
DO 3000 I=IS,IE	AU	191
LP=KJM+I	AU	192
GO TO (3001,3002),MODEL	AU	
3001 CONTINUE	AU	

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GAMLP=GAM(LP)	AU	254
GAMLYM=GAM(LYM)	AU	255
IF (J.EQ.JWLI(I,NGOTO)+1) GAMLYM=GAM(LYM-NI)	AU	256
IF (J.EQ.JWLO(I,NGOTO)-1) GAMLP=GAM(LP+NI)	AU	257
SU(LIJ)=(GAMLP*DVDYP*RMV(J+1)-GAMLYM*DVDYM*RMV(J))/YSVR(J)	AU	258
LXP=LP+1	AU	259
LXM=LP-1	AU	260
LXP1=LXP-NI	AU	261
LXM1=LXM-NI	AU	262
GAMP=0.25*(GAM(LP)+GAM(LYM)+GAM(LXP)+GAM(LXP1))	AU	263
GAMM=0.25*(GAM(LP)+GAM(LYM)+GAM(LXM)+GAM(LXM1))	AU	264
DUDYP=(U(LXP)-U(LXP1))/YDIF(J)	AU	265
DUDYM=(U(LP)-U(LYM))/YDIF(J)	AU	266
SU(LIJ)=SU(LIJ)+(GAMP*DUDYP-GAMM*DUDYM)/XS(I)	AU	267
LZP=LP+NI	AU	268
LZM=LP-NI	AU	269
LZP1=LZP-NI	AU	270
LZM1=LZM-NI	AU	271
GAMP=0.25*(GAM(LP)+GAM(LYM)+GAM(LZP)+GAM(LZP1))	AU	272
GAMM=0.25*(GAM(LP)+GAM(LYM)+GAM(LZM)+GAM(LZM1))	AU	273
DWDYP=(W(LZP)-W(LZP1))/YDIF(J)	AU	274
DWDYM=(W(LP)-W(LYM))/YDIF(J)	AU	275
SU(LIJ)=SU(LIJ)+(GAMP*DWDYP-GAMM*DWDYM)*YSV(J)/YSVR(J)/ZS(K)	AU	276
WMNM=0.5*(W(LP)+W(LYM))	AU	277
WMNP=0.5*(W(LZP)+W(LZP1))	AU	278
SU(LIJ)=SU(LIJ)+PLAXM1*(GAMM*WMNM-GAMP*WMNP)*YSV(J)/YSVR(J)/ZS(K)/	AU	279
1RM(J)	AU	280
GAMPT2=GAM(LP)+GAM(LYM)	AU	281
SU(LIJ)=SU(LIJ)+PLAXM1*(GAMPT2*(WMNM-WMNP)/RM(J)/ZS(K)/RM(J)	AU	282
SP(LIJ)=GAMPT2/RM(J)/RM(J)*PLAXM1	AU	283
201 CONTINUE	AU	284
GO TO 5000	AU	285
C +--+--+--+--+ SOURCE TERMS FOR W-VELOCITY +--+--+--+--+	AU	286
300 DO 301 J=2,M	AU	287
IS=IWL(I,J,NGOTO)	AU	288
IE=IWL(I,J,NGOTO)	AU	289
DO 301 I=IS,IF	AU	290
LIJ=J*(J)+I	AU	291
LP=LIJ+KM(K)	AU	292
LZP=LP+NI	AU	293
IF (K.EQ.NP1) LZP=LIJ+KM(3)	AU	294
LZM=LP-NI	AU	295
DWDZP=(W(LZP)-W(LP))/ZS(K)	AU	296
DWDZM=(W(LP)-W(LZM))/ZS(K-1)	AU	297
GAMLP=GAM(LP)	AU	298
GAMLZM=GAM(LZM)	AU	299
IF (K.EQ.3) GAMLZM=GAM(LZM-NI)	AU	300
SU(LIJ)=(GAMLP*DWDZP-GAMLZM*DWDZM)/R(J) /YSR(J)/ZSW(K)*YS(J)	AU	301
LXP=LP+1	AU	302
LYM=LP-1	AU	303
LXP1=LXP-NI	AU	304
LYM1=LYM-NI	AU	305
GAMP=0.25*(GAM(LP)+GAM(LZM)+GAM(LXP)+GAM(LXP1))	AU	306
GAMM=0.25*(GAM(LP)+GAM(LZM)+GAM(LYM)+GAM(LYM1))	AU	307
DUDZP=(U(LXP)-U(LXP1))/ZDIF(K)	AU	308
DUDZM=(U(LP)-U(LZM))/ZDIF(K)	AU	309
SU(LIJ)=SU(LIJ)+(GAMP*DUDZP-GAMM*DUDZM)/XS(I)/R(J)	AU	310
LZP=LP+NI	AU	311
LYM=LP-NI	AU	312
LZP1=LZP-NI	AU	313
LYM1=LYM-NI	AU	314
GAMP=0.25*(GAM(LP)+GAM(LZM)+GAM(LYP)+GAM(LYP1))	AU	315
GAMM=0.25*(GAM(LP)+GAM(LZM)+GAM(LYM)+GAM(LYM1))	AU	316
DWDZP=(V(LYP)-V(LYP1))/ZDIF(K)	AU	317

DVDZM=(V(LP)-V(LZM))/ZDIF(K)	AU	318
SU(LIJ)=SU(LIJ)+(GAMP*DVDZP-GAMH*DVDZM)/YSR(J)	AU	319
WMNM=0.5*(W(LP)+W(LYM))	AU	320
WMNP=0.5*(W(LP)+W(LYP))	AU	321
SU(LIJ)=SU(LIJ)+PLAXM1*(GAMH*WMNM-GAMP*WMNP)/YSR(J)	AU	322
VPT2=V(LP)+V(LYP)	AU	323
VMT2=V(LZM)+V(LZM+NI)	AU	324
SU(LIJ)=SU(LIJ)+PLAXM1*(GAM(LP)+VPT2-VMT2+GAM(LZM))*YS(J)/R(J)/	AU	325
YSR(J)/ZSW(K)	AU	326
GAMP=0.5*(GAM(LP)+GAM(LZM))	AU	327
SU(LIJ)=SU(LIJ)+PLAXM1*GAMP/R(J)+((WMNP-WMNM)/YS(J)+0.5*(VPT2-VMT2	AU	328
1)/R(J)/ZSW(K))	AU	329
SP(LIJ)=-GAMP/R(J)/R(J)+PLAXM1	AU	330
301 CONTINUE	AU	331
GO TO 5000	AU	332
C +--+--+--+ SOURCE TERMS FOR TURBULENT KINETIC ENERGY +--+--+--+	AU	333
400 CONTINUE	AU	334
IF (NV.NF.LVK) GO TO 500	AU	335
DO 401 J=2,N	AU	336
IS=IWL1(J,NGOTO)	AU	337
IE=IWL0(J,NGOTO)	AU	338
DO 401 I=IS,IE	AU	339
MIN=JWL1(I,NGOTO)+1	AU	340
MAX=JWL0(I,NGOTO)-1	AU	341
LIJ=JN(J)+I	AU	342
LP=LIJ+KN(K)	AU	343
LXP=LP+1	AU	344
LYP=LP+NI	AU	345
LZP=LP+MINJ	AU	346
LXM=LP-1	AU	347
LYM=LP-NI	AU	348
LZN=LP+MINJ	AU	349
LPPQ=LYP+1	AU	350
LPMQ=LYM+1	AU	351
LPPM=LZM+1	AU	352
LPPQ=LZP+1	AU	353
LMPQ=LXM+NI	AU	354
LQPP=LZP+NI	AU	355
LQPM=LZM+NI	AU	356
LMPQ=LXM+MINJ	AU	357
LQMP=LYM+MINJ	AU	358
CALCULATE THE PRODUCTION TERM	AU	359
OUTDXJ(1,1)=(U(LXP)-U(LP))/XS(I)	AU	360
OUTDXJ(2,2)=(V(LYP)-V(LP))/YS(J)	AU	361
OUTDXJ(3,3)=(W(LZP)-W(LP))/ZS(K)/R(J)	AU	362
1 +PLAXM1*0.5*(V(LP)+V(LYP))/R(J)	AU	363
IF (I-IS) 411,412,411	AU	364
411 VXM=0.5*(V(LXP)+V(LMPQ))	AU	365
WXM=0.5*(W(LXM)+W(LMPQ))	AU	366
XN=X(I-1)	AU	367
GO TO 413	AU	368
412 VXM=0.5*(V(LP)+V(LYP))	AU	369
WXM=0.5*(W(LP)+W(LZP))	AU	370
XN=X(I)	AU	371
413 IF (I-IE) 414,415,414	AU	372
414 VXP=0.5*(V(LXP)+V(LPPQ))	AU	373
WXP=0.5*(W(LXP)+W(LPPQ))	AU	374
XP=X(I+1)	AU	375
GO TO 416	AU	376
415 VXP=0.5*(V(LP)+V(LYP))	AU	377
WXP=0.5*(W(LP)+W(LZP))	AU	378
XP=X(I)	AU	379
416 DX=XP-XN	AU	380
OUTDXJ(2,1)=(VXP-VXM)/DX	AU	381

	DUIXJ(3,1)=(WXP-WXM)/DX	AU	382
	IF (J-MIN) 421,422,421	AU	383
421	WYM=0.5*(W(LYP)+W(LOMP))	AU	384
	UYM=.5*(U(LYP)+U(LPM))	AU	385
	YM=Y(J-1)	AU	386
	GO TO 423	AU	387
422	WYM=0.5*(W(LP)+W(LZP))	AU	388
	UYM=0.5*(U(LP)+U(LXP))	AU	389
	YM=Y(J)	AU	390
423	IF (J-MAX) 424,425,424	AU	391
424	WYP=0.5*(W(LYP)+W(LPP))	AU	392
	UYP=0.5*(U(LYP)+U(LPP))	AU	393
	YP=Y(J+1)	AU	394
	GO TO 426	AU	395
425	WYP=0.5*(W(LP)+W(LZP))	AU	396
	UYP=0.5*(U(LP)+U(LXP))	AU	397
	YP=Y(J)	AU	398
426	DY=YP-YM	AU	399
	DUIXJ(3,2)=(WYP-WYM)/DY-PLAXM1*0.5*(W(LP)+W(LZP))/R(J)	AU	400
	DUIXJ(1,2)=(UYP-UYM)/DY	AU	401
	IF (K-2) 431,432,431	AU	402
431	U7M=0.5*(U(LZM)+U(LPM))	AU	403
	V7M=0.5*(V(L7M)+V(LPM))	AU	404
	7M=Z(K-1)	AU	405
	GO TO 433	AU	406
432	U7M=0.5*(U(LP)+U(LXP))	AU	407
	V7M=0.5*(V(LP)+V(LYP))	AU	408
	ZM=Z(K)	AU	409
433	IF (K-N) 434,435,434	AU	410
434	U7P=0.5*(U(LZP)+U(LPP))	AU	411
	V7P=0.5*(V(LZP)+V(LPP))	AU	412
	ZP=Z(K+1)	AU	413
	GO TO 436	AU	414
435	U7P=0.5*(U(LP)+U(LXP))	AU	415
	V7P=0.5*(V(LP)+V(LYP))	AU	416
	ZP=Z(K)	AU	417
436	O7=ZP-ZM	AU	418
	DUIXJ(1,3)=(U7P-U7M)/O7/R(J)	AU	419
	DUIXJ(2,3)=(V7P-V7M)/O7/R(J)	AU	420
	SUM=0.	AU	421
	DO 402 II=1,3	AU	422
	DO 402 JJ=1,3	AU	423
402	SUM=SUM+(DUIXJ(II,JJ)+DUIXJ(JJ,II))*DUIXJ(II,JJ)	AU	424
	GENR(LP)=SUM	AU	425
	CALCULATE THE SOURCE TERM	AU	426
	LPK=LP+NM*(NVK)	AU	427
	LPO=LP+NM*(NVO)	AU	428
	SU(LI)=RHC(LP)*CD*(F(LP)+1.E-30)*SUM	AU	429
	SP(LI)=RHC(LP)*F(LP)/(F(LP)+1.E-30)	AU	430
C-----	MODIFICATIONS OF THE SOURCE TERMS AT WALL BOUNDARIES.	COMMENT	89
	IF (I.EQ.1S) GO TO 440	AU	431
	IF (JKIN(J,K).EQ.1) GO TO 440	AU	432
	DIST=.5*XDIF(1)	AU	433
	IF (I.EQ.2) DIST=XDIF(2)	AU	434
	VP=.5*SQRT((V(LP)+V(LYP))*2+(W(LP)+W(LZP))*2)	AU	435
	TAUP=AMAX1(GAM(LXM)+VP/DIST,1.E-20)	AU	436
	GAM(LXM)=0.	AU	437
	VXP=V(LP)+V(LYP)+V(LXP)+V(LPP)	AU	438
	WXP=W(LP)+W(LZP)+W(LXP)+W(LPP)	AU	439
	VC=.25*SQRT(VXP*2+WXP*2)	AU	440
	DVDY=VC/XS(I)	AU	441
	SU(LI)=TAUP*DVDY	AU	442
	SP(LI)=RHC(LP)*RHC(LP)*CD*(F(LP)+DVDY/TAUP	AU	443
440	IF (I.LT.1E) GO TO 442	AU	444

IF (J.GT.JWDT.AND.J.LT.JWDT) GO TO 442	AU	445
DIST=.5*XDIF(I+1)	AU	446
IF (I.EQ.L) DIST=XDIF(LP1)	AU	447
VP=.5*SQR((V(LP)+V(LYP))*2+(W(LP)+W(LZP))*2)	AU	448
TAUP=AMAX1(GAM(LXP)*VP/DIST,1.E-20)	AU	449
GAM(LXP)=0.	AU	450
VXM=V(LP)+V(LYP)+V(LXM)+V(LMP)	AU	451
WXM=W(LP)+W(LZP)+W(LXM)+W(LMP)	AU	452
VC=.25*SQR(VXM**2+WXM**2)	AU	453
DVDY=VC/XS(I)	AU	454
SU(IJ)=TAUP*DVDY	AU	455
SP(IJ)=RHO(LP)*RHO(LP)*CD*F(LPK)*DVDY/TAUP	AU	456
442 IF (J.GT.MIN) GO TO 444	AU	457
IF (IDW.EQ.0.OR.IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3) GO TO 444	AU	458
DIST=.5*YDIF(J)	AU	459
IF (J.EQ.2) DIST=YDIF(2)	AU	460
VP=.5*SQR((U(LP)+U(LXP))*2+(W(LP)+W(LZP))*2)	AU	461
TAUP=AMAX1(GAM(LYP)*VP/DIST,1.E-20)	AU	462
GAM(LYP)=0.	AU	463
UYP=U(LP)+U(LXP)+U(LYP)+U(LPP)	AU	464
WYP=W(LP)+W(LZP)+W(LYP)+W(LPP)	AU	465
VC=.25*SQR(UYP**2+WYP**2)	AU	466
DVDY=VC/YS(J)	AU	467
SU(IJ)=TAUP*DVDY	AU	468
SP(IJ)=RHO(LP)*RHO(LP)*CD*F(LPK)*DVDY/TAUP	AU	469
444 IF (J.LT.MAX) GO TO 401	AU	470
IF (IKIN(I,K).EQ.7.OR.IKIN(I,K).EQ.9) GO TO 401	AU	471
DIST=.5*YDIF(J+1)	AU	472
IF (J.EQ.M) DIST=YDIF(MP1)	AU	473
VP=.5*SQR((U(LP)+U(LXP))*2+(W(LP)+W(LZP))*2)	AU	474
TAUP=AMAX1(GAM(LYP)*VP/DIST,1.E-20)	AU	475
GAM(LYP)=0.	AU	476
UYM=U(LP)+U(LXP)+U(LYM)+U(LPM)	AU	477
WYM=W(LP)+W(LZP)+W(LYM)+W(LPM)	AU	478
VC=.25*SQR(UYM**2+WYM**2)	AU	479
DVDY=VC/YS(J)	AU	480
SU(IJ)=TAUP*DVDY	AU	481
SP(IJ)=RHO(LP)*RHO(LP)*CD*F(LPK)*DVDY/TAUP	AU	482
401 CONTINUE	AU	483
GO TO 5000	AU	484
C +--+--+--+--+ SOURCE TERMS FOR TURBULENCE DISSIPATION +--+--+--+--+	AU	485
500 CONTINUE	AU	486
IF (INV.NE.LVD) GO TO 600	AU	487
DO 501 J=2,M	AU	488
IS=IWL(I,J,NGCTD)	AU	489
IF=IWL(I,J,NGCTD)	AU	490
DO 501 I=IS,IF	AU	491
LIJ=JM(J)+I	AU	492
LP=LIJ+NM(K)	AU	493
LPK=LP+NM(NVK)	AU	494
LPO=LP+NM(NVD)	AU	495
SU(LIJ)=C1*CD*RHO(LP)*F(LPK)*GENR(LP)	AU	496
SP(LIJ)=C2*RHO(LP)*F(LPO)/(F(LPK)+1.E-30)	AU	497
501 CONTINUE	AU	498
GO TO 5000	AU	499
C +--+--+--+--+ SOURCE TERMS FOR FUEL +--+--+--+--+	AU	500
600 CONTINUE	AU	501
IF (INV.NE.LVFU) GO TO 700	AU	502
DO 601 J=2,M	AU	503
IS=IWL(I,J,NGCTD)	AU	504
IF=IWL(I,J,NGCTD)	AU	505
DO 601 I=IS,IF	AU	506
LIJ=JM(J)+I	AU	507
LP=LIJ+NM(K)	AU	508

LPCO=L*P+NVM(NVCO)	4STEP	236
LPFUOX=L*P+NVM(NVFUOX)	4STEP	237
LPFU=L*P+NVM(NVFU)	4STEP	238
LPTE=L*P+NVM(NVTE)	4STEP	239
LPCH=L*P+NVM(NVCH)	4STEP	240
LPH2=L*P+NVM(NVMH2)	4STEP	241
FLPTE=F(LPTE)	4STEP	242
FLPTE=AMAX1(FLPTE,100.)	4STEP	243
FLPOX=RATIO1*F(LPFU)+RATIO3*F(LPCO)+RATIO2-(RATIO2+RATIO1)*	4STEP	244
1 F(LPFUOX)+RATIO5*F(LPCH)+RATIO6*F(LPH2)	4STEP	245
FLPOX=AMAX1(FLPOX,0.0)	4STEP	246
ARRHEN=PREXP2*EXP(-ARCON2/FLPTE)	4STEP	247
RHQLP=ABS(RHQLP)	4STEP	248
SOR1=((F(LPCH)*RHQLP)**AA2)*((FLPOX*RHQLP)**BB2)*((F(LPFU)*RHQLP	4STEP	249
1+1.E-30)**CC2)*ARRHEN	4STEP	250
IF(MODER.EQ.2)GO TO 952	4STEP	251
SOR=SOR1	4STEP	252
GO TO 953	4STEP	253
952 PHI=AMIN1(F(LPCH),FLPOX/RATIO5)	4STEP	254
SOR2=-CR2*PHI*RHQLP)*EDK(LPC)	4STEP	255
SOR=AMAX1(SOR1,SOR2)	4STEP	256
953 FUB=AMAX1(0.,((RATIO2+RATIO1)*F(LPFUOX)-RATIO2-RATIO3*F(LPCO)	4STEP	257
1-RATIO1)*F(LPFU)-RATIO6*F(LPH2))/RATIO5)	4STEP	258
FUR=AMIN1(F(LPCH),FUB)	4STEP	259
DSOSP=SOR/(F(LPCH)-FUR+1.E-30)	4STEP	260
SUCH(LP)=SOR-DSOSP*F(LPCH)	4STEP	261
SPCH(LP)=DSOSP	4STEP	262
SU(LIJ)=SUCH(LP)-RATIO8*(SUFU(LP)+SPFU(LP)*F(LPFU))	4STEP	263
SP(LIJ)=DSOSP	4STEP	264
951 CONTINUE	4STEP	265
GO TO 9000	4STEP	266
960 IF(NV.NF.LVMH2)GO TO 1000	4STEP	267
C-----SOURCE TERMS FOR H2-----	4STEP	268
DO 961 J=2,M	4STEP	269
IS=IWL1(J,NGOTN)	4STEP	270
IF=IWL0(J,NGOTO)	4STEP	271
DO 961 I=IS,IF	4STEP	272
LIJ=JH(IJ)+I	4STEP	273
LP=LIJ-KM(K)	4STEP	274
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)+.MJ-2)	4STEP	275
LPCO=L*P+NVM(NVCO)	4STEP	276
LPFUOX=L*P+NVM(NVFUOX)	4STEP	277
LPFU=L*P+NVM(NVFU)	4STEP	278
LPTE=L*P+NVM(NVTE)	4STEP	279
LPCH=L*P+NVM(NVCH)	4STEP	280
LPH2=L*P+NVM(NVMH2)	4STEP	281
FLPTE=F(LPTE)	4STEP	282
FLPTE=AMAX1(FLPTE,100.)	4STEP	283
FLPOX=RATIO1*F(LPFU)+RATIO3*F(LPCO)+RATIO2-(RATIO2+RATIO1)*	4STEP	284
1 F(LPFUOX)+RATIO5*F(LPCH)+RATIO6*F(LPH2)	4STEP	285
FLPOX=AMAX1(FLPOX,0.0)	4STEP	286
ARRHEN=PREXP4*EXP(-ARCON4/FLPTE)	4STEP	287
RHQLP=ABS(RHQLP)	4STEP	288
SOR1=((F(LPH2)*RHQLP)**AA4)*((FLPOX*RHQLP)**BB4)*((F(LPCH)*RHQLP	4STEP	289
1+1.E-30)**CC4)*ARRHEN	4STEP	290
IF(MODER.EQ.2)GO TO 962	4STEP	291
SOR=SOR1	4STEP	292
GO TO 963	4STEP	293
962 PHI=AMIN1(F(LPH2),FLPOX/RATIO6)	4STEP	294
SOR2=-CR4*PHI*RHQLP)*EDK(LPC)	4STEP	295
SOR=AMAX1(SOR1,SOR2)	4STEP	296
963 FUR=AMAX1(0.,((RATIO2+RATIO1)*F(LPFUOX)-RATIO2-RATIO3*F(LPCO)	4STEP	297
1-RATIO1)*F(LPFU)-RATIO5*F(LPCH))/RATIO6)	4STEP	298
FUR=AMIN1(F(LPH2),FUR)	4STEP	299

050SP=SR/(F(LPH2)-FUB+1.E-30)	4STEP	300
SII(LIJ)=SOR-050SP*F(LPH2)-RATIO12*(SUFU(LP)+SPFU(LP)*F(LPFU))	4STEP	301
1-RATIO10*(SUCH(LP)+SPCH(LP)*F(LPCH))	4STEP	302
SPI(LIJ)=050SP	4STEP	303
961 CONTINUE	4STEP	304
GO TO 5000	500T	167
C-----SOURCE TERM FOR NUCLEI CONCENTRATION -----	500T	168
1000 IF(MV.NF.LVN)60 TO 1100	500T	169
DO 1001 J=2,M	500T	190
IS=IWL1(J,NGOTO)	500T	191
IE=IWLQ(J,NGOTO)	500T	192
DN 1001 I=IS,IF	500T	193
LIJ=JN(J)+1	500T	194
LP=LIJ+KN(K)	500T	195
LPFOX=LP+NVN(MVFUX)	500T	196
LPFU=LP+NVN(MVFU)	500T	197
LPCO=LP+NVN(MVCO)	500T	198
LPTF=LP+NVN(MVTE)	500T	199
LPCH=LP+NVN(MVCH)	4STEP	305
LPH2=LP+NVN(MVHL)	4STEP	306
T=F(LPTE)	500T	200
FLPOK=RATIO10*F(LPFU)+RATIO30*F(LPCO)+RATIO2-(RATIO2+RATIO1)*	500T	201
1 F(LPFUX)+RATIO50*F(LPCH)+RATIO60*F(LPH2)	4STEP	307
FLPOK=AMAX1(FLPOK,1.E-30)	500T	203
CARB=F(LPFUX)*12.0*CX/WFU	500T	204
LPC=1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)	500T	205
LPS1=LP+NVN(MVS1)	500T	206
LPS2=LP+NVN(MVS2)	500T	207
LPN=LP+NVN(MVN)	500T	208
FUB=F(LPFUX)-F(LPFU)	500T	209
FLPCO2=WC02*(CX*FUB/WFU-CX*F(LPCH)/WCH-F(LPCO)/WCO)	4STEP	308
FLPH20=0.5*WM20*(HY*FUB/WFU-RATIO7*F(LPCH)-F(LPH2))	4STEP	309
FLPH2=1.0-F(LPFU)-FLPCO2-F(LPCO)-FLPOK-FLPH20-F(LPCH)-F(LPH2)	4STEP	310
VMIX=F(LPFU)/WFU+FLPCO2/WCO2+F(LPCO)/WCO+FLPOK/WOX+FLPH20/WM20	500T	213
1+FLPH2/WM2+F(LPCH)/WCH+F(LPH2)/WM2	4STEP	311
RET=(AMU*EDK2(LPC)/RND(LP))*0.25	500T	215
ENDOT=25.6*RET*EDK(LPC)	500T	216
EMPR=FUB*(1.0+RATIO1)	500T	217
PSI=EMPR/(EMPR+F(LPFU)*(1.0+RATIO1))	500T	218
EMIN=AMIN1(F(LPFU),FLPOK/RATIO1)	500T	219
C-----BYPASS CALCULATION IF TEMP.LT.TINCP, OR IF	COMMENT	90
C CARBON/OXYGEN RATIO LT.CINCP (TINCP AND CINCP INPUT BY USER).	COMMENT	91
IF(T.LT.TINCP)60 TO 1006	500T	220
IF(CARB/FLPOK.LT.CINCP)60 TO 1006	500T	221
EMP=(F(LPS1)/DPART(1))*3+F(LPS2)/(DPART(2)+1.E-30)*3)	500T	222
1/(F(LPS1)+F(LPS2))	500T	223
EMP=RHCP*3.14159/(6.0*EMP)	500T	224
AND=AD*RND(LP)*F(LPFU)*EXP(-ARCONH/F(LPTE))	500T	225
GAMAS=AMIN1(1.0,9.7*RET*3)	500T	226
GPST=GAMAS*PSI	500T	227
NGPST=1.0-GPST	500T	228
INCP5=1	NOX	167
NS1=INFU	NOX	168
NS2=IOCO2	NOX	169
C-----CALCULATE MIXTURE CP.	COMMENT	92
TK=T	NOX	170
TKINV=1.000/TK	NOX	171
DO 1012 II=NS1,NS2	NOX	172
1012 S2(II)=FS(LP,II)/SMW(II)	NOX	173
CALL MCPS	NOX	174
CPR=CPSUM*UNICON	NOX	175
DELTA T=DHR*EMPIN/CPR	500T	231
TSTR=F(LPTE)+DELTA T	500T	232
RNDSTR=RNDCON/(VMIX*TSTR)	500T	233

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TD=F(LPTE)-DELTAT*GPSI/DGPSI	SOOT	234
TD=AMAX1(TD,100.0)	SOOT	235
RHOD=RHOCON/(VMI*XTD)	SOOT	236
ANOSTR=AD*RHODSTR*F(LPFU)*EXP(-ARCONN/TSTR)	SOOT	237
ANN=AD*RHOD*F(LPFU)*EXP(-ARCONN/TO)	SOOT	238
GPSIR=GPSI/RHODSTR	SOOT	239
DGPSIR=DGPSI/RHOD	SOOT	240
ENRHO=F(LPN)/RHO(LP)	SOOT	241
EMDTR=EMDOT*RHODSTR/(GPSI*DGPSI)	SOOT	242
ENN=(F(LPS1)+F(LPS2))*RHO(LP)/EMP	SOOT	243
ENNRHO=ENN/RHO(LP)	SOOT	244
A1=(ANOSTR+EMDTR*ENNRHO)/GO	SOOT	245
A2=(FMG-EMDTR/RHODSTR)/GO	SOOT	246
A3=EMDTR*A1/RHODSTR	SOOT	247
A4=EMDTR*(A2/RHODSTR-ENNRHO)	SOOT	248
A5=-RHO*A1	SOOT	249
A6=AAA-BBO*A2	SOOT	250
ARG=SQRT(ARS((A4-A5)**2+4.0*A6*A5))	SOOT	251
ENSTR1=(A4-A5+ARG)/(2.0*A6)	SOOT	252
ENSTR2=(A4-A5-ARG)/(2.0*A6)	SOOT	253
ENSTR=ENSTR1	SOOT	254
IF(ENSTR1.LT.0.0)ENSTR=ENSTR2	SOOT	255
ENSTR=AMIN1(ENSTR,ENNRHO/GPSIR)	SOOT	256
FNSTR=AMAX1(ENSTR,ENNRHO*RHODSTR)	SOOT	257
ENSTR=AMAX1(1.0,ENSTR)	SOOT	258
ENNSTR=(A1+A2*ENSTR)/ENSTR	SOOT	259
ENNSTR=AMIN1(ENNSTR,AAA/BBO)	SOOT	260
ENNSTR=AMIN1(ENNSTR,ENNRHO/GPSIR)	SOOT	261
ENNSTR=AMAX1(1.0,ENNSTR)	SOOT	262
END=(ENNRHO-ENSTR*GPSIR)/DGPSIR	SOOT	263
END=AMAX1(1.0,END)	SOOT	264
ENNO=(ENNSTR-ENNSTR*GPSIR)/DGPSIR	SOOT	265
ENNNO=AMAX1(1.0,ENNO)	SOOT	266
FMGF=FMG*F(LPN)	SOOT	267
SUF1=ANO+FMGF	SOOT	268
SPF1=GC*ENN	SOOT	269
SUF2=(ANOSTR*GPSIR+ANNO*DGPSIR+GO*ENSTR*GPSIR*(ENNO-ENNSTR))	SOOT	270
1*RHOD(LP)+FMGF	SOOT	271
SPF2=GO*ENNNO	SOOT	272
RF1=SUF1-SPF1*F(LPN)	SOOT	273
RF2=SUF2-SPF2*F(LPN)	SOOT	274
C-----FORMATION RATE.	COMMENT	93
IF(RF1.GT.RF2)GO TO 1004	SOOT	275
SU(LIJ)=SUF1	SOOT	276
SP(LIJ)=SPF1	SOOT	277
GO TO 1005	SOOT	278
1004 SU(LIJ)=SUF2	SOOT	279
SP(LIJ)=SPF2	SOOT	280
GO TO 1005	SOOT	281
1006 SU(LIJ)=0.0	SOOT	282
SP(LIJ)=0.0	SOOT	283
C-----FORMATION RATE.	COMMENT	94
1005 RNC=EMDOT*PSI*EMMIN/(F(LPFU)+1.E-30)	SOOT	284
SP(LIJ)=SP(LIJ)-RNC	SOOT	285
1001 CONTINUE	SOOT	286
GO TO 5000	SOOT	287
C-----SOURCE TERM FOR SOOT CONCENTRATION	SOOT	288
1100 IF(NV.LT.LVS1.OR.NV.GT.LVS2)GO TO 1300	SOOT	289
IT=NV-LVS1+1	SOOT	290
CONS2=6.0/(RHOD*DPART(I))	SOOT	291
DO 1101 J=2,M	SOOT	292
IS=IWL1(J,MGOTO)	SOOT	293
IF=IWL1(J,NGOTO)	SOOT	294
DO 1101 I=IS,IF	SOOT	295

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L1J=JN(J)+I
LP=L1J+KN(K)
LPFUNDV=LP+NM(NVFDUX)
LPFU=LP+NM(NVFU)
LPCO=LP+NM(NVCO)
LPTE=LP+NM(NVTE)
LPCN=LP+NM(NVCH)
LPH2=LP+NM(NVH2)
T=F(LPTE)
FLPOX=RATIO1*F(LPFU)+RATIO3*F(LPCO)+RATIO2*(RATIO2+RATIO1)*
1 F(LPFUNDV)+RATIO5*F(LPCH)+RATIO6*F(LPH2)
FLPOX=AMAX1(FLPOX,1.E-30)
CARB=F(LPFUNDV)*12.0*CX/WFU
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)
LPS1=LP+NM(NVS1)
LPS2=LP+NM(NVS2)
LPS=LP+NM(NV)
LPN=LP+NM(NVN)
FUB=F(LPFUNDV)-F(LPFU)
FLPCO2=WC02*(CX+FUB/WFU-CX*F(LPCH)/WCH-F(LPCO)/WCO)
FLPH2O=0.5*WH2O*(HY+FUB/WFU-RATIO7*F(LPCH)-F(LPH2))
FLPH2=1.0-F(LPFU)-FLPCO2-F(LPCO)-FLPOX-FLPH2O-F(LPCH)-F(LPH2)
VMIX=F(LPFU)/WFU+FLPCO2/WCO2+F(LPCO)/WCO+FLPOX/WOX+FLPH2O/WH2O
1+FLPH2/WH2+F(LPCH)/WCH+F(LPH2)/WH2
RET=(AMU*EOK2(LPC)/RHO(LP))*0.25
FMDDT=23.6*RET*EOK(LPC)
EMPR=FUB*(1.0+RATIO1)
PSI=EMPR/(EMPR+F(LPFU)*(1.0+RATIO1))
FMHIN=AMIN1(F(LPFU),FLPOX/RATIO1)
C-----BYPASS CALCULATION IF TEMP.LT.TINCP, OR IF
C CARBON/OXYGEN RATIO LT.CINCP (TINCP AND CINCP INPUT BY USER).
IF(T.LT.TINCP)GO TO 1106
IF(CARB/FLPOX.LT.CINCP)GO TO 1106
EMP=(F(LPS1)/OPART(1))*3+F(LPS2)/(OPART(2)+1.E-30)*3)
1/(F(LPS1)+F(LPS2))
EMP=RHO*3.14159/(6.0*EMP)
ANO=AQORHO(LP)*F(LPFU)*EXP(-ARCONN/F(LPTE))
GAMAS=AMIN1(1.0,9.7*RET*3)
GPSI=GAMAS*PSI
OGPSI=1.0-GPSI
IMCPS=1
NS1=IDFU
NS2=IOCO2
C-----CALCULATE MIXTURE CP.
TK=T
TKINV=1.000/TK
N7 1013 II=NS1,NS2
1013 S2(II)=FS(LP,II)/SMW(II)
CALL MCPS
CPR=CPSUM*UNICON
DELTAT=DHR*EMFIN/CPR
TSTR=F(LPTE)+DELTAT
RHOSTR=RHOCON/(VMIX*TSTR)
TD=F(LPTE)-DELTAT*GPSI/OGPSI
TO=AMAX1(TD,100.0)
RHODD=RHOCON/(VMIX*TO)
ANODSTR=AQORHOQ*F(LPFU)*EXP(-ARCONN/TSTR)
ANOD=AQORHOQ*F(LPFU)*EXP(-ARCONN/TO)
GPSIR=GPSI/RHODD
OGPSIR=OGPSI/RHODD
ENRHO=F(LPN)/RHO(LP)
EMDDTR=EMDDT*RHODD/GPSI
ENH=(F(LPS1)+F(LPS2))*RHO(LP)/EMP
ENNRHO=ENH/RHO(LP)

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SOOT 296
SOOT 297
SOOT 298
SOOT 299
SOOT 300
SOOT 301
4STEP 312
4STEP 313
SOOT 302
SOOT 303
4STEP 314
SOOT 305
SOOT 306
SOOT 307
SOOT 308
SOOT 309
SOOT 310
SOOT 311
SOOT 312
4STEP 315
4STEP 316
4STEP 317
SOOT 318
4STEP 318
SOOT 319
SOOT 320
SOOT 321
SOOT 322
COMMENT 95
COMMENT 96
SOOT 323
SOOT 324
SOOT 325
SOOT 326
SOOT 327
SOOT 328
SOOT 329
SOOT 330
SOOT 331
NOX 176
NOX 177
NOX 178
COMMENT 97
NOX 179
NOX 180
NOX 181
NOX 182
NOX 183
NOX 184
SOOT 334
SOOT 335
SOOT 336
SOOT 337
SOOT 338
SOOT 339
SOOT 340
SOOT 341
SOOT 342
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SOOT 344
SOOT 345
SOOT 346
SOOT 347

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A1=(ANQSTR+EMDQTR+ENRHO)/GO
A2=(FNG-FHQDTR/RHQSTR)/GO
A3=EMDQTR+A1/RHQSTR
A4=EMDQTR*(A2/RHQSTR-ENRHO)
A5=-RBR+A1
A6=AAA-BRB+A2
ARG=SQRT(ABS((A4-A5)*2+4.0*A6*A3))
ENSTR1=(A4-A5+ARG)/(2.0*A6)
ENSTR2=(A4-A5-ARG)/(2.0*A6)
ENSTR=ENSTR1
IF(ENSTR1.LT.C.0)ENSTR=ENSTR2
ENSTR=AMIN1(ENSTR,ENRHO/GPSIR)
ENSTR=AMAX1(ENSTR,ENRHO/RHQSTR)
ENSTR=AMAX1(1.0,ENSTR)
ENNSTR=(A1+A2+ENSTR)/ENSTR
ENNSTR=AMIN1(ENNSTR,AAA/BBB)
ENNSTR=AMIN1(ENNSTR,ENNRHO/GPSIR)
ENNSTR=AMAX1(1.0,ENNSTR)
END=(ENRHO-ENSTR*GPSIR)/OGPSIR
END=AMAX1(1.0,END)
ENNQ=(ENNRHO-ENNSTR*GPSIR)/OGPSIR
ENNQ=AMAX1(1.0,ENNQ)
C-----QUASIGLOBAL FORMATION RATE.
SUF1=PREXP*(LPTE)*ALPHA*(RHO(LP)*F(LPFU))*AAS*(RHO(LP)*FLPOX)
1009S*EXP(-ARCONS/F(LPTE))*FRACP(II)
C-----TURBULENT FORMATION RATE.
SUF2=EMP*(AAA*F(LPN)+BRB*ENNSTR*GPSIR*RHO(LP)*(END-ENSTR))
1*FRACP(II)
SPF2=RHO(LP)*BRB*END*FRACP(II)
SPF2F=SPF2*F(LPS)
SUF2=APAX1(SUF2,SPF2F)
RF2=SUF2-SPF2F
IF(SUF1.GT.RF2)GO TO 1104
SU(LIJ)=SUF1
SP(LIJ)=0.C
GO TO 1105
1104 SU(LIJ)=SUF2
SP(LIJ)=SPF2
GO TO 1105
110A SU(LIJ)=0.C
SP(LIJ)=0.0
C-----SURFACE OXIDATION RATE.
1105 AREAT=CONS2*RHO(LP)
AKA=2000.0*EXP(-15100./F(LPTE))
AKA=4.4E-1*EXP(-7640./F(LPTE))
AKZ=21.3*EXP(2060./F(LPTE))
AKT=1.51E6*EXP(-48800./F(LPTE))
PQ2=FLPOX*PRESS/(VMIX*32.0*101325.0)
PSIC=1.0/(1.0+AKT/(AKB*PQ2))
AKK=AKA*PQ2/(1.0+AKZ*PQ2)
SPC1=12.0*AREAT*(AKK*PSIC+AKB*PQ2*(1.0-PSIC))
C-----TURBULENT OXIDATION RATE.
SPC2=EMDQTR*PSI*FMIN*RHO(LP)/(F(LPFU)+1.E-30)
SPC1=AMIN1(SPC1,SPC2)
SP(LIJ)=SP(LIJ)-SPC1
1101 CONTINUE
GO TO 9000
C+---+--- OTHER SPECIES - H2O,OH,N,NO,NO2 +---+---+---+---+---+---+---+---+---+---
C THESE SOURCES CALCULATED IN KINETICS PROGRAM CREK.
C
1300 IF(MV.NF.LVM1)GO TO 1400
00 1201 J=2,M
IS=IWL1(J,NGCTO)
IF=IWL0(J,NGCTO)

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SQOT	348
SQOT	349
SQOT	350
SQOT	351
SQOT	352
SQOT	353
SQOT	354
SQOT	355
SQOT	356
SQOT	357
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SQOT	359
SQOT	360
SQOT	361
SQOT	362
SQOT	363
SQOT	364
SQOT	365
SQOT	366
SQOT	367
SQOT	368
SQOT	369
COMMENT	98
SQOT	370
SQOT	371
COMMENT	99
SQOT	372
SQOT	373
SQOT	374
SQOT	375
SQOT	376
SQOT	377
SQOT	378
SQOT	379
SQOT	380
SQOT	381
SQOT	382
SQOT	383
SQOT	384
SQOT	385
SQOT	386
COMMENT	100
SQOT	387
JAN14	1
JAN14	2
SQOT	390
SQOT	391
SQOT	392
SQOT	393
SQOT	394
SQOT	395
COMMENT	101
SQOT	396
SQOT	397
SQOT	398
SQOT	399
SQOT	400
COMMENT	102
COMMENT	103
COMMENT	104
NOX	185
NOX	186
NOX	187
NOX	188

1201 00 1201 I=IS,IF
 1(IJ=I+J,IFJ)
 50(LIJ)=0.0
 5P(LIJ)=0.0
 60 TO 5000
 1400 CONTINUE
 5000 CONTINUE
 RETURN
 END
 SUBROUTINE AUXRAD
 COMMON F(3500),DU(500),DV(500),DW(500),
 1 ANUC(500),SOOT1(500),SOOT2(500),FCH(500),FMR(500),FS(500,14),
 1 RHO(500),VISC(500),ABSR(500),SCTR(500),SU(100),SP(100),
 1 ORHNDP(500),
 1 AKP(100),AXM(100),AYP(100),AYM(100),AZP(100),
 2 AZM(100),C7(100),CY(10),CZU(100),CYU(10),
 3 C7P(100),CYP(10),DIVG(100),NTP1,NTP2
 1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
 2 SUK(192),SPK(192)
 DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
 DIMENSION GAM(500)
 EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
 EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
 EQUIVALENCE (F(3001),GAM(1))
 COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX
 COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
 1 YSV(30),ZSV(30),XOIF(40),YOIF(30),ZOIF(30),FXP(40),FXM(40),
 2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME
 COMMON
 1/CINDEF/IDCO,IDFU,IOO2,ION2,IOH2O,IDCO2,IONH,IOH2,ION1,IONO,IONO2
 1,ION,IOOH,INCP5,ILC,ILH,INAT,ITER,JJJ,N1,N2,N3,NA,NGL08,NGL0BP,
 2 NLH,NQ,NSP,NS1,NS2,IOCH
 3/CCHEMI/CPSUP,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
 4/CPAQA/ASUB(30,3),ENV,ER,HSUBO,NOEBUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOPP,
 4 SM,SMW(30),SPO,S1(30),S2(30),TK,LADIA0,LOEBUG,LEQUIL,LREACT,
 4 LENER,EDKIJ,LCONVG
 DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUBO,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,
 1 Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO
 2,FUT,FST
 COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,
 1 CEBU3,CEBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
 2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST
 LOGICAL LADIA0,LCONVG,LOEBUG,LEQUIL,LNRG,LREACT,LENER
 COMMON/INT/L,M,N,LCV,MCV,NCV,LP1,MP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,
 1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KM(30),JM(30),ISTEP,
 2 ISOLVE(32),IPRINT(33),TITLE(10,33),IKY,ISWP,JSWP,RELAX(35),NP,
 3 NRHO,NGAP,IWL(30,5),IWL0(30,5),JWL0(40,5),JWL(40,5),IWEI,
 4 IWE0,MM1,JWII,JWIO,JWOT,JWNO,IOW,JKIN(30,30),IKIN(40,30)
 COMMON/INDEX/IPAR,LREF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE
 1,PLAXP1,LVK,LVO,LVFUX,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),
 2 IJUMP,IRES,TITLEZ(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH2O,NVCO2,
 3 NVH2,NVCH,NVH2
 COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVON,LVH2O,LVN2,LVO2,
 1 LVCO2,LVFU1,LVCO1,NNOX,INOX,ITNOX,SNOX,TNOX
 COMMON/THERP/NVH,NVFU,NVOX,NVFUX,NVTE,MODEN,IOK,FSTOIC,MFU,CP,
 1 GASCON,RHOCOM,UNICOM,PRESS,NVFAV,TCYLV,TINLV,TLIP,ACDEF(4),
 2 T4,OFAC,MFU,WCO2,WCO,WDX,WM2O,WM2,MVY,CXX,RATIO1,RATIO2,
 3 RATIO3,RATIO4,HCO,TAN,ITWALL
 COMMON/CTDMA/KEND,ICTDMA(32)
 COMMON/MIS/AMU,DEM,SNAX,SSUN,LASTEP,HTCEXT,CFR,ENISW,ENISIN,
 1 FMISR,TOUT,RTCD,EMI,RADIN,RADSUR,FMA,FK,SQFF,
 2 FKFU,FDFU,TFUEL,MFNZ,FLO(40),TFHMH(40),H(40),FUEL(40),FUDX(40),
 2 UINI(40),TIN(40),FUELS(40),SEXIT,IGAM1(29),IGAM2(29)
 COMMON/TUPR/NVK,NVO,C1,C2,CD,AK,OUIDXJ(3,3),AKFAC,ALFAC,

NOX 189
 NOX 190
 NOX 191
 NOX 192
 NOX 193
 NOX 194
 AU 615
 AU 616
 AU 617
 AUR 2
 COMFB 2
 4STEP 18
 RAD 3
 RAD 4
 COMFB 4
 COMFB 5
 COMFB 6
 CTOMA 3
 CTOMA 4
 COMFB 7
 COMFB 8
 COMFB 9
 COMFB 10
 COMFB 11
 COMMON 2
 COMMON 3
 COMMON 4
 COMMON 5
 NOX 2
 NOX 3
 NOX 4
 4STEP 3
 NOX 6
 NOX 7
 NOX 8
 NOX 9
 NOX 10
 NOX 11
 4STEP 4
 4STEP 5
 4STEP 6
 4STEP 7
 NOX 12
 COMMON 6
 4STEP 8
 4STEP 9
 COMMON 9
 COMMON 10
 COMMON 11
 4STEP 10
 COMMON 13
 4STEP 11
 NOX 16
 NOX 17
 COMMON 19
 COMMON 16
 COMMON 17
 COMMON 18
 4STEP 12
 COMGEN 2
 COMGEN 3
 COMGEN 4
 4STEP 13
 COMGEN 6

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1 MODFL,PR(32),PREF(32),PJAY(32),E
COMMON/PAID/NVE,SIGMA,ABSOR,SCATR
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER
COMMON/DRNPL/EVAP(192),NTP4,MFNZ,KO(3),YQ(3),ZO(3),ALFA(3),
1 META(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SMD(3),
2 VFUEL(3),RFUEL(3),EVSU(64),MEVAP
COMMON/INJEC/FLWIN,IWINJ(20),JWINJ(20),UWINJ(20),WUWINJ(20),
1 AUWINJ(20),TUWINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),
2 FVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),NUWINJ,NVINJ,JSW1,JSW2,
3 USW,VSW,AFSW,FSW,TSW,WSW,SWNO,RHOSW
COMMON/CSOOT/NVM,NVS1,NVS2,ISOOT,SSOOT,NSOOT,AD,ARCONH,AAA,BBB,FMG
1 GO,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BBS,DHR
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT
COMMON/CRAD/IRAD,SRAD
COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BB1,CC1,
1 AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,
2 RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,WCH2,WCH3,LVCH,LVCH1,LVCH2
C 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00
ENTRY GAMRAD
C-----ENTRY GAMRAD IS USED TO CALCULATE THE GAMAS IN THE RADIATION
C EQUATIONS.
C
IF (NVE,EQ,LVRY) GO TO 3100
DO 4002 K=1,NP1
DO 4002 J=1,NP1
KJM=KM(K)+JP(J)
IS=IWL1(J,4)
IF=IWL2(J,4)
DO 4002 I=IS,IE
LP=KJM+I
C-----VALUES OF ABSORPTION AND SCATTERING COEFFICIENTS FOR
C ITRAD=2.
ABSR(LP)=ABSOR
4002 SCTR(LP)=SCATR
IF(ITRAD.NE.3160 TO 4001)
C-----ABSORPTION COEFFICIENT CALCULATED FROM SUBROUTINE ABSOR
C (ITRAD=3).
DO 4000 K=2,N
DO 4000 J=2,N
KJM=KM(K)+JP(J)
IS=IWL1(J,4)
IF=IWL2(J,4)
DO 4000 I=IS,IE
LP=KJM+I
TS=TEMP(LP)
TS=AMAX1(TS,300.0)
TS=AMIN1(TS,2000.0)
T=TS
PATH=2.0*Y(MP1)
C-----SOOT CONCENTRATION.
SOOTK=7.0*(SCCT1(LP)+SOOT2(LP))*RHOD(LP)/(RHOP*0.94E-6)
LPFU=LP+NVM(NVFU)
LPFUDX=LP+NVM(NVFUDX)
LPCO=LP+NVM(NVCO)
LPCM=LP+NVM(NVCH)
LPH2=LP+NVM(NVH2)
FUR=F(LPFUDX)-F(LPFU)
C-----CO2 AND H2O CONCENTRATIONS.
FLPCO2=WCO2*(CYX*FUR/WFU-CYX*F(LPCM)/WCH-F(LPCO)/WCO)
FLPCO2=AMAX1(1.E-30,FLPCO2)
FLPOX=AMAX1(0.0,RATIO1*F(LPFU)+RATIO3*F(LPCO)+RATIO2
1-(RATIO1+RATIO2)*F(LPFUDX)+RATIO5*F(LPCM)+RATIO6*F(LPH2))
FLPH2O=C.5*WH2O*(HYT*FUR/WFU-RATIO7*F(LPCM)-F(LPH2))
FLPH2O=AMAX1(1.E-30,FLPH2O)

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4STEP 14
COMGEN 8
COMGEN 9
COMGEN 10
COMGEN 11
COMGEN 12
COMGEN 13
COMGEN 14
COMGEN 15
COMGEN 16
SOOT 8
SOOT 9
SOOT 10
SOOT 11
4STEP 15
4STEP 16
4STEP 17
AUR 6
AUR 7
COMMENT 105
COMMENT 106
COMMENT 107
AUR 8
RAD 74
RAD 75
RAD 76
RAD 77
RAD 78
RAD 79
RAD 80
COMMENT 108
COMMENT 109
RAD 81
RAD 82
RAD 83
COMMENT 110
COMMENT 111
RAD 84
RAD 85
RAD 86
RAD 87
RAD 88
RAD 89
RAD 90
RAD 91
RAD 92
RAD 93
RAD 94
RAD 95
COMMENT 112
RAD 96
RAD 97
RAD 98
RAD 99
4STEP 319
4STEP 320
RAD 100
COMMENT 113
4STEP 321
RAD 102
RAD 103
4STEP 322
4STEP 323
RAD 106

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FLPH2=1.0-F(LPFU)-FLPCQ2-F(LPCQ)-FLPOX-FLPH2Q-F(LPH1)-F(LPH2)	4STEP	324
FLPH2=AMAX1(0.0,FLPH2)	RAD	108
VMTX=F(LPFU)/WPU+FLPCQ2/WCQ2+F(LPCQ)/WCQ+FLPOX/WOX+FLPH2Q/WH2Q	RAD	109
1+FLPH2/WH2+F(LPH1)/WCH+F(LPH2)/WH2	4STEP	325
PCQ2=FLPCQ2/(VMTX*WCQ2)	RAD	111
PH2Q=FLPH2Q/(VMTX*WH2Q)	RAD	112
PCQ2=AMIN1(PCQ2,1.0-PH2Q)	RAD	113
FACP=5.97*T/TS	RAD	114
PATH=AMIN1(PATH,FACP/PCQ2)	RAD	115
PATH=AMIN1(PATH,FACP/PH2Q)	RAD	116
CALL ABSORR(TS,T,PATH,SOOTK,PCQ2,PH2Q,ALPHAS)	RAD	117
ALPHAS=AMIN1(ALPHAS,0.999)	RAD	118
ABSR(LP)=ALOG(1.0-ALPHAS)/PATH	RAD	119
4000 CONTINUE	RAD	120
4001 CONTINUE	RAD	121
CALCULATE GAMA FOR X-DIRECTION FLUX.	COMMENT	114
DO 3000 K=1,NP1	AUR	9
DO 3000 J=1,NP1	AUR	10
KJM=KM(K)+JM(J)	AUR	11
IS=INLI(J,4)	AUR	12
IE=IWLO(J,4)	AUR	13
DO 3000 I=IS,IE	AUR	14
LP=KJM+I	AUR	15
GAM(LP)=1.0/(ABSR(LP)+SCTR(LP))	RAD	122
3000 CONTINUE	AUR	17
GO TO 3300	AUR	18
CALCULATE GAMA FOR Y-DIRECTION FLUX.	COMMENT	115
3100 DO 3200 K=1,NP1	AUR	19
DO 3200 J=1,NP1	AUR	20
KJM=KM(K)+JM(J)	AUR	21
IS=INLI(J,4)	AUR	22
IE=IWLO(J,4)	AUR	23
DO 3200 I=IS,IE	AUR	24
LP=KJM+I	AUR	25
GAM(LP)=1.0/(ABSR(LP)+SCTR(LP)+1.0/(R(J)+1.E-30))	RAD	123
3200 CONTINUE	AUR	27
3300 RETURN	AUR	28
C ** ** ** **	AUR	29
ENTRY SORAD	AUR	30
C-----ENTRY SORAD IS USED TO CALCULATE THE SOURCE TERMS IN THE	COMMENT	116
C RADIATION EQUATIONS.	COMMENT	117
C	COMMENT	118
IF (NV.EQ.LVR2) GO TO 300	AUR	31
C-----X- AND Y-DIRECTION FLUXES.	COMMENT	119
DO 101 J=2,N	AUR	32
IS=INLI(J,NGOTO)	AUR	33
IE=IWLO(J,NGOTO)	AUR	34
DO 101 I=IS,IE	AUR	35
LIJ=JM(J)+I	AUR	36
LP=LIJ+KM(K)	AUR	37
LPRX=LP+NVX(NVRX)	AUR	38
LPRY=LP+NVY(NVRY)	AUR	39
LPRZ=LP+NVZ(NVRZ)	AUR	40
LPTX=LP+NVX(NVTE)	AUR	41
FLPTE=F(LPTE)	AUR	42
FLPE=SIGMA*FLPTE**4	AUR	43
SU(LIJ)=ABSR(LP)+FLPE+SCTR(LP)*(F(LPRX)+F(LPRY)+F(LPRZ))/3.	RAD	124
SP(LIJ)=-(ABSR(LP)+SCTR(LP))	RAD	125
101 CONTINUE	AUR	46
RETURN	AUR	47
300 CONTINUE	AUR	48
C-----Z-DIRECTION FLUX.	COMMENT	120
DO 301 K=2,N	AUR	49
KJM=KM(K)+JM(JPLANE)	AUR	50

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IS=IWL I(JPLANE,NGOTO)
IF=IWL O(JPLANE,NGOTO)
NN 301 I=IS,IF
LIK=JM(K)+I
LP=KJM+I
LPRX=LP+NVH(NVRX)
LPRY=LP+NVH(NVRY)
LPRZ=LP+NVH(NVRZ)
LPTF=LP+NVH(NVTF)
FLPTE=F(LPTE)
FLPE=SIGMA*FLPTE**4
SU(LIK)=ABSR(LP)*FLPE+SCTR(LP)*(F(LPRX)+F(LPRY)+F(LPRZ))/3.
SP(LIK)=-1ABSR(L)*SCTR(LP)
301 CONTINUE
RETURN
END
SUBROUTINE SPRAY
C ***** SUBROUTINE SPRAY *****
C SUBROUTINE FOR AIRTRIP CODE WHICH CALCULATES THE TRAJECTORY
C AND EVAPORATION RATES FOR A FUEL NOZZLE SPRAY. WRITTEN NOV. 1976
C *****
COMMON F(3500),DU(500),DV(500),DW(500),
1 ANUC(500),SOUT1(500),SOUT2(500),FCH(500),FH2(500),FS(500,14),
1 RH0(500),VISC(500),ABSR(500),SCTR(500),SU(100),SP(100),
1 DRHDP(500),
1 AXP(100),AXM(100),AYP(100),AYM(100),AZP(100),
2 AZM(100),CZ(100),CY(10),CZU(100),CYU(10),
3 C7P(100),CYP(10),DIV6(100),NTP1,NTP2
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
DIMENSION GAM(500)
EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
EQUIVALENCE (F(3001),GAM(1))
COMMON/CYL/R(30),RM(30),RNV(30),YSR(30),YSVR(30),IPLAX
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSV(30),KDF(40),YDF(30),ZDF(30),FXP(40),FXM(40),
2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME
COMMON
1/CINDEX/IDCC,IDFU,IDG2,ION2,ION20,IDC02,ION1,ION2,ION0,ION02
1,IDO,IONH,IHCPS,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NGL02,NGL0P,
2 NLN,NQ,NSH,NS1,NS2,IOCH
3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNR6
4/CPARAM/ASUB(30,3),ENV,FR,HSUB0,NDEB0G,NS,PA,Q0,Q1,Q2,Q3,Q4,RHDP,
4 SM,SMW(30),SMO,S1(30),S2(30),TK,LADTAB,LDEB0G,LEQUIL,LREACT,
4 LENER,EONIJ,LCONVG
DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUB0,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,
1 Q4,RGAS,RGASIN,RHDP,SH,SHINV,SMW,S1,S2,TK,TKINV,TLN,SMO
2,FUT,FST
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,C8BU1,C8BU2,
1 CERU3,CERU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
2 CFXP1,CXP2,CXP3,CXP4,FUT,FST
LOGICAL LADTAB,LCONVG,LDEB0G,LEQUIL,LNR6,LREACT,LENER
COMMON/INT/L,N,NLCV,NCV,NCV,L01,NP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,
1 NVV,NGOTO,N,ISTR,JSTR,KSTR,NVH(35),KH(30),JM(30),ISTEP,
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISMP,JSMP,RELAX(33),NP,
3 NRM0,NGAM,IWL I(30,5),IWL O(30,5),JWL O(40,5),JWL I(30,5),IWEI,
4 IWE0,MH1,JWI1,JWI0,JWI2,ION0,ION,JKIN(30,30),IKIN(40,30)
COMMON/INDEX/IPAR,LPRF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE
1,PLAM1,LVK,LVD,LVFUD0,LVFU,LVCO,LVM,LVRX,LVRY,LVRZ,NVF(32),
2 IJUMP,IFES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH20,NVCO2,
3 NVN2,NVCH,NVH2
COMMON/CNOX/LVH1,LVH2,LVM1,LVM0,LVM02,LVD,LV0H,LVH20,LVN2,LV02,

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AUR 51
AUR 51
AUR 53
AUR 54
AUR 55
AUR 56
AUR 57
AUR 58
AUR 59
AUR 60
AUR 61
RAD 126
RAD 127
AUR 64
AUR 65
AUR 66
SP 2
SP 3
SP 4
SP 5
SP 6
CONF 2
4STEP 18
RAD 3
RAD 4
CONF 4
CONF 5
CONF 6
CTDMA 3
CTDMA 4
CONF 7
CONF 8
CONF 9
CONF 10
CONF 11
COMMON 2
COMMON 3
COMMON 4
COMMON 5
NOX 2
NOX 3
NOX 4
4STEP 3
NOX 4
NOX 8
NOX 9
NOX 10
NOX 11
4STEP 4
4STEP 5
4STEP 6
4STEP 7
NOX 12
COMMON 6
4STEP 8
4STEP 9
COMMON 9
COMMON 10
COMMON 11
4STEP 10
COMMON 13
4STEP 11
NOX 16

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1	LVC02,LVFU1,LVC01,NNOX,INNOX,ITNOX,SHOX,TNOX	NOX	17
	COMMON/THERM/NVH,NVFU,NVQX,NVUOX,NVTE,MODEN,ION,FSTQIC,HFU,CP,	COMMON	19
1	GASC0N,PHCCCN,UNIC0N,PRESS,NVFAV,TCVLM,TINLW,TIIP,ACDEF(4),	COMMON	16
2	T4,DFAC,WFO,WCO2,WCO,WQX,WH2O,WH2,HVY,CXX,RATIO1,RATIO2,	COMMON	17
3	RATIO3,RATIO4,MCO,TAN,ITWALL	COMMON	18
	COMMON/CTDMA/HEND,ICTDMA(32)	4STEP	12
	COMMON/MIS/AMU,DEN,SMAX,SSUM,LASTEP,HTCEXT,CFR,EMISM,EMISIN,	CONGEN	2
1	EMISP,TOUT,RTCD,ENI,RADIN,RADSUR,FMA,FK,SQFK,	CONGEN	3
2	FWFI,FOFU,TFUEL,WFNZ,FLO(40),TENTM(40),M(40),FUEL(40),FUOX(40),	CONGEN	4
2	UIN(40),TIN(40),FUELS(40),SEKIT,IGAM1(29),IGAM2(29)	4STEP	13
	COMMON/TURN/NVK,NVD,C1,C2,CD,AK,QUIDRJ(3,3),AKFAC,ALFAC,	CONGEN	6
1	MODEL,PR(32),PREF(32),PJAY(32),E	4STEP	14
	COMMON/RAO/NVE,SIGMA,ABSOR,SCATR	CONGEN	8
	COMMON/PEACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	CONGEN	9
	COMMON/DROPI/EVAP(192),NTP4,WFNZ,XO(3),YO(3),ZO(3),ALFA(3),	CONGEN	10
1	BETA(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SHD(3),	CONGEN	11
2	VFUEL(3),RFUEL(3),EVSU(64),HEVAP	CONGEN	12
	COMMON/INJEC/FLOWIN,IUINJ(20),JUINJ(20),UINJ(20),WUINJ(20),	CONGEN	13
1	AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	CONGEN	14
2	EVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),WUINJ,NVINJ,JSW1,JSW2,	CONGEN	15
1	USW,VSW,AFSW,FSW,TSW,MSW,SWMO,RHDSW	CONGEN	16
	COMMON/CSOBT/NVN,NVS1,NVS2,TSOOT,SSOOT,MSOOT,AQ,ARCONH,AAA,888,FHG	SOOT	8
1	GO,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,889,DHR	SOOT	9
2	LVN,LVS1,LVS2,CINCP,TINCP,FUTOT	SOOT	10
	COMMON/CRAD/IRAD,SRAD	SOOT	11
	COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,881,CC1,	4STEP	15
1	AA2,AA3,CC2,AA3,AA3,CC3,AA4,884,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2	RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,WH2,WC2H4,LVCH,LVCH1,LVH21	4STEP	17
	DIMENSION VFCK(30),VECY(30),VEZ(30),DSMD(3),XN(40),YN(30),ZN(30)	SP	12
	DIMENSION PO(4),EE(4),FRACT(7),MW(7),MWCOND(4),ACOND(4),BCOND(4)	SP	13
	DIMENSION EVAPU(192),EVAPV(192),EVAPW(192),RVECK(30),RVECY(30),	NASAX	30
1	RVEZ(30)	NASAX	31
	REAL MW,MWCOND,MWT	SP	15
C	***** REWARE OF EQUIVALENCE STATEMENTS *****	SP	16
	EQUIVALENCE (EVAPU(1),AXMK(1)),(EVAPV(1),AYMK(1))	SP	17
	EQUIVALENCE (EVAPW(1),AZMK(1))	SP	18
C	*****	SP	19
	DATA DSMO/.0,9,1.2,1.5,2.1/	SP	20
	DATA PC,EE/-114.,41.574,96.534,146.57,41.026,30.857,27.340,23.997/	SP	21
	DATA FRACT,MW/O.,.1,.3,.5,.7,.9,1.,93.26,114.6,126.61,138.16	SP	22
1	,150.59,173.21,204.76/	SP	23
	DATA ACOND,BCOND,MWCOND/-6.362E-3,-6.358E-3,-6.284E-3,-6.01E-3	SP	24
	1,5.36F-3,4.91E-3,4.66E-3,4.23E-3,50.,100.,150.,300./	SP	25
	DATA NG,RNG,PI,PT2/5,5.,3.14159,6.28318/	SP	26
C	*****	SP	27
C	***** SOME PRELIMINARIES *****	SP	28
	IF (NFNZ.LE.0) RETURN	SP	29
	SC3=.9203	SP	30
	PR3=.9203	SP	31
	OLIM=.1	SP	32
	ULIM=.1	SP	33
	TF=2300.	SP	34
	HEVAP=30676.6*(1092.88-1.8*TFUEL)**.89	SP	35
	WFUEL=4.5F+7	SP	36
	WQFO=1000.*(1.775+.20R-.00072*TFUEL)	SP	37
	ZSMALL=(2*(NP1)-7(1))/FLOAT(NP1)/100.	SP	38
	DO 7 K=2,N	SP	39
	DO 7 J=2,M	SP	40
	DO 7 I=2,L	SP	41
	LPC=I-1+(J-2)*(NI-2)+(K-2)*(NI-2)*(NJ-2)	SP	42
	EVAPU(LPC)=0.	SP	43
	EVAPV(LPC)=0.	SP	44
	EVAPW(LPC)=0.	SP	45
7	EVAP(LPC)=0.	SP	46

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      XM(1)=X(1)
      DO 115 I=2,L
115  YM(1)=YM(I-1)+XS(I)
      XM(LP1)=XM(L)
      YM(1)=Y(1)
      DO 17 J=2,M
17  YM(J)=YM(J-1)+YS(J)
      YM(MP1)=YM(M)
      ZM(1)=Z(1)
      DO 19 K=2,N
19  ZM(K)=ZM(K-1)+ZS(K)
      ZM(NP1)=ZM(N)
C *****
C -----LOOP OVER FUEL NOZZLES
      DO 2000 NM=1,MFN7
      RFE=0.
      NSL2=NSL(NM)
      RNSL=NSL2
      WFI=WFF(NM)/RNSL
C -----CALCULATE UNIT VECTORS OF SPRAY LINES
      SINA=SIN(ALFA(NM)/2.)
      SINR=SIN(ETA(NM))
      SIND=SIN(DELTA(NM))
      COSA=COS(ALFA(NM)/2.)
      COSR=COS(BETA(NM))
      COSD=COS(DELTA(NM))
      DTHETA=THETA2(NM)-THETA1(NM)
      IF (DTHETA.LT.0.0) DTHETA=DTHETA+PT2
      DANG=DTHETA/(RNSL-1.)
      IF (DTHETA.GT.0.9*PT2) DANG=DTHETA/RNSL
      THETA=THETA1(NM)
      DO 10 IL=1,NSL2
      SINT=SIN(THETA)
      COST=COS(THETA)
      THETA=THETA+DANG
      IF (THETA.GT.PT2) THETA=THETA-PT2
      VECX(IL)=-SINA*SINT*COSD-COSA*SIND
      VECY(IL)=SINA*COST*COSD+SINA*SINT*SIND-COSA*COSD*SIND
      VECZ(IL)=SINA*COST*SIND-SINA*SINT*SIND-COSA*COSR*COSD
      RVECX(IL)=-SINT*COSA
      RVECY(IL)=COST*COSD+SINT*SIND*SIND
      RVECZ(IL)=COST*SIND-SINT*SIND*COSD
10 CONTINUE
C *****
C -----START CALCULATIONS FOR EVAPORATION RATES-----
      DO 1000 IL=1,NSL2
      DO 1000 IG=1,NG
      UF=VECX(IL)*VFUEL(NM)
      VF=VECY(IL)*VFUEL(NM)
      WF=VE CZ(IL)*VFUEL(NM)
      DIA=SND(NM)*1.E-6*DSND(IG)
      TFU=VFUEL
      ITPF=1
      DIAQ=DIA
      CON2=0.
      IGNT=-10
      IF (ISTEP.NE.IGPNT) GO TO 7746
      WRITE (6,7747)
7747  FORMAT (1/10X,'UF',10X,'VF',10X,'WF',9X,'US',9X,'VST',9X,'WST',
1 7X,'FEVAP',10X,'XF',10X,'YF',10X,'ZF')
7746 CONTINUE
      FEVAP=C.
      DO 11 I=1,LP1
      ILOC=I

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      IF (X0(MN).GT.XM(I)) GO TO 11
      GO TO 12
11  CONTINUE
12  DO 13 J=1,NP1
      JLOC=J
      IF (Y0(MN).GT.YM(J)) GO TO 13
      GO TO 14
13  CONTINUE
14  DO 15 K=1,NP1
      KLOC=K
      IF (Z0(MN).GT.ZM(K)) GO TO 15
      GO TO 16
15  CONTINUE
16  XF=X0(MN)+RFUEL(MN)*RVECX(IL)
      YF=Y0(MN)+RFUEL(MN)*RVECY(IL)
      ZF=Z0(MN)+RFUEL(MN)*RVECZ(IL)/(R(1)+PLAXM1*YF)
C-----LOCATION OF THE DROPLET-----
110 CONTINUE
      IOLD=ILOC
      JOLD=JLOC
      KOLD=KLOC
C ----X DROPLET LOCATION
      IF (XF.GE.XM(ILOC-1).AND.XF.LT.XM(ILOC)) GO TO 27
      DO 22 I=1,LP1
      ILOC=I
      IF (XF.GT.XM(I)) GO TO 22
      GO TO 27
22  CONTINUE
C ----Y DROPLET LOCATION
27  IF (YF.GE.YM(JLOC-1).AND.YF.LT.YM(JLOC)) GO TO 23
      DO 24 J=1,NP1
      JLOC=J
      IF (YF.GT.YM(J)) GO TO 24
      GO TO 23
24  CONTINUE
C ----Z DROPLET LOCATION
23  IF (ZF.GE.ZM(KLOC-1).AND.ZF.LT.ZM(KLOC)) GO TO 63
      DO 26 K=1,NP1
      KLOC=K
      IF (ZF.GT.ZM(K)) GO TO 26
      GO TO 40
26  CONTINUE
40  IF (KLOC.GT.1) GO TO 28
      KLOC=N
      ZF=Z(NP1)-ZSMALL
28  IF (KLOC.LT.NP1) GO TO 63
      KLOC=2
      ZF=Z(1)+ZSMALL
C ----DROPLET NEAR A WALL
63  INDX=0
      IF (ILOC.GE.IWLI(JLOC,4)) GO TO 43
      ILOC=IOLD
      XF=AMAX1(XF,XM(ILOC-1)+DIA/2.)
      XF=AMIN1(XF,XM(ILOC)-DIA/2.)
      INDX=1
43  IF (ILOC.LE.IWLO(JLOC,4)) GO TO 47
      IF (JLOC.GT.JWOL.AND.JLOC.LT.JWOD) GO TO 1000
      ILOC=ICLO
      XF=AMAX1(XF,XM(ILOC-1)+DIA/2.)
      XF=AMIN1(XF,XM(ILOC)-DIA/2.)
      INDX=2
47  IF (JLOC.GT.JWLI(ILOC,4)) GO TO 44
      IF (IOW.EQ.0) GO TO 50
      JLOC=JOLD

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YF=AMAX1(YF,YM(JLOC-1)+DIA/2.)	SP	175
YF=AMIN1(YF,YM(JLOC)-DIA/2.)	SP	176
INDX=3	SP	177
44 IF (JLOC.LT.JWLO(ILOC,4)) GO TO 41	SP	178
JLOC=JOLD	SP	179
YF=AMAX1(YF,YM(JLOC-1)+DIA/2.)	SP	180
YF=AMIN1(YF,YM(JLOC)-DIA/2.)	SP	181
INDX=4	SP	182
C ----CHECK FOR SLOTS	SP	183
41 IF (NUINJ.LE.0) GO TO 45	SP	184
DO 149 II=1,NUINJ	SP	185
IU=IUINJ(II)-1	SP	186
JU=JUINJ(II)	SP	187
IF (ILOC.EQ.IU.AND.JLOC.EQ.JU) GO TO 50	SP	188
149 CONTINUE	SP	189
45 CONTINUE	SP	190
GO TO 60	SP	191
C -----DROPLET HAS HIT SOLID BOUNDARY	SP	192
50 ILOC=ICLD	SP	193
JLOC=JOLD	SP	194
KLOC=KOLD	SP	195
DEFAP=1.-FEVAP	SP	196
HF=0.	SP	197
VF=0.	SP	198
WF=0.	SP	199
FX=0.	SP	200
FY=0.	SP	201
FZ=0.	SP	202
GO TO 249	SP	203
C -----NO BOUNDARIES HAVE BEEN HIT	SP	204
60 CONTINUE	SP	205
LP=KM(KLOC)+JM(JLOC)+ILOC	SP	206
LTP=LP+1	SP	207
LTP=LP+NI	SP	208
LTP=LP+NI	SP	209
LPTE=(LP+NM(NVTE)	SP	210
LPFUOX=LP+NM(NVFUOX)	SP	211
C ----- CAREFUL HERE	SP	212
LPFU=LP+NM(NVFU+3)	SP	213
LPCD=LP+NM(NVCO+1)	SP	214
LRCH=LP+NM(NVCH)	4STEP	326
LRH2=LP+NM(NVH2)	4STEP	327
C -----FREESTREAM PROPERTIES	SP	215
RST=RHO(LP)	SP	216
TST=F(LPTE)	SP	217
UST=FXP(ILOC)*U(LP)+FXM(ILOC)*U(LXP)	SP	218
VST=FXP(JLOC)*V(LP)+FXM(JLOC)*V(LYP)	SP	219
WST=FXP(KLOC)*W(LP)+FXM(KLOC)*W(L7P)	SP	220
IR=IWL(I(JLOC,4))	SP	221
IF (XF.GE.X(IR)) GO TO 51	SP	222
IF (JKN(JLOC,KLOC).EQ.1) GO TO 51	SP	223
FAC=((XF-XM(IR-1))/(X(IR)-XM(IR-1)))*.14286	SP	224
UST=0.	SP	225
VST=VST+FAC	SP	226
WST=WST+FAC	SP	227
IF (INDX.NE.1) GO TO 51	SP	228
HF=UST	SP	229
VF=VST	SP	230
WF=WST	SP	231
51 IR=IWL(I(JLOC,4))	SP	232
IF (XF.LE.X(IR)) GO TO 56	SP	233
IF (JLOC.GT.JWDI.AND.JLOC.LT.JWDD) GO TO 56	SP	234
FAC=((XM(IR)-XF)/(XM(IR)-X(IR)))*.14286	SP	235
UST=0.	SP	236

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VST=WST*FAC	SP	237
WST=WST*FAC	SP	238
IF (INDX.NE.2) GO TO 56	SP	239
UF=UST	SP	240
VF=VST	SP	241
WF=WST	SP	242
56 JR=JWL1(ILOC,4)	SP	243
IF (VF.GE.Y(JR+1)) GO TO 53	SP	244
IF (IKIN(ILOC,KLOC).EQ.1.)JR=IKIN(ILOC,KLOC).EQ.3) GO TO 53	SP	245
FAC=((VF-YM(JR))/(Y(JR+1)-YM(JR)))*.14286	SP	246
UST=UST*FAC	SP	247
VST=0.	SP	248
WST=WST*FAC	SP	249
IF (INDX.NE.3) GO TO 53	SP	250
UF=UST	SP	251
VF=VST	SP	252
WF=WST	SP	253
53 JR=JWL1(ILOC,4)	SP	254
IF (VF.LE.Y(JR-1)) GO TO 54	SP	255
IF (IKIN(ILOC,KLOC).EQ.2.)JR=IKIN(ILOC,KLOC).EQ.3) GO TO 54	SP	256
FAC=((YM(JR-1)-VF)/(YM(JR-1)-Y(JR-1)))*.14286	SP	257
UST=UST*FAC	SP	258
VST=0.	SP	259
WST=WST*FAC	SP	260
IF (INDX.NE.4) GO TO 54	SP	261
UF=UST	SP	262
VF=VST	SP	263
WF=WST	SP	264
54 CONTINUE	SP	265
IF (ABS(UF).LT.1.E-30.AND.ABS(VF).LT.1.E-30.AND.ABS(UST).LT.1.E-30.	NASAX	32
1 AND.ABS(WST).LT.1.E-30)GO TO 50	NASAX	33
FLPOX=RATIO1*F(LPFU)+RATIO3*F(LPCD)+RATIO2*(RATIO2+RATIO1)*	SP	266
1 F(LPFUNX)+RATIO3*F(LPCM)+RATIO3*F(LPM2)	4STEP	328
FLPOX=AMAX1(FLPOX,0.)	SP	268
IF (ISTEP.NF.IGPNT) GO TO 7744	SP	269
WRITE (6,7745) UF,VF,WF,UST,VST,WST,FEVAP,XF,YF,ZF	SP	270
7745 FORMAT (10E12.4)	SP	271
7744 CONTINUE	SP	272
C -----BOILING TEMPERATURE OF FUEL-----	SP	273
POT=PD(4)	SP	274
ET=EE(4)	SP	275
IF (FEVAP.GE.0.9) GO TO 200	SP	276
POT=TAR(FEVAP,FRACT,PD,4)	SP	277
ET=TAR(FEVAP,FRACT,EE,4)	SP	278
200 TR=ET*ALOG(PRESS)+POT	SP	279
T1=(TR+TF)/2.	SP	280
TFU=AMIN1(TFU,T8)	SP	281
C-----DENSITY OF LIQUID FUEL AT T8	SP	282
RDF=1.076/(1.+(1.076/.775-1.)*(1.-.67*FEVAP))	SP	283
RDF=1000.+(RDF+.208-.00072*TFU)	SP	284
C-----MOLECULAR WEIGHT OF FUEL VAPORS	SP	285
MWT=TAR(FEVAP,FRACT,MW,7)	SP	286
AT=TAR(MWT,MWCOND,ACOND,4)	SP	287
300 RT=TAR(MWT,MWCOND,RCOND,4)	SP	288
C-----THERMAL CONDUCTIVITY AND SPECIFIC HEAT OF FUEL VAPORS	SP	289
COND1=1.729*(AT+RT*T1)	SP	290
HCPS=1	NOX	195
NS1=IDFU	NOX	196
NS2=IDFU	NOX	197
TK=T1	NOX	198
TKINV=1.000/TK	NOX	199
S2(IDFU)=1.000/SHW(IDFU)	NOX	200
CALL HCPS	NOX	201
CP1=CPSUM*UNICOM	NOX	202

400 COND1=0.4*COND1+0.6*.064*SQRT(T1/1111.)	SP	292
C -----RELATIVE VEL. REYNOLDS NO., DRAG COEF AND FORCE COMPONENTS	SP	293
VR=SQRT((UF-UST)**2+(VF-VST)**2+(WF-WST)**2)	SP	294
VISCO=4.464E-5*SQRT(TST/1111.)	SP	295
*REI=ROST*VR*DIA/VISCO	SP	296
SREI=SQRT(REI)	SP	297
COS=2.C	SP	298
IF (REI.GT.22.16.AND.REI.LE.80.) COS=27./REI**0.84	SP	299
IF (REI.GT.80..AND.REI.LT.10000.) COS=.271*REI**0.217	SP	300
CD1=AMAX1(COS/2.,COS/(1.+BEE))	SP	301
CONS=CD1*3.14159/4.*DIA**2/2.*ROST	SP	302
DM=PI*DIA**3*ROF/6.	SP	303
FX=CONS*VR*(UST-UF)	NASAX	34
FY=CONS*VR*(VST-VF)+PLAXM1*DM*VF*WF/R(JLOC)	NASAX	35
FZ=CONS*VR*(WST-WF)-PLAXM1*DM*VF*WF/R(JLOC)	NASAX	36
VFU=SQRT(UF**2+VF**2+WF**2)	SP	307
FAC=AMAX1(1.0,25./(VR*VR+1.E-20))	SP	308
DTI1=ULIM*VFU*DM*FAC/(ABS(FX)+1.E-30)	SP	309
DTI2=ULIM*VFU*DM*FAC/(ABS(FY)+1.E-30)	SP	310
DTI3=ULIM*VFU*DM*FAC/(ABS(FZ)+1.E-30)	SP	311
DTI4=DLIM/(CON2+1.E-30)	SP	312
DTI5=KSI(JLOC)/(ABS(UF)+1.E-20)	SP	313
DTI6=YS(JLOC)/(ABS(VF)+1.E-20)	SP	314
DTI7=R(JLOC)*7S(KLOC)/(ABS(WF)+1.E-20)	SP	315
DTI=AMIN1(DTI1,DTI2,DTI3,DTI4,DTI5,DTI6,DTI7)	SP	316
CONS=DM/DTI	SP	317
C-----VELOCITY AND LOCATION OF THE DROPLET	SP	318
UFQ=UF	SP	319
VFQ=VF	SP	320
WFQ=WF	SP	321
UF=UF+FX/CONS	SP	322
VF=VF+FY/CONS	SP	323
WF=WF+FZ/CONS	SP	324
IF (UFQ.GT.UST) UF=AMAX1(UF,UST+.001)	SP	325
IF (UFQ.LT.UST) UF=AMIN1(UF,UST+.001)	SP	326
IF (VFQ.GT.VST) VF=AMAX1(VF,VST+.001)	SP	327
IF (VFQ.LT.VST) VF=AMIN1(VF,VST+.001)	SP	328
IF (WFQ.GT.WST) WF=AMAX1(WF,WST+.001)	SP	329
IF (WFQ.LT.WST) WF=AMIN1(WF,WST+.001)	SP	330
DX=.5*(UF+UFQ)*DTI	SP	331
DY=.5*(VF+VFQ)*DTI	SP	332
DZ=.5*(WF+WFQ)*DTI	SP	333
XF=XF+DX	SP	334
YF=YF+DY	SP	335
ZF=ZF+DZ/R(JLCC)	SP	336
IF (TFU.GE.TB) ITYPE=2	SP	337
GO TO (180,199), ITYPE	SP	338
C-----HEATING DROPLET -----	SP	339
C ----HEAT TRANSFER	SP	340
180 HT=COND1*(2.+6*PR3*SREI)/DIA	SP	341
AS=PI*DIA*DIA	SP	342
QDOT=AS*HT*(TST-TFU)	SP	343
CPLE=0.407+4.1372*TFU	SP	344
DTF=DTI*QDOT/DM/CPLE	SP	345
TFU=TFU+DTF	SP	346
GO TO 11C	SP	347
C -----BOILING DROPLET -----	SP	348
C ----MASS TRANSFER NUMBER	SP	349
190 TF=(F(PFUCX)-FSTOIC) 210,209,201	SP	350
201 REF=AMAX1(CP1*(TST-TB)/HEVAP,0.)	SP	351
GO TO 215	SP	352
205 REF=FLPMX/RATIO1	SP	353
GO TO 215	SP	354
210 REF=(FLPMX*HFUEL/RATIO1+AMAX1(CP1*(TST-TB),0.))/HEVAP	SP	355

219 RATE=8./ROF*COND1/CP1*ALOG(1.+REE)*(1.+0.276*SREI*SC9)
 C-----FRACTION EVAPORATED
 CON2=1.5/ROFO/DIAO**3*ROF*DIA*RATE
 DEVAP=CON2*DTI

240 FEVAP=FEVAP+DEVAP
 IF (FEVAP.LT.1.0) GO TO 250
 DEVAP=DEVAP-FEVAP+1.
 FEVAP=1.

C-----NEW DROPLET DIAMETER
 250 ARG=DIA*DIA-RATE*DTI
 IF (ARG.GT.0.0) GO TO 262
 DEVAP=DEVAP+1.-FEVAP
 FEVAP=1.0
 GO TO 252

262 DIA=SQRT(ARG)

C-----FUEL EVAPORATION FLOW RATE -----

252 AMT=DEVAP*WFI/RNG
 LPC=(LPC-1)+(JLOC-2)*(NI-2)+(KLOC-2)*(NJ-2)+(MJ-2)
 EVAP(LPC)=EVAP(LPC)+AMT
 EVAPU(LPC)=EVAPU(LPC)+AMT*UF
 EVAPV(LPC)=EVAPV(LPC)+AMT*VF
 EVAPW(LPC)=EVAPW(LPC)+AMT*WF

900 IF (FEVAP.LT.0.99) GO TO 110

1000 CONTINUE

2000 CONTINUE

C *****

C-----STORE MOMENTUM DATA ON TAPE4

REWIND NTP4

00 1100 K=2,M

00 1110 J=2,M

KJC=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)

00 1110 I=3,L

LIJ=(J-2)*(NI-2)+(I-1)

LPC=KJC+(I-1)

LYNC=LPC-1

EVSU(LIJ)=FXM(I-1)*EVAPU(LXNC)+FXP(I)*EVAPU(LPC)

IF (I.EQ.3) EVSU(LIJ)=EVSU(LIJ)+FXP(2)*EVAPU(LXNC)

IF (I.EQ.L) EVSU(LIJ)=EVSU(LIJ)+FXM(L)*EVAPU(LPC)

1110 CONTINUE

WRITE (NTP4) EVSU

1100 CONTINUE

00 1200 K=2,M

00 1210 J=3,M

KJC=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)

00 1210 I=2,L

LIJ=(J-2)*(NI-2)+(I-1)

LPC=KJC+(I-1)

LYNC=LPC-(NI-2)

EVSU(LIJ)=FYM(J-1)*EVAPV(LXNC)+FYP(J)*EVAPV(LPC)

IF (J.EQ.3) EVSU(LIJ)=EVSU(LIJ)+FYP(2)*EVAPV(LXNC)

IF (J.EQ.M) EVSU(LIJ)=EVSU(LIJ)+FYM(M)*EVAPV(LPC)

1210 CONTINUE

WRITE (NTP4) EVSU

1200 CONTINUE

00 1300 K=3,MP1

00 1310 J=2,M

KJC=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)

00 1310 I=2,L

LIJ=(J-2)*(NI-2)+(I-1)

LPC=KJC+(I-1)

LYNC=LPC-(NI-2)+(NJ-2)

EVSU(LIJ)=FZM(K-1)*EVAPW(LXNC)

IF (K.EQ.MP1) GO TO 1309

EVSU(LIJ)=EVSU(LIJ)+FZP(K)*EVAPW(LPC)

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GO TO 1310
1309 FVSU(LIJ)=EVSU(LIJ)+FZP(2)*EVAPW(LIJ)
1310 CONTINUE
      WRITE (NTP4) EVSU
1300 CONTINUE
      RETURN
      END
      FUNCTION TAR (X,XX,YY,NTAB)
      DIMENSION XX(1),YY(1)
      IF (NTAB.GT.0) GO TO 3
      TAR=0.C
      RETURN
3 F=1.
  IF (XX(1).GT.XX(2)) F=-F
  ON 10 J=1,NTAB
  I=J
  IF (F*(XX(I)-X)) 10,40,20
10 CONTINUE
20 IF (I.NE.1) GO TO 30
  I=2
30 J=I-1
  DEL=XX(I)-XX(J)
  IF (DEL.FO.0.C) GO TO 50
  TAB=(YY(I)*(X-XX(J))-YY(J)*(X-XX(I)))/DEL
  RETURN
40 TAR=YY(I)
  RETURN
50 WRITE (6,60) X,I,J
60 FORMAT (' *** ERROR IN SUBROUTINE TAR ***',E15.4,2I5)
  STOP
  END
  SUBROUTINE STRIDE
  COMMON/CFDK/EOK(192)
  COMMON F(3500),OU(500),DV(500),OW(500),
1 AMUC(500),SOOT1(500),SOOT2(500),FCH(500),FH2(500),FS(500,14),
1 RHO(500),VISC(500),ABSR(500),SCTR(500),SU(100),SP(100),
1 RHOOPP(500),
1 AXP(100),AXM(100),AYP(100),AYM(100),AZP(100),
2 AZM(100),CZ(100),CY(10),CZU(100),CYU(10),
3 CZP(100),CYP(10),DIVG(100),NTP1,NTP2
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
  DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
  DIMENSION GAM(500)
  EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
  EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
  EQUIVALENCE (F(3001),GAM(1))
  COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX
  COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSV(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXM(40),
2 FYP(30),FYM(30),F7P(30),F7M(30),DT,TIME
  COMMON
1/CINDEX/IOCC,IOFU,IOO2,ION2,IOH2O,IOCO2,IOH1,IOH2,ION1,IONO,IONO2
1,ION,IONH,IOHPS,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NGL0B,NGL0B,
2 NLH,NQ,NSH,NS1,NS2,IOCH
1/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG
4/CPARAM/ASUR(30,3),EMV,EP,HSUBO,NDERUG,NS,PA-Q0,Q1,Q2,Q3,Q4,RHOPP,
4 SM,SMW(30),SPO,S1(30),S2(30),TK,LADIA0,LDERUG,LFOUIL,LRFAC,
4 LENER,FDRIJ,LCONVG
  COMMON PRECISION CPSUM,EMV,EP,FQ,HSUBO,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,
1 Q4,RGAS,RGASIN,RHOPP,SM,SHINV,SMW,S1,S2,TK,TKINV,TLN,SPO
2,FUT,FST
  COMMON/STFPA/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CERU1,CERU2,
1 CERU3,CERU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,

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SP	421
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SP	446
SP	447
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SP	449
SP	450
ST	2
NOX	203
CONF8	2
4STEP	18
RAD	3
RAO	4
CONF8	4
CONF8	5
CONF8	6
CTOMA	3
CTOMA	4
CONF8	7
CONF8	8
CONF8	9
CONF8	10
CONF8	11
COMMON	2
COMMON	3
COMMON	4
COMMON	5
NOX	2
NOX	3
NOX	4
4STEP	3
NOX	6
NOX	7
NOX	8
NOX	9
NOX	10
NOX	11
4STEP	4
4STEP	5
4STEP	6

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2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST
LOGICAL LADTAB,LCONVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER
COMMON/INT/L,M,N,LCV,PCV,NCV,LP1,MP1,NI,NJ,NK,NENJ,NINJNK,NV,
1 NVV,NGOTD,K,ISTR,JSTR,KSTR,NVM(33),KM(30),JM(30),ISTEP,
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXV,ISWP,JSWP,REFLX(33),NP,
3 NRND,NGAM,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWEI,
4 IWEO,MM1,JWII,JWIO,JMOI,JMOO,IDW,JKIN(30,30),IKIN(40,30)
COMMON/INDEX/IPAR,LPRF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE
1,PLANM1,LVK,LVD,LVFUOX,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),
2 TJUMP,IRES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH2O,NVCO2,
3 NVN2,NVCH,NVH2
COMMON/CHOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVON,LVH2O,LVN2,LVO2,
1 LVCO2,LVFU1,LVCO1,MNOX,INOX,ITNOX,SMOX,TMOX
COMMON/THERM/NVM,NVFU,NVON,NVFOX,NVTE,MODEN,IOK,FSTOIC,MFU,CP,
1 GASCON,RHOCN,UNICON,PRESS,NVPAV,TCYLU,TINLU,TLIP,ACOE(4),
2 T4,DFAC,MFU,WCO2,WCO,WON,W2O,W2,NVY,CXX,RATIO1,RATIO2,
3 RATIO3,RATIO4,MCO,TAN,ITWALL
COMMON/CTOMA/KEND,ICTOMA(32)
COMMON/MIS/AMU,DEN,SNAX,SSUM,LASTEP,HTCXT,CFR,EMISW,EMISIN,
1 EMISP,TOUT,RTCD,EMI,RADTN,RADSUR,FMA,FK,SQFK,
2 KKFU,FOFU,TFUEL,MFNZ,FLN(40),TENTH(40),H(40),FUEL(40),FUOX(40),
2 UIN(40),TIN(40),FUELS(40),SEXT,IGAM1(29),IGAM2(29)
COMMON/TURB/NVK,NVO,C1,C2,CD,AK,QUIDXJ(3,3),AKFAC,ALFAC,
1 MODFL,PR(32),PRF(32),PJAY(32),E
COMMON/RAD/NVE,SIGMA,ABSOR,SCATR
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER
COMMON/DRDPL/EVAP(192),NTP4,MFNZ,XO(3),YO(3),ZO(3),ALFA(3),
1 BETA(3),DELTA(3),THETA1(3),THETA2(3),MSL(3),WTF(3),SMD(3),
2 VFUEL(3),RFUEL(3),EVSU(64),HEVAP
COMMON/INJEC/FLOWIN,IUINJ(20),JUINJ(20),UINJ(20),WUINJ(20),
1 AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),WVINJ(20),VINJ(20),
2 EVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),WVINJ,NVINJ,JSW1,JSW2,
3 USW,VSW,AFSW,FSW,TSW,USW,SWND,RHOSH
COMMON/CSOCT/NVN,NVS1,NVS2,ISOOT,SSOOT,MSOOT,AQ,ARCONN,AAA,BBS,FMS
1,GO,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BBS,DHR
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT
COMMON/CRAD/IPAD,SRAD
COMMON/CFDUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BB1,CC1,
1 AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,
2 RATIO8,RATIO9,RATIO10,RATIO11,RATIO12,WCH,W2,W2H4,LVCH,LVCH1,LVH21
ENTRY STRIDO
C-----ENTRY STRIDO IS USED FOR PRELIMINARY CALCULATIONS.
C
IXV=1
ISWP=1
JSWP=1
TIF=0.
L=LP1-1
M=MP1-1
N=NP1-1
LCV=L-1
NCV=M-1
NCV=N-1
MM1=M-1
NINJ=NINJ
NINJNK=NINJNK
NVM(1)=0
DO 1 NV=2,NGAM
NVM(NV)=NVM(NV-1)+NINJNK
KM(1)=0
DO 2 K=2,MP1
KM(K)=KM(K-1)+NINJ
JM(1)=0
MAX=MAXO(MP1,MP1)

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4STEP 7
NOX 12
COMMON 6
4STEP 8
4STEP 9
COMMON 9
COMMON 10
COMMON 11
4STEP 10
COMMON 13
4STEP 11
NOX 16
NOX 17
COMMON 15
COMMON 16
COMMON 17
COMMON 18
4STEP 12
COMMON 2
COMMON 3
COMMON 4
4STEP 13
COMMON 6
4STEP 14
COMMON 8
COMMON 9
COMMON 10
COMMON 11
COMMON 12
COMMON 13
COMMON 14
COMMON 15
COMMON 16
SOOT 8
SOOT 9
SOOT 10
SOOT 11
4STEP 15
4STEP 16
4STEP 17
ST 5
COMMENT 121
COMMENT 122
ST 6
ST 7
ST 8
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      ON 3 J=2,MAX
      JM(J)=JM(J-1)+NI
      RETURN
C ** ** ** **
      ENTRY STRID1
C-----ENTRY STRID1 IS USED TO CALCULATE INTER-MODAL DISTANCES,
C      CONTROL VOLUME AREAS AND VOLUMES.
C
C-----X-GRID.
      DO 101 I=2,LP1
101    XDIF(I)=X(I)-X(I-1)
      DO 111 I=2,L
111    YS(I)=0.5*(X(I+1)-X(I-1))
        XS(2)=XS(2)+0.5*XDIF(2)
        XS(L)=XS(L)+0.5*XDIF(LP1)
      DO 121 I=3,L
        XSU(I)=XDIF(I)
        FXP(I)=XDIF(I)/(2.*XS(I))
121    FXM(I)=1.-FXP(I)
        XSU(3)=XSU(3)+XDIF(2)
        XSU(L)=XSU(L)+XDIF(LP1)
        FXP(2)=FXP(3)
        FXM(2)=1.-FXP(2)
        FXP(L)=FXP(L-1)
        FXM(L)=1.-FXP(L)
C-----Y-GRID.
      DO 102 J=2,MP1
102    YDIF(J)=Y(J)-Y(J-1)
      DO 112 J=2,M
112    YS(J)=0.5*(Y(J+1)-Y(J-1))
        YS(2)=YS(2)+0.5*YDIF(2)
        YS(M)=YS(M)+0.5*YDIF(MP1)
        RM(2)=R(1)
      DO 122 J=3,M
        RM(J)=.5*(R(J)+R(J-1))
        RMV(J+1)=R(J)
        YSV(J)=YDIF(J)
        FYP(J)=YDIF(J)/(2.*YS(J))
122    FYM(J)=1.-FYP(J)
        RM(MP1)=R(MP1)
        RMV(3)=R(1)
        RMV(MP1)=R(MP1)
        YSV(3)=YSV(3)+YDIF(2)
        YSV(M)=YSV(M)+YDIF(MP1)
        FYP(2)=FYP(3)
        FYM(2)=1.-FYP(2)
        FYP(M)=FYP(M-1)
        FYM(M)=1.-FYP(M)
      DO 132 J=2,P
132    YSR(J)=.5*(RM(J+1)+RM(J))*YS(J)
      DO 142 J=3,P
142    YSVR(J)=.5*(RMV(J+1)+RMV(J))*YSV(J)
C-----Z-GRID.
      DO 103 K=2,NP1
103    ZDIF(K)=Z(K)-Z(K-1)
      DO 113 K=2,N
113    ZS(K)=0.5*(Z(K+1)-Z(K-1))
        ZS(2)=ZS(2)+0.5*ZDIF(2)
        ZS(N)=ZS(N)+0.5*ZDIF(NP1)
        ZS(NP1)=ZS(2)
      DO 123 K=3,N
        ZSW(K)=ZDIF(K)
        FZP(K)=ZDIF(K)/(2.*ZS(K))
123    FZM(K)=1.-FZP(K)

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      ST      27
      ST      28
      ST      29
      ST      30
      ST      31
      COMMENT 123
      COMMENT 124
      COMMENT 125
      COMMENT 126
      ST      32
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      ST      34
      ST      35
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      ST      45
      ST      46
      ST      47
      COMMENT 127
      ST      48
      ST      49
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      ST      73
      COMMENT 128
      ST      74
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      ST      82
      ST      83
      ST      84

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T7=AMAX1(T7,ARS(ALZ))
C7U(LP)=2.0*ALZ
30 C7(LP)=T7+ALZ
DO 301 K=2,M
C-----OBTAIN SOURCE TERMS AND EVAPORATION RATES.
CALL SOURCE
CALL SOMAS
DO 31 I=3,L
JS=JWL1(I,NGOTO)+1
ARSA=XSU(I)*ZS(K)*RM(JS)
LP=KM(K)+JM(JS)+I
LYM=LP-NI
LXM1=LYM-1
LXM=LP-1
IF (JWL1(I,4).EQ.JS-1) GO TO 150
ALY=.5*(RHQ(LP)+RHQ(LYM))*V(LP)*AREA
TY=.5*(GAM(LP)+GAM(LYM))*AREA/YDIF(JS)
GO TO 152
150 ALY=RHQ(LYM)*V(LP)*AREA
DIST=.5*YDIF(JS)
IF (JS.EQ.2) DIST=YDIF(2)
TY=GAM(LYM)*AREA/DIST
152 IF (JWL1(I-1,4).EQ.JS-1) GO TO 154
ALY1=.5*(RHQ(LXM)+RHQ(LXM1))*V(LXM)*AREA
TY1=.5*(GAM(LXM)+GAM(LXM1))*AREA/YDIF(JS)
GO TO 156
154 ALY1=RHQ(LXM1)*V(LXM)*AREA
DIST=.5*YDIF(JS)
IF (JS.EQ.2) DIST=YDIF(JS)
TY1=GAM(LXM1)*AREA/DIST
156 ALY=.5*(ALY+ALY1)
TY=.5*(TY+TY1)
TV=AMAX1(TY,-ALY)
CYU(I)=ALY
31 CY(I)=TV+ALY
DO 32 J=2,M
KJM=KM(K)+JM(J)
AREA=YSP(J)*ZS(K)
IS=JWL1(J,NGOTO)
IE=JWL1(J,NGOTO)
I=IS-1
LXP=KJM+IS
LP=LXP-1
LXM=LP-1
200 ALXM=RHQ(LXM)*U(LP)*AREA
ALXP=0.
TX=GAM(LXM)*AREA/XS(I)
CXU=ALXM
202 TX=AMAX1(TX,ALXP)
TX=AMAX1(TX,-ALXM)
CX=TX+ALXM
TZFAC=R(J)/(R(M)+DFAC*(R(J)-R(M)))
DO 32 I=IS,IE
MAX=JWLO(I,NGOTO)-1
LTJ=J*(J)+I
LP=KJM+I
LXP=LP+1
LYP=LP+NI
L7P=LP+MINJ
LP11=LP-1
LYP1=LYP-1
L7P1=L7P-1
AXM(LIJ)=CX
AYM(LIJ)=CY(I)

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ST	144
ST	145
ST	146
ST	147
COMMENT	134
ST	148
ST	149
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	AZM(LIJ)=CZ(LIJ)	ST	207
	AREA=YSR(J)*ZS(K)	ST	208
	IF (I.EQ.1) GO TO 33	ST	209
	ALX=RHO(LP)*AREA*(FRP(I)*U(LXP)+FXM(I)*U(LP))	ST	210
	ALXP=FYP(I)*ALX	ST	211
	ALXM=FXM(I)*ALX	ST	212
	TX=GAM(LP)*AREA/XS(I)	ST	213
	CKUP=ALX	ST	214
	GO TO 34	ST	215
33	ALXP=RHO(LXP)*U(LXP)*AREA	ST	216
	ALXM=0.	ST	217
	TX=GAM(LXP)*AREA/XS(L)	ST	218
	CKUP=ALXP	ST	219
34	TX=AMAX1(TX,ALXP)	ST	220
	TX=AMAX1(TX,-ALXM)	ST	221
	AXP(LIJ)=TX-ALXP	ST	222
	CX=TX+ALXM	ST	223
	DIVG(LIJ)=DIVG(LIJ)+CKUP-CXU	ST	224
	CXU=CKUP	ST	225
	AREA=ZS(K)*XSU(I)*RM(J+1)	ST	226
	IF (J.EQ.MAX) GO TO 35	ST	227
	ALY=.25*(RHO(LP)+RHO(LYP))*V(LYP)*AREA	ST	228
	ALY1=.25*(RHO(LP1)+RHO(LYP1))*V(LYP1)*AREA	ST	229
	ALY=.5*(ALY+ALY1)	ST	230
	TY=.25*(GAM(LP)+GAM(LYP)+GAM(LP1)+GAM(LYP1))*AREA/YDIF(J+1)	ST	231
	TY=AMAX1(TY,ABS(ALY))	ST	232
	CYUP=2.*ALY	ST	233
	GO TO 36	ST	234
35	IF (JWLO(I,4).EQ.MAX+1) GO TO 157	ST	235
	ALY=.5*(RHO(LP)+RHO(LYP))*V(LYP)*AREA	ST	236
	TY=.5*(GAM(LP)+GAM(LYP))*AREA/YDIF(MAX+1)	ST	237
	GO TO 158	ST	238
157	ALY=RHO(LYP)*V(LYP)*AREA	ST	239
	DIST=.5*YDIF(MAX+1)	ST	240
	IF (MAX.EQ.M) DIST=YDIF(MP1)	ST	241
	TY=GAM(LYP)*AREA/DIST	ST	242
158	IF (JWLO(I-1,4).EQ.MAX+1) GO TO 159	ST	243
	ALY1=.5*(RHO(LP1)+RHO(LYP1))*V(LYP1)*AREA	ST	244
	TY=.5*(GAM(LP1)+GAM(LYP1))*AREA/YDIF(MAX+1)	ST	245
	GO TO 160	ST	246
159	ALY1=RHO(LYP1)*V(LYP1)*AREA	ST	247
	DIST=.5*YDIF(MAX+1)	ST	248
	IF (MAX.EQ.M) DIST=YDIF(MP1)	ST	249
	TY1=GAM(LYP1)*AREA/DIST	ST	250
160	ALY=.5*(ALY+ALY1)	ST	251
	TY=.5*(TY+TY1)	ST	252
	TY=AMAX1(TY,ALY)	ST	253
	CYUP=ALY	ST	254
36	AYP(LIJ)=TY-ALY	ST	255
	CY(I)=TY+ALY	ST	256
	DIVG(LIJ)=DIVG(LIJ)+CYUP-CYU(I)	ST	257
	CYU(I)=CYUP	ST	258
	AREA=XSU(I)*YS(J)	ST	259
	IF (K.EQ.N) GO TO 37	ST	260
	AL7=.25*(RHO(LP)+RHO(LZP))*W(LZP)*AREA	ST	261
	AL71=.25*(RHO(LP1)+RHO(LZP1))*W(LZP1)*AREA	ST	262
	AL7=.5*(AL7+AL71)	ST	263
	GAMLP=.25*(GAM(LP)+GAM(LZP)+GAM(LP1)+GAM(LZP1))	ST	264
	T7=GAMLP*AREA*ZFACF(ZDIF(K+1)*R(J))	ST	265
	T7=AMAX1(T7,ABS(AL7))	ST	266
	C7UP=2.*AL7	ST	267
	GO TO 38	ST	268
37	AL7=RHO(LZP)*W(LZP)*AREA	ST	269
	AL71=RHO(LZP1)*W(LZP1)*AREA	ST	270

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ALZ=.5*(ALZ+ALZ1)	ST	271
ALZ=ALZ/2.	ST	272
TZ=.5*(GAM(LP)+GAM(LZP1))*AREA+TZFAC/(ZSW(NP1)+RN(J))	ST	273
TZ=AMAX1(TZ,ABS(ALZ))	ST	274
CZUP=2.*ALZ	ST	275
38 A7P(LIJ)=TZ-ALZ	ST	276
CZ(LIJ)=TZ+ALZ	ST	277
DIVG(LIJ)=DIVG(LIJ)+CZUP-CZU(LIJ)	ST	278
CZU(LIJ)=CZUP	ST	279
VOL=XSU(I)*VSR(J)+ZS(K)	ST	280
IF (I.EQ.IWLI(J,NGOTO).AND.I.GT.3) VOL=VOL*(1+.5*XSU(I-1)/XSU(I))	ST	281
IF (I.EQ.IWLO(J,NGOTO).AND.I.LT.L) VOL=VOL*(1+.5*XSU(I+1)/XSU(I))	ST	282
LXM=LP-1	ST	283
39 ROT=0.	ST	284
392 DIVG(LIJ)=AMAX1(ROT,DIVG(LIJ))	ST	285
DU(LP)=VOL/VDIF(I)	ST	286
SU(LIJ)=SU(LIJ)+VOL*DU(LP)*(P(LXM)-P(LP))+DIVG(LIJ)*U(LP)	ST	287
SP(LIJ)=SP(LIJ)+VOL-DIVG(LIJ)	ST	288
92 CONTINUE	ST	289
C-----SOURCE TERM MODIFICATIONS - BOUNDARY CONDITIONS.	COMMENT	132
CALL SCMOD	ST	290
C-----SOLVE FINITE-DIFFERENCE EQUATIONS IN SOLVE1 AND SOLVE2.	COMMENT	136
CALL SOLVE1	ST	291
301 CONTINUE	ST	292
CALL SOLVE2	ST	293
CALL FMOD	ST	294
302 CONTINUE	ST	295
C +---+---+---+---+---+---+--- V-VELOCITY +---+---+---+---+---+---+---	ST	296
ON 440 LP=1,NINJNK	ST	297
460 DV(LP)=0.0	ST	298
IF(ISOLVE(2)) 403,402,403	ST	299
403 IF(MOD(ISTEP,ISOLVE(2))) 402,404,402	ST	300
404 CONTINUE	ST	301
ISTR=2	ST	302
JSTR=3	ST	303
KSTR=2	ST	304
NV=2	ST	305
NGOTO=2	ST	306
C-----OBTAIN DIFFUSION COEFFICIENTS.	COMMENT	137
CALL GAMMA	ST	307
ON 40 J=3,M	ST	308
IS=IWLI(J,NGOTO)	ST	309
IF=IWLO(J,NGOTO)	ST	310
TZFAC=PM(J)/(RM(M)+DFAC*(RM(J)-RM(M)))	ST	311
ON 40 I=IS,IF	ST	312
LP=JM(J)+I	ST	313
LZP=LP+NINJ	ST	314
LP1=LP-NI	ST	315
LZP1=LZP-NI	ST	316
AREA=XS(I)*YSV(I)	ST	317
ALZ=RHC(LP)*W(LZP)+AREA	ST	318
ALZ1=RHC(LP1)*W(LZP1)+AREA	ST	319
ALZ=.5*(ALZ+ALZ1)	ST	320
ALZ=ALZ/2.	ST	321
TZ=.5*(GAM(LP)+GAM(LP1))*AREA+TZFAC/(ZSW(NP1)+RN(J))	ST	322
TZ=AMAX1(TZ,ABS(ALZ))	ST	323
CZU(LP)=2.*ALZ	ST	324
40 CZ(LP)=TZ+ALZ	ST	325
ON 401 K=2,M	ST	326
C-----OBTAIN SOURCE TERMS AND EVAPORATION RATES.	COMMENT	138
CALL SOURCE	ST	327
CALL SCMAS	ST	328
ON 41 I=2,L	ST	329
J=JWLI(I,NGOTO)	ST	330

AREA=ZS(K)*XS(I)*RMV(J+1)
 LP=KM(K)+JM(J)+I
 LYP=LP+NI
 LYM=LP-NI
 206 ALYM=RHO(LYM)*V(LP)*AREA
 ALYP=0.
 TY=GAM(LYM)*AREA/YS(J)
 CYU(I)=ALYM
 208 TY=AMAX1(TY,ALYP)
 TY=AMAX1(TY,-ALYM)
 41 CY(I)=TY+ALYM
 DO 42 J=3,N
 KJM=KM(K)+JM(J)
 IS=IWL1(J,NGOTO)
 IE=IWL0(J,NGOTO)
 LXP=KJM+IS
 LP=LXP-1
 LP11=LP-NI
 LXP1=LXP-NI
 AREA=YSVR(J)*ZS(K)
 IF (IWL1(J,4).EQ.IS) GO TO 162
 ALX=.5*(RHO(LP)+RHO(LXP))*U(LXP)*AREA
 TX=.5*(GAM(LP)+GAM(LXP))*AREA/XDIF(IS)
 GO TO 163
 162 ALX=RHO(LP)*U(LXP)*AREA
 DIST=.5*XDIF(IS)
 IF (IS.FQ.2) DIST=XDIF(2)
 TX=GAM(LP)*AREA/DIST
 163 IF (IWL1(J-1,4).EQ.IS) GO TO 164
 ALX1=.5*(RHO(LP11)+RHO(LXP1))*U(LXP1)*AREA
 TX1=.5*(GAM(LP11)+GAM(LXP1))*AREA/XDIF(IS)
 GO TO 165
 164 ALX1=RHO(LP11)*U(LXP1)*AREA
 DIST=.5*XDIF(IS)
 IF (IS.FQ.2) DIST=XDIF(2)
 TX1=GAM(LP11)*AREA/DIST
 165 ALX=.5*(ALX+ALX1)
 TX=.5*(TX+TX1)
 TX=AMAX1(TX,-ALX)
 CVU=ALX
 CX=TX+ALX
 TZFAC=RM(J)/(RM(N)+DFAC*(RM(J)-RM(N)))
 DO 42 I=IS,IE
 MAX=JWL0(I,NGOTO)-1
 LTJ=JM(J)+I
 LP=KJM+I
 LXP=LP+1
 LYP=LP+NI
 L7P=LP+NI+J
 LP11=LP-NI
 LXP1=LXP-NI
 L7P1=L7P-NI
 AXN(LIJ)=CX
 AYM(LIJ)=CY(I)
 AZM(LIJ)=CZ(LIJ)
 AREA=YSVR(J)*ZS(K)
 IF (I.FQ.IF) GO TO 43
 ALX=.25*(RHO(LP)+RHO(LXP))*U(LXP)*AREA
 ALX1=.25*(RHO(LP11)+RHO(LXP1))*U(LXP1)*AREA
 ALX=.5*(ALX+ALX1)
 TX=.25*(GAM(LP)+GAM(LXP)+GAM(LP11)+GAM(LXP1))*AREA/XDIF(I+1)
 TX=AMAX1(TX,ABS(ALX))
 CVUP=P*.4ALX
 GO TO 44

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43	IF (IWL0(J,4),EQ,IE) GO TO 167	ST	395
	ALX=.5*(RHO(LP)+RHO(LXP))+U(LXP)*AREA	ST	396
	TX=.5*(GAM(LP)+GAM(LXP))*AREA/XDIF(I+1)	ST	397
	GO TO 168	ST	398
167	ALX=RHO(LXP)+U(LXP)*AREA	ST	399
	DIST=.5*XDIF(I+1)	ST	400
	IF (I,EQ,L) DIST=XDIF(LP1)	ST	401
	TX=GAM(LXP)*AREA/DIST	ST	402
168	IF (IWL0(J-1,4),EQ,IE) GO TO 169	ST	403
	ALX1=.5*(RHO(LP1)+RHO(LXP1))+U(LXP1)*AREA	ST	404
	TX1=.5*(GAM(LP1)+GAM(LXP1))*AREA/XDIF(I+1)	ST	405
	GO TO 170	ST	406
169	ALX1=RHO(LXP1)+U(LXP1)*AREA	ST	407
	DIST=.5*XDIF(I+1)	ST	408
	IF (I,EQ,L) DIST=XDIF(LP1)	ST	409
	TX1=GAM(LXP1)*AREA/DIST	ST	410
170	ALX=.5*(ALX+ALX1)	ST	411
	TX=.5*(TX+TX1)	ST	412
	TX=AMAX1(TX,ALX)	ST	413
	CKUP=ALX	ST	414
44	AX*(I,J)=TX-ALX	ST	415
	CU=TX+ALX	ST	416
	DIVG(I,J)=DIVG(I,J)+CKUP-CU	ST	417
	CU=CKUP	ST	418
	AREA=7S(K)*XS(I)*RMV(J+1)	ST	419
	IF (J,EQ,JWL0(I,NGOT0)-1) GO TO 45	ST	420
	ALY=RHC(LP)*AREA*(FYP(J)+V(LYP)+FYM(J)+V(LP))	ST	421
	ALYP=FYP(J)*ALY	ST	422
	ALYM=FYM(J)*ALY	ST	423
	TY=GAM(LP)*AREA/YS(J)	ST	424
	CYUP=ALY	ST	425
	GO TO 46	ST	426
45	ALYP=RHO(LYP)*V(LYP)*AREA	ST	427
	ALYM=0.	ST	428
	TY=GAM(LYP)*AREA/YS(J)	ST	429
	CYUP=ALYP	ST	430
46	TY=AMAX1(TY,ALYP)	ST	431
	TY=AMAX1(TY,-ALYM)	ST	432
	A7P(I,J)=TY-ALYP	ST	433
	CY(I)=TY+ALYM	ST	434
	DIVG(I,J)=DIVG(I,J)+CYUP-CYU(I)	ST	435
	CYU(I)=CYUP	ST	436
	AREA=XS(I)*YSV(J)	ST	437
	IF (K,EQ,N) GO TO 47	ST	438
	AL7=.25*(RHO(LP)+RHO(L7P))*W(L7P)*AREA	ST	439
	AL71=.25*(RHO(LP1)+RHO(L7P1))*W(L7P1)*AREA	ST	440
	AL7=.5*(AL+AL71)	ST	441
	GAMLP=.25*(GAM(LP)+GAM(L7P)+GAM(LP1)+GAM(L7P1))	ST	442
	T7=GAMLP*AREA*T7FAC/(ZDIF(K+1)*RM(J))	ST	443
	T7=AMAX1(T7,ARS(AL7))	ST	444
	CZUP=.2*AL7	ST	445
	GO TO 48	ST	446
47	AL7=RHO(L7P)*W(L7P)*AREA	ST	447
	AL71=RHO(L7P1)*W(L7P1)*AREA	ST	448
	AL7=.5*(AL7+AL71)	ST	449
	AL7=AL7/2.	ST	450
	T7=GAM(L7P)*AREA*T7FAC/(ZSW(NP1)*RM(J))	ST	451
	T7=AMAX1(T7,ARS(AL7))	ST	452
	C7UP=.2*AL7	ST	453
48	A7P(I,J)=T7-AL7	ST	454
	C7(I,J)=T7+AL7	ST	455
	DIVG(I,J)=DIVG(I,J)+C7UP-C7U(I,J)	ST	456
	C7U(I,J)=C7UP	ST	457
	WOL=XS(I)*YSV(J)*ZS(K)	ST	458

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ALY=.5*(ALY+ALY1)	ST	519
NTST=.5*XDIF(J)	ST	520
IF (J.EQ.2) DIST=VU1F(2)	ST	521
TY=.5*(GAM(LP)+GAM(LP11))+AREA/DIST	ST	522
TY=AMAX1(TY,-ALY)	ST	523
CVU(I)=ALY	ST	524
91 CV(I)=TY+ALY	ST	525
DO 52 J=2,M	ST	526
KJM=KM(K)+JF(J)	ST	527
IS=IWL(I(J,NGOTO))	ST	528
IF=IWL(I(J,NGOTO))	ST	529
LXP=KJM+IS	ST	530
LP=LXP-1	ST	531
LP11=LP-NINJ	ST	532
LXP1=LXP-NINJ	ST	533
AREA=YSR(J)+ZSW(K)	ST	534
ALX=RHO(LP)+U(LXP)+AREA	ST	535
ALX1=RHO(LP11)+U(LXP1)+AREA	ST	536
ALX=.5*(ALX+ALX1)	ST	537
DIST=.5*XDIF(IS)	ST	538
IF (IS.EQ.2) DIST=XDIF(2)	ST	539
TX=.5*(GAM(LP)+GAM(LP11))+AREA/DIST	ST	540
TX=AMAX1(TX,-ALX)	ST	541
CKU=ALX	ST	542
CX=TX+ALX	ST	543
TZFA=1.0	ST	544
DO 52 I=IS,IF	ST	545
MAX=JWL(I(J,NGOTO))-1	ST	546
LIJ=JM(J)+I	ST	547
LP=KJM+I	ST	548
LXP=LP+1	ST	549
LYP=LP+NI	ST	550
L7P=LP+NINJ	ST	551
LP11=LP-NINJ	ST	552
LXP1=LXP-NINJ	ST	553
LYP1=LYP-NINJ	ST	554
AXM(LIJ)=CX	ST	555
AYM(LIJ)=CV(I)	ST	556
A7M(LIJ)=C7(LIJ)	ST	557
AREA=YSR(J)+ZSW(K)	ST	558
IF (I.EQ.IF) GO TO 53	ST	559
ALX=.25*(RHO(LP)+RHO(LXP))+U(LXP)+AREA	ST	560
ALX1=.25*(RHO(LP11)+RHO(LXP1))+U(LXP1)+AREA	ST	561
ALX=.5*(ALX+ALX1)	ST	562
TX=.25*(GAM(LP)+GAM(LXP)+GAM(LP11)+GAM(LXP1))+AREA/XDIF(I+1)	ST	563
TX=AMAX1(TX,ARS(ALX))	ST	564
CKUP=2.0*ALX	ST	565
GO TO 54	ST	566
93 ALX=RHO(LXP)+U(LXP)+AREA	ST	567
ALX1=RHO(LXP1)+U(LXP1)+AREA	ST	568
ALX=.5*(ALX+ALX1)	ST	569
DIST=.5*XDIF(I+1)	ST	570
IF (I.EQ.L) DIST=XDIF(LP1)	ST	571
TX=.5*(GAM(LXP)+GAM(LXP1))+AREA/DIST	ST	572
TX=AMAX1(TX,ALX)	ST	573
CKUP=ALX	ST	574
94 AXD(LIJ)=TX-ALX	ST	575
CX=TX+ALX	ST	576
DIVG(LIJ)=DIVG(LIJ)+CKUP-CXU	ST	577
CKU=CKUP	ST	578
AREA=7SW(K)+NS(I)+RM(J+1)	ST	579
IF (J.EQ.MAX) GO TO 55	ST	580
ALY=.25*(RHO(LP)+RHO(LYP))+V(LYP)+AREA	ST	581
ALY1=.25*(RHO(LP11)+RHO(LYP1))+V(LYP1)+AREA	ST	582

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ALY=.5*(ALY+ALY1)
TY=.25*(GAM(LP)+GAM(LYP)+GAM(LP11)+GAM(LYP11))*AREA/YDIF(J+1)
TY=AMAX1(TY,APS(ALY))
CYUP=2.*ALY
GO TO 56
ALY=RHD(LYP)*V(LYP)*AREA
ALY1=RHD(LYP1)*V(LYP1)*AREA
ALY=.5*(ALY+ALY1)
DIST=.9*YDIF(J+1)
IF (J.EQ.M) DIST=YDIF(MP1)
TY=.5*(GAM(LYP)+GAM(LYP1))*AREA/DIST
TY=AMAX1(TY,ALY)
CYUP=ALY

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NASAX	37
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NASAX	40
NASAX	41
NASAX	42
NASAX	43
ST	626
COMMENT	143
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COMMENT	144
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ISTR=2
JSTR=2
KSTR=2
NV=4
A000 CONTINUE
CALCULATE CONTINUITY ERRORS.
DO 60 J=2,P
  TS=IWL(I,J,NGOTO)
  IE=IWL(I,J,NGOTO)
  DO 60 I=TS,IE
    LP=JN(J)+I
    LTP=LP+MINJ
    RHQA=RHO(LP)*XS(I)*YS(J)
    CZU(LP)=R*DA*W(LTP)
  A0 CZ(LP)=RHQA*DW(LTP)
  DO 601 K=2,M
    DO 61 I=2,L
      J=JWL(I,I,NGOTO)+1
      LP=KN(K)+JN(J-1)+I
      LYP=LP+NI
      RHQA=RHO(LP)*ZS(K)*XS(I)*RM(J)
      CYU(I)=RHQA*V(LYP)
    A1 CY(I)=RHQA*CV(LYP)
    DO 62 J=2,M
      KJM=KN(K)+JN(J)
      TS=IWL(I,J,NGOTO)
      IE=IWL(I,J,NGOTO)
      LP=KJM+IS-1
      LXP=LP+1
      RHQA=RHO(LP)*YSR(J)*ZS(K)
      CKU=RHQA*U(LXP)
      CY=RHQA*DU(LXP)
      DO 62 I=TS,IE
        MAX=JWL(I,I,NGOTO)-1
        LTJ=JN(J)+I
        LP=KJM+I
        LXP=LP+1
        LYP=LP+NI
        LTP=LP+MINJ
        AXH(LTJ)=CX
        AYH(LTJ)=CY(I)
        AZH(LTJ)=CZ(LTJ)
        IF (I.EQ.IE) GO TO 63
        RHQA=0.5*(RHO(LP)+RHO(LXP))*YSR(J)*ZS(K)
        GO TO 64
      A3 RHQA=RHO(LXP)*YSR(J)*ZS(K)
    A4 CX=RHQA*DU(LXP)
    CKUP=RHQA*U(LXP)
    SU(LTJ)=CKU-CKUP
    CXU=CKUP
    AXH(LTJ)=CX
    IF (J.EQ.MAX) GO TO 65
    RHQA=0.5*(RHO(LP)+RHO(LYP))*ZS(K)*XS(I)*RM(J+1)
    GO TO 66
  A5 RHQA=RHO(LYP)*ZS(K)*XS(I)*RM(J+1)
  A6 CY(I)=RHQA*DV(LYP)
  CYUP=RHQA*V(LYP)
  SU(LTJ)=SU(LTJ)+CYU(I)-CYUP
  CYU(I)=CYUP
  AYH(LTJ)=CY(I)
  IF (K.EQ.M) GO TO 67
  RHQA=0.5*(RHO(LP)+RHO(LTP))*XS(I)*YS(J)
  GO TO 68
A7 RHQA=RHO(LTP)*XS(I)*YS(J)

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C ----- HERE PP IS KE, P IS DISSIPATION
  READ (NTP1) PP,P
710 IF (INV,NE,LVFUNK) GO TO 714
C ----- HERE PP IS KE, P IS DISS
  WRITE (NTP2) PP,P
C ----- HERE PP IS PHI, P IS MFU, DU IS MCD
  READ (NTP1) PP,P,DU
714 IF (INV,NE,LVH) GO TO 720
C ----- HERE DV IS ENTHALPY, DW IS FAV
  READ (NTP1) DV,DW
  : ICPS=3
  NS1=ION2
  NS2=ION2
  S2(ION2)=RATIO2/SMW(ION2)
  S2(ION2)=(1.0-RATIO2)/SMW(ION2)
C ----- BOUNDARY VALUES OF ENTHALPY.
  DO 716 K=1,NP1
  DO 717 I=1,LP1
    IF (IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3) GO TO 712
    LP=KM(K)+JM(JWLI(I,4))+I
    LPH=LP+NVH(NVH)
    TK=TEMP(LP)
    TKINV=1.000/TK
    CALL MCPS
    F(LPH)=HSUM+UNICON*TK
712 IF (IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3) GO TO 717
    LP=KM(K)+JM(JWLI(I,4))+I
    LPH=LP+NVH(NVH)
    TK=TEMP(LP)
    TKINV=1.000/TK
    CALL MCPS
    F(LPH)=HSUM+UNICON*TK
717 CONTINUE
  DO 716 J=1,NP1
    IF (JKIN(J,K).EQ.1) GO TO 760
    LP=KM(K)+JM(J)+JWLI(J,4)-1
    LPH=LP+NVH(NVH)
    TK=TEMP(LP)
    TKINV=1.000/TK
    CALL MCPS
    F(LPH)=HSUM+UNICON*TK
760 IF (J.EQ.JWOT.AND.J.LT.JWOD) GO TO 716
    LP=KM(K)+JM(J)+JWLI(J,4)+1
    LPH=LP+NVH(NVH)
    TK=TEMP(LP)
    TKINV=1.000/TK
    CALL MCPS
    F(LPH)=HSUM+UNICON*TK
716 CONTINUE
720 IF (ISOLVE(NV)) 703,702,703
703 IF (MOD(ISTEP,ISOLVE(NV))) 702,704,702
704 CONTINUE
  ISTR=2
  JSTR=2
  KSTR=2
C ----- OBTAIN DIFFUSION COEFFICIENTS.
  CALL GAMMA
  DO 70 J=2,M
    IS=JWLI(J,NGOTO)
    IF=JWLI(J,NGOTO)
    TFAC=4(J)/(R(M)+DFAC*(R(J)-R(M)))
    DO 70 I=IS,IE
      LP=JM(J)+I
      LPH=LP+NIJ

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NOX	213
COMMENT	149
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AREA=XS(I)*YS(J)
ALZ=RHO(LP)*W(LZP)*AREA
ALZ=ALZ/2.
TZ=GAM(LP)*AREA*TZFAC/(ZSW(NP1)*R(J))
TY=AMAX1(TZ,ABS(ALZ))
CVU(LP)=2.*ALZ
70 C7(LP)=TZ+ALZ
DO 701 K=2,N
C-----OBTAIN SOURCE TERMS AND EVAPORATION RATES.
CALL SOURCE
CALL SOMAS
DO 71 I=2,L
J=JML(I,NGOTO)+1
LP=KN(K)+JM(J-1)+I
LYP=LP+NI
AREA=ZS(K)*XS(I)*RM(J)
ALY=RHO(LP)*V(LYP)*AREA
DIST=.9*YDIF(J)
IF (J.EQ.2) DIST=YDIF(2)
TY=GAM(LP)*AREA/DIST
TY=AMAX1(TY,-ALY)
CVU(I)=ALY
71 CY(I)=TY+ALY
DO 72 J=2,M
KJM=KN(K)+JM(J)
IS=JML(I,NGOTO)
IE=JVL(I,NGOTO)
LXP=KJM+IS
LP=LXP-1
AREA=YSR(J)*ZS(K)
ALX=RHO(LP)*U(LXP)*AREA
DIST=.9*XDIF(IS)
IF (IS.EQ.2) DIST=XDIF(2)
TX=GAM(LP)*AREA/DIST
TX=AMAX1(TX,-ALX)
CXU=ALX
CX=TX+ALX
TZFAC=R(J)/(R(N)+DFAC*(R(J)-R(N)))
DO 72 I=IS,IE
MAX=JVL(I,NGOTO)-1
LIJ=JM(J)+I
LP=KJM+I
LYP=LP+1
LYP=LP+NI
LYP=LP+NI*J
AXM(LIJ)=CX
AYM(LIJ)=CY(I)
AZM(LIJ)=CZ(LIJ)
AREA=YSR(J)*ZS(K)
IF (I.EQ.IF) GO TO 73
ALX=.25*(RHO(LP)+RHO(LXP))*U(LXP)*AREA
TX=.5*(GAM(LP)+GAM(LXP))*AREA/XDIF(I+1)
TX=AMAX1(TX,ABS(ALX))
CXUP=2.*ALX
GO TO 74
73 ALX=RHO(LXP)*U(LXP)*AREA
DIST=.9*XDIF(I+1)
IF (I.EQ.L) DIST=XDIF(LP1)
TX=GAM(LXP)*AREA/DIST
TX=AMAX1(TX,ALX)
CXUP=ALX
74 AXD(LIJ)=TX-ALX
CX=TX+ALX
DIVG(LIJ)=DIVG(LIJ)+CXUP-CXU

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CYU=CYUP
AREA=7S(K)*XS(I)*RM(J+1)
IF (J.EQ.MAX) GO TO 75
ALY=.25*(RHC(LP)+RHD(LYP))*V(LYP)*AREA
TY=.5*(GAM(LP)+GAM(LYP))*AREA/YDIF(J+1)
TY=AMAX1(TY,ABS(ALY))
CYUP=2.*ALY
GO TO 76
75 ALY=RHD(LYP)*V(LYP)*AREA
DIST=.5*YDIF(J+1)
IF (J.EQ.M) DIST=YDIF(MP1)
TY=GAM(LYP)*AREA/DIST
TY=AMAX1(TY,ALY)
CYUP=ALY
76 AYP(LIJ)=TY-ALY
CY(I)=TY+ALY
DIVG(LIJ)=DIVG(LIJ)+CYUP-CYU(I)
CYU(I)=CYUP
AREA=XS(I)*YS(J)
IF (K.EQ.N) GO TO 77
ALZ=.25*(RHO(LP)+RHO(LZP))*W(LZP)*AREA
TZ=.5*(GAM(LP)+GAM(LZP))*AREA+TZFAC/(ZDIF(K+1)*R(J))
TZ=AMAX1(TZ,ABS(ALZ))
CZUP=2.*ALZ
GO TO 78
77 ALZ=RHO(LZP)*W(LZP)*AREA
ALZ=ALZ/2.
TZ=GAM(LZP)*AREA+TZFAC/(ZSW(MP1)*R(J))
TZ=AMAX1(TZ,ABS(ALZ))
CZUP=2.*ALZ
78 AZP(LIJ)=TZ-ALZ
CZ(LIJ)=TZ+ALZ
DIVG(LIJ)=DIVG(LIJ)+CZUP-CZU(LIJ)
CZU(LIJ)=CZUP
VOL=XS(I)*YSR(J)*ZS(K)
79 ROT=0.
792 DIVG(LIJ)=AMAX1(ROT,DIVG(LIJ))
LPF=LP+NUM(NVF(NV))
SU(LIJ)=SU(LIJ)+VOL+DIVG(LIJ)*F(LPF)
SP(LIJ)=SP(LIJ)+VOL-DIVG(LIJ)
72 CONTINUE
C-----SOURCE TERM MODIFICATIONS - BOUNDARY CONDITIONS.
CALL SOMOD
C-----CHEMICAL KINETICS CALCULATIONS.
C
IF(NV.NF.LVM1)GO TO 722
PA=PRESS
DO 723 J=2,M
TS=TWL(IJ,NGOTO)
IF=TWLO(J,NGOTO)
DO 723 I=IS,IE
LIJ=I+JM(J)
LP=LIJ+KM(K)
TK=TEMP(LP)
FMV=AKP(LIJ)+AKM(LIJ)+AYP(LIJ)+AYM(LIJ)+AZP(LIJ)+AZM(LIJ)
C-----NONE IN BLOCKAGE - SKIP CALCULATION - GO TO 723
IF(FMV.LT.1.0E-10)GO TO 723
FMV=FMV-SP(LIJ)
IF(FMV.GT.1.0E20)GO TO 723
LPF=LP+1
LPW=LP-1
LPN=LP+NI
LPS=LP-NI
LPT=LP+MINJ

```

ST	867
ST	868
ST	869
ST	870
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ST	890
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ST	897
ST	898
ST	899
ST	900
ST	901
ST	902
ST	903
ST	904
ST	905
ST	906
ST	907
COMMENT	192
ST	908
COMMENT	193
COMMENT	194
NOX	230
NOX	231
NOX	232
NOX	233
NOX	234
NOX	235
NOX	236
NOX	237
NOX	238
NOX	239
COMMENT	199
NOX	240
NOX	241
NOX	242
NOX	243
NOX	244
NOX	245
NOX	246
NOX	247

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LPH=LP-NHJ
LIJ2=LIJ+NH(2)
LPFHUX=LP+NHV(NVHUX)
IF(IIR.NF.1)GO TO 741
IF(IISTEP.NE.IHNOX)GO TO 741
C-----FIRST ITERATION - SET SPECIES CONCENTRATIONS EQUAL TO THOSE
C AT NEIGHBORING NODE WHICH HAS ALREADY BEEN SOLVED.
IF(IRES.NF.0)GO TO 741
IF(I.EQ.1)GO TO 743
DO 742 II=9,NS
FS(LP,II)=FS(LPW,II)
IF(I.NE.IE)FS(LPE,II)=FS(LPW,II)
IF(J.NE.JWLO(I,NGOTO)-1)FS(LPN,II)=FS(LPW,II)
FS(LPT,II)=FS(LPW,II)
742 IF(K.FQ.N)FS(LPT,II)=FS(LIJ2,II)
GO TO 741
743 IF(J.EC.JWLI(I,NGOTO)+1)GO TO 741
DO 744 II=9,NS
FS(LP,II)=FS(LPS,II)
IF(I.NE.IE)FS(LPE,II)=FS(LPS,II)
IF(J.NE.JWLO(I,NGOTO)-1)FS(LPN,II)=FS(LPS,II)
FS(LPT,II)=FS(LPS,II)
744 IF(K.FQ.N)FS(LPT,II)=FS(LIJ2,II)
741 CONTINUE
C-----PREPARE INPUTS TO CHEMICAL KINETICS PROGRAM CREK.
DO 724 II=1,NS
S2(II)=FS(LP,II)/SMW(II)
724 S1(II)=(AXP(LIJ)*FS(LPE,II)+AKM(LIJ)*FS(LPW,II)+AYP(LIJ)
1*FS(LPN,II)+AYM(LIJ)*FS(LPS,II)+AZP(LIJ)*FS(LPT,II)+A7M(LIJ)
2*FS(LPB,II))/(ENV*SMW(II))
MSURO=FP+NVH(NVH)
LPC=1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)
EDKIJ=EDK(LPC)
C-----MODEP=1, LAPINAR RATES USED.
IF(MODEP.EQ.1)EDKIJ=1.0E50
FUT=F(LPFUX)
IF(MFZ.NE.0)S1(IDFU)=S1(IDFU)+EVAP(LPC)/(ENV*SMW(IDFU))
FMV=ENV/(XS(I)*YS(J)*ZS(K))
IF(TK.LT.THCK)GO TO 735
C-----BYPASS CALCULATION IF TEMPERATURE,LT,THCK (THCK INPUT
C BY USER).
CALL CREK
C-----OBTAIN RESULTS FROM CREK.
RHO(LP)=RHOPP
TEMP(LP)=TK
C-----STORE SPECIES CONCENTRATIONS IN RESPECTIVE ARRAYS.
DO 725 II=1,NS
FSLP=S2(II)*SMW(II)
IF(FSLP.LT.1.0E-20)GO TO 725
C-----CHECK CONVERGENCE.
IF(ABS(FSLP-FS(LP,II))/FSLP.GT.0.01)CONVG=1
725 FS(LP,II)=FSLP
GO TO 735
735 CONTINUE
DO 736 II=9,NS
FSLP=S1(II)*SPW(II)
IF(FSLP.LT.1.0E-20)GO TO 736
IF(ABS(FSLP-FS(LP,II))/FSLP.GT.0.01)CONVG=1
736 FS(LP,II)=FSLP
735 CONTINUE
LPN2=LP+NVH(LVQ2)
LPFU=LP+NVH(NVFU)
LPFUI=LP+NVH(LVFI)
LPCD=LP+NVH(NVCD)

```

NOX	248
NOX	249
NOX	250
NOX	251
NOX	252
COMMENT	156
COMMENT	157
JAN18	1
NOX	254
4STEP	329
NOX	256
NOX	257
NOX	258
NOX	259
NOX	260
NOX	261
NOX	262
4STEP	330
NOX	264
NOX	265
NOX	266
NOX	267
NOX	268
NOX	269
COMMENT	158
NOX	270
NOX	271
NOX	272
NOX	273
NOX	274
NOX	275
NOX	276
NOX	277
COMMENT	159
NOX	278
4STEP	331
FEB2	3
NOX	280
NOX	281
COMMENT	160
COMMENT	161
NOX	282
COMMENT	162
NOX	283
NOX	284
COMMENT	163
NOX	285
NOX	286
NOX	287
COMMENT	164
NOX	288
NOX	289
NOX	290
NOX	291
4STEP	332
NOX	293
NOX	294
NOX	295
NOX	296
NOX	297
NOX	298
NOX	299
NOX	300
NOX	301

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LPC01=LP+NVN(LVCO1)
F(LPFU1)=AMIN1(F(LPFU1),F(LPFU0K1))
F(LP02)=AMIN1(F(LP02),RATIO2)
F(LPFU)=F(LPFU1)
F(LPC0)=F(LPC01)
LPCN=LP+NVN(NVCH)
LPCN1=LP+NVN(LVCH1)
LPH2=LP+NVN(NVM2)
LPH21=LP+NVN(LVH21)
F(LPCN)=F(LPCN1)
F(LPH2)=F(LPH21)
723 CONTINUE
GO TO 701
C-----SOLVE FINITE-DIFFERENCE EQUATIONS IN SOLVE1 AND SOLVE2.
722 CALL SOLVE1
701 CONTINUE
IF(NV.NE.LVM1)CALL SOLVE2
CALL FMOD
702 CONTINUE
IF(ICONV6.EQ.0)GO TO 700
706 CONTINUE
700 CONTINUE
C-----UPDATE DEPENDENT VARIABLE VALUES IN FMOD.
DO 705 INV=LVFU1,LVCH
NV=INV
705 CALL FMOD
NV=LVFU1
CALL FMOD
NV=LVCO1
CALL FMOD
NV=LVFU
CALL FMOD
NV=LVCO
CALL FMOD
NV=LVCH
CALL FMOD
NV=LVH2
CALL FMOD
CALL DENMOD
C-----OUTLET BOUNDARY.
DO 1005 J=1,NP1
DO 1005 K=2,N
LP=LP1+JM(J)+KM(K)
1005 TEMP(LP)=TEMP(LP-1)
IF(IONV.NE.C)GO TO 1044
C-----SYMMETRY AXIS.
DO 1006 I=2,LP1
DO 1006 K=2,N
LP=I+KM(K)
LPN=LP+JM(2)
1006 TEMP(LP)=TEMP(LPN)
C-----CYCLIC BOUNDARY CONDITIONS.
1044 DO 1002 J=1,NP1
DO 1002 I=1,LP1
LIJ=I+JM(J)
LP2=I+JM(J)+KM(2)
LPN=LIJ+KM(N)
LPNP1=LIJ+KM(NP1)
TEMP(LIJ)=TEMP(LPN)
1002 TEMP(LPNP1)=TEMP(LP2)
C ++++++-----+-----+-----+-----+-----+-----+-----+
C ++++++ HERE U IS FX, V IS FY, W IS FZ
READ (NTP1) U,V,W
END=0

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NOX	302
NOX	303
NOX	304
NOX	305
NOX	306
4STEP	333
4STEP	334
4STEP	335
4STEP	336
4STEP	337
4STEP	338
NOX	307
NOX	308
COMMENT	165
NOX	309
ST	910
NOX	310
ST	912
ST	913
NOX	311
NOX	312
ST	914
COMMENT	166
NOX	313
NOX	314
NOX	315
NOX	316
NOX	317
NOX	318
NOX	319
NOX	320
NOX	321
NOX	322
NOX	323
4STEP	339
4STEP	340
4STEP	341
4STEP	342
NOX	324
COMMENT	167
NOX	325
NOX	326
NOX	327
NOX	328
NOX	329
COMMENT	168
NOX	330
NOX	331
NOX	332
NOX	333
NOX	334
COMMENT	169
NOX	335
NOX	336
NOX	337
NOX	338
NOX	339
NOX	340
NOX	341
NOX	342
ST	915
ST	916
ST	917
ST	918

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DO 730 NV=LVRX,LVRZ
IF (ISOLVE(NV)) 733,730,733
733 IF (MOD(ISTEP,ISOLVE(NV))) 730,734,730
734 IF (IND.FO.O) CALL GAMRAD
IF (IPLAX.FO.1) IND=1
CALL STRAD
CALL FMOD
730 CONTINUE
C ----- COMPUTE AVG RADIATION FLUX -----
DO 740 K=1,NP1
DO 740 J=1,NP1
KJM=K*(K)+J*(J)
DO 740 I=1,LP1
LP=KJM+I
LPRX=LP+NVX(NVRX)
LPRY=LP+NVY(NVRY)
LPRZ=LP+NVZ(NVRZ)
LPAFV=LP+NVF(NVFAV)
740 F(LPAFV)=(F(LPRX)+F(LPRY)+F(LPRZ))/3.
C ----- HERE PP IS PHI, P IS MFU, DU IS MCD
WRITE (NTP2) PP,P,DU
C ----- HERE DV IS ENTHALPY, DW IS FAV
WRITE (NTP2) DV,DW
C ----- HERE U IS FX, V IS FY, W IS FZ
WRITE (NTP2) U,V,W
WRITE (NTP2) TEMP,RHO
WRITE (NTP2) FCH,FH2
WRITE (NTP2) ANUC,SOOT1,SOOT2
WRITE (NTP2) FS
799 NTP1=NTP1+NTP2
NTP1=NTP1-NTP1
NTP2=NTP2-NTP2
800 ISTEP=ISTEP+1
IXY= 3-IXY
RETURN
END
SUBROUTINE STRAD
COMMON/COEFF/A(40),B(40),EP(30),DP(30),APP(30),BPP(30)
COMMON F(3500),DU(500),DV(500),DW(500),
1 ANUC(500),SOOT1(500),SOOT2(500),FCH(500),FH2(500),FS(500,14),
1 RHO(500),VISC(500),ANSR(500),SCTR(500),SU(100),SP(100),
1 DRHODP(500),
1 AXP(100),AXM(100),AYP(100),AYM(100),AZP(100),
2 AYM(100),C7(100),CY(10),CZU(100),CYU(10),
3 CZP(100),CYP(10),DIVG(100),NTP1,NTP2
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
DIMENSION GAM(500)
EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
EQUIVALENCE (F(3001),GAM(1))
COMMON/CVL/R(30),RM(30),RNV(30),YSR(30),YSVR(30),IPLAX
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSV(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXM(40),
2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME
COMMON
1/CINDEX/IDCQ,IDFU,IDD2,IDN2,IDH20,IDC02,IDN1,IDH2,IDN0,IDN02
1,IDN,IDDM,IMCPS,ILC,ILM,IMAT,ITER,JJJ,N1,N2,N3,NA,NGL00,NGL00P,
2 NLM,NQ,NSP,NS1,NS2,IOCH
3/CHEM/CPSUM,MSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG
4/CPAPAP/ASUB(30,3),ENV,ER,MSUB0,NDERUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOPP,
4 SM,SMW(30),SMO,S1(30),S2(30),TK,LAOTAR,LOEBUG,LEQUIL,LREACT,
4 LEMER,EDKIJ,LCONVG

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ST	919
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ST	938
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ST	940
ST	941
ST	942
ST	943
ST	944
4STEP	343
SOOT	403
NOX	343
ST	945
ST	946
ST	947
ST	948
ST	949
ST	950
ST	951
STR	2
NASAX	44
CONF8	2
4STEP	18
RAD	3
RAD	4
CONF8	4
CONF8	5
CONF8	6
CTDMA	3
CTDMA	4
CONF8	7
CONF8	8
CONF8	9
CONF8	10
CONF8	11
COMMON	2
COMMON	3
COMMON	4
COMMON	5
NOX	2
NOX	3
NOX	4
4STEP	3
NOX	6
NOX	7
NOX	8
NOX	9

DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUBO,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FIIT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,	4STEP	5
1 CENU3,CENU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CFXP2,CENP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADIAN,LCONVG,LDEBUG,LEQUIL,INRG,LREACT,LENER	NOX	12
COMMON/INT/L,M,N,LCV,NCV,NCV,LP1,MP1,MP1,NI,NJ,NK,NINJ,NINJNK,NV,	COMMON	6
1 NVV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KM(30),JM(30),ISTEP,	4STEP	8
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,	4STEP	9
3 NRHO,NGAM,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWEI,	COMMON	9
4 TWEQ,MN1,JWTI,JWTO,JMO1,JWNO,IDM,JKIN(30,30),IKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LREF,ISTUM,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1,PLAXM1,LVK,LVD,LVFX,LVFO,LVCO,LVM,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
2 TJHMP,IFES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUMCC,NVH2O,NVCO2,	COMMON	13
3 NVH2,NVCH,NVH2	4STEP	11
COMMON/CNOX/LVM1,LVM2,LVN1,LVNO,LVNO2,LVD,LVDH,LVM2O,LVN2,LVD2,	NOX	16
1 LVCO2,LVFU1,LVCO1,MNOX,INOX,ITNOX,SMOX,TNOX	NOX	17
COMMON/THERM/NVM,NVFX,NVFX,NVFX,NVTE,NODEN,IDX,FSTOIC,HFU,CP,	COMMON	15
1 GASCON,RHOCN,UNICON,PRESS,NVFAV,TCYLW,TINLW,TLIP,ACDEF(4),	COMMON	16
2 T4,DFAC,WFO,WCO2,WCO,WOX,WH2O,WH2,HYY,CXX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIO4,WCO,TAN,ITWALL	COMMON	18
COMMON/CTDMA/KEND,ICTDMA(32)	4STEP	12
C-----SUBROUTINE STRAD IS USED FOR CALCULATING THE FINITE-	COMMENT	170
C DIFFERENCE COEFFICIENTS IN THE RADIATION FLUX EQUATIONS	COMMENT	171
C AND FOR SOLVING THESE EQUATIONS BY USING THE	COMMENT	172
C TRI-DIAGONAL-MATRIX-ALGORITHM(TDMA).	COMMENT	173
C	COMMENT	174
KONTRO=NV-LVRX+1	STR	6
GO TO (100,200,300),KONTRO	STR	7
C ----- X-DIRECTION FLUX -----	STR	8
100 CONTINUE	STR	9
DO 101 K=2,N	STR	10
NVKM=NVM(NVRX)+KM(K)	STR	11
C-----OBTAIN SOURCE TERMS (SORAD) AND BOUNDARY CONDITIONS (SOMOD).	COMMENT	175
CALL SORAD	STR	12
CALL SOMOD	STR	13
DO 102 J=2,M	STR	14
TX=0.	STR	15
IS=IWLI(J,NGOTO)	STR	16
IE=IWLO(J,NGOTO)	STR	17
DO 103 I=IS,IE	STR	18
LIJ=JM(J)+I	STR	19
LO=LIJ+KM(K)	STR	20
LXP=LJ+1	STR	21
AXM(LIJ)=TX	STR	22
TX=.5*(GAM(LP)+GAM(LXP))/XDIF(I+1)	STR	23
AXP(LIJ)=TX	STR	24
SU(LIJ)=SU(LIJ)+XS(I)	STR	25
SP(LIJ)=SP(LIJ)+XS(I)	STR	26
103 CONTINUE	STR	27
AXP(LIJ)=0.	STR	28
102 CONTINUE	STR	29
C-----TDMA SOLUTION.	COMMENT	176
DO 104 J=2,M	STR	30
LRF=NVM+JM(J)	STR	31
IS=IWLI(J,NGOTO)	STR	32
IE=IWLO(J,NGOTO)	STR	33
ISTR1=IS-1	STR	34
A(ISTR1)=0.	STR	35
A(ISTR1)=0.	STR	36
DO 105 I=IS,IE	STR	37
LIJ=JM(J)+I	STR	38
STORE=AXP(LIJ)+AXM(LIJ)-SP(LIJ)-AXM(LIJ)+A(I-1)	STR	39

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      A(I)=AXP(LIJ)/STORE
105 R(I)=(SU(LIJ)+AXP(LIJ)*R(I-1))/STORE
      ISUM=IS+IF
      DO 106 II=IS,IE
      I=ISUM-II
      LP=LPF+I
106 F(LP)=A(I)*F(LP+1)+B(I)
104 CONTINUE
101 CONTINUE
      RETURN
C ----- Y-DIRECTION FLUX -----
200 CONTINUE
      DO 201 K=2,N
      NVKM=NVN(NVRY)+KM(K)
C----- OBTAIN SOURCE TERMS (SORAD) AND BOUNDARY CONDITIONS (SOMD).
      CALL SORAD
      CALL SOMD
      DO 202 I=2,L
      TY=0.
      JS=JWL(I,NGOTO)+1
      JF=JWL(I,NGOTO)-1
      DO 203 J=JS,JF
      LIJ=JM(J)+I
      LP=LIJ+KM(K)
      LYP=LP+NI
      AYM(LIJ)=TY
      TY=.7*(GAM(LP)+GAM(LYP))/YDIF(J+1)*RN(J+1)
      AYP(LIJ)=TY
      SU(LIJ)=SU(LIJ)+YS(J)*R(J)
      SP(LIJ)=SP(LIJ)+YS(J)*R(J)
203 CONTINUE
      AYP(LIJ)=0.
202 CONTINUE
C----- TMA SOLUTION.
      DO 204 I=2,L
      LPF=NVKM+I
      JS=JWL(I,NGOTO)+1
      JF=JWL(I,NGOTO)-1
      JSTR1=JS-1
      A(JSTR1)=0.
      R(JSTR1)=0.
      DO 205 J=JS,JF
      LIJ=JM(J)+I
      STORE=AYP(LIJ)+AYM(LIJ)-SP(LIJ)-AYM(LIJ)*A(J-1)
      A(J)=AYP(LIJ)/STORE
205 R(J)=(SU(LIJ)+AYM(LIJ)*R(J-1))/STORE
      JSUM=JS+JF
      DO 206 JJ=JS,JF
      J=JSUM-JJ
      LP=LPF+JM(J)
      LYP=LP+NI
206 F(LP)=A(J)*F(LYP)+R(J)
204 CONTINUE
201 CONTINUE
      RETURN
C ----- Z-DIRECTION FLUX -----
300 KSUM=2+N
      DO 301 J=2,N
      JPLANF=J
      NVJM=NVN(NVZZ)+JM(J)
C----- OBTAIN SOURCE TERMS (SORAD) AND BOUNDARY CONDITIONS (SOMDZ).
      CALL SORAD
      CALL SOMDZ
      IS=IWL(IJ,NGOTO)

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STR 40
STR 41
STR 42
STR 43
STR 44
STR 45
STR 46
STR 47
STR 48
STR 49
STR 50
STR 51
STR 52
STR 53
COMMENT 177
STR 54
STR 55
STR 56
STR 57
STR 58
STR 59
STR 60
STR 61
STR 62
STR 63
STR 64
STR 65
STR 66
STR 67
STR 68
STR 69
STR 70
STR 71
COMMENT 178
STR 72
STR 73
STR 74
STR 75
STR 76
STR 77
STR 78
STR 79
STR 80
STR 81
STR 82
STR 83
STR 84
STR 85
STR 86
STR 87
STR 88
STR 89
STR 90
STR 91
STR 92
STR 93
STR 94
STR 95
STR 96
STR 97
COMMENT 179
STR 98
STR 99
STR 100

```


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```

IF=IWLO(J,NGOTO)
DO 302 I=15,IF
  IJ=JM(J)+I
  T7=0.
DO 303 K=2,N
  LTK=JM(K)+I
  LP=IJ+HN(K)
  L7P=LP+MINJ
  AZM(LIK)=T7
  TZ=.5*(GAM(LP)+GAM(L7P))/(ZDIF(K+1)*R(J))
  AZP(LIK)=TZ
  SU(LIK)=SU(LIK)+ZS(K)*R(J)
  SP(LIK)=SP(LIK)+ZS(K)*R(J)
303 CONTINUE
  AZP(LIK)=0.
302 CONTINUE
C-----TOMA SOLUTION.
DO 304 I=15,IE
  A(1)=0.
  R(1)=0.
  LPF=NVJM+I
DO 305 K=2,N
  LK=JM(K)+I
  STORE=AZP(LIK)+AZM(LIK)-SP(LIK)-AZM(LIK)*A(K-1)
  A(K)=AZP(LIK)/STORE
305 R(K)=(SU(LIK)+AZM(LIK)*B(K-1))/STORE
DO 306 KK=2,N
  K=KSUM-KK
  LP=LPF+KK(K)
  L7P=LP+MINJ
306 F(LP)=A(K)+F(L7P)+B(K)
304 CONTINUE
301 CONTINUE
  RETURN
  END
FUNCTION TSOLVE(TWN,TGAS,RAD,HTCI,SIG,EMI,ITRAD)
C-----SOLVE FOR WALL TEMPERATURES.
  ITR=MIND(ITRAD,2)
  KOUNT=0
10 TW=TWN
  KOUNT=KOUNT+1
  IF(KOUNT.GT.10)GO TO 30
  TW2=TW*TW
C-----RADIATION.
  QRH=2.0*EMI*(SIG*TW2*TW2-RAD)*FLOAT(ITR-1)
C-----CONVECTION.
  QCH=HTCI*(TW-TGAS)
  QCRH=0.0*EMI*SIG*TW*TW2*FLOAT(ITR-1)
  DOCH=HTCI
  FTW=QRH+QCH
  QFTW=QCRH+DOCH
  TWN=TW-FTW/(OFTW+1.E-30)
  IF(ABS(TWN/TW-1.).GT..001)GO TO 10
30 TSOLVE=TWN
  RETURN
  END
SUBROUTINE ABSORR(TS,T,PATH,SOOTK,PCO2,PH2O,ALPHA)

```

SUBROUTINE ABSROB COMPUTES THE ABSORPTIVITIES (WITH RESPECT TO A BLACKBODY SOURCE) OF ISOTHERMAL, HOMOGENEOUS MIXTURES OF SOOT AND H2O AT A TOTAL PRESSURE OF 1 ATMOSPHERE. ABSORPTIVITIES CALCULATED BY SUBROUTINE ABSORR ARE IN GOOD AGREEMENT WITH

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COMMENT	117
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STR	130
STR	131
STR	132
STR	133
STR	134
TSO	2
COMMENT	181
TSO	3
TSO	4
TSO	5
TSO	6
TSO	7
TSO	8
COMMENT	182
TSO	9
COMMENT	183
TSO	10
TSO	11
TSO	12
TSO	13
TSO	14
TSO	15
TSO	16
TSO	17
TSO	18
TSO	19
ABSOR	2
ABSOR	3
ABSOR	4
ABSOR	5
ABSOR	6
ABSOR	7
ABSOR	8
ABSOR	9

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EXPERIMENTAL MEASUREMENTS.

FOR A BLACKBODY SOURCE TEMPERATURE EQUAL TO THE MIXTURE
TEMPERATURE, ABSORPTIVITY EQUALS EMISSIVITY. EMISSIVITIES SO
CALCULATED ARE IN GOOD AGREEMENT WITH SPECTRAL CALCULATIONS
AND WITH EXPERIMENTAL MEASUREMENTS.

EACH CALL ON SUBROUTINE ABSORR REQUIRES LESS THAN 12 MILLISECON
OF CPU TIME ON AN IBM 370/158.

INPUTS

1. TS (IN DEGREES KELVIN) & BLACKBODY SOURCE TEMPERATURE.
TS MUST BE GREATER THAN OR EQUAL TO 300.K AND LESS THAN OR
EQUAL TO 2000.K.
2. T (IN DEGREES KELVIN) & MIXTURE TEMPERATURE. T MUST BE GREAT
THAN OR EQUAL TO 300.K AND LESS THAN OR EQUAL TO 2000.K.
3. PATH (IN METRES) & MIXTURE PATHLENGTH. PATH MUST BE
GREATER THAN OR EQUAL TO 0.0 METRES.
4. SOOTK (IN INVERSE METRES) & ABSORPTION COEFFICIENT OF SOOT
AT A WAVELENGTH OF 0.94 MICROMETRES. SOOTK IS (APPROXIMATELY)
RELATED TO THE SOOT VOLUME FRACTION, FV, BY $SOOTK = 7FV/0.94E-6$.
SOOTK MUST BE GREATER THAN OR EQUAL TO 0.0 INVERSE METRES.
5. PCO2 (IN ATMOSPHERES) & PARTIAL PRESSURE OF CO2 IN A MIXTURE
WHOSE TOTAL PRESSURE IS 1 ATMOSPHERE. PCO2 MUST BE GREATER
THAN OR EQUAL TO 0.0 ATMOSPHERES AND LESS THAN OR EQUAL TO
1.0 ATMOSPHERES. FOR PCO2 LESS THAN 0.0011 ATMOSPHERES, THE
CONTRIBUTION OF CO2 TO THE MIXTURE ABSORPTIVITY IS ASSUMED TO
BE ZERO. FOR (PATH*TS/T*PCO2) LESS THAN 0.0011 ATM-METRE, THE
CONTRIBUTION OF CO2 TO THE MIXTURE ABSORPTIVITY IS ASSUMED TO
BE ZERO. IF (PATH*TS/T*PCO2) EXCEEDS 9.98 ATM-METRE,
SUBROUTINE ABSORR ABORTS AND RETURNS A VALUE OF ABSORPTIVITY
SET AT -1.E30. A DIAGNOSTIC MESSAGE IS PROVIDED.
6. PH2O (IN ATMOSPHERES) & PARTIAL PRESSURE OF H2O IN A MIXTURE
WHOSE TOTAL PRESSURE IS 1 ATMOSPHERE. PH2O MUST BE GREATER
THAN OR EQUAL TO 0.0 ATM AND LESS THAN OR EQUAL TO (1.0-PCO2) A
FOR PH2O LESS THAN 0.0011 ATM, THE CONTRIBUTION OF H2O TO THE
MIXTURE ABSORPTIVITY IS ASSUMED TO BE ZERO. FOR (PATH*TS/T*PH2O)
LESS THAN 0.0011 ATM-METRE, THE CONTRIBUTION OF H2O TO THE
MIXTURE ABSORPTIVITY IS ASSUMED TO BE ZERO. IF (PATH*TS/T*PH2O)
EXCEEDS 9.98 ATM-METRE, SUBROUTINE ABSORR ABORTS AND RETURNS A
VALUE OF ABSORPTIVITY SET AT -1.E30. A DIAGNOSTIC MESSAGE
IS PROVIDED.

OUTPUTS

ABSOR	10
ABSOR	11
ABSOR	12
ABSOR	13
ABSOR	14
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ABSOR	73

SUBROUTINE ABSORP RETURNS ALPHA THE (DIMENSIONLESS)
ABSORPTIVITY OF A MIXTURE OF SOOT, CO₂ AND H₂O AT A TOTAL
PRESSURE OF 1 ATMOSPHERE.

THE FOLLOWING SUBROUTINES MUST BE USED WITH

1. ACSOPE
2. CHEBY
3. DLECK
4. FGAS
5. PENTA
6. SDOY
7. SCRTCH

QUESTIONS ABOUT SUBROUTINE ABSORP MAY BE ADDRESSED TO:
ASHOK T. MODAK
NORTHERN RESEARCH AND ENGINEERING CORPORATION
WOBURN, MASS. 01801
USA
TEL. NO. (617) 935-9050 EXT 264.

```
IF(TS.LT.300. .OR. TS.GT.2000.)GOTO 1
IF(T .LT.300. .OR. T .GT.2000.)GOTO 2
PSUM=PCO2+PH2O
IF(PSUM.GT.1.0) GOTO 3
COMPUTE RATIO OF MIXTURE AND SOURCE TEMPERATURES.
RATIO=T/TS
COMPUTE EFFECTIVE PATHLENGTH,PATHL
PATHL=PATH/RATIO
PCL=PCO2*PATHL
PWL=PH2O*PATHL
IF(PCL.GT.5.98 .OR. PWL.GT.5.98) GOTO 4
COMPUTE SOOT ABSORPTIVITY,AS
AS=0.0
IF(SOOTK.LE.0.0) GOTO 51
CALL SDOY(SOOTK,PATH,TS,TAUS)
AS=1.-TAUS
```

```
51 CONTINUE
COMPUTE GAS ABSORPTIVITY,AG
```

```
AG=0.0
IF(PCO2.LT.0.0011 .AND. PH2O.LT.0.0011)GOTO 52
IF(PCL .LT.0.0011 .AND. PWL .LT.0.0011)GOTO 52
AG=FGAS(PATHL,PCO2,PH2O,TS)
COMPUTE WATER VAPOR FRACTION,ZETA
ZETA=PH2O/PSUM
POWER=0.65-0.2*ZETA
AG=AG*RATIO**POWER
```

```
52 CONTINUE
ALPHA=AS+AG-AS*AG
RETURN
```

```
4 CONTINUE
WRITE(6,*)
FORMAT(* EITHER THE PRODUCT,PATH,TS/T,PCO2,OR PATH,TS/T,PH2O EXCEE
105 5.98 ATM-PETRES*)
WRITE(6,*)
```

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ABSOR	137

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6	FORMAT(* THIS CALCULATION LIES OUTSIDE THE RANGE OF SUBROUTINE ABS	ABSOR	138
10	PR, SUBROUTINE ABSORR ABOATS AND RETURNS A VALUE OF*)	ABSOR	139
	WRITE(6,7)	ABSOR	140
7	FORMAT(* ALPHA SET EQUAL TO -1.E30*)	ABSOR	141
	GOTO 8	ABSOR	142
3	CONTINUE	ABSOR	143
	WRITE(6,9)	ABSOR	144
9	FORMAT(* SUM OF GAS PARTIAL PRESSURES, PCO2+PH2O, EXCEEDS 1 ATM*)	ABSOR	145
	WRITE(6,6)	ABSOR	146
	WRITE(6,7)	ABSOR	147
	GOTO 8	ABSOR	148
2	CONTINUE	ABSOR	149
	WRITE(6,11)	ABSOR	150
11	FORMAT(* MIXTURE TEMPERATURE ,T, LIES OUTSIDE THE TEMPERATURE RANG	ABSOR	151
	IF 300 TO 2000 DEGREES KELVIN*)	ABSOR	152
	WRITE(6,6)	ABSOR	153
	WRITE(6,7)	ABSOR	154
	GOTO 8	ABSOR	155
1	CONTINUE	ABSOR	156
	WRITE(6,10)	ABSOR	157
10	FORMAT(* BLACKBODY SOURCE TEMPERATURE, TS, LIES OUTSIDE THE TEMPERAT	ABSOR	158
	URE RANGE 300 TO 2000 DEGREES KELVIN*)	ABSOR	159
	WRITE(6,6)	ABSOR	160
	WRITE(6,7)	ABSOR	161
9	CONTINUE	ABSOR	162
	ALPHA=-1.E30	ABSOR	163
	RETURN	ABSOR	164
	END	ABSOR	165
	SUBROUTINE ASYMP(Z,ZV)	ABSOR	166
C	SURROUTINE ASYMP COMPUTES THE ASYMPTOTIC EXPANSION FOR THE	ABSOR	167
C	PENTAGAMMA FUNCTION.	ABSOR	168
C		ABSOR	169
	ZI1=1.77	ABSOR	170
	ZI2=ZI1*ZI1	ABSOR	171
	ZI3=ZI1*ZI2	ABSOR	172
	ZV=ZI3*((2.+9.*ZI1)+ZI2*(2.+ZI2*(-1.+ZI2*(1.3333333333	ABSOR	173
	1 +ZI2*(-3.+10.*ZI2))))	ABSOR	174
	RETURN	ABSOR	175
	END	ABSOR	176
	SUBROUTINE CHERY(N,X,V)	ABSOR	177
C	V REPRESENTS VALUE OF CHEBYSHEV POLYNOMIAL OF ORDER N	ABSOR	178
C	AND ARGUMENT X.	ABSOR	179
	V=1.	ABSOR	180
	IF(N) 1,1,2	ABSOR	181
1	RETURN	ABSOR	182
C		ABSOR	183
	2 V=X	ABSOR	184
	IF(N=1) 1,1,3	ABSOR	185
3	F=N+X	ABSOR	186
	VM1=X	ABSOR	187
	VM2=1.	ABSOR	188
	DO 4 I=2,N	ABSOR	189
	V=F+VM1-VM2	ABSOR	190
	VM2=VM1	ABSOR	191
	VM1=V	ABSOR	192
4	CONTINUE	ABSOR	193
	RETURN	ABSOR	194
	END	ABSOR	195
	FUNCTION OLECK(X,PL,T)	ABSOR	196
C	SUBROUTINE OLECK COMPUTES THE 2.7 AND 19 MICROMETRE OVERLAP	ABSOR	197
C	CORRECTION FOR MIXTURES OF CO2 AND H2O. THE OVERLAP CORRECTION	ABSOR	198
C	IS COMPUTED BY USING A TEMPERATURE-ADJUSTED VERSION OF THE	ABSOR	199
C	OVERLAP CORRECTION FACTOR SUGGESTED BY B. LECKNEY	ABSOR	200
C	(COMBUSTION AND FLAME VOLUME 19 PAGES 33-46, 1972)	ABSOR	201

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```

IF(PL.LT.0.1) GOTO 1
TERM=X/(10.7+101.0X) -X**10.4/111.7
TERM2=ALOG10(101.325*PL)
TERM2=TERM2**2.76
TT=T/1000.
TT2=TT*TT
A=-1.020408Z
R=2.244R979
C=-0.23449306
TERM3=A*TT2+ B*TT + C
C
  TERM3 REPRESENTS THE TEMPERATURE ADJUSTMENT
DLECK=TERM +TERM2*TERM3
RETURN
1 DLECK=0.0
RETURN
END
C
  FUNCTION EGAS(PATHL,PC,PW,T)
  FUNCTION EGAS COMPUTES THE EMISSIVITY OF A GIVEN PATH (PATHL)
  OF A MIXTURE OF CO2 AND H2O AT TEMPERATURE T.
  PC = PARTIAL PRESSURE OF CO2
  PW = PARTIAL PRESSURE OF H2O
  EGAS=0.0
  IF(T.LT.300. .OR. T.GT.2000.) RETURN
  FC=0.0
  IF(PC.LT.0.0011 .OR. PC.GT.1.0) GOTO 1
  PCL=PC*PATHL
  IF(PCL.LT.0.0011 .OR. PCL.GT.5.98) GOTO 1
  CALL SCRTCH(PC,PCL,T,1,EC)
1 CONTINUE
  IF(PW.LT.0.0011 .OR. PW.GT.1.0) GOTO 2
  PWL=PW*PATHL
  IF(PWL.LT.0.0011 .OR. PWL.GT.5.98) GOTO 2
  CALL SCRTCH(PW,PWL,T,2,EW)
  EGAS=FC+FW
  IF(EC.LE.0.0) RETURN
  PCPW=PC*PW
  XI=PW/PCPW
  IF(XI.LT.0.01) RETURN
  PCWL=PCPW*PATHL
  IF(PCWL.LT.0.1 ) RETURN
  DELE=DLECK(XI,PCWL,T)
  EGAS=EGAS-DELE
  RETURN
2 CONTINUE
  EGAS=FC
  RETURN
END
C
  SUBROUTINE PENTA(X,V)
  SUBROUTINE PENTA RETURNS THE VALUE V OF THE PENTAGAMMA FUNCTION
  OF ARGUMENT X. RECURRENCE FORMULA 6.4.6, AND ASYMPTOTIC FORMUL
  6.4.14 (PAGE 260) OF ABRAHAWITZ AND STEGUN ARE USED IN
  THIS CALCULATION.
  C
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  C
  IF(X.GE.4.) GOTO 1
  IF(X.GE.3.) GOTO 2
  IF(X.GE.2.) GOTO 3
  S=(1./((X+2.)**4+1./((X+1.)**4+1./X**4)*6.
  Z=X+3.
  CALL ASYMP(Z,ZV)
  GOTO 4
  3 CONTINUE
  S=(1./((X+1.)**4+1./X**4)*6.

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Z=X+2.
CALL ASYMP(Z,ZV)
GOTO 4
2 CONTINUE
S=6./X**4
Z=X+1.
CALL ASYMP(Z,ZV)
GOTO 4
1 CONTINUE
S=0.0
CALL ASYMP(X,ZV)
4 CONTINUE
V=ZV+S
RETURN
END
SUBROUTINE SNOT(ZKLED,PATHL,TBLACK,TAUS)
  SUBROUTINE SNOT COMPUTES THE TRANSMISSIVITY (TAUS) OF PATH (PAT
  OF SNOT TO A BLACKBODY RADIATION SOURCE AT A GIVEN
  TEMPERATURE (TBLACK).
  IF(ZKLED.LE. 0.) GOTO 1
  ARG=1.+ZKLED*PATHL*TBLACK*6.5337E-9
  TBLACK - SOURCE TEMPERATURE OR GAS TEMPERATURE
  CALL PENTA(ARG,V)
  SUBROUTINE PENTA COMPUTES THE PENTAGAMMA FUNCTION
  ARG - ARGUMENT OF THE PENTAGAMMA FUNCTION
  TAUS=V*.1539097336
  TAUS - SNOT TRANSMISSIVITY
  RETURN
1 TAUS=1.
  RETURN
END
SUBROUTINE SCRTCH(P,PL,T,INDEX,V)
  DIMENSION CC(3,4,4),CW(3,4,4),          SC(3,4,4)
  IF(INDEX.EQ.2) GOTO 2
  CC REPRESENTS AN ARRAY OF 48 COEFFICIENTS FOR CO2
  CC(1,1,1)=-0.2754568E+01
  CC(1,1,2)=-0.2997857E+00
  CC(1,1,3)=-0.1232494E+00
  CC(1,1,4)=0.1279287E-01
  CC(1,2,1)=0.1503051E+01
  CC(1,2,2)=0.3156449E+00
  CC(1,2,3)=0.1058126E-01
  CC(1,2,4)=-0.3729625E-01
  CC(1,3,1)=-0.2474119E+00
  CC(1,3,2)=-0.3323846E-01
  CC(1,3,3)=-0.1819471E-01
  CC(1,3,4)=0.2289789E-01
  CC(1,4,1)=0.4994029E-01
  CC(1,4,2)=-0.1986786E-02
  CC(1,4,3)=0.3007898E-02
  CC(1,4,4)=-0.1175598E-02
  CC(2,1,1)=0.5737722E-02
  CC(2,1,2)=-0.9328458E-02
  CC(2,1,3)=0.2906266E-02
  CC(2,1,4)=0.4227520E-03
  CC(2,2,1)=-0.3151784E-02
  CC(2,2,2)=0.5632821E-02
  CC(2,2,3)=-0.3260295E-02
  CC(2,2,4)=0.7065884E-03
  CC(2,3,1)=0.1668751E-03

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CC(2,3,2)=-0.7326533E-03
CC(2,3,3)=-0.3639855E-03
CC(2,3,4)=-0.3226318E-03
CC(2,4,1)=-0.7306638E-03
CC(2,4,2)=-0.7277073E-03
CC(2,4,3)=-0.5925968E-03
CC(2,4,4)=-0.2021413E-03
CC(3,1,1)=-0.3305611E-02
CC(3,1,2)=-0.5439189E-02
CC(3,1,3)=-0.1764560E-02
CC(3,1,4)=-0.3035031E-03
CC(3,2,1)=-0.1862700E-02
CC(3,2,2)=-0.3236275E-02
CC(3,2,3)=-0.1952250E-02
CC(3,2,4)=-0.3474022E-03
CC(3,3,1)=-0.1204807E-03
CC(3,3,2)=-0.4479927E-03
CC(3,3,3)=-0.2497521E-03
CC(3,3,4)=-0.1812996E-03
CC(3,4,1)=-0.4218169E-03
CC(3,4,2)=-0.4046608E-03
CC(3,4,3)=-0.3256061E-03
CC(3,4,4)=-0.9514981E-04
GOTO4

2 CONTINUE

CW REPRESENTS AN ARRAY OF 48 COEFFICIENTS FOR H2O

CW(1,1,1)=-0.2594279E+01
CW(1,1,2)=-0.7118472E+00
CW(1,1,3)=-0.4956839E-03
CW(1,1,4)=-0.1226960E-01
CW(1,2,1)=-0.2510331E+01
CW(1,2,2)=-0.6481808E+00
CW(1,2,3)=-0.3330597E-01
CW(1,2,4)=-0.5524345E-02
CW(1,3,1)=-0.4191636E+00
CW(1,3,2)=-0.1379180E+00
CW(1,3,3)=-0.3877930E-01
CW(1,3,4)=-0.8862328E-03
CW(1,4,1)=-0.3223912E-01
CW(1,4,2)=-0.1820241E-01
CW(1,4,3)=-0.2223143E-01
CW(1,4,4)=-0.5940781E-03
CW(2,1,1)=-0.1126569E+00
CW(2,1,2)=-0.8133829E-01
CW(2,1,3)=-0.1514940E-01
CW(2,1,4)=-0.1393880E-02
CW(2,2,1)=-0.4298805E-02
CW(2,2,2)=-0.4550660E-01
CW(2,2,3)=-0.2082009E-01
CW(2,2,4)=-0.2013961E-02
CW(2,3,1)=-0.4375032E-01
CW(2,3,2)=-0.1924197E-01
CW(2,3,3)=-0.8859877E-02
CW(2,3,4)=-0.4618414E-02
CW(2,4,1)=-0.7077876E-02
CW(2,4,2)=-0.2096188E-01
CW(2,4,3)=-0.1458262E-02
CW(2,4,4)=-0.3851421E-02
CW(3,1,1)=-0.5341517E-01
CW(3,1,2)=-0.3407693E-01
CW(3,1,3)=-0.4374611E-02
CW(3,1,4)=-0.1492038E-02

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CW(3,2,1)=-0.4708178E-02
CW(3,2,2)=-0.2086888E-01
CW(3,2,3)=-0.9477533E-02
CW(3,2,4)=-0.6153272E-03
CW(3,3,1)=-0.2104622E-01
CW(3,3,2)=-0.7915796E-02
CW(3,3,3)=-0.5965509E-02
CW(3,3,4)=-0.2756144E-02
CW(3,4,1)=-0.4318975E-02
CW(3,4,2)=-0.1005744E-01
CW(3,4,3)=-0.4091084E-03
CW(3,4,4)=-0.2950495E-02
4 CONTINUE
X=ALOG(P)/3.45+1.0
Y=(ALOG(PL)+2.555)/4.345
Z=(T-1150.)/850.
V=0.0
DO 5 II=1,3
I=II-1
CALL CHEBY(I,X,TIX)
V6=0.0
DO 6 JJ=1,4
J=JJ-1
CALL CHEBY(J,V,TJY)
V7=0.0
DO 7 KK=1,4
K=KK-1
CALL CHEBY(K,Z,TKZ)
IF(INDEX.EQ.1)SC(II,JJ,KK)=CC(II,JJ,KK)
IF(INDEX.EQ.2)SC(II,JJ,KK)=CW(II,JJ,KK)
V7=V7+TKZ*SC(II,JJ,KK)
7 CONTINUE
V6=V6+V7*TJY
6 CONTINUE
V=V+V6*TIX
5 CONTINUE
V=EXP(V)
RETURN
END
SUBROUTINE SOLVE
COMMON/CCEFF/AP(40),BP(40),EP(30),DP(30),APP(30),RPP(30)
COMMON F(3500),DH(500),DV(500),DW(500),
1 ANUC(500),SNOT1(500),SNOT2(500),FCH(500),FH2(500),FS(500,14),
1 RHO(500),VISC(500),ABSR(500),SCTR(500),SU(100),SP(100),
1 ORHOND(500),
1 AXP(100),AXM(100),AYP(100),AYM(100),AZP(100),
2 AZM(100),CZ(100),CY(10),CZU(100),CYU(10),
3 CZP(100),CYP(10),DIV6(100),NTP1,NTP2
1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
DIMENSION GAM(500)
EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
EQUIVALENCE (F(3001),GAM(1))
COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSV(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXM(40),
2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME
COMMON
1/CINDEX/INCC,IOFU,IOOZ,IONZ,IONZQ,IOCOZ,IONH,IONH2,IONH,IONQ,IONQZ
1,ION,IONH,IMCPS,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NGLOR,NGLORP,
2 NLM,NQ,NSP,NS1,NS2,IOCH
3/CHEM/I/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG

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CTOMA 3
CTOMA 4
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CONF 11
COMMON 2
COMMON 3
COMMON 4
COMMON 5
NOX 2
NOX 3
NOX 4
4STEP 3
NOX 6

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4/CPARAM/ASUB(30,3),ENV,ER,HSUBO,NDEBUB,NS,PA,OO,Q1,Q2,Q3,Q4,RHOPP,	NOX	7
4 SM,SMW(30),SMO,S1(30),S2(30),TK,LADIAE,LDEBUB,LEQUIL,LREACT,	NOX	8
4 LENER,EOKIJ,LCONVG	NOX	9
DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUBO,HSUM,PA,PPLN,OO,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO	NOX	11
2,FUT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,	4STEP	5
1 CEBU3,CFRU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADIAE,LCONVG,LDEBUB,LEQUIL,LNRG,LREACT,LENER	NOX	12
COMMON/INT/L,P,N,LCV,NCV,NCV,LP1,MP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,	COMMON	6
1 NNW,NGOTO,K,ISTR,JSTR,KSTR,NVN(35),KN(30),JN(30),ISTEP,	4STEP	8
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,	4STEP	9
3 NRHO,NGAN,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWEI,	COMMON	9
4 IWEI,MM1,JWII,JWIO,JWOT,JWOO,IOW,JKIN(30,30),IKIN(40,30)	COMMON	10
COMMON/INDEX/IPAR,LREF,ISTUN,INCONP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1,PLAXM1,LVK,LVO,LVFOX,LVFU,LVCO,LVH,LVRX,LVRZ,NVF(32),	4STEP	10
2 IJUMP,IRES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH20,NVCO2,	COMMON	13
3 NVN2,NVCH,NVH2	4STEP	11
COMMON/CNOX/LVH1,LVH2,LVN1,LVN0,LVN02,LVO,LVOH,LVH20,LVN2,LV02,	NOX	16
1 LVCO2,LVFU1,LVCO1,NNOX,INOX,ITNOX,SNOK,TNOX	NOX	17
COMMON/THERP/NVH,NVFU,NVQX,NVFOX,NVTE,MODEN,IDX,FSTOIC,MFU,CP,	COMMON	15
1 GASCON,RHOCN,UNICON,PRESS,NVFAV,TCYLW,TINLW,TLIP,ACOE(4),	COMMON	16
2 T4,DFAC,MFU,WCO2,WCO,MQX,WM20,WM2,HVY,CXX,RATIO1-RATIO2,	COMMON	17
3 RATIO3,RATIO4,MCO,TAN,ITWALL	COMMON	18
COMMON/CTOMA/KEND,ICTOMA(32)	4STEP	12
C-----ROUTINE SOLVE IS USED TO SOLVE THE FINITE-DIFFERENCE	COMMENT	184
C EQUATIONS BY THE TRI-DIAGONAL-MATRIX-ALGORITHM(TOMA).	COMMENT	185
C	COMMENT	186
ENTRY SOLVE1	SO	7
RELAXM=1.-RELAX(NV)	SO	8
DO 10 J=JSTR,M	SO	9
KJM=KN(K)+JM(J)	SO	10
IS=IWLI(J,NGOTO)	SO	11
IF=IWLO(J,NGOTO)	SO	12
DO 10 I=IS,IE	SO	13
LIJ=JM(J)+I	SO	14
LP=KJM+I	SO	15
LPE=LP+NVH(NVF(NV))	SO	16
L7P=LPE+MINJ	SO	17
L7M=LPE-MINJ	SO	18
FL7P=F(L7P)	SO	19
IF (NV.EQ.3.AND.K.EQ.NP1) FL7P=W(LIJ+2*NINJ)	SO	20
15 CONTINUE	SO	21
SP(LIJ)=(AXM(LIJ)+AXP(LIJ)+AYM(LIJ)+AYP(LIJ)+AZM(LIJ)+AZP(LIJ)-	SO	22
1SP(LIJ))/RELAX(NV)	SO	23
C-----STORE COEFFICIENTS FOR CYCLIC TOMA.	COMMENT	187
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)	CTOMA	5
AYMK(LPC)=AXP(LIJ)	CTOMA	6
AXPK(LPC)=AXP(LIJ)	CTOMA	7
AYMK(LPC)=AYM(LIJ)	CTOMA	8
AYPK(LPC)=AYP(LIJ)	CTOMA	9
A7MK(LPC)=A7M(LIJ)	CTOMA	10
A7PK(LPC)=A7P(LIJ)	CTOMA	11
SUM(LPC)=SU(LIJ)+SP(LIJ)*RELAXM+F(LPF)	CTOMA	12
SPK(LPC)=SP(LIJ)+1.0E-30	CTOMA	13
SU(LIJ)=SU(LIJ)+SP(LIJ)*RELAXM+F(LPF)+AZM(LIJ)*F(L7M)+AZP(LIJ)*	SO	24
1 FL7P	SO	25
GO TO (11,12,13,10),NGOTO	SO	26
11 DU(LP)=DU(LP)/SP(LIJ)	SO	27
GO TO 10	SO	28
12 DV(LP)=DV(LP)/SP(LIJ)	SO	29
GO TO 10	SO	30
13 DW(LP)=DW(LP)/SP(LIJ)	SO	31

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10	CONTINUE	SO	32
	NVKN=KN(K)+NVF(NVF(NV))	SO	33
	ISUM=ISTP+L	SO	34
	JSUM=JSTR+N	SO	35
	INOMAX=ICTDMA(NV)	SO	36
	DO 45 INO=1,INOMAX	SO	37
	GO TO (20,30),INX	SO	38
20	CONTINUE	SO	39
C----	TDMA TRAVERSE IN X-DIRECTION.	COMMENT	100
	DO 21 JJ=JSTR,M	SO	40
	GO TO (24,29),JSWP	SO	41
24	J=JJ	SO	42
	GO TO 26	SO	43
25	J=JSUM-JJ	SO	44
26	CONTINUE	SO	45
	LPF=NVKN+JM(J)	SO	46
	IS=IWL(I,J,NGOTO)	SO	47
	IF=IWL(I,J,NGOTO)	SO	48
	ISTR1=IS-1	SO	49
	LPF1=LPF+ISTR1	SO	50
	AP(ISTR1)=0.	SO	51
	AP(ISTR1)=F(LPF1)	SO	52
	DO 22 I=IS,IF	SO	53
	LIJ=JM(J)+I	SO	54
	LYP=LPF+NI+I	SO	55
	LYN=LPF-NI+I	SO	56
	STORE=SP(LIJ)-AXN(LIJ)+AP(I-1)+1.E-30	SO	57
	AP(I)=AXP(LIJ)/STORE	SO	58
22	AP(I)=(SU(LIJ)+AYP(LIJ)+F(LYP)+AYN(LIJ)+F(LYN)+AXM(LIJ)+BP(I-1))/	SO	59
	1STORE	SO	60
	ISUM1=IS+IF	SO	61
	DO 23 II=IS,IF	SO	62
	I=ISUM1-II	SO	63
	LP=LPF+I	SO	64
23	F(LP)=AP(I)+F(LP+1)+BP(I)	SO	65
21	CONTINUE	SO	66
	JSWP=3-JSWP	SO	67
	GO TO (28,20),JSWP	SO	68
28	CONTINUE	SO	69
	GO TO (30,40),INX	SO	70
C----	TDMA TRAVERSE IN Y-DIRECTION.	COMMENT	189
30	DO 31 II=ISTR,L	SO	71
	GO TO (34,39),ISWP	SO	72
34	I=II	SO	73
	GO TO 36	SO	74
35	I=ISUM-II	SO	75
36	CONTINUE	SO	76
	LPF=NVKN+I	SO	77
	JS=JWL(I,I,NGOTO)+1	SO	78
	JE=JWL(I,I,NGOTO)-1	SO	79
	JSTR1=JS-1	SO	80
	LPF1=LPF+JM(JSTR1)	SO	81
	AP(JSTR1)=0.	SO	82
	AP(JSTR1)=F(LPF1)	SO	83
	DO 32 J=JS,JE	SO	84
	LIJ=JM(J)+I	SO	85
	LXP=NVKN+LIJ+1	SO	86
	LXM=LXP-2	SO	87
	STORE=SP(LIJ)-AYN(LIJ)+AP(J-1)+1.E-30	SO	88
	AP(J)=AYP(LIJ)/STORE	SO	89
32	AP(J)=(SU(LIJ)+AXP(LIJ)+F(LXP)+AXM(LIJ)+F(LXM)+AYN(LIJ)+BP(J-1))/	SO	90
	1STORE	SO	91
	JSUM1=JS+JE	SO	92
	DO 33 JJ=JS,JE	SO	93

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	J=JSUM1-JJ	SO	94
	LP=LRF+JM(J)	SO	95
	LVP=L+NI	SO	96
33	F(LP)=AP(J)*F(LVP)+BP(J)	SO	97
31	CONTINUE	SO	98
	ISWP=3-ISWP	SO	99
	GO TO (3P,3Q),ISWP	SO	100
38	CONTINUE	SO	101
	GO TO (40,20),IXY	SO	102
40	CONTINUE	SO	103
45	CONTINUE	SO	104
	RETURN	SO	105
C	** ** *	SO	106
	ENTRY SOLVE2	SO	107
C	-----CYCLIC TQMA IN Z-DIRECTION.	COMMENT	190
	KEND=N	CTQMA	14
	IF(NV.EQ.3)KEND=NP1	CTQMA	15
	IF(1CTQMA(NV).EQ.0)GO TO 606	CTQMA	16
	INOMAX=1CTQMA(NV)	CTQMA	17
	DO 605 INO=1,INOMAX	CTQMA	18
	DO 600 J=JSTR,M	CTQMA	19
	IS=IWL1(J,NGOTO)	FEB2	4
	IE=IWL0(J,NGOTO)	FEB2	5
	DO 600 I=IS,IE	FEB2	6
	LIJ=I+JM(J)	CTQMA	21
	LIJNV=LIJ+NVN(NVF(NV))	CTQMA	22
	LPSTR=LIJNV+KM(KSTR)	CTQMA	23
	LPCSTR=I-1+(J-2)*(NI-2)	CTQMA	24
	AP(KSTR)=A7PK(LPCSTR)	CTQMA	25
	BP(KSTR)=A7MK(LPCSTR)	CTQMA	26
	FP(KSTR)=SUM(LPCSTR)+AXMK(LPCSTR)*F(LPSTR-1)+AXPK(LPCSTR)*F(LPSTR+	CTQMA	27
	21)+AYMK(LPCSTR)*F(LPSTR-NI)+AYPK(LPCSTR)*F(LPSTR+NI)	CTQMA	28
	DP(KSTR)=SPK(LPCSTR)	CTQMA	29
	IF(DP(KSTR).LT.1.E-30)DP(KSTR)=1.E30	CTQMA	30
	KMIN=KSTR+1	CTQMA	31
	DO 603 K=KMIN,KEND	CTQMA	32
	LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)+(NJ-2)	CTQMA	33
	LP=LIJNV+KM(K)	CTQMA	34
	AP(K)=A7PK(LPC)	CTQMA	35
	BK=A7MK(LPC)	CTQMA	36
	CK=SUM(LPC)+AXMK(LPC)*F(LP-1)+AXPK(LPC)*F(LP+1)+AYMK(LPC)*F(LP-NI)	CTQMA	37
	2 +AYPK(LPC)*F(LP+NI)	CTQMA	38
	DK=SPK(LPC)	CTQMA	39
	AP(K)=AK+BP(K-1)/DP(K-1)	CTQMA	40
	EP(K)=EP(K-1)+BK/DP(K-1)+CK	CTQMA	41
	OP(K)=DK-BK+AP(K-1)/DP(K-1)	CTQMA	42
	IF(OP(K).LT.1.E-30)OP(K)=1.E30	CTQMA	43
601	CONTINUE	CTQMA	44
	KSUM=KEND-2+KSTR	CTQMA	45
	APP(KEND-1)=(AP(KEND-1)+BP(KEND-1))/DP(KEND-1)	CTQMA	46
	APP(KEND-1)=EP(KEND-1)/DP(KEND-1)	CTQMA	47
	KENDM2=KEND-2	CTQMA	48
	DO 602 KK=KSTR,KENDM2	CTQMA	49
	K=KSUM-KK	CTQMA	50
	APP(K)=(AP(K)+APP(K+1)+BP(K))/(DP(K)+1.0E-30)	CTQMA	51
	BPP(K)=(AP(K)+BPP(K+1)+EP(K))/(DP(K)+1.0E-30)	CTQMA	52
602	CONTINUE	CTQMA	53
	OENOM=DP(KEND)-BP(KEND)-APP(KSTR)+AP(KEND)	CTQMA	54
	IF(ABS(OENOM).LT.1.E-30)OENOM=1.E30	CTQMA	55
	FEND=(BPP(KSTR)+AP(KEND)+EP(KEND))/OENOM	CTQMA	56
	KENDM1=KEND-1	CTQMA	57
	DO 603 K=KSTR,KENDM1	CTQMA	58
	LP=LIJNV+KM(K)	CTQMA	59
	F(LP)=APP(K)+FEND+BP(K)	CTQMA	60

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603 CONTINUE
  LPCE=LIJNV+KMKEND)
  F(LPCE)=FEND
604 CONTINUE
605 CONTINUE
606 CONTINUE
  RETURN
  FND
  SUBROUTINE FPRINT (ISTRT,ISTOP,NVVV)
  COMMON F(3500),DU(500),DV(500),DW(500),
  1 ANUC(500),SNOT1(500),SNOT2(500),FCH(500),FH2(500),FS(500,14),
  1 RHO(500),VISC(500),ANSR(500),SCTR(500),SU(100),SP(100),
  1 NRHOP(500),
  1 AXP(100),AXN(100),AP(100),AYN(100),AZP(100),
  2 AZM(100),CZ(100),CY(10),CZU(100),CYU(10),
  3 CZP(100),CYP(10),DIVG(100),NTP1,NTP2
  1,AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
  2 SUK(192),SPK(192)
  DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
  DIMENSION GAM(500)
  EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
  EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
  EQUIVALENCE (F(3001),GAM(1))
  COMMON/CRYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAX
  COMMON/GRIN/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
  1 YSV(30),ZSW(30),XOIF(40),YOIF(30),ZOIF(30),FXP(40),FXM(40),
  2 FYP(30),FYM(30),FZP(30),FZM(30),DT,TIME
  COMMON
  1/CTNOFX/IDCO,IDFU,IDO2,ION2,IOH2O,IOCO2,IDH1,IOH2,IDN1,IONO,IONO2
  1,ION,IONH,IHCP5,ILC,ILM,IMAT,ITER,JJJ,N1,N2,N3,NA,NGL08,NGL08P,
  2 NLM,NQ,NSM,NS1,NS2,IOCH
  3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
  4/CPARAM/ASUB(30,3),ENV,ER,HSUBO,NOEBUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOPP,
  4 SM,SMW(30),SMO,S1(30),S2(30),TK,LADTAB,LDEBUG,LEQUIL,LREACT,
  4 LENER,EDKIJ,LCONVG
  DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUBO,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,
  1 Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO
  2,FUT,FST
  COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,
  1 CEBU3,CBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
  2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST
  LOGICAL LADTAB,LCONVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER
  COMMON/INT/L,M,N,LCV,MCV,NCV,LP1,MP1,NP1,NT,NJ,NK,NINJ,NINJK,NV,
  1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KN(30),JM(30),ISTEP,
  2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,
  3 NRHO,NCAP,IWLI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWET,
  4 IWEN,PMI,JWII,JWIO,JWNI,JWNO,ION,JKIN(30,30),IKIN(40,30)
  COMMON/INDEX/IPAP,LPREF,ISTUN,INCNP,ITRAD,NVRX,NVRY,NVRZ,JPLANE
  1,PLAXM1,LVH,LVO,LVFUOX,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),
  2 IJUMP,IWFS,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNCO,NVH2O,NVCO2,
  3 NVN2,NVCH,NVH2
  COMMON/CHDX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVON,LVH2O,LVN2,LVNO2,
  1 LVC02,LVFU1,LVCO1,MNOX,INOX,ITNOX,SMOX,TNOX
  COMMON/TEMP/NVH,NVFU,NVOX,NVFUOX,NVTE,MODEN,IOK,FSTOIC,MFU,CP,
  1 GASCON,RHOCEN,UNICON,PRESS,NVFAV,TCYLV,TINLM,TLIP,ACDEF(4),
  2 T4,DFAC,MFU,WCO2,WCO,WOK,WM2O,WM2,NVY,CXX,RATIO1,RATIO2,
  3 RATIO3,RATIO4,HCO,TAM,ITWALL
  COMMON/CTOPA/KEND,ICTOMA(92)
C-----SUBROUTINE FPRINT IS USED TO PRINT THE FIELD VALUES OF
C ALL THE DEPENDENT VARIABLES.
C
  NVV=NVVV-1
  ON 108 NV=ISTRT,ISTOP
  NVV=NVVV+1

```

```

CTOMA 61
CTOMA 62
CTOMA 63
CTOMA 64
CTOMA 65
CTOMA 66
SO 108
SO 109
FP 2
CONF8 2
4STEP 10
RAD 3
RAD 4
CONF8 4
CONF8 5
CONF8 6
CTOMA 3
CTOMA 4
CONF8 7
CONF8 8
CONF8 9
CONF8 10
CONF8 11
COMMON 2
COMMON 3
COMMON 4
COMMON 5
NOX 2
NOX 3
NOX 4
4STEP 3
NOX 6
NOX 7
NOX 8
NOX 9
NOX 10
NOX 11
4STEP 4
4STEP 5
4STEP 6
4STEP 7
NOX 12
COMMON 6
4STEP 8
4STEP 9
COMMON 9
COMMON 10
COMMON 11
4STEP 10
COMMON 13
4STEP 11
NOX 16
NOX 17
COMMON 19
COMMON 16
COMMON 17
COMMON 18
4STEP 12
COMMENT 191
COMMENT 192
COMMENT 193
FP 7
FP 8
FP 9

```

```

      IF (7*PRINT(NVV),EQ,0) GO TO 108
      WRITE (6,101) (TITLE(I,NVV),I=1,10)
101  FORMAT (1H0,20(2H+),10A4,3X,20(2H+))
      KONE=1
      IF (NVV,EQ,3) KONE=2
      NSKIP=1*PRINT(NVV)
      DO 100 K=KONE,NP1,NSKIP
      WRITE(6,102) K
102  FORMAT(1H0,50X,4HK = ,I2)
      NVKM=NUM(NV)+KM(K)
      JONE=1
      IF (NVV,EQ,2) JONE=2
      IONE=1
      IF (NVV,EQ,1) IONE=2
      ISTART=IONE-12
105  CONTINUE
      ISTART=ISTART+12
      IEND=ISTART+11
      IEND=MIND(IEND,LP1)
      WRITE(6,103) (I,I=ISTART,IEND)
103  FORMAT(1H0,6H I = ,I3,11I10)
      WRITE(6,104)
104  FORMAT(2H J)
      JSUM=JONE+NP1
      DO 106 JJ=JONE,NP1
      J=JSUM-JJ
      LPF=NVKM+JM(J)
      LPL=LPF+IEND
      LPE=LPF+ISTART
106  WRITE(6,107) J,(F(LP),LP=LPF,LPL)
107  FORMAT(I3,1P12F10,2)
      IF(IEND,LT,LPL) GO TO 105
108  CONTINUE
      RETURN
      END
      SUBROUTINE CREK

```

```

      FP      10
      FP      11
      FP      12
      FP      13
      FP      14
      FP      15
      FP      16
      FP      17
      FP      18
      FP      19
      FP      20
      FP      21
      FP      22
      FP      23
      FP      24
      FP      25
      FP      26
      FP      27
      FP      28
      FP      29
      FP      30
      FP      31
      FP      32
      FP      33
      FP      34
      FP      35
      FP      36
      FP      37
      FP      38
      FP      39
      FP      40
      FP      41
      FP      42
      FP      43
      FP      44
      FP      45
      NOXXX   1
      CREK    3
      CREK    4
      CREK    5
      CREK    6
      CREK    7
      CREK    8
      CREK    9
      CREK   10
      CREK   11
      CREK   12
      CREK   13
      CREK   14
      CREK   15
      CREK   16
      CREK   17
      CREK   18
      CREK   19
      CREK   20
      CREK   21
      CREK   22
      CREK   23
      CREK   24
      CREK   25
      CREK   26
      CREK   27
      CREK   28
      CREK   29

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```

C
C
C  A COMPUTER PROGRAM FOR CALCULATION OF
C  CHEMICAL REACTION EQUILIBRIUM AND KINETICS
C  IN LAMINAR OR TURBULENT FLOWS
C
C  CALLING PROGRAM MUST FIRST EXPRESS SPECIES AND ENERGY CONSERVATION
C  FINITE-DIFFERENCE EQUATIONS IN THE STANDARD FORM
C
C      APOS2(I),P = AEOS2(I),E + AHOS2(I),H + AMOS2(I),M + ASOS2(I),S
C                  +AHOS2(I),H + ALOS2(I),L + SOLS2(I), , I=1,NS
C  DEPT M.E. WASHINGTON STATE UNIVERSITY
C  PULLMAN, WASHINGTON 99163
C  MARCH 1976
C  DAVID T. PRATT AND JOHN J. MORNECK
C
C
C  ***SUMMARY***
C  CREK CONSISTS OF 9 FORTRAN-IV SUBROUTINES CREK,CRENO,SPRCE,CALC,HCPS
C  WHICH ENABLES THE EXTENSION OF ANY EXISTING HYDRODYNAMIC COMPUTER
C  CODE TO THE CALCULATION OF COMPLEX FLOW WITH CHEMICALLY COMPLEX
C  EQUILIBRIUM OR KINETIC STATIONARY STATES
C  THIS VERSION OF CREK IS LIMITED TO IDEAL HOMOGENEOUS GAS-PHASE
C  CHEMICAL EQUILIBRIUM AND NON-EQUILIBRIUM (KINETIC) STATES
C
C  ***CALLING CREK***
C  CALLING PROGRAM SEEKS SOLUTION FOR VALUES AT A POINT P OF MOLE

```

```

C NUMBERS OF CHEMICAL SPECIES, (S2(I), I=1, NS) AND THE TEMPERATURE TK,
C GIVEN THE VALUES OF SAME VARIABLES AT NEIGHBORING NODES, AND VALUES
C AT P AT A PREVIOUS TIME STEP OR ESTIMATES FROM PREVIOUS ITERATION
C
C WHERE
C   AP = AE + AM + AN + AS + AH + AL + APP
C   AD DEMOTES CONVECTIVE AND DIFFUSIVE FLUX COEFFICIENTS
C       AT NEIGHBORING NODES D=E,W,N,S,H AND L, KG/CM M-SEC
C   APP IS INFLUENCE TERM FROM P AT PREVIOUS TIME STEP
C   S2(I) IS THE MOLE NO. OF SPECIES I AT THE POINT P, KG-MOLE I/KG
C   S2(I),D IS THE MOLE NO. OF SPECIES I AT NEAR-NODE D,
C       KG-MOLE I/KG
C   SO(S2(I)) IS RATE OF APPEARANCE OF SPECIES I DUE TO
C       CHEMICAL REACTION, KG-MOLES I/CM M-SEC
C
C AND
C   AP*H,P = AE*H,E + AM*H,W + AN*H,N + AS*H,S + AH*H,H + AL*H,L
C       + SO(H)
C
C WHERE
C   H,P IS THE MIXTURE ENTHALPY AT POINT P, J/KG
C   H,D IS THE MIXTURE ENTHALPY AT NEIGHBOR NODES D,
C   SO(H) IS RATE OF HEAT ADDITION TO CONTROL VOLUME BY
C       RADIATIVE AND KINETIC HEATING, J/CM M-SEC
C
C CALLING PROGRAM MUST SUPPLY FOLLOWING VARIABLES THROUGH LABELLED
C COMMON BLOCK /CPARAM/
C
C   TK = TEMPERATURE AT NODE P, DEGREES KELVIN (ESTIMATE)
C   PA = PRESSURE AT POINT P, PASCALS (NT/SQ M)
C   FMV = AP, KG/CM M-SEC
C   S1(I) = (1E*S2(I),E+AM*S2(I),W+AL*S2(I),L) / AP
C   * S2(I) = PREVIOUS SOLUTIONS OR ESTIMATES FOR S2(I)... *
C   *** IF TEMP TK IS SET TO ZERO, PROGRAM CONSTRUCTS ***
C   *** OWN ESTIMATES ***
C   * HSUBO = (AE*H,E+AM*H,W+AL*H,L) / AP, J/KG *
C   Q0,Q1,Q2,Q3,Q4, = COEFFICIENTS IN EXPRESSION FOLLOWING...
C   SO(H) = -100+Q1T+Q2*T**2+Q3*T**3+Q4*T**4, J/CM M-SEC
C
C LADIAN = T --- IGNORES ABOVE EXPRESSION FOR SO(H), TAKES
C SOURCE(H)=0.0
C LEQUIL = T --- EQUILIBRIUM SOLUTION SOUGHT
C           = F --- KINETIC SOLUTION SOUGHT
C LREACT = T --- CHEMICAL REACTION (EOL OR KIN)
C           = F --- ADIABATIC NON-REACTING MIXING
C LDEBUG = T --- INTERMEDIATE DEBUG PRINTING
C           = F --- NO INTERMEDIATE DEBUG PRINTING
C
C ***RETURN***
C S2(I), I=1, NS IS THE MOLE NUMBER OF CHEMICAL SPECIES I (KG-MOLE I/KG)
C TK IS THE TEMPERATURE (DEGREES K) FROM THERMAL ENERGY EQUATION
C HSUBO IS STATIC ENTHALPY AT NODE POINT P (J/KG)
C QHNP IS THE MASS DENSITY AT NODE POINT P (KG/CM M)
C SM IS RECIPROCAL OF MIXTURE MOLECULAR WEIGHT (KG-MOLE/KG)
C ASUM(I,3) IS THE SPECIES NAME (MOLLERITH FIELD)
C
C ****DIMENSIONS****
C   NLN = NUMBER OF ELEMENTS (7)
C   NS = NUMBER OF CHEMICAL SPECIES (20)
C   JJ = NUMBER OF CHEMICAL REACTIONS (36)
C
C THESE DIMENSIONS MAY BE ADJUSTED BY SIMPLY CHANGING THE
C FOLLOWING LABELLED COMMON BLOCKS

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CREK 30
CREK 31
CREK 32
CREK 33
CREK 34
CREK 35
CREK 36
CREK 37
CREK 38
CREK 39
CREK 40
CREK 41
CREK 42
CREK 43
CREK 44
CREK 45
CREK 46
CREK 47
CREK 48
CREK 49
CREK 50
CREK 51
CREK 52
CREK 53
CREK 54
CREK 55
CREK 56
CREK 57
CREK 58
CREK 59
CREK 60
CREK 61
CREK 62
CREK 63
CREK 64
CREK 65
CREK 66
CREK 67
CREK 68
CREK 69
CREK 70
CREK 71
CREK 72
CREK 73
CREK 74
CREK 75
CREK 76
CREK 77
CREK 78
CREK 79
CREK 80
CREK 81
CREK 82
CREK 83
CREK 84
CREK 85
CREK 86
CREK 87
CREK 88
CREK 89
CREK 90
CREK 91
CREK 92
CREK 93

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```

C      CEQUIL...MLM,NS
C      CINDEX...
C      CKINET...
C      CMATRI...NS+2
C      CPARAM...NS
C      CFACT...JJ
C      CSPECF...NS
C
C      AND THE FOLLOWING DIMENSION STATEMENT IN ROUTINE CALC WHICH
C      SHOULD BE DOUBLE DIMENSIONED FOR IBM MACHINES
C
C      A(NS+2,NS+3)
C
C      DOUBLE PRECISION AL,RQ,CPSUM,ENV,ER,FQ,HSUBQ,HSUM,HQ,PA,PI,PPLN,
C      1 Q0,Q1,Q2,Q3,Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,SSAVE,S0,S1,S2,TK,
C      2 TKINV,TLN,7,SMO
C      DOUBLE PRECISION ENVSAV,FACTOR,SMALL,TSAVE,XHI,XLO
C      LOGICAL LADTAB,LCONVG,LDEBUG,LEQUIL,LNRG,LREACT,LEMER
C
C      COMMON
C      3/CHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
C      1/CEQUIL/AL(7,30),ATOM(3,7),HQ(7),PI(7)
C      1/CINDEX/IDC0,IDFU,IDX2,IDX2,IDX20,IDX02,IDX1,IDX2,IDX1,IDX0,IDX02
C      1,IDX,IDX0,INCPS,ILC,ILH,IMAT,ITER,JJ,N1,N2,N3,NA,NGLOB,NGLOSP,
C      2 MLM,NQ,NSM,NS1,NS2,IOCM
C      1/CPARAM/ASUR(30,3),ENV,ER,HSUBQ,LDEBUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOP,
C      1 SM,SMW(30),SMO,S1(30),S2(30),TK,LADTAB,LDEBUG,LEQUIL,LREACT,LEMER
C      2,FCKIJ,LCONVG
C      1/CSPECF/HQ(30),S0(30),SSAVE(30),Z(7,2,30)
C
C      *****
C      THIS SUBROUTINE IS THE MAIN EQUILIBRIUM AND KINETIC SOLUTION ROUTINE.
C      THE CALLING PROGRAM MUST SUPPLY ALL THE VARIABLES EXCEPT RHOP AND SM
C      THROUGH THE LABELLED COMMON BLOCK CPARAM IN SI UNITS. BOTH EQUIL
C      SOLUTIONS (LEQUIL=. ) -- BY MINIMIZATION OF THE GIBBS FUNCTION --
C      AND KINETIC (LEQUIL=F) SOLUTIONS ARE CALCULATED BY A NEW --RAPHSON
C      TECHNIQUE. CREK ALSO CONTROLS THE LOGIC FOR PROBLEM CELLS
C      REFERENCE CREK (WASHINGTON STATE UNIVERSITY) MARCH 1976
C      *****
C
C      DATA FACTOR/5.000/,SMALL/1.00-6/
C
C      ***NORMAL SOLUTION***
C
C      DETERMINE EQUIVALENCE RATIO AND IF OUTSIDE INTERVAL (0.1,10) ASSUME
C      NO REACTION AND RETURN ADIABATIC NON-REACTION MIXTURE PROPERTIES
C      SAVE GIVEN ESTIMATES OR PROGRAM GENERATED ESTIMATES IF TK IS SMALL
C      IF SOLUTION IS SUCCESSFUL, RETURN TO CALLING ROUTINE OTHERWISE,
C      ENTER PROBLEM CELL LOGIC BELOW
C      LCONVG=.TRUE.
C
C      CALL FRATIC
C      IF (.NOT.LDEBUG) GO TO 30
C      WRITE(A,10) LREACT,LEQUIL,LADTAB,ENV,ER,HSUBQ,Q0,Q1,Q2,Q3,Q4,PA,TK
C      10 FORMAT(1X,3L3,10P10D12.3)
C      IF (LDEBUG.FQ.1) GO TO 30
C      WRITE(A,20) (S1(I),I=1,NS)
C      WRITE(A,20) (S2(I),I=1,NS)
C      20 FORMAT(1X,10P10D12.3)
C      30 IF (.NOT.LREACT) GO TO 400
C      ENVSAV=ENV

```

```

CREK      94
CREK      95
CREK      96
CREK      97
CREK      98
CREK      99
CREK     100
CREK     101
CREK     102
CREK     103
CREK     104
CREK     105
CREK     106
CREK     107
CREK     108
NOXX      1
NOXXX     3
NOXXX     4
NOXX      2
NOXX      3
CREK     113
CREK     114
NOXX      4
CREK     116
NOXX      5
NOXX      6
ASTEP     344
CREK     119
NOXX      0
NOXX      0
NOXX      10
CREK     122
CREK     123
CREK     124
CREK     125
CREK     126
CREK     127
CREK     128
CREK     129
CREK     130
CREK     131
CREK     132
CREK     133
CREK     134
CREK     135
CREK     136
CREK     137
CREK     138
CREK     139
CREK     140
CREK     141
CREK     142
NOXX      11
CREK     143
CREK     144
CREK     145
CREK     146
CREK     147
CREK     148
CREK     149
CREK     150
CREK     151
CREK     152
CREK     154

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C	11.92609 IS E-LOG OF STD PATH=101925.0 M/M42	CREK	155
	PPLM=DELG(PA)-11.9260 00	CREK	156
	TSAVE=TK	CREK	157
	DO 40 I=1,NS	CREK	158
40	SSAVE(I)=S2(I)	CREK	159
	IF (TK.LT.SMALL) GO TO 100	CREK	160
C	CALL SPECE	CREK	161
C	IF (LCONVG) GO TO 900	CREK	162
	DO 101 I=1,NS	CREK	163
	IF(S2(I).LT.2.00-20)S2(I)=S1(I)	CREK	164
101	CONTINUE	NOXX	12
	IF(.NOT.LCONVG)GO TO 900	NOXX	13
		NOXX	14
		NOXX	15
C		CREK	165
C	***PRNLEN CELL***	CREK	166
C		CREK	167
C	SOLUTION LOGIC IS DIFFERENT FOR FOUR TYPES OF PROBLEMS AS FOLLOWS	CREK	168
C	MODE 1 ... LEQUIL = T, LADIAN = T	CREK	169
C	MODE 2 ... LEQUIL = T, LADIAB = F	CREK	170
C	MODE 3 ... LEQUIL = F, LADIAN = T	CREK	171
C	MODE 4 ... LEQUIL = F, LADIAB = F	CREK	172
C		CREK	173
C	ALWAYS TRY RT=0.0 (LMRG=F) AFTER SOLUTION FAILURE WHEN LEQUIL=F.	CREK	174
C	LOGIC TO FIND SOLUTION IS CONTROLLED IN CHAPTERS 1 AND 2 BELOW	CREK	175
C	WHERE IN EACH SECTION, NEW ESTIMATES ARE DETERMINED EITHER BY	CREK	176
C	SAVED GIVEN ONES, NEW ASSIGNED ONES, OR SOLUTION FOUND NOT AT	CREK	177
C	REQUIRED CONDITIONS. THE VARIABLES NEXTOK AND NEXTNG ARE ASSIGNED	CREK	178
C	THE STATEMENT NUMBERS OF WHERE TO GO IF THE SOLUTION ATTEMPT IS	CREK	179
C	SUCCESSFUL OR NOT, RESPECTIVELY.	CREK	180
C		CREK	181
	ASSIGN 900 TO NEXTOK	CREK	182
	ASSIGN 100 TO NEXTNG	CREK	183
	GO TO 320	CREK	184
C		CREK	185
C	***** CHAPTER 1 *****	CREK	186
C	***** CHAPTER 1 *****	CREK	187
C		CREK	188
C	***EQUILIBRIUM***	CREK	189
C	THIS CHAPTER MAKES EQUILIBRIUM ESTIMATES AND INITIATES STRATEGY FOR	CREK	190
C	CASES IN WHICH CONVERGENCE WAS NOT ACHIEVED ON FIRST CALL TO SPECE	CREK	191
C		CREK	192
100	MODE=4	CREK	193
	IF (LEQUIL) MODE=MODE-2	CREK	194
	IF (LADIAB) MODE=MODE-1	CREK	195
	LEQUIL=.TRUE.	CREK	196
	LADIAB=.TRUE.	CREK	197
	IF (MODE.LT.3.OR.TK.LT.SMALL) GO TO 170	CREK	198
C		CREK	199
C	-----FIRST USE GIVEN ESTIMATES FOR EQUIL SOLN IN MODE 3 AND 4 PROBLEMS	CREK	200
C		CREK	201
	TK=TSAVE	CREK	202
	DO 120 I=1,NS	CREK	203
120	S2(I)=SSAVE(I)	CREK	204
	ASSIGN 200 TO NEXTOK	CREK	205
	ASSIGN 170 TO NEXTNG	CREK	206
	GO TO 300	CREK	207
C		CREK	208
C	-----GARBAGE ESTIMATES (GORDON AND MCBRIDE)	CREK	209
C		CREK	210
170	TK=3000.000	CREK	211
	SM=0.100/FLOAT(NS)	CREK	212
	DO 171 I=1,NS	NOXX	6
		CREK	214

ORIGINAL PAGE IS
OF POOR QUALITY

TK=TSAVE	CREK	279
DO 251 I=1,NS	CREK	280
251 S2(I)=SSAVE(I)	CREK	281
ASSIGN 250 TO NEXTOK	CREK	282
IF (EMV.GE.EMVSAV.AND.MODE.EQ.3) ASSIGN 900 TO NEXTOK	CREK	283
IF (EMV.GE.EMVSAV.AND.MODE.EQ.4) ASSIGN 900 TO NEXTOK	CREK	284
ASSIGN 270 TO NEXTNG	CREK	285
GO TO 300	CREK	286
C	CREK	287
HALF-INTERVAL SEARCHING	CREK	288
C HAVE SOLUTION AT XLO BUT NOT AT XHI, HENCE START INTERVAL	CREK	289
C SEARCHING BY SETTING EMV TO THE LOGARITHMIC AVERAGE	CREK	290
C IF ITERATING MORE THAN TEN TIMES, TERMINATE.	CREK	291
C	CREK	292
270 IX=IX+1	CREK	293
TK=TSAVE	CREK	294
DO 271 I=1,NS	CREK	295
271 S2(I)=SSAVE(I)	CREK	296
IF (IX.GT.10) GO TO 620	CREK	297
EMV=DSORT(XLO,XHI)	CREK	298
XHI=EMV	CREK	299
ASSIGN 250 TO NEXTOK	CREK	300
ASSIGN 270 TO NEXTNG	CREK	301
GO TO 300	CREK	302
C	CREK	303
***	CREK	304
***	CREK	305
***	CREK	306
***	CREK	307
***	CREK	308
***	CREK	309
***	CREK	310
***	CREK	311
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***	CREK	338
***	CREK	339
***	CREK	340
***	CREK	341
***	CREK	342

C****	****	****	****	****	****	CHAPTER 4	****	***	CREK	343
C****	****	****	****	****	****	CHAPTER 4	****	***	CREK	344
C									CREK	345
C	***FAILURE EXITS***								CREK	346
C	FAILED EQUIL OR KINETIC SOLN OR EQUIV RATIO OUTSIDE (0.1,10)								CREK	347
C	RETURN ADIABATIC, NON-REACTION MIXTURE PROPERTIES								CREK	348
400	SM=0.000								CREK	349
	ON 401 I=1,NS								CREK	350
	S2(I)=S1(I)								CREK	351
	SM=SM+S2(I)								CREK	352
401	CONTINUE								CREK	353
	TK=1000.000								CREK	354
	XLO=TK								CREK	355
	HCP=1								CREK	356
	NS1=1								NOXX	16
	NS2=NS								NOXX	17
	TKINV=1.00-3								CREK	357
	ON 403 I=1,30								NOXX	18
	CALL HCP								CREK	359
	HSUM=0.000								CREK	360
	ON 402 K=1,NS								CREK	361
	HSUM=HSUM+H0(K)*S2(K)								CREK	362
402	CONTINUE								CREK	363
	IF(.NOT.LA01AB)HSUM=HSUM+(((Q4*TK+Q3)*TK+Q2)*TK+Q1+Q0*TKINV)/								CREK	364
	1(RGAS*EMV)								CREK	365
	TK=TK*(1.000+0.500*(HSUBD*RGASIN*TKINV-HSUM)/CPSUM)								NOXX	19
	TKINV=1.000/TK								CREK	367
	XHI=DARS(TK-XLO)								CREK	368
	XLO=TK								CREK	369
	IF (XHI,LT,1.000) GO TO 404								CREK	370
403	CONTINUE								CREK	371
404	CONTINUE								CREK	375
	IF(.NOT.LA01AB)HSUBD=HSUM*RGAS*TK								CREK	376
C									CREK	377
	GO TO 900								CREK	378
C									CREK	379
C****	****	****	****	****	****	CHAPTER 5	****	*	CREK	380
C****	****	****	****	****	****	CHAPTER 5	****	*	CREK	381
C									CREK	382
C	***PROBLEM CELL CALL TO SPECE***								CREK	383
C	TAKE THE ESTIMATES GENERATED IN CHAPTERS 1,2 AND ATTEMPT A SOLUTION								CREK	384
C	WITH FULL EQUATIONS. IF SUCCESSFUL, UPDATE THE SAME ANSWERS WITH THE								CREK	385
C	SOLUTION AND RETURN TO STATEMENT NUMBER NEXTOK. IF NOT, THE ACTION								CREK	386
C	DEPENDS ON WHETHER AN EQUIL OR KINETIC SOLN IS SOUGHT. FAILED								CREK	387
C	EQUIL SOLN, RETURN TO STATEMENT NUMBER NEXTNG, WHILE FAILURE IN A								CREK	388
C	KINETIC SOLN WILL BE FOLLOWED BY AN ATTEMPT WITH LNRG=F --- RT=0.0								CREK	389
C	AND SAME ESTIMATES. SETTING RT=0.0 IMPLIES THAT A CHANGE IN TEMP								CREK	390
C	FIELD HAS NO EFFECT ON SPECIES DISTRIBUTION FOR THAT PARTICULAR								CREK	391
C	ITERATION, BUT DOES ALLOW THE SPECIES CHANGES TO INFLUENCE THE TEMP								CREK	392
C	CHANGE --- PARTIAL DECOUPLING OF THE ENERGY EQUATION.								CREK	393
C	IF STILL NO GOOD, RETURN TO STATEMENT NUMBER NEXTNG.								CREK	394
C									CREK	395
500	CALL SPECE								CREK	396
	IF (LCONVG) GO TO 540								CREK	397
C	SOLUTION FAILED TRY RT=0.0								CREK	398
	IF (LNRG) GO TO 520								CREK	399
	LNRG=.TRUE.								CREK	400
510	GO TO NEXTNG. (100,170,210,250,270,330,600)								CREK	401
520	IF (LFQUL) GO TO 510								CREK	402
530	LNRG=.FALSE.								CREK	403
	GO TO 500								CREK	404
540	IF (LNRG) GO TO 550								CREK	405
	LNRG=.TRUE.								CREK	406
C									CREK	407

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C      GO TO 500      ***REMOVED PER D.T.PRATT 7/19/78**
C*****IF COMPLEX CASES DO NOT CONVERGE, IT MAY BE NECESSARY TO*****
C*****RETURN THIS STATEMENT TO THE PROGRAM.*****
C
C
C-----SOLUTION IS SUCCESSFUL, UPDATE SAVE ANSWERS AND CONTINUE.
C
  550 TSAVE=TK
      DO 560 I=1,NS
  560 SSAVE(I)=S2(I)
C
      GO TO NEXTOK, (200,230,250,300,320,900)
C
C*****          *****          *****          *****          CHAPTER 6          *****
C*****          *****          *****          *****          CHAPTER 6          *****
C
C ***ERROR MESSAGES***
C
  600 WRITE(6,601)
  601 FORMAT(1H0,10X,3(4H***),30H FAILURE TO FIND EQUIL SOLN...,
    A24H AVG INLET PROPS RETURNED/)
      GO TO 650
  610 WRITE(6,611)
  611 FORMAT(1H0,10X,3(4H***),35H FAILURE TO FIND NEAR-EQUIL SOLN...,
    A24H AVG INLET PROPS RETURNED/)
      GO TO 650
  620 WRITE(6,621)
  621 FORMAT(1H0,10X,3(4H***),37H FAILURE TO OBTAIN KINETIC SOLN AFTER,
    A48H TFN INTERVAL HALVING...AVG INLET PROPS RETURNED/)
      GO TO 650
  630 WRITE(6,631)
  631 FORMAT(1H0,10X,3(4H***),29H NON-ADIABATIC SOLN FAILED...,
    A10H ADIAB SOLN RETURNED/)
      GO TO 670
C
C-----RESTORE FAILED PROBLEM MODE PRIOR TO RETURN
C
  650 IF (MODE.EQ.2) LADIAB=.FALSE.
      IF (MODE.EQ.3) LEQUIL=.FALSE.
      IF (MODE.EQ.4) LADIAB=.FALSE.
      GO TO 400
C
C-----FAILED NON-ADIABATIC SOLUTION...RETURN ADIABATIC
C-----EQUIL OR KINETIC SOLUTION
C
  670 TK=TSAVE
      SM=0.000
      DO 671 I=1,NS
  671 SM=SM+S2(I)
  900 RHOP=PA/(RGAS*TK*SM)
      RETURN
      END
      SUBROUTINE CALC
C
      DOUBLE PRECISION AL,B0,CPSUM,ENV,ER,F0,HSUB0,HSUM,MO,PA,PI,PPLN,
  1 Q0,Q1,Q2,Q3,Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,SSAVE,S0,S1,S2,TN,
  2 TKINV,TLN,Z,SMO
      DOUBLE PRECISION BX,BX2,TACT,TACT2,TEN,TEN2,Y1,X2,CERU
      DOUBLE PRECISION XCYH,FUT,FST,SSS
      DOUBLE PRECISION X,Y
      DOUBLE PRECISION ANO,BIG,BXX,DSUM,EN,HH,HIN,Q,QDRV,RHSH,RHSQ,
  1 RM,RT,P1,R2,SS,SUM,S2I,TK1,TK2,TM1,TM2,TM3,TM2,XC,YH
      LOGICAL LADTAR,LCONVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER

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CREK 408
CREK 409
CREK 410
CREK 411
CREK 412
CREK 413
CREK 414
CREK 415
CREK 416
CREK 417
CREK 418
CREK 419
CREK 420
CREK 421
CREK 422
CREK 423
CREK 424
CREK 425
CREK 426
CREK 427
CREK 428
CREK 429
CREK 430
CREK 431
CREK 432
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CREK 446
CREK 447
CREK 448
CREK 449
CREK 450
CREK 451
CREK 452
CREK 453
CREK 454
CREK 455
CREK 456
CREK 457
CREK 458
CREK 459
CREK 460
CALC 2
CALC 3
NOXXX 20
NOXXX 8
NOXXX 9
NOXXX 21
4STEP 345
NOXXX 11
NOXXX 12
NOXXX 13
NOXXX 14

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C	DOUBLE PRECISION RLAM,RTURN,PHI	NOXX	22
C	THE FOLLOWING DOUBLE PRECISION REQUIRED ONLY FOR IBM MACHINES	CALC	6
C	DOUBLE PRECISION A,DTM1	CALC	7
C	COMMON	CALC	8
	3/CHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG	CALC	9
	1/CEQUIL/AL(7,30),ATOM(3,7),RO(7),PI(7)	CALC	10
	1/CINOFK/IDCN,IOFU,IOO2,ION2,IOH2O,IONO2,ION1,ION2,ION1,IONO,IONO2	NOXX	23
	1,ION,IOOH,IMCPS,ILC,ILH,IMAT,ITER,JJ,N1,N2,N3,NA,NGLOR,NGLORP,	CALC	12
	2 NLM,NQ,NSM,NS1,NS2,IOCH	NOXX	24
	1/CMATRI/X(32),Y(32)	NOXX	25
	1/CPARAM/ASUB(30,31),ENV,ER,MSUBO,NDEBUG,NS,PA,QO,Q1,Q2,Q3,Q4,RHOP,	4STEP	346
	1 SM,SNW(30),SMO,S1(30),S2(30),TK,LADIAO,LDEBUG,LEQUIL,LREACT,LENER	NOXX	27
	2,ENKI,J,LCNVG	CALC	16
	1/CREACT/RX(36),RX2(36),IO(4,36),MODR(36),TACT(36),TACT2(36),	NOXX	29
	2 TEN(36),TEN2(36),X1(36),X2(36),CEBU(36)	CALC	18
	1/CSPECE/HO(30),SO(30),SSAVE(30),Z(7,2,30)	NOXX	30
	COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,	NOXX	31
	1 CERU3,CERU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	347
	2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	348
C	*****	4STEP	349
C	THIS SUBROUTINE CONSTRUCTS THE NEWTON-RAPHSON DERIVATIVE MATRIX FOR	CALC	21
C	BOTH KINETIC AND EQUILIBRIUM SOLUTIONS AND SOLVES IT BY PIVOTAL	CALC	22
C	GAUSSIAN REDUCTION. WHENEVER TEMP IS LESS THAN 1500K, THE REVERSE	CALC	23
C	RATE IS CALCULATED FROM THE FORWARD RATE AND EQUILIBRIUM CONSTANT.	CALC	24
C	PROVISION IS MADE FOR GLOBAL REACTIONS	CALC	25
C	REFERENCE CREK (WASHINGTON STATE UNIVERSITY) MARCH 1976	CALC	26
C	*****	CALC	27
C	DIMENSION A(32,33)	CALC	28
C	DATA RIG/46.05100/	CALC	29
C	DO 10 I=1,NQ	CALC	30
	X(I)=0.0	CALC	31
C	DO 10 K=1,NA	CALC	32
10	A(I,K)=0.000	CALC	33
C	IMCPS=1	CALC	34
	IF (LEQUIL) IMCPS=2	CALC	35
	IF (TK.LT.1500.000) IMCPS=2	CALC	36
	MS1=1	CALC	37
	MS2=NS	CALC	38
	CALL MCPS	CALC	39
	MIN=MSUBO+RGASIN+TKINV	CALC	40
	Q=0.000	CALC	41
	QDRV=0.000	CALC	42
	IF (LADIAO) GO TO 20	CALC	43
C	Q AND QDRV ARE NON-DIMENSIONAL	CALC	44
	TM1=RQ/(ENV+RGAS)	CALC	45
	O=((104*TK+Q3)*TK+Q2)*TK+Q1+QO*TKINV)*TM1	CALC	46
	QDRV=((14.000+Q4*TK+3.000*Q3)*TK+2.000*Q2)*TK+Q1)*TM1	CALC	47
20	CONTINUE	CALC	48
C	IF (LEQUIL) GO TO 300	CALC	49
C	RHSM=PA+RGASIN+TKINV	CALC	50
	RHOP=RHSM+SMINV	CALC	51
	RHSO=RHOP**2	CALC	52
C	*****	CALC	53
C	*****	CALC	54
C	*****	CALC	55
C	*****	CALC	56
C	*****	CALC	57
C	*****	CALC	58
C	*****	CALC	59
C	*****	CALC	60

GLOBAL RATE EQUATIONS OF POOR QUALITY

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C
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR HYDROCARBON PYROLYSIS...
C GLOBAL RATE EXPRESSIONS DUE TO KOLLRACK...
C (1) C12H23 + O2 --- 5 C2H4 + C2H6 + O2
C (2) C12H23 + OH --- 6 C2H4 + O
C
    IF (NGLOR.EQ.0) GO TO 110
    IF (TK.LT.500.00) GO TO 110
    DO 100 J=1,NGLOR
    I=ID(1,J)
    M=ID(2,J)
    N=ID(4,J)
    O=ID(5,J)
    IF(I.EQ.IDFU.AND.M.EQ.IDCH.AND.N.EQ.IDH2)GO TO 150
    IF(I.EQ.IDCH.AND.K.EQ.IDO2)GO TO 160
    IF(I.EQ.IDCO.AND.K.EQ.IDO2)GO TO 170
    IF(I.EQ.IDH2.AND.K.EQ.IDO2)GO TO 180
    IF(M.EQ.IDCO.AND.N.EQ.IDH2) GO TO 105
    IF(M.EQ.IDCO.AND.N.EQ.IDH2O)GO TO 111
    IF(I.EQ.IDCO.AND.K.EQ.IDO2)GO TO 121
    TK1=TACT(J)*TKINV
    TM2=TK1-TEN(J)*TLN-BX(J)
    IF (DAOS(TM2).GT.RIG) GO TO 100
    R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX
    R1=X1(J)*R1
    R1=R1*S2(I)*RHSO*S2(K)
    RT=R1*(TEN(J)+TK1-2.00)
    RN=R1*2.00
C-----A(ANY,M)=A(ANY,N)=0 BECAUSE NO REVERSE REACTION ASSUMED
    A(I,I)=A(I,I)+R1
    A(I,K)=A(I,K)+R1
    A(I,NA)=A(I,NA)-R1
    A(I,NSM)=A(I,NSM)-RN
    A(I,NQ)=A(I,NQ)+RT
    A(N,I)=A(N,I)-R1
    A(N,K)=A(N,K)-R1
    A(N,NA)=A(N,NA)+R1
    A(N,NSM)=A(N,NSM)+RN
    A(N,NQ)=A(N,NQ)-RT
    ANO=5.00
    IF (J.FO.1) GO TO 101
    A(K,I)=A(K,I)+R1
    A(K,K)=A(K,K)+R1
    A(K,NA)=A(K,NA)-R1
    A(K,NSM)=A(K,NSM)-RN
    A(K,NQ)=A(K,NQ)+RT
    ANO=6.00
101 CONTINUE
    R1=R1+ANO
    RN=RN+ANO
    RT=RT+ANO
    A(M,I)=A(M,I)-R1
    A(M,K)=A(M,K)-R1
    A(M,NA)=A(M,NA)+R1
    A(M,NSM)=A(M,NSM)+RN
    A(M,NQ)=A(M,NQ)-RT
    GO TO 100
105 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR HYDROCARBON PYROLYSIS...
C GLOBAL RATE EXPRESSION DUE TO EOEYMAN AND FORTUNE

```

CALC	61
CALC	62
CALC	63
CALC	64
CALC	65
CALC	66
CALC	67
CALC	68
CALC	69
CALC	70
CALC	71
CALC	72
CALC	73
CALC	74
4STEP	350
4STEP	351
4STEP	352
4STEP	353
CALC	75
NOXX	35
NOXX	36
CALC	76
CALC	77
CALC	78
CALC	79
CALC	80
CALC	81
CALC	82
CALC	83
CALC	84
CALC	85
CALC	86
CALC	87
CALC	88
CALC	89
CALC	90
CALC	91
CALC	92
CALC	93
CALC	94
CALC	95
CALC	96
CALC	97
CALC	98
CALC	99
CALC	100
CALC	101
CALC	102
CALC	103
CALC	104
CALC	105
CALC	106
CALC	107
CALC	108
CALC	109
CALC	110
CALC	111
CALC	112
CALC	113
CALC	114
CALC	115
CALC	116
CALC	117
CALC	118

C CHWY + (X/2) Q2 ---- X CD + (Y/2) H2
C

XC=AL(IIC,I)
YM=AL(ILM,I)
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)-(0.3*PPLN)
IF(TEN(J).NE.C.)TM2=TM2-TEN(J)*TLN
IF(DARS(TM2).GT.BIG)GO TO 100
R1=DEXP(-TM2)

C
C-----PROVISION FOR CONTACT INDEX

R1=X1(J)*R1
R1=R1*(RHOP+S2(K))*DSORT(RHOP+S2(I))
TM1=R1*0.5
A(I,I)=A(I,I)+TM1
A(I,K)=A(I,K)+R1
A(K,I)=A(K,I)+R1*XC*0.25
A(K,K)=A(K,K)+TM1*XC
A(M,I)=A(M,I)-TM1*XC
A(M,K)=A(M,K)-R1*XC
A(N,I)=A(N,I)-R1*YM*0.25
A(N,K)=A(N,K)-TM1*YM

C-----A(ANY,M)=A(ANY,N)=0 BECAUSE NO REVERSE REACTION ASSUMED

RN=R1*1.5
A(I,NSM)=A(I,NSM)-RN
A(K,NSM)=A(K,NSM)-RN*XC*0.5
A(M,NSM)=A(M,NSM)+RN*XC
A(N,NSM)=A(N,NSM)+RN*YM*0.5
A(I,NA)=A(I,NA)-R1
A(K,NA)=A(K,NA)-R1*XC*0.5
A(M,NA)=A(M,NA)+R1*XC
A(N,NA)=A(N,NA)+R1*YM*0.5
IF (.NOT.(LNRG)) GO TO 100
RT=R1*(TK1+TFN(J)-1.5)
A(I,NQ)=A(I,NQ)+RT
A(K,NQ)=A(K,NQ)+RT*XC*0.5
A(M,NQ)=A(M,NQ)-RT*XC
A(N,NQ)=A(N,NQ)-RT*YM*0.5
GO TO 100

111 CONTINUE

C ***GLOBAL REACTION***

C GLOBAL RATE EQUATIONS FOR 2-STEP REACTION.

C FIRST STEP CHWY+(X/2+Y/4)Q2 --- XCD+(Y/2)H2O

C

XC=AL(IIC,I)
YM=AL(ILM,I)
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)-TFN(J)*TLN
IF(DARS(TM2).GT.BIG)GO TO 100
R1=DEXP(-TM2)

C

C-----PROVISION FOR CONTACT INDEX.

R1=X1(J)*R1
R1=R1*(RHOP+S2(K))*DSORT(RHOP+S2(I))
RLAM=R1
PHI=DMIN1(S2(I),S2(K)/(XC+0.25*YM))
RTIIR=CRAU(J)*RHOP*PHI*EOKIJ
IF(RLAM.LT.PTIIR)GO TO 130
P1=RTIIR
FN=1.000
IF(S2(K)/(XC+0.25*YM).LT.S2(I))GO TO 131
R1=RTIIR
R1K=0.0
GO TO 132

CALC	119
CALC	120
CALC	121
NOXX	15
CALC	123
CALC	124
CALC	125
CALC	126
CALC	127
CALC	128
CALC	129
CALC	130
CALC	131
CALC	132
CALC	133
CALC	134
CALC	135
CALC	136
CALC	137
CALC	138
CALC	139
CALC	140
CALC	141
CALC	142
CALC	143
CALC	144
CALC	145
CALC	146
CALC	147
CALC	148
CALC	149
CALC	150
CALC	151
CALC	152
CALC	153
CALC	154
CALC	155
CALC	156
NOXX	37
NOXX	38
NOXX	39
NOXX	40
NOXX	41
NOXX	42
NOXX	43
NOXX	44
NOXX	45
NOXX	46
NOXX	47
NOXX	48
NOXX	49
NOXX	50
NOXX	51
NOXX	52
NOXX	53
NOXX	54
NOXX	55
NOXX	56
NOXX	57
NOXX	58
NOXX	59
NOXX	60
NOXX	61
NOXX	62

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131 R1I=0.0
    R1K=RTURB
    GO TO 132
130 R1I=0.500*RLAM
    R1K=RLAM
    R1=RLAM
    EN=1.500
132 CONTINUE
    A(I,I)=A(I,I)+R1I
    A(I,K)=A(I,K)+R1K
    A(K,I)=A(K,I)+R1I*0.5*(XC+0.5*YH)
    A(K,K)=A(K,K)+0.5*R1K*(XC+0.5*YH)
    A(M,I)=A(M,I)-R1I*XC
    A(M,K)=A(M,K)-R1K*XC
    A(N,I)=A(N,I)-R1I*YH*0.5
    A(N,K)=A(N,K)-0.5*R1K*YH
C-----A(ANY,N)=A(ANY,N)+0 BECAUSE NO REVERSE REACTION ASSUMED.
    RN=R1*EN
    A(I,NSM)=A(I,NSM)-RN
    A(K,NSM)=A(K,NSM)-RN*0.5*(XC+0.5*YH)
    A(M,NSM)=A(M,NSM)+RN*XC
    A(N,NSM)=A(N,NSM)+RN*YH*0.5
    A(I,NA)=A(I,NA)-R1
    A(K,NA)=A(K,NA)-R1*0.5*(XC+0.5*YH)
    A(M,NA)=A(M,NA)+R1*XC
    A(N,NA)=A(N,NA)+R1*YH*0.5
    IF(.NOT.LNRG)GO TO 100
    IF(RTURB.LT.RLAM)GO TO 100
    RT=R1*(TK1+TEN(J)-1.5)
    A(I,NO)=A(I,NO)+RT
    A(K,NO)=A(K,NO)+RT*0.5*(XC+0.5*YH)
    A(M,NO)=A(M,NO)-RT*XC
    A(N,NO)=A(N,NO)-RT*YH*0.5
    GO TO 100
121 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 2-STEP REACTION.
C SECOND STEP CO*(1/2)O2 --- CO2
C
    TK1=TACT(J)*TKINV
    TM2=TK1-BX(J)-TEN(J)*TLN
    IF(DABS(TM2).GT.DIG)GO TO 100
    R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX.
    R1=X1(J)*R1
    R1=R1*RHSG*S2(K)*S2(I)
    RLAM=R1
    PHI=DMIN1(2.*S2(K),S2(I))
    RTURN=CERU(J)*RHNP*PHI*ENKIJ
    IF(RLAM.LT.RTURN)GO TO 140
    R1=RTURB
    EN=1.000
    IF(2.*S2(K).LT.S2(I))GO TO 141
    R1I=RTURN
    R1K=0.0
    GO TO 142
141 R1I=0.0
    R1K=RTURN
    GO TO 142
140 R1I=RLAM
    R1K=RLAM
    R1=RLAM
    EN=2.000

```

NOXX	63
NOXX	64
NOXX	65
NOXX	66
NOXX	67
NOXX	68
NOXX	69
NOXX	70
NOXX	71
NOXX	72
NOXX	73
NOXX	74
NOXX	75
NOXX	76
NOXX	77
NOXX	78
NOXX	79
NOXX	80
NOXX	81
NOXX	82
NOXX	83
NOXX	84
NOXX	85
NOXX	86
NOXX	87
NOXX	88
NOXX	89
NOXX	90
NOXX	91
NOXX	92
NOXX	93
NOXX	94
NOXX	95
NOXX	96
NOXX	97
NOXX	98
NOXX	99
NOXX	100
NOXX	101
NOXX	102
NOXX	103
NOXX	104
NOXX	105
NOXX	106
NOXX	107
NOXX	108
NOXX	109
NOXX	110
NOXX	111
NOXX	112
NOXX	113
NOXX	114
NOXX	115
NOXX	116
NOXX	117
NOXX	118
NOXX	119
NOXX	120
NOXX	121
NOXX	122
NOXX	123
NOXX	124
NOXX	125
NOXX	126

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142 CONTINUE
  A(I,I)=A(I,I)+R1I
  A(I,K)=A(I,K)+R1K
  A(K,I)=A(K,I)+0.5*R1I
  A(K,K)=A(K,K)+0.5*R1K
  A(M,I)=A(M,I)+R1I
  A(M,K)=A(M,K)+R1K
C-----A(ANY,M)=A(ANY,M)=0 BECAUSE NO REVERSE REACTION ASSUMED.
  RN=R1*EN
  A(I,NSM)=A(I,NSM)-RN
  A(K,NSM)=A(K,NSM)-RN*0.5
  A(M,NSM)=A(M,NSM)+RN
  A(I,NA)=A(I,NA)-R1
  A(K,NA)=A(K,NA)-R1*0.5
  A(M,NA)=A(M,NA)+R1
  IF(.NOT.LNR6)GO TO 100
  IF(RTURB.LT.RLAM)GO TO 100
  RT=R1*(TK1+TEN(J)-2.0)
  A(I,NQ)=A(I,NQ)+RT
  A(K,NQ)=A(K,NQ)+RT*0.5
  A(M,NQ)=A(M,NQ)+RT
  GO TO 100
150 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.
C FIRST STEP  CXHY --- CXHY-2+H2
C
  XC=AL(ILC,I)
  YM=AL(ILM,I)
  TACT(J)=ER1
  TEN(J)=0.000
  CERU(J)=CEBU1
  RX(J)=PEXP1
  TK1=TACT(J)*TKINV
  TM2=TK1-RX(J)-TEN(J)*TLN
  IF(DARS(TM2).GT.0IG)GO TO 100
  R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX.
  R1=X1(J)*R1
  R1=R1*((RHCP*S2(IDFU))**AEXP1)*((RHOP*S2(IDO2))**BEXP1)
  R1=((RHOP*S2(IDCH))**CEXP1)
  PLAM=R1
  PHT=S2(I)
  RTURR=CERU(J)*RHOP*PHI*EDKIJ
  IF(OLAP.LT.RTURR)GO TO 151
  R1=RTURR
  EN=1.000
  R1=RTURR
  R1M=0.0
  R1O2=0.0
  GO TO 152
151 R1=AFXP1*RLAM
  R1O2=REXP1*RLAM
  R1M=CFXP1*RLAM
  R1=RLAM
  FN=AEXP1+BEXP1+CEXP1
152 A(I,I)=A(I,I)+R1I
  A(I,M)=A(I,M)+R1M
  A(I,IOO2)=A(I,IOO2)+R1O2
  A(M,I)=A(M,I)+R1I
  A(M,M)=A(M,M)+R1M
  A(M,IOO2)=A(M,IOO2)+R1O2
  A(N,I)=A(N,I)+R1I

```

NOXX	127
NOXX	128
NOXX	129
NOXX	130
NOXX	131
NOXX	132
NOXX	133
NOXX	134
NOXX	135
NOXX	136
NOXX	137
NOXX	138
NOXX	139
NOXX	140
NOXX	141
NOXX	142
NOXX	143
NOXX	144
NOXX	145
NOXX	146
NOXX	147
4STEP	354
4STEP	355
4STEP	356
4STEP	357
4STEP	358
4STEP	359
4STEP	360
4STEP	361
4STEP	362
4STEP	363
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4STEP	387
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4STEP	389
4STEP	390
4STEP	391
4STEP	392
4STEP	393
4STEP	394
4STEP	395
4STEP	396

OF POOR QUALITY

```

A(N,M)=A(N,M)-R1M
A(N,IOQ2)=A(N,IOQ2)-R1O2
RN=R1*FN
A(I,NSM)=A(I,NSM)-RN
A(M,NSM)=A(M,NSM)+RN
A(N,NSM)=A(N,NSM)+RN
A(I,NA)=A(I,NA)-R1
A(M,NA)=A(M,NA)+R1
A(N,NA)=A(N,NA)+R1
IF(.NOT.LNRG)GO TO 100
IF(RTURN.LT.RLAM)GO TO 100
RT=R1*(TK1+TEN(J)-EN)
A(I,NO)=A(I,NO)+RT
A(M,NO)=A(M,NO)-RT
A(N,NO)=A(N,NO)-RT
GO TO 100
160 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.
C SECOND STEP CXHY=2+(X/2)O2 --- XCO+(Y-2)/2)H2
C
XC=AL(ILC,IDFU)
YM=AL(ILM,IDFU)
XCYH=XC+C.2500*(YM-2.000)
TACT(J)=FR2
TEN(J)=O.000
CERU(J)=CERU2
RX(J)=DEXP2
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)-TEN(J)*TLN
IF(DABS(TM2).GT.RIG)GO TO 100
R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX.
R1=X1(J)*R1
R1=R1*([RHOP*S2(IOCH)]**AEXP2)*([RHOP*S2(IOQ2)]**BEXP2)
1*(IRHOP*S2(IDFU)+1.0-30)**CEXP2)
RLAM=R1
PHY=O*IN1(S2(IOCH),S2(IOQ2)/XCYH)
RTURN=CERU(J)*RHOP*PHI*EDKIJ
IF(RLAM.LT.RTURN)GO TO 161
R1=RTURN
RIFU=O.0
EN=1.000
IF(S2(IOQ2)/XCYH.LT.S2(IOCH))GO TO 162
R1=RTURN
R1K=O.0
GO TO 163
162 R1=O.0
R1K=RTURN
GO TO 163
161 R1=AFXP2*RLAM
R1K=REXP2*RLAM
RIFU=CEXP2*RLAM
R1=RLAM
EN=AFXP2+REXP2+CEXP2
163 A(I,I)=A(I,I)+R1I
A(I,K)=A(I,K)+R1K
A(I,IOFU)=A(I,IOFU)+R1FU
A(K,I)=A(K,I)+R1I*O.500*XC
A(K,K)=A(K,K)+R1K*O.500*XC
A(K,IOFU)=A(K,IOFU)+R1FU*O.500*XC
A(M,I)=A(M,I)-R1I*XC
A(M,K)=A(M,K)-R1K*XC
4STEP 397
4STEP 398
4STEP 399
4STEP 400
4STEP 401
4STEP 402
4STEP 403
4STEP 404
4STEP 405
4STEP 406
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4STEP 459
4STEP 460

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ORIGINAL FROM 25
OF POOR QUALITY

```

A(M,INFU)=A(M,INFU)-P1FU*XC
A(M,T)=A(M,T)-R1I*(YH-2.000)*0.500
A(M,K)=A(M,K)-R1K*(YH-2.000)*0.500
A(M,INFU)=A(M,INFU)-R1FU*(YH-2.000)*0.500
RN=R1*EN
A(I,NSM)=A(I,NSM)-RN
A(K,NSM)=A(K,NSM)-RN*0.500*XC
A(M,NSM)=A(M,NSM)+RN*XC
A(N,NSM)=A(N,NSM)+RN*(YH-2.000)*0.500
A(I,NA)=A(I,NA)-R1
A(K,NA)=A(K,NA)-R1*0.500*XC
A(M,NA)=A(M,NA)+R1*XC
A(N,NA)=A(N,NA)+R1*(YH-2.000)*0.500
IF(LMNT,LNR6)GO TO 100
IF(RTURN,LT,PLAM)GO TO 100
RT=R1*(TK1+TEN(J)-EN)
A(I,NQ)=A(I,NQ)+RT
A(K,NQ)=A(K,NQ)+RT*0.500*XC
A(M,NQ)=A(M,NQ)+RT*XC
A(N,NQ)=A(N,NQ)+RT*(YH-2.000)*0.500
GO TO 100

```

170 CONTINUE

```

C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.
C THIRD STEP CQ+(1/2)O2 --- CO2
C

```

```

TACT(J)=ER3
TEN(J)=0.000
CFRU(J)=CERU3
RX(J)=PEXP3
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)-TEN(J)*TLN
IF(DARS(TM2),GT,RIG)GO TO 100
R1=DEXP1-TM2

```

```

C
C-----PROVISION FOR CONTACT INDEX.
R1=Y1(J)*R1
SSS=7.9300*DEXP(-2.4800*FUT*(1.000-FST)/(FST*(1.000-FUT)))
SSS=DMIN1(1.000,SSS)
R1=R1*((RHOP*S2(IDC1))*AEXP3)*((RHOP*S2(IDO2))*BEXP3)
1*(RHOP*S2(IDH2O))*CEXP3)*SSS
PLAM=R1
PHI=DMIN1(2.000*S2(K),S2(I))
RTURN=CERU(J)*RHOP*PHI*ENKIJ
IF(PLAM,LT,RTURN)GO TO 171
R1=RTURN
R1H2O=C.0
FN=1.000
IF(2.000*S2(K),LT,S2(I))GO TO 172
R1I=RTURN
R1K=C.0
GO TO 173
172 R1I=0.0
R1K=RTURN
GO TO 173
171 R1I=AEXP3*PLAM
R1K=BEXP3*PLAM
R1H2O=CEXP3*PLAM
R1=PLAM
FN=AEXP3+BEXP3+CEXP3
173 A(I,I)=A(I,I)+R1I
A(I,K)=A(I,K)+R1K
A(I,IDH2O)=A(I,IDH2O)+R1H2O
A(K,I)=A(K,I)+R1I*C.500

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4STEP 461
4STEP 462
4STEP 463
4STEP 464
4STEP 465
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4STEP 523
4STEP 524

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```

A(K,K)=A(K,K)+R1K*0.500
A(K,IOH2O)=A(K,IOH2O)+R1H2O*0.500
A(M,I)=A(M,I)-R1I
A(M,K)=A(M,K)-R1K
A(M,IOH2O)=A(M,IOH2O)-R1H2O
RN=R1*EN
A(I,NSM)=A(I,NSM)-RN
A(K,NSM)=A(K,NSM)-RN*0.500
A(M,NSM)=A(M,NSM)+RN
A(I,NA)=A(I,NA)-R1
A(K,NA)=A(K,NA)-R1*0.500
A(M,NA)=A(M,NA)+R1
IF(.NOT.LNPG)GO TO 100
IF(RTURB.LT.RLAM)GO TO 100
RT=R1*(TK1+TEN(J)-EN)
A(I,NQ)=A(I,NQ)+RT
A(K,NQ)=A(K,NQ)+RT*0.500
A(M,NQ)=A(M,NQ)-RT
GO TO 100
180 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.
C FOURTH STEP H2+(1/2)O2 --- H2O
C
TACT(J)=ER4
TEN(J)=0.000
CEX4(J)=CEX4
RX(J)=PEXP4
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)-TEN(J)*TLN
IF(DARS(TM2).GT.R16)GO TO 100
R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX.
R1=R1(J)*R1
R1=R1*((RHOP*S2(IOH2))**AEXP4)*((RHOP*S2(IOO2))**BEXP4)
1*(RHOP*S2(IDCH)+1.0-30)**CEXP4)
RLAM=R1
PHI=DNINI(2.000*S2(K),S2(I))
RTURR=CFBU(J)*RHL*POPHI*EOKIJ
IF(RLAM.LT.RTURR)GO TO 181
R1=RTURR
R1CH=0.0
EN=1.000
IF(2.000*S2(K).LT.S2(I))GO TO 182
R1=RTURR
R1K=0.0
GO TO 183
182 R1=0.0
R1K=RTURR
GO TO 183
181 R1=AEXP4*RLAM
R1K=AEXP4*RLAM
R1CH=CEXP4*RLAM
EN=AEXP4*BEXP4+CEXP4
183 A(I,I)=A(I,I)+R1I
A(I,K)=A(I,K)+R1K
A(I,IDCH)=A(I,IDCH)+R1CH
A(K,I)=A(K,I)+R1I*0.500
A(K,K)=A(K,K)+R1K*0.500
A(K,IDCH)=A(K,IDCH)+R1CH*0.500
A(M,I)=A(M,I)-R1I
A(M,K)=A(M,K)-R1K
A(M,IDCH)=A(M,IDCH)-R1CH
4STEP 525
4STEP 526
4STEP 527
4STEP 528
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4STEP 580
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4STEP 584
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4STEP 586
4STEP 587
4STEP 588

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RN=R1*FN
A(I,NSM)=A(I,NSM)-RN
A(K,NSM)=A(K,NSM)-RN*0.500
A(M,NSM)=A(M,NSM)+RN
A(I,NA)=A(I,NA)-R1
A(K,NA)=A(K,NA)-R1*0.500
A(M,NA)=A(M,NA)+R1
IF(.NOT.LNNG)GO TO 100
IF(RTURN.LT.RLAM)GO TO 100
RT=R1*(TK1+TEN(J)-EN)
A(I,NQ)=A(I,NQ)+RT
A(K,NQ)=A(K,NQ)+RT*0.500
A(M,NQ)=A(M,NQ)-RT
100 CONTINUE
C
110 CONTINUE
IF(NGLOOP.GT.JJ)GO TO 271
C
NN 270 J=NGLOOP,JJ
C
C** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** **
C** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** **
C
***REACTION RATES***
CALCULATE FORWARD AND REVERSE RATES R1 AND R2
THREE TYPES OF REACTIONS
C
MODR 1 ... A + B (+C) --- D + E (+F)
MODR 2 ... AB + M --- A + R + M
MODR 3 ... A + B + M --- AB + M
C
I=ID(1,J)
K=ID(2,J)
KK=ID(3,J)
M=ID(4,J)
N=ID(5,J)
NN=ID(6,J)
MODE=MODR(J)
C
R1=0.000
R2=0.000
TM1=0.000
TM2=0.000
RN=0.000
RT=0.000
R1I=0.0
R1K=0.0
R1KK=0.0
R2N=0.0
R2M=0.0
R2NN=0.0
C
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)
IF (TFN(J).NE.0.00) TM2=TM2-TFN(J)*TLM
IF (OANS(TM2).GT.RIG) GO TO 205
R1=DEXP(-TM2)
C-----PROVISION FOR CONTACT INDEX
R1=R1*X1(J)
IF (MODE-2) 200,201,202
200 R1=R1*S2(I)*RMSQ*S2(K)
RLAM=R1
PHI=DMIN1(S2(K),S2(I))
RTURN=CERU(J)*RHNP*PHI*EDKIJ

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4STEP	589
4STEP	590
4STEP	591
4STEP	592
4STEP	593
4STEP	594
4STEP	595
4STEP	596
4STEP	597
4STEP	598
4STEP	599
4STEP	600
4STEP	601
CALC	157
CALC	158
CALC	159
4STEP	602
CALC	160
CALC	161
CALC	162
CALC	163
CALC	164
CALC	165
CALC	166
CALC	167
CALC	168
CALC	169
CALC	170
CALC	171
CALC	172
CALC	173
CALC	174
CALC	175
CALC	176
CALC	177
CALC	178
CALC	179
CALC	180
CALC	181
CALC	182
CALC	183
CALC	184
CALC	185
CALC	186
CALC	187
NOXX	188
NOXX	189
NOXX	190
NOXX	191
NOXX	192
NOXX	193
CALC	194
CALC	195
CALC	196
CALC	197
NOXX	198
NOXX	199
NOXX	199

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```

IF(RLAM,LT,RTURB)GO TO 291
R1=RTUPR
EN=1.000
IF(S2(K).LT.S2(I))GO TO 292
R1I=RTURB
R1K=0.0
GO TO 293
292 R1I=0.0
R1K=RTURB
GO TO 293
291 R1I=RLAM
R1K=RLAM
R1=RLAM
EN=2.000
293 CONTINUE
IF(KK.EQ.0) GO TO 290
RLAM=RLAM+RHOP+S2(KK)
PHI=DMIN1(PHI,S2(KK))
RTURB=CEBU(J)+RHOP+PHI+EDKIJ
IF(RLAM,LT,RTURB)GO TO 294
EN=1.000
R1=RTUPR
IF(S2(K).LT.S2(I))GO TO 295
IF(S2(I).LT.S2(KK))GO TO 296
GO TO 298
295 IF(S2(K).LT.S2(KK))GO TO 297
298 R1KK=RTURB
R1K=0.0
R1I=0.0
GO TO 299
297 R1K=RTURB
R1KK=0.0
R1I=0.0
GO TO 299
296 R1I=RTURB
R1K=0.0
R1KK=0.0
GO TO 299
294 R1I=RLAM
R1K=RLAM
R1KK=RLAM
R1=RLAM
EN=3.000
299 CONTINUE
290 RN=R1+EN
IF(.NOT.LNRG)GO TO 205
IF(RTURB,LT,RLAM)GO TO 205
R1=R1+(TEN(J)+TK1-EN)
GO TO 205
C
201 R1=R1+RHSM+RHOP+S2(I)
RLAM=R1
PHI=S2(I)
RTURB=CEBU(J)+RHOP+PHI+EDKIJ
R1I=DMIN1(RLAM,RTURB)
R1=R1I
RN=R1
IF(.NOT.LNRG)GO TO 205
IF(RTURB,LT,RLAM)GO TO 205
RT=R1+(TEN(J)+TK1-2.000)
GO TO 205
C
202 R1=R1+RHSM+S2(I)+RHSM+S2(K)
RLAM=R1

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NOXX	157
NOXX	158
NOXX	159
NOXX	160
NOXX	161
NOXX	162
NOXX	163
NOXX	164
NOXX	165
NOXX	166
NOXX	167
NOXX	168
NOXX	169
CALC	198
NOXX	170
CALC	199
NOXX	171
NOXX	172
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NOXX	193
NOXX	194
NOXX	195
NOXX	196
NOXX	197
NOXX	198
CALC	202
NOXX	199
NOXX	200
NOXX	201
CALC	204
CALC	205
CALC	206
NOXX	202
NOXX	203
NOXX	204
NOXX	205
NOXX	206
CALC	207
NOXX	207
NOXX	208
NOXX	209
CALC	209
CALC	210
CALC	211
NOXX	210

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```

PHI=DMINI(S2(K),S2(I))
RTURN=CERU(J)*PHOP*PHI*EDKIJ
IF(RLAP.LT.RTURN)GO TO 301
R1=RTURN
EN=1.000
IF(S2(K).LT.S2(I))GO TO 302
P1I=RTURN
R1K=0.0
GO TO 303
302 R1I=0.0
R1K=RTURN
GO TO 303
301 R1I=RLAM
R1K=RLAM
R1=RLAM
EN=2.000
303 CONTINUE
RN=R1*EN
IF(.NOT.LNP6)GO TO 205
IF(RTURN.LT.RLAM)GO TO 205
RT=R1*(TEN(J)+TK1-3.000)
C
205 TM1=R1
C
C-----CALCULATE REVERSE RATE CONST FROM FWD RATE CONST AND EQUIL CONST
C-----WHENEVER TEMP IS LESS THAN 1500 K
C
IF (TK.GT.1500.000) GO TO 220
C
HM=HO(I)-HO(M)
SS=SO(I)-SO(M)
IF (MONF-2) 210,211,212
C
210 HM=HM+HO(K)-HO(N)
SS=SS+SO(K)-SO(N)
IF(KK.F0.0) GO TO 218
HM=HM+HO(KK)
SS=SS+SO(KK)
218 IF(NN.F0.0) GO TO 219
HM=HM+HO(NN)
SS=SS+SO(NN)
219 CONTINUE
RXK=RX(J)+SS
TK2=TK1+HM
TN2=TFN(J)
GO TO 230
C
211 HM=HM+HO(N)
SS=SS+SO(N)
C
-2.500304 IS E-LNG OF GAS CONST 0.00206 M*3-ATM/KGMOL-DEG K.
RXK=RX(J)+SS-2.50030400
TK2=TK1+HM
TN2=TFN(J)+1.000
GO TO 230
C
212 HM=HM+HO(K)
SS=SS+SO(K)
RXK=RX(J)+SS+2.50030400
TK2=TK1+HM
TN2=TFN(J)-1.000
GO TO 230
C
220 RXK=RX2(J)

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NOXX	211
NOXX	212
NOXX	213
NOXX	214
NOXX	215
NOXX	216
NOXX	217
NOXX	218
NOXX	219
NOXX	220
NOXX	221
NOXX	222
NOXX	223
NOXX	224
NOXX	225
NOXX	226
NOXX	227
NOXX	228
NOXX	229
NOXX	230
NOXX	231
CALC	214
CALC	215
CALC	216
CALC	217
CALC	218
CALC	219
CALC	220
CALC	221
CALC	222
CALC	223
CALC	224
CALC	225
CALC	226
CALC	227
CALC	228
CALC	229
CALC	230
CALC	231
CALC	232
CALC	233
CALC	234
CALC	235
CALC	236
CALC	237
CALC	238
CALC	239
CALC	240
CALC	241
CALC	242
CALC	243
CALC	244
CALC	245
CALC	246
CALC	247
CALC	248
CALC	249
CALC	250
CALC	251
CALC	252
CALC	253
CALC	254
CALC	255
CALC	256

ORIGINAL PROGRAMS
OF POOR QUALITY

```

TK2=TK2(J)*TKINV
TN2=TN2(J)
C
230 TM2=TK2-RXX
IF (TM2.NE.0.D0) TM2=TM2-TN2*TLN
IF (NABS(TM2).GT.816) GO TO 250
R2=DEXP(-TM2)
C-----MULTIPLY HOMOGENEOUS RATE CONSTANT BY CONTACT INDEX
R2=R2*X7(J)
C
IF (MODE=2) 240,241,242
C
240 R2=R2*S2(M)*RHS0*S2(N)
RLAM=R2
PHI=DMIN1(S2(M),S2(N))
RTURR=CERU(J)*RHQP*PHI*EOKIJ
IF(RLAM.LT.RTURR)GO TO 311
R2=RTURR
EN=1.000
IF(S2(M).LT.S2(N))GO TO 312
R2M=RTURR
P2M=0.0
GO TO 313
312 R2N=0.0
R2M=RTURR
GO TO 313
311 R2M=RLAM
R2N=RLAM
R2=RLAM
EN=2.000
313 CONTINUE
IF(INN.EQ.0) GO TO 249
RLAM=RLAM*RHQP*S2(NN)
PHI=DMIN1(PHI,S2(NN))
RTURR=CERU(J)*RHQP*PHI*EOKIJ
IF(PLAM.LT.RTURR)GO TO 314
R2=RTURR
EN=1.000
IF(S2(M).LT.S2(NN))GO TO 315
IF(S2(M).LT.S2(NN))GO TO 316
GO TO 318
315 IF(S2(M).LT.S2(NN))GO TO 317
316 R2NN=RTURR
R2M=0.0
R2N=0.0
GO TO 319
317 R2M=RTURR
R2NN=0.0
R2N=0.0
GO TO 319
318 R2N=RTURR
R2NN=0.0
R2M=0.0
GO TO 319
319 R2M=RLAM
R2N=RLAM
R2NN=RLAM
R2=RLAM
EN=3.000
319 CONTINUE
249 RN=RN+R2*EN
IF(.NOT.LNRG)GO TO 250
IF(RTURR.LT.RLAM)GO TO 250
RT=RT-R24(TN2+TK2-FN)

```

CALC	257
CALC	258
CALC	259
CALC	260
CALC	261
CALC	262
CALC	263
CALC	264
CALC	265
CALC	266
CALC	267
CALC	268
CALC	269
NOXX	232
NOXX	233
NOXX	234
NOXX	235
NOXX	236
NOXX	237
NOXX	238
NOXX	239
NOXX	240
NOXX	241
NOXX	242
NOXX	243
NOXX	244
NOXX	245
NOXX	246
NOXX	247
CALC	270
NOXX	248
CALC	271
NOXX	249
NOXX	250
NOXX	251
NOXX	252
NOXX	253
NOXX	254
NOXX	255
NOXX	256
NOXX	257
NOXX	258
NOXX	259
NOXX	260
NOXX	261
NOXX	262
NOXX	263
NOXX	264
NOXX	265
NOXX	266
NOXX	267
NOXX	268
NOXX	269
NOXX	270
NOXX	271
NOXX	272
NOXX	273
NOXX	274
NOXX	275
NOXX	276
CALC	274
NOXX	277
NOXX	278
NOXX	279

ORIGINAL PAGE IS
OF POOR QUALITY

```

C      GO TO 250
241  R2=R2+RHS*H+S2(M)*RHS*H+S2(M)
    RLAN=R2
    PHI=DMINI(S2(M),S2(M))
    RTURB=CERU(J)*RHOP*PHI*EDKIJ
    IF(RLAN.LT.RTURB)GO TO 321
    R2=RTURB
    FN=1.000
    IF(S2(M).LT.S2(M))GO TO 322
    R2N=RTURB
    R2M=0.0
    GO TO 323
322  R2N=0.0
    R2M=RTURB
    GO TO 323
321  R2H=RLAN
    R2M=RLAN
    R2=RLAN
    FN=2.000
323  CONTINUE
    RN=RN-R2*FN
    IF(.NOT.LNRG)GO TO 250
    IF(RTURB.LT.RLAN)GO TO 250
    RT=RT-R2*(TN2+TK2-3.000)
    GO TO 250

C
242  R2=R2+RHS*H+RHP*S2(M)
    RLAN=R2
    PHI=S2(M)
    RTURB=CERU(J)*RHOP*PHI*EDKIJ
    R2M=DMINI(RLAN,RTURB)
    R2=R2M
    RN=RN-R2
    IF(.NOT.LNRG)GO TO 250
    IF(RTURB.LT.RLAN)GO TO 250
    RT=RT-R2*(TN2+TK2-2.000)

C
250  TM1=TM1-R2
C
C
C      ***KINETIC***
C      DERIVATIVE AND FUNCTION MATRIX FOR KINETIC SOLUTION
C
    A(I,I)=A(I,I)+R1I
    A(M,I)=A(M,I)-R1I
    A(I,M)=A(I,M)-R2M
    A(M,M)=A(M,M)+R2M
    A(I,NSM)=A(I,NSM)-RN
    A(M,NSM)=A(M,NSM)+RN
    A(I,NQ)=A(I,NQ)+RT
    A(M,NQ)=A(M,NQ)-RT
    A(I,NA)=A(I,NA)-TM1
    A(M,NA)=A(M,NA)+TM1
    IF (MODE.EQ.3) GO TO 260

C
    A(N,I)=A(N,I)-R1I
    A(M,M)=A(M,M)+R2M
    A(I,N)=A(I,N)-R2N
    A(M,N)=A(M,N)+R2N
    A(N,N)=A(N,N)+R2N
    A(N,NSM)=A(N,NSM)+RN
    A(N,NQ)=A(N,NQ)-RT
    A(N,NA)=A(N,NA)+TM1

```

CALC	276
CALC	277
CALC	278
NOXX	280
NOXX	281
NOXX	282
NOXX	283
NOXX	284
NOXX	285
NOXX	286
NOXX	287
NOXX	288
NOXX	289
NOXX	290
NOXX	291
NOXX	292
NOXX	293
NOXX	294
NOXX	295
NOXX	296
NOXX	297
NOXX	298
NOXX	299
NOXX	300
NOXX	301
CALC	301
CALC	302
CALC	303
NOXX	302
NOXX	303
NOXX	304
NOXX	305
NOXX	306
CALC	306
NOXX	307
NOXX	308
NOXX	309
CALC	306
CALC	307
CALC	308
CALC	309
CALC	309
CALC	310
NOXX	311
NOXX	312
NOXX	313
CALC	297
CALC	298
CALC	299
CALC	300
CALC	301
CALC	302
CALC	303
CALC	304
NOXX	314
NOXX	315
NOXX	316
NOXX	317
NOXX	318
CALC	310
CALC	311
CALC	312

OF POOR QUALITY

```

IF (MODE.EQ.2) GO TO 270
C
260 CONTINUE
A(K,I)=A(K,I)+R1I
A(I,K)=A(I,K)+R1K
A(K,K)=A(K,K)+R1K
A(M,K)=A(M,K)-R1K
A(K,M)=A(K,M)-R2M
A(K,NSM)=A(K,NSM)-RM
A(K,NQ)=A(K,NQ)+RT
A(K,NA)=A(K,NA)-TM1
IF (MODE.EQ.3) GO TO 270

```

```

C
A(N,K)=A(N,K)-R1K
A(K,N)=A(K,N)-R2N
IF(KK.EQ.0) GO TO 260
A(I,KK)=A(I,KK)+R1KK
A(K,KK)=A(K,KK)+R1KK
A(KK,I)=A(KK,I)+R1I
A(KK,K)=A(KK,K)+R1K
A(KK,KK)=A(KK,KK)+R1KK
A(M,KK)=A(M,KK)-R1KK
A(N,KK)=A(N,KK)-R1KK
A(KK,M)=A(KK,M)-R2M
A(KK,N)=A(KK,N)-R2N
A(KK,NSM)=A(KK,NSM)-RM
A(KK,NQ)=A(KK,NQ)+RT
A(KK,NA)=A(KK,NA)-TM1
260 IF(NN.EQ.0) GO TO 260
A(I,NN)=A(I,NN)-R2NN
A(K,NN)=A(K,NN)-R2NN
A(NN,I)=A(NN,I)-R1I
A(NN,K)=A(NN,K)-R1K
A(M,NN)=A(M,NN)+R2NN
A(N,NN)=A(N,NN)+R2NN
A(NN,M)=A(NN,M)+R2M
A(NN,N)=A(NN,N)+R2N
A(NN,NN)=A(NN,NN)+R2NN
A(NN,NSM)=A(NN,NSM)+RM
A(NN,NQ)=A(NN,NQ)+RT
A(NN,NA)=A(NN,NA)+TM1

```

269 CONTINUE

```

C
270 CONTINUE

```

```

C
271 CONTINUE
MSUM=0.000
DO 280 I=1,NS
S2I=S2(I)
A(I,I)=A(I,I)+ENV+S2I
A(I,NA)=A(I,NA)+ENV*(S1(I)-S2I)
A(NSM,I)=S2I
A(NSM,NA)=A(NSM,NA)-S2I
A(NQ,I)=HQ(I)+S2I
MSUM=MSUM+A(NQ,I)

```

280 CONTINUE

```

C
A(NSM,NSM)=-SM
C-----A(NSM,NQ) AND A(NQ,NSM) ARE EQUAL TO ZERO.
A(NSM,NA)=A(NSM,NA)+SM
A(NQ,NQ)=CPSUP+QDRV
A(NQ,NA)=MTN-Q-MSUM
TMAT=NQ
IF(LENER)GO TO 282

```

CALC	313
CALC	314
CALC	315
NOXX	319
NOXX	320
NOXX	321
NOXX	322
NOXX	323
CALC	321
CALC	322
CALC	323
CALC	324
CALC	325
NOXX	324
NOXX	325
CALC	326
NOXX	326
NOXX	327
NOXX	328
NOXX	329
NOXX	330
NOXX	331
NOXX	332
NOXX	333
NOXX	334
CALC	338
CALC	339
CALC	340
CALC	341
NOXX	335
NOXX	336
NOXX	337
NOXX	338
NOXX	339
NOXX	340
NOXX	341
NOXX	342
NOXX	343
CALC	351
CALC	352
CALC	353
CALC	354
CALC	355
CALC	356
CALC	357
4STEP	603
CALC	358
CALC	359
CALC	360
CALC	361
CALC	362
CALC	363
CALC	364
CALC	365
CALC	366
CALC	367
CALC	368
CALC	369
CALC	370
CALC	371
CALC	372
CALC	373
CALC	374
NOXX	344

ORIGINAL PAGE IS
OF POOR QUALITY

```

      IMAT=NS
      DO 281 I=1,NS
281  A(I,NSM)=A(I,NA)
282  CONTINUE
      GO TO 400
C
C*** EQUILIBRIUM ***
C  DERIVATIVE AND FUNCTION MATRIX FOR EQUILIBRIUM SOLUTION
C
      300 DO 310 L=1,NLM
      310 RO(L)=0.000
C
      HSUM=0.000
      SUM=0.000
      DO 340 I=1,NS
      SUM=SUM+S2(I)
      TM1=H0(I)*S2(I)
      HSUM=HSUM+TM1
      TM2=(H0(I)-S0(I)+Y(I)-Y(NSM)+PPLN)*S2(I)
      A(N1,N3)=A(N1,N3)+TM2
      A(N2,N2)=A(N2,N2)+H0(I)*TM1
      A(N2,N3)=A(N2,N3)+H0(I)*TM2
C
      DO 330 L=1,NLM
      IF (AL(L,I).EQ.0.000) GO TO 330
      TM3=AL(L,I)*S2(I)
C-----CROSS-DERIVATIVES OF ELEMENT EQUATIONS, D F(L)/D P(K)
      DO 320 K=L,NLM
      IF (AL(K,I).EQ.0.000) GO TO 320
      A(L,K)=A(L,K)+AL(K,I)*TM3
      320 CONTINUE
C-----DERIVATIVES OF L-ELEMENT EQN W.R.T. LN SM AND LN T
      A(L,N1)=A(L,N1)+TM3
      A(L,N2)=A(L,N2)+AL(L,I)*TM1
C-----NEGATIVE OF L-ELEMENT FON, F(L)
      A(L,N3)=A(L,N3)+AL(L,I)*TM2
      RO(L)=RO(L)+AL(L,I)*S1(I)
      330 CONTINUE
      340 CONTINUE
C
      A(N1,N1)=SUM-SM
      A(N1,N3)=A(N1,N3)-(SUM-SM)
      A(N1,N2)=HSUM
      A(N2,N2)=A(N2,N2)+CPSUM+ODRV
      A(N2,N3)=A(N2,N3)+HIN-HSUM=0
C
C-----NEGATIVE OF L-ELEMENT EQNS, F(L)
      DO 350 L=1,NLM
      A(L,N3)=A(L,N3)+RO(L)-A(L,N1)
      350 CONTINUE
C
C-----STORE SYMPETRIC ELEMENTS OF MATRIX
C
      DO 360 I=1,N2
      DO 360 J=I,N2
      A(J,I)=A(I,J)
      360 CONTINUE
C
C-----INTERCHANGE SM-EQN WITH ELEMENT ROW L WITH LARGEST A(L,N1) TO
C-----AVOID POTENTIAL ZERO IN DIAGONAL ELEMENT A(N1,N1)
C

```

NOXX	345
NOXX	346
NOXX	347
NOXX	348
CALC	375
CALC	376
CALC	377
CALC	378
CALC	379
CALC	380
CALC	381
CALC	382
CALC	383
CALC	384
CALC	385
CALC	386
CALC	387
CALC	388
CALC	389
CALC	390
CALC	391
CALC	392
CALC	393
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CALC	400
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CALC	407
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CALC	409
CALC	410
CALC	411
CALC	412
CALC	413
CALC	414
CALC	415
CALC	416
CALC	417
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CALC	420
CALC	421
CALC	422
CALC	423
CALC	424
CALC	425
CALC	426
CALC	427
CALC	428
CALC	429
CALC	430
CALC	431
CALC	432
CALC	433
CALC	434

ORIGINAL VALUE IS
OF POOR QUALITY

```

      TM1=0.000
      DO 370 I=1,NLM
      IF (A(I,N1).LT.TM1) GO TO 370
      TM1=A(I,N1)
      LL=L
370  CONTINUE
C
      DO 380 J=1,N3
      TM1=A(N1,J)
      A(N1,J)=A(LL,J)
      A(LL,J)=TM1
380  CONTINUE
      IMAT=N2
C
C****      ****      ****      ****      ****      ****      CHAPTER 4      ****      ***
C****      ****      ****      ****      ****      ****      CHAPTER 4      ****      ***
C
C ***MATRIX SOLUTION***
C SOLVE FOR CORRECTIONS BY STANDARD PIVOTAL GAUSSIAN ELIMINATION
C
      400 KMAT=IMAT+1
C-----OPTIONAL OUTPUT OF INTERMEDIATE VALUES FOR DEBUGGING
      IF (.NOT.LOERUG) GO TO 410
      IF (NDERUG.LT.5) GO TO 410
      WRITE(6,4C1)
      401 FORMAT(10X,10X,36HELEMENTS A(I,K) OF CORRECTION MATRIX/)
      DO 403 K=1,IMAT
      WRITE(6,402) (A(K,I),I=1,KMAT)
      402 FORMAT(1X,1P16D0.0)
      403 CONTINUE
      410 CONTINUE
      DO 450 NN=1,IMAT
      IF (A(NN,NN).EQ.0.000) GO TO 500
C-----CHANGE 1.000 TO 1.0 FOR NON-IBM MACHINES NOT REQUIRING DOUBLE PRE
C
      DTM1=1.000/A(NN,NN)
      DTM1=1.000/A(NN,NN)
      K=NN+1
      DO 420 J=K,KMAT
      A(NN,J)=A(NN,J)*DTM1
      420 CONTINUE
      IF (K.EQ.KMAT) GO TO 450
      DO 440 I=K,IMAT
      IF (A(I,NN).EQ.0.000) GO TO 440
      DO 430 J=K,KMAT
      A(I,J)=A(I,J)-A(I,NN)*A(NN,J)
      430 CONTINUE
      440 CONTINUE
      450 CONTINUE
C
C-----BACK SOLVE FOR CORRECTION VECTOR
C
      K=IMAT
      J=K+1
      OSUM=0.000
      X(K)=0.000
      IF (IMAT.LT.J) GO TO 460
      DO 470 I=J,IMAT
      OSUM=OSUM+A(K,I)*X(I)
      470 CONTINUE
      480 CONTINUE
      X(K)=A(K,KMAT)-OSUM
      K=K-1
      IF (K.NE.0) GO TO 460

```

CALC	433
CALC	436
CALC	437
CALC	438
CALC	439
CALC	440
CALC	441
CALC	442
CALC	443
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CALC	446
CALC	447
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CALC	450
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CALC	464
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CALC	466
CALC	467
CALC	468
CALC	469
CALC	470
CALC	471
CALC	472
CALC	473
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CALC	490
CALC	491
CALC	492
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CALC	496
CALC	497
CALC	498

SPEC	47
SPEC	48
SPEC	49
SPEC	50
SPEC	51
SPEC	52
SPEC	53
SPEC	54
SPEC	55
SPEC	56
SPEC	57
SPEC	58
SPEC	59
NOXX	362
SPEC	60
SPEC	61
SPEC	62
SPEC	63
SPEC	64
SPEC	65
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SPEC	100
SPEC	101
SPEC	102
SPEC	103
SPEC	104
SPEC	105
SPEC	106
NOXX	363
SPEC	108
SPEC	109

ORIGINALS OF POOR QUALITY

ORIGINAL PAGE IS
OF POOR QUALITY

```

IF(SUM.GT.0.200)ETA=0.200/SUM
IF (ETA.LT.ETA) ETA=ETA1
IF(LEQUIL)GO TO 400
C
C ***CONVERGENCE MONITORING***
C AFTER TEN SUCCESSIVE UNDERRELAXED ITERATIONS, IN WHICH ETA DOES NOT
C INCREASE BY 1.1 OR MORE, OR AFTER SIX ITERATIONS IN WHICH ETA
C DECREASES, DIVERGENCE IS ASSUMED AND THE SOLUTION TERMINATED
C
C LNRG=.TRUE. --- FULL EQUATIONS
  IF (ETA.EQ.1.000) NRLX=-1
  IF((ETA/ETA0).GE.1.100)NRLX= 1
  NRLX=NRLX+1
  IF (NRLX.GT.10) GO TO 900
  IF (ETA.LT.ETA0) NDEC=NDEC+1
  IF (.NOT.LNRG) NDEC=1
  IF (NDEC.GT.6) GO TO 900
C
C****      ****      ****      ****      ****      ****      CHAPTER 4      ****      ***
C****      ****      ****      ****      ****      ****      CHAPTER 4      ****      ***
C
C  APPLY CORRECTIONS TO ESTIMATES
C
C
C 400 CONTINUE
  SUM=0.000
  DO 420 I=1,NS
    Y(I)=Y(I)+ETA*X(I)
    IF (Y(I).LT.TNY) GO TO 410
    S2(I)=DEXP(Y(I))
    SUM=SUM+S2(I)*SMW(I)
  GO TO 420
C
C 410 Y(I)=TNY
  S2(I)=TINY
C-----INSURE CONVERGENCE TEST PASSED WHENEVER Y(I)=TNY
  X(I)=0.000
C 420 CONTINUE
  DO 450 I=1,NS
    S2(I)=S2(I)/SUM
C 450 Y(I)=DLOG(S2(I))
    Y(NSM)=Y(NSM)+ETA*X(NSM)
    SM=DEXP(Y(NSM))
    SMINV=1.000/SM
    Y(NQ)=Y(NQ)+ETA*X(NQ)
    TLN=Y(NQ)
    TK=DEXP(TLN)
    TKINV=1.000/TK
C
  IF (.NOT.LDEBUG) GO TO 500
  IF (NDEBUG.GE.3) WRITE(6,430) ITER,ETA,LREACT,LEQUIL,LADTAB,
1      LNRG,MSUB0,SM,ENV,TK
  IF (NDEBUG.GE.4) WRITE(6,440) (I,ASUB(I,1),S1(I),S2(I),Y(I),
1      X(I),MO(I),SO(I),I=1,MS)
C 430 FORMAT(2X,I3,1P012.3,4L8,1P4012.3)
C 440 FORMAT(20X,7MSPECIFS,4X,5MS1(I),7X,5MS2(I),7X,4MV(I),8X,
1      A4MX(I),8X,5MHQ(I),7X,5HSO(I)/(16X,I2,3X,A4,2X,1P6012.3))
C
C*****      *****      *****      *****      *****      CHAPTER 5      *****
C*****      *****      *****      *****      *****      CHAPTER 5      *****
C
C  CONVERGENCE CHECK...ALL MOLE NUMBER CORRECTIONS MUST BE .LT. 1.0 PCT
C
C 500 IF (ETA.LT.1.000) GO TO 550

```

NOXX	364
SPEC	111
SPEC	112
SPEC	113
SPEC	114
SPEC	115
NOXX	365
SPEC	117
SPEC	118
SPEC	119
SPEC	120
NOXX	366
SPEC	122
SPEC	123
SPEC	124
SPEC	125
SPEC	126
SPEC	127
SPEC	128
SPEC	129
SPEC	130
SPEC	131
SPEC	132
SPEC	133
SPEC	134
NOXX	367
SPEC	135
SPEC	136
SPEC	137
SPEC	138
NOXX	368
SPEC	139
SPEC	140
SPEC	141
SPEC	142
SPEC	143
SPEC	144
SPEC	145
NOXX	369
NOXX	370
NOXX	371
SPEC	146
SPEC	147
SPEC	148
SPEC	149
SPEC	150
SPEC	151
SPEC	152
SPEC	153
SPEC	154
SPEC	155
SPEC	156
SPEC	157
SPEC	158
SPEC	159
SPEC	160
SPEC	161
SPEC	162
SPEC	163
SPEC	164
SPEC	165
SPEC	166
SPEC	167
SPEC	168

```

      DO 510 I=1,NS
      IF (DABS(X(I)).GT.0.0100) GO TO 550
510 CONTINUE
      LCONVG=.TRUE.
      HSIRO=HSUM+RGAS*TK
      RETURN
C
C 550 CONTINUE
C
C
      RETURN
C
C *****      *****      *****      *****      CHAPTER 6      *****
C *****      *****      *****      *****      CHAPTER 6      *****
C
      ENTRY ERATIO
C
C CALCULATES FUEL/AIR EQUIV RATIO, GIVEN MOLE NUMBERS IN S1 ARRAY,
C USING POSITIVE AND NEGATIVE OXIDATION STATES (VALENCES)
C
      VP=0.000
      VM=0.000
      DO 610 I=1,NS
      IF (S1(I).LE.TINY) GO TO 610
      DO 600 L=1,NLM
      IF (AL(L,I).EQ.0.00) GO TO 600
      IF (ATOM(3,L).GT.0.000) VP=VP+AL(L,I)*ATOM(3,L)*S1(I)
      IF (ATOM(3,L).LT.0.000) VM=VM+AL(L,I)*ATOM(3,L)*S1(I)
600 CONTINUE
610 CONTINUE
C
      VM=-VM
      IF (VM.LT.TINY) GO TO 620
      IF (VP.LT.TINY) GO TO 630
      ER=VP/VM
      RETURN
C
620 ER=1000000.000
      RETURN
C
630 ER=0.000
C
900 RETURN
      END
      SUBROUTINE CREKO
C
      DOUBLE PRECISION AL,RO,CPSUM,ENV,ER,FQ,HSUBO,HSUM,HO,PA,PI,PPLN,
1 QO,Q1,Q2,Q3,Q4,RGAS,RGASIN,RHOP,SM,SHINV,SMW,SSAVE,SO,S1,S2,TK,
2 TKINV,TLN,Z,SMO
      DOUBLE PRECISION RX,RX2,TACT,TACT2,TEN,TEN2,X1,X2,CERU
      DOUBLE PRECISION X,Y
      DOUBLE PRECISION AMOLE,B,DX,GF,PECWT,RTLN,SUM,SUMX,SUMY,SUM1,
1 TENLN,TM1,TM2,T1,T2,XBAR,XMAX,XMIN,YBAR
      LOGICAL LADIAN,LCONVG,LDERUG,LEQUIL,LMOLES,LNRG,LRFAC,LSI,LENER
C
      COMMON
      3/CHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG
      1/CEQUIL/AL(7,30),ATOM(3,7),BO(7),PI(7)
      1/CTINDEX/IDCO,IOFU,ION2,ION2,IOH2O,IOCO2,ION1,ION2,ION1,IONO,IONO2
      1,ION,IONH,THCPS,ILC,ILH,IMAT,ITER,JJ,N1,N2,N3,N4,NGL0B,NGL0P,
2 NLM,NQ,NSM,NS1,NS2,IDCH
      1/CMATRI/X(32),Y(32)
      1/CPARAM/ASUR(30,3),ENV,ER,HSUBO,LDERUG,NS,PA,QO,Q1,Q2,Q3,Q4,RHOP,
      1 SM,SMW(30),SMO,S1(30),S2(30),TK,LADIAN,LDERUG,LEQUIL,LREACT,LENER

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SPEC      169
SPEC      170
SPEC      171
SPEC      172
SPEC      173
SPEC      174
SPEC      175
SPEC      176
SPEC      177
SPEC      178
SPEC      179
SPEC      180
SPEC      181
SPEC      182
SPEC      183
SPEC      184
SPEC      185
SPEC      186
SPEC      187
SPEC      188
SPEC      189
SPEC      190
SPEC      191
SPEC      192
SPEC      193
SPEC      194
SPEC      195
SPEC      196
SPEC      197
SPEC      198
SPEC      199
SPEC      200
SPEC      201
SPEC      202
SPEC      203
SPEC      204
SPEC      205
SPEC      206
SPEC      207
SPEC      208
SPEC      209
SPEC      210
SPEC      211
SPEC      212
CRKO      2
CRKO      3
NOXX      372
NOXXX     22
NOXXX     23
NOXX      373
NOXXX     25
NOXXX     26
NOXXX     27
NOXX      374
CRKO      6
CRKO      7
NOXX      375
CRKO      9
NOXX      376
NOXX      377
4STEP     405
NOXX      379
CRKO      13
NOXX      380

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2,EDKIJ,LCNVG
1/CREACT/RX(36),RX2(36),ID(6,36),MDDR(36),TACT(36),TACT2(36),
2 TFM(36),TFM2(36),X1(36),X2(36),CEBU(36)
1/CSPECE/HQ(30),SQ(30),SSAVE(30),Z(7,2,30)
C
C*****
C THIS SUBROUTINE IS THE INITIALIZING ROUTINE. THE FIRST CALL READS
C (1) ELEMENT DATA DECK, (2) THERMO DATA DECK, AND (3) MECHANISM DATA
C DECK. EACH SUBSEQUENT CALL READS ONE REACTANTS DATA DECK...NO LIMIT
C ON NUMBER OF CALLS...ONE FOR EACH DIFFERENT REACTANT STREAM
C PRESSURE AND TEMPERATURE OF EACH REACTANT STREAM MUST BE SUPPLIED BY
C CALLING PROGRAM IN PA AND TK, RESPECTIVELY
C ON RETURN, CALLING PROGRAM MUST STORE MOLE NUMBERS S2(I), PRESSURE,
C TEMPERATURE, ENTHALPY AND DENSITY AT APPROPRIATE INLET GRID NODE
C REFERENCE CREK (WASHINGTON STATE UNIVERSITY) PARC 1976
C*****
C
C DIMENSION CDATA(12),AT(4),B(4)
C
C DATA ACC/4HCO /,ACD2/4HCO2 /,AH2/4HH2 /,AH2O/4HH2O /,
1ANCH/4HPECH/,AN2/4HN2 /,AO2/4HO2 /,BLANK/4H /,BLNK/2H /,
2ELEM/4HELEM/,GAZ/1HG/,GLDR/4HGLDR/,MOL/1HM/,NSTRM/0/,
3REAC/4HREAC/,REVE/4HREVE/,TENLM/2.302585093D0/,THER/4HTHER/,
4THIRD/4HM /,XMAX/0.001D0/,XMIN/0.00033333D0/
DATA CARB,CGS,COMM,HYDR/1HC,4HCGS ,4HCMM,1HM/
C
10 READ(5,20) (CDATA(I),I=1,12)
20 FORMAT(12A4)
WRITE(6,30) (CDATA(I),I=1,12)
30 FORMAT(1H0,5X,12A4)
C
IF (CDATA(1).EQ.BLANK) GO TO 10
IF (CDATA(1).EQ.ELEM) GO TO 100
IF (CDATA(1).EQ.THER) GO TO 200
IF (CDATA(1).EQ.ANCH) GO TO 300
IF (CDATA(1).EQ.REAC) GO TO 400
GO TO 10
C
C * * * * * CHAPTER 1 * * * * *
C * * * * * CHAPTER 1 * * * * *
C
C ***ELEMENTS***
C READ ELEMENT DATA FROM CARDS
C ATOM(1,K) = SYMROL, ATOM(2,K) = ATOMIC WT, ATOM(3,K) = VALENCE
C
100 RGAS=R314.4D0
RGASIN=1.0D0/RGAS
IDC0 =0
IDC02 =0
IDM2 =0
IDM20 =0
IDM2 =0
IDM2 =0
IDM2 =0
ILC=0
ILH=0
LANTAR=.TRUE.
LDERUG=.FALSE.
NDRUG=5
LEQUIL=.FALSE.
LREACT=.TRUE.
LSI=.TRUE.
LNG=.TRUE.
LENER=.TRUE.
EO=1.0D0

```

NOXX	301
CRKO	15
NOXX	382
NOXX	383
CRKO	18
CRKO	19
CRKO	20
CRKO	21
CRKO	22
CRKO	23
CRKO	24
CRKO	25
CRKO	26
CRKO	27
CRKO	28
CRKO	29
CRKO	30
CRKO	31
CRKO	32
CRKO	33
CRKO	34
CRKO	35
CRKO	36
CRKO	37
CRKO	38
CRKO	39
CRKO	40
CRKO	41
CRKO	42
CRKO	43
CRKO	44
CRKO	45
CRKO	46
CRKO	47
CRKO	48
CRKO	49
CRKO	50
CRKO	51
CRKO	52
CRKO	53
CRKO	54
CRKO	55
CRKO	56
CRKO	57
CRKO	58
CRKO	59
CRKO	60
CRKO	61
CRKO	62
CRKO	63
CRKO	64
CRKO	65
CRKO	66
CRKO	67
CRKO	68
CRKO	69
CRKO	70
CRKO	71
NOXX	384
CRKO	73
CRKO	74
NOXX	385
NOXX	386
CRKO	76

```

C
  NLM=1
  110 READ(5,120) (ATOM(K,NLM),K=1,3)
  120 FORMAT(A2,7X,2F10.6)
  IF (ATOM(1,NLM).EQ.BLANK) GO TO 140
  WRITE(6,130) (ATOM(K,NLM),K=1,3)
  130 FORMAT(1X,A2,5X,2F10.6/)
  IF (ATOM(1,NLM).EQ.CARB) ILC=NLM
  IF (ATOM(1,NLM).EQ.HYDR) ILH=NLM
  NLM=NLM+1
  GO TO 110

C
  140 CONTINUE
  NLM=NLM-1
  N1=NLM+1
  N2=NLM+2
  N3=NLM+3
  GO TO 10

C
  C** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** * CHAPTER 2 ** ** **
  C** ** ** ** * CHAPTER 2 ** ** **
C
  C ***THERMO***
C READ THERMODYNAMIC DATA CARDS
C
  200 NS=1
  201 READ(5,210) (CDATA(I),I=1,3),DT1,DT2,(AT(J),B(J),J=1,4),PHAZ,
  1T1,T2,NCD
  210 FORMAT(3A4,6X,2A3,4(A2,F3.0),A1,2F10.3,I19)
  IF (CDATA(1).EQ.BLANK) GO TO 260
  WRITE(6,211)(CDATA(I),I=1,3),DT1,DT2,(AT(J),B(J),J=1,4),PHAZ,
  1T1,T2,NCD
  211 FORMAT(10X,3A4,6X,2A3,2X,4(A2,2X,F3.0),2X,A1,2X,2F10.3,I19)
  IF (PHAZ.NE.GAZ) WRITE(6,212) (CDATA(I),I=1,3),PHAZ
  212 FORMAT(1ND,10X,26HWARNING...DATA FOR SPECIES,2X,3A4,3X,
  A13HNOT GAS BUT,2X,A1//)
C-----READ 2 WITH FIRST AND SECOND SUBSCRIPTS REVERSED
  READ(5,213) (Z(J,1,NS),J=1,5),NCD
  213 FORMAT(5D15.8,I5)
  WRITE(6,214) (Z(J,1,NS),J=1,5),NCD
  214 FORMAT(10X,5D15.8,I5)
  READ(5,213) (Z(J,1,NS),J=6,7),(Z(K,2,NS),K=1,3),NCD
  WRITE(6,214) (Z(J,1,NS),J=6,7),(Z(K,2,NS),K=1,3),NCD
  READ(5,215) (Z(J,2,NS),J=4,7),NCD
  215 FORMAT(4D15.8,I20)
  WRITE(6,216) (Z(J,2,NS),J=4,7),NCD
  216 FORMAT(10X,4D15.8,I20/)
C
C-----ESTABLISH ATOM STOICHIOMETRY...AL(L,N) = (KG-ATOMS ELEMENT L
C-----PER KG-MOLECULE OF SPECIES N)
C
  DO 220 L=1,NLM
  220 AL(L,NS)=0.000
C
  SUM=0.000
  DO 240 K=1,4
  IF (R(K).EQ.0.000) GO TO 240
  DO 230 L=1,NLM
  IF (ATOM(L,L).NE.AT(K)) GO TO 230
  AL(L,NS)=AL(L,NS)+R(K)
C
C-----ESTABLISH MOLECULAR WEIGHT OF SPECIES
C
  SUM=SUM+ATOM(2,L)*B(K)

```

```

CRKO 77
CRKO 78
CRKO 79
CRKO 80
CRKO 81
CRKO 82
CRKO 83
CRKO 84
CRKO 85
CRKO 86
CRKO 87
CRKO 88
CRKO 89
CRKO 90
CRKO 91
CRKO 92
CRKO 93
CRKO 94
CRKO 95
CRKO 96
CRKO 97
CRKO 98
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CRKO 100
CRKO 101
CRKO 102
CRKO 103
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CRKO 106
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CRKO 119
CRKO 120
CRKO 121
CRKO 122
CRKO 123
CRKO 124
CRKO 125
CRKO 126
CRKO 127
CRKO 128
CRKO 129
CRKO 130
CRKO 131
CRKO 132
CRKO 133
CRKO 134
CRKO 135
CRKO 136
CRKO 137
CRKO 138
CRKO 139
CRKO 140

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230 CONTINUE
240 CONTINUE
    SHW(NS)=SUM
    S2(NS)=1.00-6
C
C-----STORE MOLLERITH NAME OF SPECIES
C
    DO 250 I=1,3
      250 ASUR(NS,I)=CDATA(I)
C
C-----STORE INDEX NUMBER OF SPECIES
C
    IF (ASUR(NS,1).EQ.AC0) I0C0=NS
    IF (ASUR(NS,1).EQ.AC02) I0C02=NS
    IF (ASUR(NS,1).EQ.AM2) I0H2=NS
    IF (ASUR(NS,1).EQ.AM20) I0H20=NS
    IF (ASUR(NS,1).EQ.AN2) I0N2=NS
    IF (ASUR(NS,1).EQ.A02) I002=NS
    IF(NS.NE.I0CH)GO TO 252
    DO 251 I=1,2
    DO 251 J=1,7
      251 7(J,I,I0CH)=2(J,I,I0CH)*(SHW(I0FU)-2.000)/28.000
      252 CONTINUE
C
    NS=NS+1
    GO TO 201
C
      260 NS=NS-1
      NSM=NS+1
      NQ=NS+2
      NA=NS+3
      GO TO 10
C
C***      ***      ***      ***      ***      ***      ***      ***      ***      ***
C***      ***      ***      ***      ***      ***      ***      ***      ***      ***
C
C ***MECHANISM***
C READ MECHANISM/RATE DATA CARDS
C THE VARIABLE DT1 (COLUMNS 73/76) IS USED AS A FLAGG
C CGS --- CGS UNITS, RATE CONSTANTS IN GM-MOLES, CM, SEC
C          AND EACT IN (KCAL/GM-MOLE)
C COMM --- COMMENT CARD, FIRST 40 CHARACTERS PRINTED OUT
C REVE --- REVERSE RATE DATA, IN SAME UNITS AS FORWARD DATA
C GLOB --- GLOBAL RATE EXPRESSION DATA IN SI UNITS
C OTHERWISE THE SI UNITS (KG-MOLES, M, SEC) ARE ASSUMED
C DT1 AND DT2 (COL 73/80) CAN HAVE ANYTHING (COMMENTS) IF ABOVE FOUR
C WORDS ARE NOT REQUIRED
C TACT IS ACTIVATION TEMPERATURE, = EACT/GASCON, DEG K
C
      300 JJ=1
      NGLOR=0
C
      310 READ(5,311)(CDATA(I),I=1,12),5X(JJ),TEN(JJ),TACT(JJ),
        1 CERU(JJ),DT1,DT2
      311 FORMAT(12A4,F7.3,F5.3,F7.3,F5.3,2A4)
      IF (CDATA(1).EQ.BLANK.AND.DT1.NE.COMM) GO TO 356
C-----CHECK FOR COMMENT CARD
      IF (DT1.NE.COMM) GO TO 313
      WRITE(6,312) (CDATA(I),I=1,12)
      312 FORMAT(1H0,5X,3H***,12A4,3H***)
      GO TO 310
C-----CHECK FOR REVERSE RATE DATA...ORDER OF CARDS MUST BE CORRECT
C-----UNITS OF REVERSE DATA ASSUMED SAME AS FORWARD DATA
      313 IF (DT1.NE.REVE) GO TO 315

```

CRKO	141
CRKO	142
CRKO	143
CRKO	144
CRKO	145
CRKO	146
CRKO	147
CRKO	148
CRKO	149
CRKO	150
CRKO	151
CRKO	152
CRKO	153
CRKO	154
CRKO	155
CRKO	156
CRKO	157
CRKO	158
4STEP	606
4STEP	607
4STEP	608
4STEP	609
4STEP	610
CRKO	159
CRKO	160
CRKO	161
CRKO	162
CRKO	163
CRKO	164
CRKO	165
CRKO	166
CRKO	167
CRKO	168
CRKO	169
CRKO	170
CRKO	171
CRKO	172
CRKO	173
CRKO	174
CRKO	175
CRKO	176
CRKO	177
CRKO	178
CRKO	179
CRKO	180
CRKO	181
CRKO	182
CRKO	183
CRKO	184
CRKO	185
CRKO	186
CRKO	187
NQXX	387
NQXX	388
NQXX	389
CRKO	190
CRKO	191
CRKO	192
CRKO	193
CRKO	194
CRKO	195
CRKO	196
CRKO	197
CRKO	198

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J=JJ-1
RX2(J)=RX(JJ)
TEN2(J)=TEN(JJ)
TACT2(J)=TACT(JJ)
WRITE(6,314) RX2(J),TEN2(J),TACT2(J),DT1,DT2
314 FORMAT(14X,17HREVERSE RATE DATA,20X,3F15.3,2A4)
C-----CONVERT RX2 FOR INTERNAL CALCULATIONS
RX2(J)=RX2(J)*TENLN
IF (LSI) GO TO 310
RX2(J)=RX2(J)-TENLN*3.000
TACT2(J)=TACT2(J)*1000.000/1.98700
IF (MDDR(J).EQ.2) RX2(J)=RX2(J)-TENLN*3.000
GO TO 310
C-----CHECK FOR UNITS
315 LSI=.TRUE.
IF (DT1.EQ.CGS) LSI=.FALSE.
C
WRITE(6,316) JJ,(CDATA(I),I=1,12),RX(JJ),TEN(JJ),TACT(JJ),DT1,DT2
316 FORMAT(1H0,5X,15,4H,12A4,3F15.3,5X,2A4)
F(.NOT. LSI) TACT(JJ)=TACT(JJ)*1000.00/1.98700
IF (DT1.EQ.GLOS) NGLOS=NGLOS+1
C-----CONVERT RX FOR INTERNAL CALCULATIONS
RX(JJ)=RX(JJ)*TENLN
C
C-----ID(I,J) IS THE INDEX NUMBER OF THE I-TH DISTINCT SPECIES IN
C-----REACTION J ... I=1,4 AS NO DISTINCT THIRD BODIES ARE CONSIDERED
C
DO 320 I=1,6
320 ID(I,JJ)=0
C
DO 325 N=1,6
K=N*2-1
IF (CDATA(K).EQ.BLANK) GO TO 325
IF (CDATA(K).NE.THIRD) GO TO 321
CDATA(K)=BLANK
GO TO 325
321 CONTINUE
DO 322 I=1,NS
IF (CDATA(K).NE.ASUB(I,1)) GO TO 322
IF (CDATA(K+1).NE.ASUB(I,2)) GO TO 322
II=I
GO TO 323
322 CONTINUE
323 CONTINUE
ID(N,JJ)=II
325 CONTINUE
C
C
C-----STORE THE TYPE OF REACTION...THREE TYPES
C
MDDR 1 ... A + B (+C) --- D + E (+F)
C
MDDR 2 ... AB + M --- A + B + M
C
MDDR 3 ... A + B + M --- AB + M
C
MDDR(JJ)=1
IF (ID(2,JJ).EQ.0) MDDR(JJ)=2
IF (ID(5,JJ).EQ.0) MDDR(JJ)=3
C
C
C
THE FOLLOWING SECTION, UP TO STATEMENT 395 INCLUSIVE, MAY BE
ELIMINATED IF REVERSE (AS WELL AS FORWARD) RATE DATA IS SUPPLIED
FOR ** ALL ** REACTIONS.
C
C
CALCULATES REVERSE RATE CONSTANTS FROM EQUILIBRIUM CONSTANTS
AND FORWARD RATE CONSTANTS FOR FIFTEEN POINTS

```

CRKO 199
CRKO 200
CRKO 201
CRKO 202
CRKO 203
CRKO 204
CRKO 205
CRKO 206
CRKO 207
CRKO 208
CRKO 209
CRKO 210
CRKO 211
CRKO 212
CRKO 213
CRKO 214
CRKO 215
CRKO 216
CRKO 217
CRKO 218
CRKO 219
CRKO 220
CRKO 221
CRKO 222
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CRKO 242
CRKO 243
CRKO 244
CRKO 245
CRKO 246
CRKO 247
CRKO 248
CRKO 249
CRKO 250
CRKO 251
CRKO 252
CRKO 253
CRKO 254
CRKO 255
CRKO 256
CRKO 257
CRKO 258
CRKO 259
CRKO 260
CRKO 261
CRKO 262

```

C OVER THE TEMPERATURE RANGE 1000 TO 3000 DEG K
C
C INSERTED 1 STEP (M.D.HONNVEH, 7/22/79)
IF (DT1.EQ.GLOB) GO TO 357
IF (DT1.EQ.GLOB) GO TO 355
DX=(XMAX-XMIN)/14.000
SUMX=0.000
SUMY=0.000
HCPS=2
DO 351 N=1,15
X(N)=XMIN+DX*FLOAT(N-1)
SUMX=SUMX+X(N)
TKINV=X(N)
TV=1.000/TKINV
TLN=DILOG(TK)
NS1=1
NS2=NS
CALL HCPS
SUM1=0.000
DO 350 ND=1,6
K=ID(ND,JJ)
IF (K.EQ.0) GO TO 350
GF=H0(K)-S0(K)
IF (ND.LT.4) SUM1=SUM1+GF
IF (ND.GE.4) SUM1=SUM1-GF
350 CONTINUE
TM1=0.000
C NATURAL LOGS OF GAS CONSTANTS...R=82.057 CM3-ATM/GMOL,K (CGS)
C AND R=C.082057 M3-ATM/KGMOL,K (SI)
RTLN=TLN+4.407400
IF (LSI) RTLN=TLN-2.5003400
IF (MOPR(JJ).GT.1) GO TO 3501
IF (ID(3,JJ).EQ.0) TM1=TM1+RTLN
IF (ID(6,JJ).EQ.0) TM1=TM1-RTLN
GO TO 3502
3501 CONTINUE
IF (ID(2,JJ).EQ.0) TM1=RTLN
IF (ID(5,JJ).EQ.0) TM1=-RTLN
3502 CONTINUE
Y(N)=TM1-SUM1+TEN(JJ)*TLN-TACT(JJ)*TKINV+RX(JJ)
SUMY=SUMY+Y(N)
351 CONTINUE
XRAR=SUMX/15.000
YRAR=SUMY/15.000
SUMX=0.000
SUM1=0.000
SUMY=0.000
DO 352 N=1,15
SUMX=SUMX+Y(N)*(Y(N)-XRAR)
SUM1=SUM1+(Y(N)-XRAR)**2
SUMY=SUMY+(Y(N)-YRAR)**2
352 CONTINUE
TEN2(JJ)=0.000
TACT2(JJ)=-SUMX/SUM1
RX2(JJ)=(YRAR+TACT2(JJ)*XRAR)/TENLN
SUMX=0.000
DO 353 N=1,15
SUMX=SUMX+(Y(N)+TACT2(JJ)*X(N)-TENLN+RX2(JJ))**2
353 CONTINUE
SUMY=DSQRT(1.000-SUMX/SUMY)
SUMX=DSQRT(SUMX/14.000)
CDATA(1)=TACT2(JJ)
IF (.NOT.LSI) CDATA(1)=TACT2(JJ)*1.98700*0.00100
WRITE(6,354) RX2(JJ),TEN2(JJ),CDATA(1),SUMX,SUMY

```

```

CRKD 263
CRKD 264
CRKD 265
CRKD 266
CRKD 267
CRKD 268
CRKD 269
CRKD 270
CRKD 271
CRKD 272
NOXXX 273
CRKD 274
CRKD 275
CRKD 276
CRKD 277
NOXXX 278
NOXXX 279
CRKD 280
CRKD 281
CRKD 282
CRKD 283
CRKD 284
CRKD 285
CRKD 286
CRKD 287
CRKD 288
CRKD 289
CRKD 290
CRKD 291
CRKD 292
CRKD 293
CRKD 294
CRKD 295
CRKD 296
CRKD 297
CRKD 298
CRKD 299
CRKD 300
CRKD 301
CRKD 302
CRKD 303
CRKD 304
CRKD 305
CRKD 306
CRKD 307
CRKD 308
CRKD 309
CRKD 310
CRKD 311
CRKD 312
CRKD 313
CRKD 314
CRKD 315
CRKD 316
CRKD 317
CRKD 318
CRKD 319
CRKD 320
CRKD 321
CRKD 322
CRKD 323
CRKD 324

```

354 FORMAT(6X,57H CALCULATED REVERSE RATE DATA, STD DEV AND CORR COEF	CRKO	325
1 = ,3F13.3,4X,1P2010.3)	CRKO	326
C-----CONVERT RX2 FOR INTERNAL CALCULATIONS	CRKO	327
RX2(JJ)=RX2(JJ)*TENLN	CRKO	328
C	CRKO	329
C-----SET REVERSE REACTION RATE VARIABLES=0 FOR GLOBAL REACTIONS	CRKO	330
C-----SO THAT THESE VARIABLES ARE DEFINED FOR THE KINETIC RATE	CRKO	331
C-----PRINTOUT (M.D.HOOVEN 7/22/79)	CRKO	332
357 IF (DT1.NE.GLOB) GO TO 355	CRKO	333
TACT2(JJ)=C	CRKO	334
TEN2(JJ)=0	CRKO	335
RX2(JJ)=0	CRKO	336
355 JJ=JJ+1	CRKO	337
C-----CONVERT ALL RATE DATA TO SI UNITS	CRKO	338
IF (LST) GO TO 310	CRKO	339
J=JJ-1	CRKO	340
RX(J)=RX(J)-TENLN*3.000	CRKO	341
RX2(J)=RX2(J)-TENLN*3.000	CRKO	342
IF (MODR(J).EQ.2) RX2(J)=RX2(J)-TENLN*3.000	CRKO	343
IF (MODR(J).EQ.3) RX(J)=RX(J)-TENLN*3.000	CRKO	344
IF (MODR(J).NE.1) GO TO 310	CRKO	345
IF (ID(3,J).NE.0) RX(J)=RX(J)-TENLN*3.000	CRKO	346
IF (ID(6,J).NE.0) RX2(J)=RX2(J)-TENLN*3.000	CRKO	347
GO TO 310	CRKO	348
C	CRKO	349
356 JJ=JJ-1	CRKO	350
NGLORP=NGLORP+1	CRKO	351
C	CRKO	352
C-----PRINT OUT ARRAY OF STOICHIOMETRIC COEFFICIENTS	CRKO	353
C	CRKO	354
DO 372 J=1,JJ	CRKO	355
DO 370 N=1,6	CRKO	356
K=N*2-1	CRKO	357
L=N	CRKO	358
CDATA(K)=BLANK	CRKO	359
CDATA(K+1)=BLANK	CRKO	360
IDLJ=ID(L,J)	CRKO	361
IF (IDLJ.EQ.0) GO TO 370	CRKO	362
CDATA(K)=ASUB(IDLJ,1)	CRKO	363
CDATA(K+1)=ASUB(IDLJ,2)	CRKO	364
370 CONTINUE	CRKO	365
IF (ID(2,J).EQ.0) CDATA(5)=THIRD	CRKO	366
IF (ID(5,J).EQ.0) CDATA(5)=THIRD	CRKO	367
IF (MODR(J).GT.1) CDATA(11)=THIRD	CRKO	368
WRITE(6,371) J,(CDATA(K),K=1,12)	CRKO	369
371 FORMAT(5X,15,1H,,5X,6A4,,H----,6X,6A4/)	CRKO	370
372 CONTINUE	CRKO	371
C	CRKO	372
C-----PRINT OUT ALL RATE DATA IN SI UNITS	CRKO	373
C	CRKO	374
WRITE(6,380)	CRKO	375
380 FORMAT(/,1H0,40X,29H KINETIC RATE DATA IN SI UNITS/	CRKO	376
41H0,6X,1HJ,2X,4HMODR,16X,2HID,19X,2HMX,10X,3HTEN,9X,4HTACT,	CRKO	377
413X,3HMX2,9X,4HTEN2,9X,5HTACT2/)	CRKO	378
DO 382 J=1,JJ	CRKO	379
TM1=RX(J)/TENLN	CRKO	380
TM2=RX2(J)/TENLN	CRKO	381
WRITE(6,381) J,MODR(J),(ID(I,J),I=1,6),TM1,TEN(J),TACT(J),	CRKO	382
1TM2,TEN2(J),TACT2(J)	CRKO	383
382 CONTINUE	CRKO	384
381 FORMAT(5X,12,1H,,14,3X,6I4,2(3X,3F13.3))	CRKO	385
C	CRKO	386
C-----SET CONTACT INDEXES TO UNITY	CRKO	387
DO 390 J=1,JJ	CRKO	388


```

C4X,17H(KGMOLE I)/(KG X),9X,13H(KG I)/(KG X)/)
HSUM=0.000
SM=0.000
DO 480 I=1,NS
S2(I)=S2(I)/SUM1
C-----S2(I) IN MOLE NUMBERS, KG-MOLES I/KG MIXTURE
HSUM=HSUM+MO(I)*S2(I)
SM=SM+S2(I)
DT1=S2(I)*SMW(I)
WRITE(6,470) I,(ASUB(I,J),J=1,3),SMW(I),S2(I),DT1
470 FORMAT(9X,I2,1H,,4X,3A4,1P3D20.3)
480 CONTINUE
C-----HSUBO IN JOULES/KG REACTANT MIXTURE
HSUBO=HSUM*PGAS*TK
C-----RHOP IS MASS DENSITY, KG/CM3
RHOP=PA/(RGAS*TK+SM)
C
SMINV=1.000/SM
WRITE(6,490) TK,HSUBO,PA,RHOP,SMINV
490 FORMAT(1HC//12X,13HTEMPERATURE =,1PD12.3,3X,5HDEG K/
12X,10HENTHALPY =,3X,1PD12.3,3X,9HJOULES/KG/
12X,10HPRESSURE =,3X,1PD12.3,3X,6HM/M**2/
12X,9HODENSITY =,4X,1PD12.3,3X,7HKG/M**3/
12X,13HMEAN MOL WT =,1PD12.3,3X,9HKG/KGMOLE//)
C
C-----ON RETURN, CALLING PROGRAM MUST STORE MOLE NUMBERS S2(I),
C-----PRESSURE, TEMPERATURE, ENTHALPY AND DENSITY AT APPROPRIATE INLET
C-----INLET GRID NODE
C
RETURN
END
SURROUTINE HCPS
C *** MODIFIED FOR CONDENSED SPECIES 7-79 D.T.PRATT
C
DOUBLE PRECISION CPSUM,FMV,FR,FQ,HSUBO,HSUM,HO,PA,PPLN,
1 QO,Q1,Q2,Q3,Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,SSAVE,SO,S1,S2,TK,
2 TKINV,TLN,Z,SMO
DOUBLE PRECISION CP1,CP2,CP3,CP4,CP5,P2,P25,P333,P5,TKCU,TKSQ,TK4
LOGICAL LADIAP,LCONVG,LOFBUG,LEQUIL,LNRG,LREACT,LENER
C
COMMON
3/CHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
1/CINDEX/IDCO,IDFU,IDO2,ION2,ION2O,IDCO2,ION1,ION2,ION1,IONO,IONO2
1,ION,IOCH,HCPS,ILC,ILM,IMAT,ITER,JJ,N1,N2,N3,NA,NGLOR,NGLORP,
2 NLM,NQ,NSM,NS1,NS2,IOCH
1/CPARAM/ASUB(30,3),EMV,ER,HSUBO,NDEBUG,NS,PA,QO,Q1,Q2,Q3,Q4,RHOP,
1 SM,SMW(30),SPO,S1(30),S2(30),TK,LADIAP,LDEBUG,LEQUIL,LREACT,LENER
2,EDKIJ,LCONVG
1/CSPCE/HC(30),SO(30),SSAVE(30),Z(420)
C
C*****
C THIS SURROUTINE CALCULATES THE NON-DIMENSIONAL, 1-ATM VALUES OF
C ENTHALPY, SPECIFIC HEAT, AND ENTROPY FOR A GIVEN VALUE OF TEMPERATURE
C (DEG K) THE Z ARRAY IS REFERENCED AS HAVING ONLY ONE SUBSCRIPT
C TO SAVE INTERNAL SUBSCRIPT CALCULATIONS.
C Z(IC,IT,IS) --- Z(IC+7*(IT-1)+7*(IS-1)) FOR Z(7,2,20)
C WHERE IC=1,7, COEF FOR TEMP RANGE IT=1 OR 2, FOR SPECIES IS=1,NS.
C NOTE THAT THE FIRST 2 SUBSCRIPTS ARE REVERSED FROM THE
C GORDON AND MCBRIDE PRACTICE
C REFERENCE GORDON AND MCBRIDE (NASA SP-273, 1971)
C*****
C
DATA ICIT/14/
DATA P2,P25,P333,P5/Q,200,0.2500,0.333333300,0.500/

```

CRKO	453
CRKO	454
CRKO	455
CRKO	456
CRKO	457
CRKO	458
CRKO	459
CRKO	460
CRKO	461
CRKO	462
CRKO	463
CRKO	464
CRKO	465
CRKO	466
CRKO	467
CRKO	468
CRKO	469
CRKO	470
CRKO	471
CRKO	472
CRKO	473
CRKO	474
CRKO	475
CRKO	476
CRKO	477
CRKO	478
CRKO	479
CRKO	480
CRKO	481
CRKO	482
CRKO	483
HCPS	2
HCPS	3
HCPS	4
NOXX	392
NOXXX	30
NOXXX	31
NOXXX	32
NOXX	393
HCPS	7
HCPS	8
NOXX	394
NOXX	395
NOXX	396
4STEP	611
HCPS	12
NOXX	398
NOXX	399
NOXX	400
HCPS	15
HCPS	16
HCPS	17
HCPS	18
HCPS	19
HCPS	20
HCPS	21
HCPS	22
HCPS	23
HCPS	24
HCPS	25
HCPS	26
HCPS	27
HCPS	28
NOXXX	33

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C      IT=0
      IF (TK.LT.1000.000) IT=7
C      TKSQ=TK**2
      TKCU=TKSQ*TK
      TK4=TKCU*TK
      CPSUM=0.000
      GO TO (11,21,31,41),IMCPS
C
C-----IMCPS=1 --- JUST CPSUM AND MO(I) REQUIRED
C
11 DO 10 I=NS1,NS2
   K=IT+ICIT*(I-1)
   CP1=7*(K+1)
   CP2=TK**7*(K+2)
   CP3=TKSQ**2*(K+3)
   CP4=TKCU**2*(K+4)
   CP5=TK4**2*(K+5)
   CPSUM=CPSUM+(CP1+CP2+CP3+CP4+CP5)*S2(I)
   MO(I)=P2*CP5+P25*CP4+P333*CP3+P5
      *CP2+CP1+TKINV**2*(K+6)
10 CONTINUE
   RETURN
C
C-----IMCPS=2 --- CPSUM, MO(I) AND SO(I) REQUIRED
C
21 DO 30 I=NS1,NS2
   K=IT+ICIT*(I-1)
   CP1=7*(K+1)
   CP2=TK**7*(K+2)
   CP3=TKSQ**2*(K+3)
   CP4=TKCU**2*(K+4)
   CP5=TK4**2*(K+5)
   CPSUM=CPSUM+(CP1+CP2+CP3+CP4+CP5)*S2(I)
   MO(I)=P2*CP5+P25*CP4+P333*CP3+P5
      *CP2+CP1+TKINV**2*(K+6)
   SO(I)=P25*CP5+P333*CP4+P5*CP3
      +CP2+TLN*CP1+7*(K+7)
30 CONTINUE
   RETURN
C-----IMCPS=3 --- HSUP REQUIRED
31 HSUM=0.000
   DO 40 I=NS1,NS2
   K=IT+ICIT*(I-1)
   CP1=7*(K+1)
   CP2=TK**7*(K+2)
   CP3=TKSQ**2*(K+3)
   CP4=TKCU**2*(K+4)
   CP5=TK4**2*(K+5)
   MO(I)=P2*CP5+P25*CP4+P333*CP3+P5*CP2+CP1+TKINV**2*(K+6)
   HSUM=HSUM+MO(I)*S2(I)
40 CONTINUE
   RETURN
C-----IMCPS=4 --- HSUP AND CPSUM REQUIRED
41 HSUM=0.000
   DO 50 I=NS1,NS2
   K=IT+ICIT*(I-1)
   CP1=7*(K+1)
   CP2=TK**7*(K+2)
   CP3=TKSQ**2*(K+3)
   CP4=TKCU**2*(K+4)
   CP5=TK4**2*(K+5)
   CPSUM=CPSUM+(CP1+CP2+CP3+CP4+CP5)*S2(I)

```

```

HCPS      30
HCPS      31
HCPS      32
HCPS      33
HCPS      34
HCPS      35
HCPS      36
HCPS      37
NOXX      401
HCPS      39
HCPS      40
HCPS      41
NOXX      402
HCPS      43
HCPS      44
HCPS      45
HCPS      46
HCPS      47
HCPS      48
HCPS      49
HCPS      50
HCPS      51
HCPS      52
HCPS      53
HCPS      54
HCPS      55
HCPS      56
NOXX      403
HCPS      59
HCPS      60
HCPS      61
HCPS      62
HCPS      63
HCPS      64
HCPS      65
HCPS      66
HCPS      67
HCPS      68
HCPS      69
HCPS      70
HCPS      71
NOXX      404
NOXX      405
NOXX      406
NOXX      407
NOXX      408
NOXX      409
NOXX      410
NOXX      411
NOXX      412
NOXX      413
NOXX      414
NOXX      415
NOXX      416
NOXX      417
NOXX      418
NOXX      419
NOXX      420
NOXX      421
NOXX      422
NOXX      423
NOXX      424
NOXX      425
NOXX      426

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MO(I)=P2*CP5+P25*CP4+P333*CP3+P5*CP2+CP1+TKINV*Z(K+6)
 HSIH=HSHM+MO(I)*S2(I)
 50 CONTINUE
 RETURN
 END

NOXX	427
NOXX	428
NOXX	429
NOXX	430
MCPS	72

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APPENDIX E
LIST OF DEPENDENT VARIABLES
AND SOURCE TERMS

APPENDIX E

LIST OF DEPENDENT VARIABLES AND SOURCE TERMS

TABLE E-1

Dependent Variable	Source Term
u (axial velocity)	$\frac{\partial}{\partial x} (\mu_{\text{eff}} \frac{\partial u}{\partial x}) + \frac{1}{r} \frac{\partial}{\partial r} (\mu_{\text{eff}} r \frac{\partial v}{\partial r}) + \frac{1}{r} \frac{\partial}{\partial \theta}$ $(\mu_{\text{eff}} \frac{\partial w}{\partial x}) + S_{\text{spray}}^u - \frac{\partial p}{\partial x}$
v (radial velocity)	$\frac{\partial}{\partial x} (\mu_{\text{eff}} \frac{\partial u}{\partial r}) + \frac{1}{r} \frac{\partial}{\partial r} (\mu_{\text{eff}} r \frac{\partial v}{\partial r}) + \frac{1}{r} \frac{\partial}{\partial \theta}$ $[\mu_{\text{eff}} (\frac{\partial w}{\partial r} - \frac{w}{r})] - 2 \frac{\mu_{\text{eff}}}{r} (\frac{1}{r} \frac{\partial w}{\partial \theta} + \frac{v}{r}) + \frac{\rho w^2}{r}$ $+ S_{\text{spray}}^v - \frac{\partial p}{\partial r}$
w (tangential velocity)	$\frac{\partial}{\partial x} (\frac{\mu_{\text{eff}}}{r} \frac{\partial u}{\partial \theta}) + \frac{1}{r} \frac{\partial}{\partial r} [\mu_{\text{eff}} r (\frac{1}{r} \frac{\partial v}{\partial \theta} - \frac{w}{r})]$ $+ \frac{1}{r} \frac{\partial}{\partial \theta} [\frac{\mu_{\text{eff}}}{r} (\frac{\partial w}{\partial \theta} + 2v)] - \frac{\rho v w}{r} + \frac{\mu_{\text{eff}}}{r} (\frac{\partial w}{\partial r} +$ $\frac{\partial v}{r \partial \theta} - \frac{w}{r}) + S_{\text{spray}}^w - \frac{1}{r} \frac{\partial p}{\partial \theta}$
k (Turbulent kinetic energy)	$G_k - \rho \epsilon$
ϵ (Dissipation rate)	$(C_1 G_k - C_2 \rho \epsilon) / k$

TABLE E-1 (Contd)

Dependent Variable	Source Term
ϕ (Mixture fraction)	\dot{m}_{evap}
m_{fu} (Unburnt fuel mass fraction)	<p>As per four-step mechanism, (Chapter VI) and modified by the eddy-break-up model as in Ref. 1, Page 23.</p> <p>\dot{m}_{evap} added on to m_{fu} source.</p>
m_{CH} (Intermediate hydrocarbon mass fraction)	
m_{CO} (CO mass fraction)	
m_{H_2} (H_2 mass fraction)	
Soot nuclei and particle concentrations	As given in Chapter III, equations (28) and (29).
\tilde{h} (Stagnation enthalpy)	$2a [(R^x - E) + (R^r - E) + (R^z - E)]$ $+ \dot{m}_{\text{evap}} H_{\text{fuel}}$

In the above table, the symbols have the meanings:

x, r, θ = axial, radial, tangential directions;

μ_{eff} = effective viscosity;

p = pressure;

ρ = density;

$$G_k = \mu_{\text{eff}} \left[2 \left\{ \left(\frac{\partial u}{\partial x} \right)^2 + \left(\frac{\partial v}{\partial r} \right)^2 + \left(\frac{\partial w}{r \partial \theta} + \frac{v}{r} \right)^2 \right\} \right. \\ \left. + \left(\frac{\partial w}{\partial x} + \frac{1}{r} \frac{\partial u}{\partial \theta} \right)^2 + \left(\frac{\partial u}{\partial r} + \frac{\partial v}{\partial x} \right)^2 + \left(\frac{\partial w}{\partial r} + \right. \right. \\ \left. \left. \frac{\partial v}{r \partial \theta} - \frac{w}{r} \right)^2 \right];$$

C_1, C_2 = Turbulence model constants;

$\left. \begin{matrix} S_{\text{spray}}^u \\ S_{\text{spray}}^v \\ S_{\text{spray}}^w \end{matrix} \right\}$ = Momentum transfer from spray to the gas phase u, v, and w - momentum equations;

\dot{m}_{evap} = rate of spray evaporation per unit volume;

a = Absorption coefficient defined as radiation absorbed per unit length;

E = Blackbody emissive power;

R^x, R^r, R^z = Composite radiation fluxes (See equations 37, 38, and 39);

H_{fuel} = Heat of formation of fuel.

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APPENDIX F
INPUT DATA FOR JT8D-17 COMBUSTOR TEST CASE

APPENDIX F

INPUT DATA FOR JT8D-17 COMBUSTOR TEST CASE

In this Appendix, a listing of the input data used for the JT8D-17 Combustor computations is provided. The data shown is for the takeoff case using the four-step hydrocarbon oxidation mechanism. The specification of the X , r , and θ grids is contained in lines 630-670. Other inputs may be easily interpreted with reference to the input description provided in Appendix B.

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U-VELOCITY
 V-VELOCITY
 W-VELOCITY
 PRESSURE
 TURBULENCE KINETIC ENERGY
 TURBULENCE LENGTH SCALE
 PHI (TOTAL FUEL)
 FUEL MASS FRACTION
 TEMPERATURE
 SPECIFIC ENTHALPY
 AVG. KAG.
 PX
 PY
 RZ
 CG
 H2O
 I2
 CO2
 N2
 RHO
 EFF. VISCOSITY
 EVAPORATION RATE
 NUCLEI CONCENTRATION
 SOOT CONCENTRATION - SIZE 1
 SOOT CONCENTRATION - SIZE 2
 H
 N
 NO
 NO2
 O
 OH
 C-HY-2
 H2

OPERATIONAL DATA
 OF POOR QUALITY

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 640

JT8D-COARSE GRID-TAKEOFF-JETA-4 STEP

IC	10	05	02	02	02	02	03	350
01	02	00	00	00				360
01	01	01	01	01	01	01	01	370
01	01	01	01					380
								390
								400
01	01	01	03	01	01	01	01	410
01	01	01	01	01	01	01	01	420
01	01	01	01	01	01	01	01	430
01	01	01	01	01	01	01	01	440
01	01	01	00	00	00	01	01	450
01	00	00	00	00	00	01	00	460
00	00	00	00	00	00	00	00	470
	00	01	01	01	00	00	01	480
01								490
0.2	0.2	0.2	1.0	0.5	0.5	0.5	0.5	500
0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	510
0.5	0.5	0.5	0.5	0.5	0.5	0.5	0.5	520
0.5	0.5	0.5	0.5	0.5	1.0	1.0	1.0	530
0.2	0.3	0.3						540
1.0	1.0	1.0	1.0	0.7	0.7	0.7	0.7	550
0.7	0.7	0.7	0.7	0.7	0.7	0.7	0.7	560
0.7	0.7	0.7	0.7	0.7	0.7	0.7	0.7	570
0.7	0.7	0.7	0.7	0.7	1.0	1.0	1.0	580
1.0	1.0	1.0	1.0	0.9	0.9	0.9	0.9	590
0.9	0.9	0.9	0.9	0.9	0.9	0.9	0.9	600
0.9	0.9	0.9	0.9	0.9	0.9	0.9	0.9	610
0.9	0.9	0.9	0.9	0.9	1.0	1.0	1.0	620
0.9	0.9	0.9	0.9	0.9	1.0	1.0	1.0	630
0.9	0.9	0.9	0.9	0.9	1.0	1.0	1.0	640

0.0	0.005	0.015	0.025	0.035	0.045	0.057	0.07	650
0.001	0.0064							660
0.0	0.1496	0.4488	0.7480	0.9376				670
02	10	04	10					680
1.7650E+04	1.0	0.1	0.01	0.003	0.02			690
10	19.00	-49317.	.001					700
2.0843E+22	2.0000.	1.0	5.0117E+19	25000.	3.0			710
3.9811E+17	2.0000.	1.0	3.3113E+18	20500.	1.0			720
0.5	1.07	0.4	0.3	1.18	-0.37			730
1.0	0.75	0.5	0.85	1.42	-0.20			740
1.45	0.92	0.99	1.7100E-05	0.000001	713.0	713.0	713.0	750
075	100	04	04	00	02			760
40.410	0.3	1.10	0.081	0.0	713.0			770
01	02	100.0						780
.0001	.0001	0.4488	1.570795	-1.570795	0.0	5.83438	0.4488	790
5.00	0.01910	40.0	00.00	0.0				800
03	07							810
10	10							820
03	03							830
-80.0	-80.0							840
05.	05.							850
0.0001	0.0001							860
0.2620	0.7119							870
713.0	713.0							880
01	30	02						890
0.05	1.1000E+31	40000.	1.0000E+038	0.0000E-16	100.0	1.0000E-15	2000.0	900
1.5020E+13	10000.0	-1.94	1.81	-0.5	4.5000E+070.1	400.0		910
0.025	1.0							920
40.0	10.0							930
30	0.001							940
01	49	02	0.0005	500.0				950
ELEMENTS								
C	12.01115	4.000000						970
H	1.007470	1.000000						980
N	14.006700	0.0						990
C	12.994400	-2.000000						1000
THERMO								
C10H19	J 3701C 10.4 19.00 0.00 0.0	300.000	5000.000					1010
	C.26845736E+02	0.46470050E-01	-0.22957813E-04	0.48494610E-08	-0.37080219E-12			1020
	-C.24819829E+05	0.10707143E+02	0.57799475E+01	0.50561468E-01	0.51144255E-04			1030
	-C.94908140E-07	0.34003875E-10	-0.24819829E+05	0.86690068E+00				1040
02	J 4705J 2.0 0.0 0.0 0.0	300.000	5000.000					1050
	C.36219521E-01	0.73018250E-03	-0.19052219E-05	0.36201550E-10	-0.28945023E-14			1060
	-C.12019472E-04	0.36150942E-01	0.36255980E-01	-0.18782182E-02	0.74554543E-05			1070
	-C.67635571E-08	0.21555477E-11	-0.10475225E-04	0.43052764E-01				1080
N2	J 4705N 2.0 0.0 0.0 0.0	300.000	5000.000					1090
	C.28963194E-01	0.15154863E-02	-0.57235275E-06	0.99807385E-10	-0.65223530E-14			1100
	-C.90586182E-03	0.61615143E-01	0.36748257E-01	-0.12081496E-02	0.23240100E-05			1110
	-C.63217570E-04	-0.22577253E-12	-0.10611587E-04	0.23580418E-01				1120
00	J 4705C 1.0 1.00 0.00 0.0	300.000	5000.000					1130
	C.29843069E-01	0.14841387E-02	-0.57399678E-04	0.10364570E-04	-0.69353499E-14			1140
	-C.14245227E-05	0.63479147E-01	0.37100915E-01	-0.16190964E-02	0.38423584E-05			1150
	-C.20319673E-08	0.23453344E-12	-0.14355109E-05	0.24555340E-01				1160
C2H4	J 3701C 2.04 4.000 0.00 0.0	300.000	5000.000					1170
	2.23312189E+00	1.32141704E-02	-5.11224078E-05	8.83920414E-10	-5.63643019E-14			1180
	5.10533927E+03	9.38901110E+00	2.41824070E+00	1.22421229E-02	-4.24080270E-06			1190
	2.13889578E-04	-1.44584497E-12	5.05491829E+03	0.02623340E+00				1200
02	J 3701H 2.0 0.0 0.0 0.0	300.000	5000.000					1210
	C.31001584E-01	0.51119455E-03	0.52644204E-07	-0.34909964E-10	0.3645341E-14			1220
	-C.47730013E-03	-0.19544412E-01	0.30574444E-01	0.26765198E-02	-0.58049144E-05			1230
	C.54210445E-08	0.18122726E-11	-0.98390430E-03	-0.22997046E-01				1240
020	J 3701D 2.0 1.00 0.00 0.0	300.000	5000.000					1250
	C.27107610E-01	0.24451470E-02	-0.80224368E-05	0.10226681E-05	-0.48472104E-14			1260

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APPENDIX G
DIMENSIONS OF VARIABLE ARRAYS

APPENDIX G
DIMENSIONS OF VARIABLE ARRAYS

The program listing shown in Appendix D is for a 10 x 10 x 5 (axial x radial x tangential) grid. In order to change the number of nodes to any NX, NY, NZ, the dimensions of various variable arrays have to be changed as indicated on the following page. Some of the variables are dimensioned as (NX, NY, NZ) in some subroutines and as (NXYZ) in others. Both forms are indicated below. In addition, in BLOCK DATA, NI, NJ, and NK have to be set to NX, NY, and NZ, respectively.

NXYZ = NX*NY*NZ

NXY = NX*NY

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Variable	Dimensions
F	(NXYZ, 7) or (7* NXYZ)
DU, DV, DW, ANUC, SOOT1, SOOT2, FCH, FH2, RHO, VISC, ABSR, SCTR, DRHODP, U, V, W, PP, P, TEMP, GAM	(NX, NY, NZ) or (NXYZ)
FS	(NXYZ, 14)
GENR, SUFU, SPFU	(NXYZ)
SU, SP, AXP, AXM, AYP, AYM, AZP, AZM, CZ, CZU, CZP, DIVG	(NX, NY) or (NXY)
AXMK, AXPk, AYMK, AYPk, AZMK, AZPK, SUK, SPK, EVAP, EVAPU, EVAPV, EVAPW, EDK, EDK 2	(NX-2) * (NY-2) * (NZ-2)
EVSU	(NX-2) * (NY-2)
CY, CYU, CYP, X, XS, XSU, XDIF, FXP, FXM, FLO, TEMTM, H, FUEL, FUOX, UIN, TIN, FUELS	GE. (NX)
R, RM, RMV, YSR, YSVR, Y, YS, YSV YDIF, FYP, FYM, JM	GE. (NY)
Z, ZS, ZSW, ZDIF, FZP, FZM, KM	GE. (NZ)
IWLI, IWLO	GE. (NY, 5)
JWLO, JWLI	GE. (NX, 5)
JKIN	GE. (NY, NZ)
IKIN	GE. (NX, NZ)